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Compute gas/water interface geometry during drainage and imbibition in model sediments (Task 5.2 Technical Report)

Mechanisms Leading to Co-Existence of Gas and Hydrate in Ocean Sediments

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Office of Fossil Energy

MECHANISMS LEADING TO CO-EXISTENCE OF GAS AND HYDRATE IN OCEAN SEDIMENTS

CONTRACT NO. DE-FC26-06NT43067

Deliverable 5.2:

Report on Task 5.2 "Compute gas/water interface geometry during drainage and imbibition in model sediments"

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Objective of Task 5.2

In the conceptual model to be examined in this project, hydrate formation depends upon the location and geometry of the gas/water interface. In previous tasks we have extracted physically representative networks of pore throats and pore bodies in a large set of model sediments (dense, disordered packings of spheres of different sorting). We also determined the critical curvatures for pore-level events during drainage (gas phase invasion of water-saturated sediment) and imbibition (water invasion of sediment partially filled with gas phase).

In this task we use the previous results to carry out a standard invasion percolation simulation of drainage, then of imbibition in the model sediments. The simulations provide the detailed geometry of the gas/water interface at each step of drainage or imbibition. This will be used in future tasks to model the growth of methane hydrate at these interfaces. The simulations are conveniently summarized with capillary pressure curves, appended to this report; we also report the interfacial area during drainage as this is expected to be the primary mode of hydrate growth.

Summary of Findings in Task 5.2

We extended our earlier investigation of the **critical curvature** for drainage in a pore throat in a model sediment. We generalized the Mayer-Stowe-Princen method to converging/diverging pore throats defined by grains of three different sizes. The results improve the estimate of critical curvature for throats that have larger-than-average cross-section. This in turn improves the consistency of predicted drainage curves in model sediments that are not well sorted.

The simulations of **drainage** yield a systematic decrease in the percolation threshold (capillary pressure when most of the water drains from the pore space) as the sorting of the model sediment becomes poorer. This observation is consistent with the shift of the frequency distribution of critical curvatures toward smaller values. The number fraction of pores containing irreducible wetting phase increases as the sorting becomes poorer. However the volume fraction, and hence the phase saturation, does not necessarily increase because the pores containing water are proportionately smaller than average in the poorly sorted sediments. Hence the irreducible wetting phase saturation does not change significantly as sorting changes.

The simulations of **imbibition** yield consistent hysteresis (the water invades at a smaller capillary pressure than that at which the gas invades) for all the sediments. A remarkable observation is that infinite-acting networks yield larger residual gas saturations than are commonly observed in laboratory experiments in sediments. By way of explanation we note that simulations in finite networks (i.e. having a set of exit pores for gas to leave the domain) yield smaller residual gas saturations that are comparable to laboratory data. The difference is the criterion for trapping the gas phase in the infinite-acting networks: gas phase which occupies a percolating cluster of pores can be displaced by water, but gas phase which occupies a finite cluster of pores is deemed disconnected from the bulk gas phase. Disconnected gas cannot be displaced and is therefore part of the residual phase. In the finite network simulations, gas in a pore can be displaced if that pore is part of a cluster of gas-filled pores that are connected to an exit pore.

Clearly the **percolating-cluster criterion** is more stringent than the finite-network criterion. As a result, larger residual gas saturations occur in the simulations. We argue that the larger residual saturations are the physically relevant ones in the field, where the "exit pores" that characterize the laboratory experiment do not exist. We remark that measurements of residual saturation in the field (obtained by conducting single well partitioning tracer tests) typically yield larger values than observed in the laboratory. This supports the applicability of the infinite-acting network simulations reported here. The literature contains no such simulations in physically realistic networks, so this constitutes an important advance in understanding the behavior of imbibition.

For completeness and for reference we include here the results of the network model approach for the **poorly sorted** sediments. For poorly sorted model sediments, our approach for identifying pore throats (the Delaunay tessellation) is not well suited for capturing the essential geometry. In the Delaunay tessellation every throat is comprised of three nearest-neighbor grains. But the gas/water interface is frequently supported by more than three grains when small grains are mixed in with larger grains. Accounting for this phenomenon would require substantial modification of the network-based approach for simulating gas or water invasion (e.g. the "fourth sphere correction" by Thane [2006]). While this is possible, it is not within the scope of the original program of work. Regardless of that we believe a technically superior alternative exists. This would be to apply the level set method directly to simulate drainage and imbibition in poorly sorted sediments. We think this is feasible based on our progress on other tasks in this project with the level set method. While this too is beyond the scope of the original program of work, it may be possible to demonstrate the idea during Phase 2 of the project.

Results of Task 5.2

The full set of simulations are reported in Appendix B. Here we review the approach.

5.2.1 Drainage Simulation in Model Sediments with Different Sorting

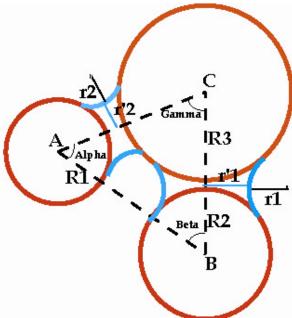
Previously we reported on the application of the Mason and Mellor estimate of critical curvature estimate

$$C_{drain}^* = \frac{2R_{avg}}{r_{inscribed}} - 1.6 \tag{1}$$

where $r_{inscribed}$ is the radius of a circle inscribed in the pore throat. This estimate is good for very well sorted packings. During the execution of Task 5.2 we found that this estimate yields drainage curves that are not physically realistic when applied to packings with broader distributions of grain sizes. A more rigorous estimate can be obtained from the Mayer-Stowe-Princen (MSP) theory. That theory was developed for equal-size grains. It agrees very well with the Mason/Mellor estimate, which in turn yields drainage curves that agree with experiments. We therefore generalized the MSP theory in two ways: first to account for the 3D nature of the pore throats (original MSP assumes that a throat has constant cross section for arbitrary distance) and second to apply to spheres of different sizes. To our knowledge this is the first time the theory has been so generalized. The methodology is described in the following section. We then used the MSP values to compute drainage curves.

Mayer-Stowe-Princen theory for unequal spheres

MSP calculation is essentially two-dimensional and is valid for constant-cross-section throats. Here we rather present a 3D calculation of MSP theory for pore throat critical curvature. We thus present formulas for throats formed by three spheres of arbitrary sizes R_1 , R_2 , and R_3 .



Assume that the non-wetting fluid (gas) fills cross-sectional area A_{eff} at capillary pressure P_c . The work involved in moving the meniscus configuration by a small distance dx along the perpendicular walls is equal to P_cA_{eff} dx and has to overcome the surface tension. Thus the energy balance reads:

$$P_{c}A_{eff}dx = \sigma P_{L}dx + (\sigma_{SG} - \sigma_{SL})P_{S}dx$$

where P_L is the total perimeter between the non-wetting and wetting fluids (gas and liquid), P_S is the total perimeter between non-wetting fluid (gas) and solid, and σ , σ_{SG} , and σ_{SL} are the liquid–gas, solid–gas and solid–liquid surface tensions.

From the Young–Dupre equation we know that $\sigma_{SG} - \sigma_{SL} = \sigma \cos(\theta)$ where θ is the contact angle so we obtain:

$$P_c A_{eff} dx = \sigma (P_L + P_S \cos \theta) dx$$

We introduce effective perimeter,

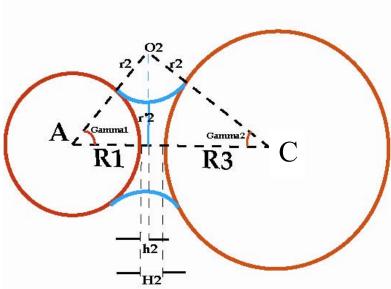
$$P_{eff} = P_L + P_S \cos \theta$$

Then from $P_c = \sigma C$ and the above equation we get the relation $C = \frac{P_{eff}}{A_{eff}}$. We have:

$$\begin{cases} A' = A_{\Delta} - \frac{\alpha R_1^2}{2} - \frac{\beta R_2^2}{2} - \frac{\gamma R_3^2}{2} \\ P' = \alpha R_1 + \beta R_2 + \gamma R_3 \end{cases}$$

$$\begin{cases} \Delta A = \Delta A_{AB} + \Delta A_{AC} + \Delta A_{BC} \\ \Delta P = \Delta P_{AB} + \Delta P_{AC} + \Delta P_{BC} \end{cases}$$
 and
$$P_{e\!f\!f} = P' - \Delta P \\ A_{e\!f\!f} = A' - \Delta A \end{cases}$$
 Therefore, $C = \frac{P' - \Delta P}{A' - \Delta A}$

For the pendular ring between the spheres A and C which is shown in the following figure we would have:



$$\begin{cases} \gamma_{1} = \arctan(\frac{r_{2} + r_{2}'}{R_{1} + h_{2}}) \\ \gamma_{2} = \arctan(\frac{r_{2} + r_{2}'}{R_{3} + H_{2} - h_{2}}) \end{cases}$$

$$A_{1} = \frac{1}{2}(R_{1} + h_{2})^{2} \tan \gamma_{1} + \frac{1}{2}(R_{3} + H_{2} - h_{2})^{2} \tan \gamma_{2} = \frac{1}{2}b(r_{2} + r_{2}') = \frac{1}{2}b(r_{2} + \frac{r_{2}}{1 - Cr_{2}})$$

$$\Delta P_{AC} = \gamma_{1}R_{1} + \gamma_{2}R_{3} - (\pi - \gamma_{1} - \gamma_{2})r_{2}$$

$$\Delta A_{AC} = A_{1} - \frac{1}{2}\gamma_{1}R_{1}^{2} - \frac{1}{2}\gamma_{2}R_{3}^{2} - \frac{1}{2}(\pi - \gamma_{1} - \gamma_{2})r_{2}^{2}$$

$$\begin{cases} \frac{r_2 - h_2}{r_2 - H_2 + h_2} = \frac{2R_3 + r_2 + H_2 - h_2}{2R_1 + r_2 + h_2} \\ (r_2 + \frac{r_2}{1 - Cr_2})^2 = (2R_1 + r_2 + h_2)(r_2 - h_2) \end{cases}$$

Similarly for the pendular ring between the spheres A and B we would have:

$$\begin{cases} \alpha_1 = \arctan(\frac{r_3 + r_3}{R_1 + h_3}) \\ \alpha_2 = \arctan(\frac{r_3 + r_3}{R_2 + H_3 - h_3}) \\ A_3 = \frac{1}{2}(R_1 + h_3)^2 \tan \alpha_1 + \frac{1}{2}(R_2 + H_3 - h_3)^2 \tan \alpha_2 = \\ = \frac{1}{2}c(r_3 + r_3') = \frac{1}{2}c(r_3 + \frac{r_3}{1 - Cr_3}) \\ \Delta A_{AB} = A_3 - \frac{1}{2}\alpha_1R_1^2 - \frac{1}{2}\alpha_2R_2^2 - \frac{1}{2}(\pi - \alpha_1 - \alpha_2)r_3^2 \\ \Delta P_{AB} = \alpha_1R_1 + \alpha_2R_2 - (\pi - \alpha_1 - \alpha_2)r_3 \\ \begin{cases} \frac{r_3 - h_3}{r_3 - H_3 + h_3} = \frac{2R_2 + r_3 + H_3 - h_3}{2R_1 + r_3 + h_3} \\ (r_3 + \frac{r_3}{1 - Cr_3})^2 = (2R_1 + r_3 + h_3)(r_3 - h_3) \end{cases}$$

And for the spheres B and C we would have the following relationships:

$$\begin{cases} \beta_{1} = \arctan(\frac{r_{1} + r_{1}'}{R_{2} + h_{1}}) \\ \beta_{2} = \arctan(\frac{r_{1} + r_{1}'}{R_{3} + H_{1} - h_{1}}) \end{cases}$$

$$A_{2} = \frac{1}{2}(R_{2} + h_{1})^{2} \tan \beta_{1} + \frac{1}{2}(R_{3} + H_{1} - h_{1})^{2} \tan \beta_{2} = \frac{1}{2}a(r_{1} + r_{1}') = \frac{1}{2}a(r_{1} + \frac{r_{1}}{1 - Cr_{1}})$$

$$\Delta P_{BC} = \beta_{1}R_{2} + \beta_{2}R_{3} - (\pi - \beta_{1} - \beta_{2})r_{1}$$

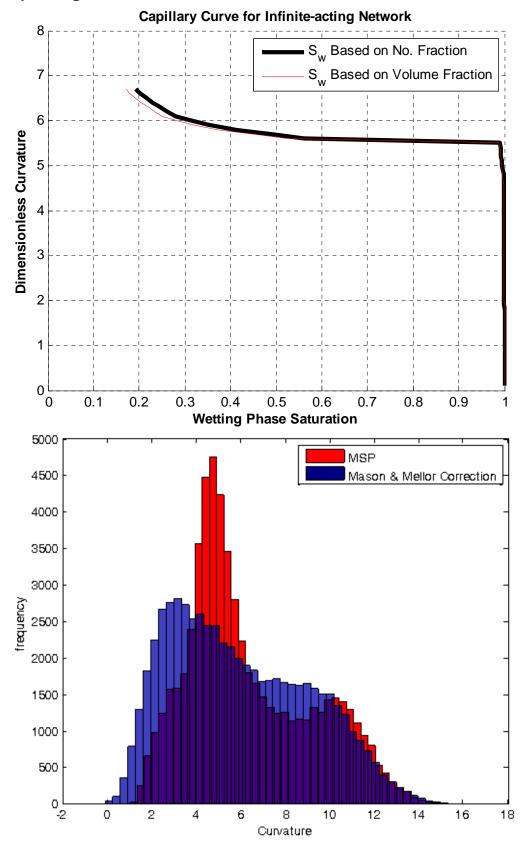
$$\Delta A_{BC} = A_{2} - \frac{1}{2}\beta_{1}R_{2}^{2} - \frac{1}{2}\beta_{2}R_{3}^{2} - \frac{1}{2}(\pi - \beta_{1} - \beta_{2})r_{1}^{2}$$

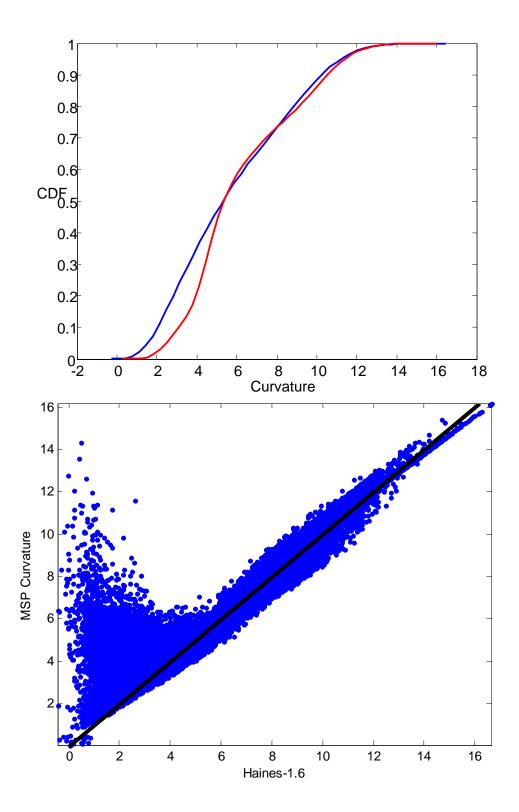
$$\begin{cases} \frac{r_1 - h_1}{r_1 - H_1 + h_1} = \frac{2R_3 + r_1 + H_1 - h_1}{2R_2 + r_1 + h_1} \\ (r_1 + \frac{r_1}{1 - Cr_1})^2 = (2R_2 + r_1 + h_1)(r_1 - h_1) \end{cases}$$

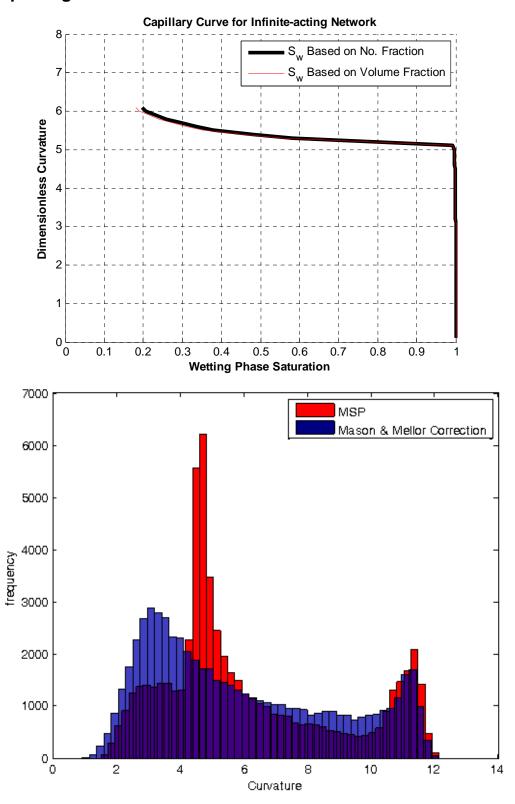
Solving the system all above equations the MSP critical values of the pore throats are calculated.

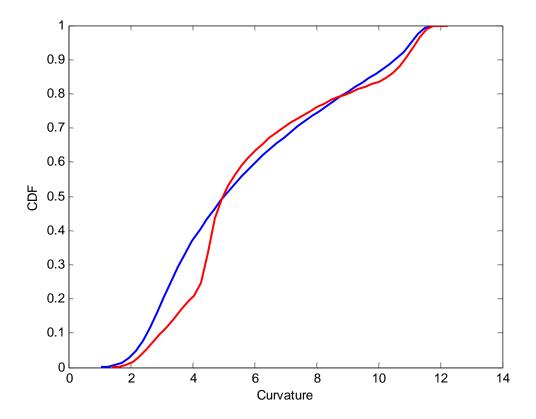
In the following we have compared the MSP critical values and the Mason and Mellor approximation (which we used to use in drainage simulations before) for some sample packings (#11, #41, #49 and #53_reduced, which is #53 with grains smaller that 0.1 R_{mean} removed to avoid spurious throats.) For each packing we show (i) the drainage capillary pressure vs. saturation curve using the MSP critical curvatures; (ii) histogram of MSP and Mason/Mellor critical curvatures for all throats in the model sediment; (iii) cumulative distribution of MSP and Mason/Mellor critical curvatures; and (iv) a cross-plot of the MSP and Mason/Mellor estimate for each throat. The Mason/Mellor estimate is labeled as "Haines – 1.6" in the latter plot, indicating its origin. The drainage curves are reported in two ways, as number fraction of pores still containing water and as volume fraction of pores still containing water held in pendular rings at grain contacts is included in all the drainage curves.

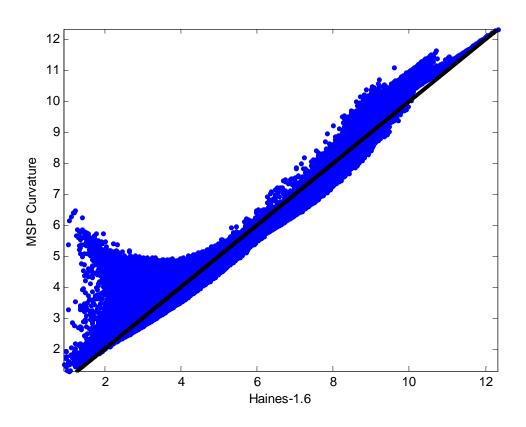
An important improvement afforded by the MSP calculation is that it eliminates the need for the empirical correction of -1.6, introduced by Mason and Mellor for very well sorted packings. This value works very well for those packings, but it results in negative critical curvatures for a few of the Delaunay throats in the poorly sorted packings. This is evident in the histograms. Clearly negative critical curvatures are nonphysical, since the grains are water-wet. The negative values occur partly because these throats do not correspond to the full set of grains that support the gas/water interface in that region of pore space. But it is also true that the correction should vary with the size of the grains comprising the throat. This matters in a poorly sorted packing, because throats can be made of several large grains or several small grains. But with the generalized MSP method, it is not possible to obtain negative critical curvatures.

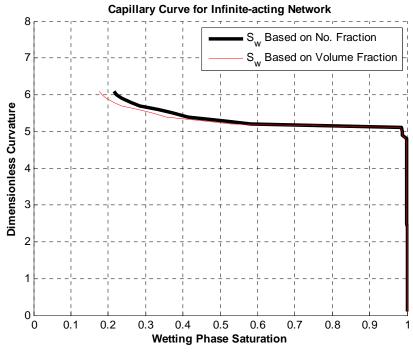


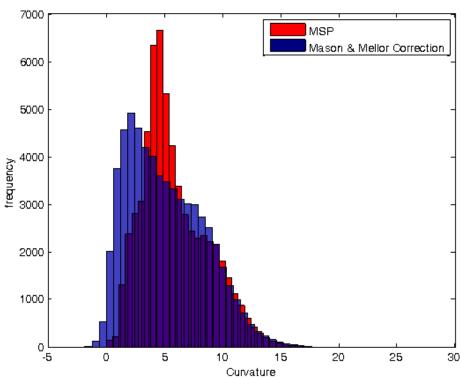


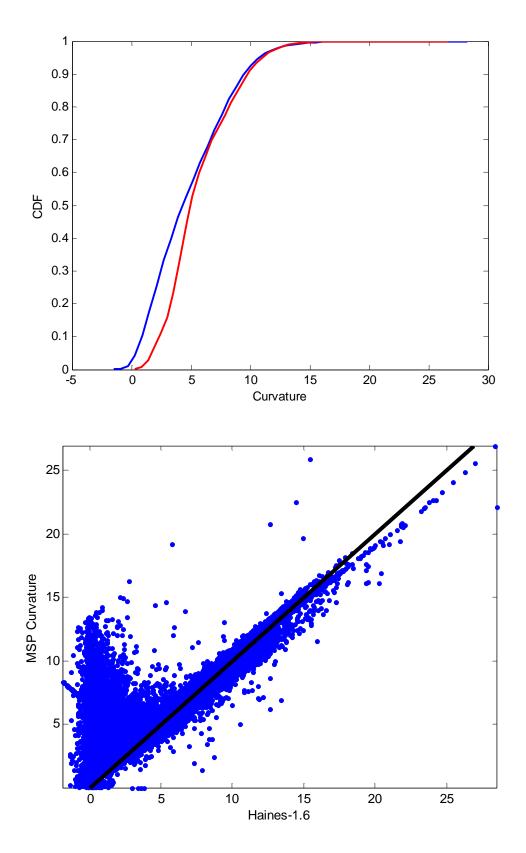


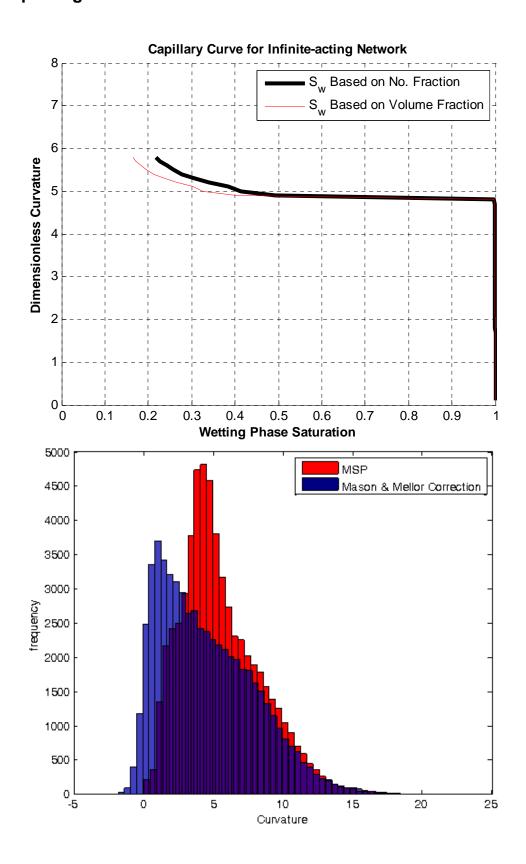


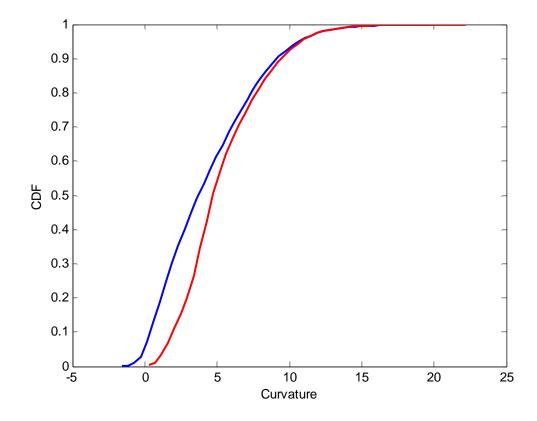


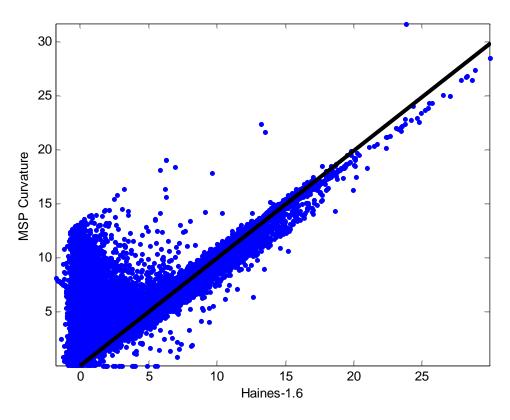












5.2.2 Imbibition Simulation from Drainage Endpoint in Model Sediments

The full set of simulations is reported in Appendix C. Here we review the approach taken.

We implemented a invasion percolation algorithm for imbibition. The simulation is analogous to the drainage simulation. Key differences are the initial condition (we start from the drainage endpoint, i.e. from irreducible water saturation as described in previous section) and the critical curvature for imbibition of a pore. An important similarity is the condition for trapping the displaced phase (gas in this case). A pore containing gas cannot be imbibed by water unless that pore is part of a cluster of connected, gas-filled pores which spans the network. Here "spans" means that the cluster is connected through at least one pair of periodic boundaries. If this condition is satisfied, the cluster is effectively infinite in extent, because it will be connected through any number of copies of the periodic unit cell placed adjacent to the original cell.

The simulations in very well sorted packings predict the same percolation threshold as observed in experiments, viz. at a dimensionless curvature of about 4. For most model sediments the residual saturations range from 30% to 40%, which are larger than observed in experiments. This is because the infinite-acting networks impose a more stringent condition for displacement of the gas phase, viz. percolation of the cluster of pores containing the gas. The predicted residual saturations are however consistent with typical observations in single well tracer tests applied to injection wells. The latter tests are conducted by injecting a solution containing a conservative tracer and a partitioning tracer into the reservoir around an injector, where all oil saturation is likely to be at or near residual. The injected fluid is then produced back from the same well. The difference in return times of the two tracers is a measure of residual oil saturation. Values are typically 40% or so.

Appendix A: Summary of Properties of Model Sediments

For convenience we reproduce from earlier reports that summary of the properties of the model sediments used in this research. All are dense, disordered, computer-generated packings of spheres. We use the nouns "sphere" and "grain" interchangeably. Packings with similar grain size distribution and similar sorting index values are grouped together:

	Table 1. Summary of Properties of Model Sediments								
	Grain sizes (arbitrary units)				Porosity (fraction)	Sorting I	ndex	Notes*	
Packing No.	Minimum Radius	Maximum radius	Mean radius	Standard deviation		Number fraction basis	Volume or weight fraction basis	Grain Surface Area/Bulk Volume	
1	0.32	2.58	2.18	0.11	0.37	1.04	1.04	0.873398	LN
2	1.84	2.64	2.18	0.11	0.36	1.03	1.03	0.873713	LN
3	1.8	2.6	2.18	0.11	0.37	1.03	1.03	0.871821	LN
4	0.32	2.59	2.18	0.11	0.35	1.03	1.03	0.874216	LN
5	1.82	2.52	2.15	0.11	0.41	1.03	1.03	0.845784	LN
Average	1.22	2.59	2.17	0.11	0.37	1.03	1.03		
6	1.5	3.22	2.17	0.22	0.36	1.07	1.07	0.870069	LN
7	1.5	3.08	2.16	0.22	0.36	1.07	1.07	0.862364	LN
8	1.48	2.99	2.17	0.22	0.36	1.07	1.07	0.867997	LN
9	1.47	3.06	2.16	0.22	0.37	1.07	1.07	0.862127	LN
Average	1.49	3.09	2.16	0.22	0.36	1.07	1.07		
10	0.96	4.12	2.12	0.42	0.35	1.14	1.14	0.853125	LN
11	0.93	4.64	2.12	0.43	0.34	1.14	1.14	0.855595	LN
12	1.07	4.49	2.11	0.42	0.35	1.14	1.14	0.852085	LN
13	0.99	4.27	2.11	0.43	0.35	1.14	1.14	0.846668	LN
Average	0.99	4.38	2.11	0.43	0.35	1.14	1.14		
14	4.24E-03	7.05	1.9	0.8	0.32	1.31	1.32	0.853125	LN
15	3.44E-03	6.44	1.9	0.79	0.35	1.31	1.31	0.855595	LN
16	3.91E-01	6.38	1.91	0.78	0.33	1.31	1.29	0.852085	LN
17	7.81E-03	7.01	1.9	0.79	0.32	1.31	1.3	0.846668	LN
18	1.59E-03	7.62	1.91	0.79	0.32	1.31	1.29	0.779363	LN
Average	8.17E-02	6.9	1.9	0.79	0.33	1.31	1.3		
19	1.86E-03	11.3	1.31	1.16	0.29	1.72	1.48	0.774083	LN; Trn
20	2.39E-03	10.16	1.31	1.17	0.25	1.72	1.54	0.782817	LN; Trn
21	7.85E-03	11.26	1.31	1.15	0.3	1.72	1.53	0.77599	LN; Trn
22	1.17E-03	11.17	1.3	1.16	0.3	1.69	1.53	0.780766	LN; Trn
Average	3.32E-03	10.97	1.31	1.16	0.29	1.71	1.52		
23	3.45E-05	11.31	0.69	1.25	0.31	3.11	1.32	0.561808	LN; Trn
24	1.63E-05	11.19	0.71	1.26	0.3	3.12	1.38	0.566764	LN; Trn
25	3.80E-05	11.28	0.7	1.25	0.37	3.16	1.3	0.556885	LN; Trn

26	1.44E-05	12.16	0.72	1.23	0.32	3.07	1.46	0.556307	LN; Trn
Average	2.58E-05	11.49	0.71	1.25	0.33	3.11	1.37		
27	8.10E-06	18.29	0.3	1.07	0.31	3.63	1.38	0.375571	LN; Trn
28	2.04E-06	21.32	0.3	1.04	0.29	3.77	1.37	0.385136	LN; Trn
29	6.94E-06	22.46	0.31	1.04	0.32	3.95	1.41	0.377781	LN; Trn
Average	5.69E-06	20.69	0.31	1.05	0.31	3.79	1.39		
30	1.24E-03	11.93	1.01	1.2	0.29	2	1.5	0.373962	LN; Trn
31	6.31E-04	11.99	1.04	1.22	0.32	2	1.56	0.227332	LN; Trn
32	5.70E-04	12.34	1.02	1.21	0.3	2.03	1.48	0.215402	LN; Trn
33	4.21E-05	12.57	1.07	1.22	0.31	1.94	1.51		LN; Trn
34	5.47E-04	11.63	1.03	1.19	0.34	2.01	1.49		LN; Trn
Average	6.06E-04	12.09	1.03	1.21	0.31	2	1.51		
35	4.62E-04	9.67	1.63	1.03	0.3	1.51	1.4	0.213955	LN
36	1.89E-03	9.7	1.61	1.04	0.3	1.5	1.43	0.451858	LN
37	1.35E-03	9.3	1.59	1.04	0.27	1.49	1.46	0.466817	LN
38	3.98E-03	9.41	1.6	1.05	0.27	1.51	1.44	0.457397	LN
Average	1.92E-03	9.52	1.6	1.04	0.29	1.5	1.43		
39	2	2.4	2.19	0.07	0.34	1.02	1.02	0.679516	N
40	2	2.41	2.19	0.07	0.35	1.02	1.02	0.671683	N
41	2	2.39	2.17	0.07	0.38	1.02	1.02	0.662955	N
42	2	2.4	2.19	0.07	0.37	1.02	1.02	0.666658	N
Averages	2	2.4	2.18	0.07	0.36	1.02	1.02		
43	1	3.2	2.14	0.35	0.36	1.12	1.1	0.878862	N
44	1	3.2	2.14	0.35	0.36	1.12	1.1	0.879162	N
45	1	3.2	2.14	0.36	0.35	1.12	1.11	0.86555	N
46	1	3.2	2.14	0.35	0.37	1.12	1.11	0.877698	N
Averages	1	3.2	2.14	0.35	0.36	1.12	1.1		
47	#	4.01	2.01	0.68	0.34	1.27	1.17	0.862418	
48	#	4.01	2.01	0.66	0.33	1.25	1.17	0.861402	
49	#	4.03	2.01	0.67	0.34	1.25	1.18	0.864378	
50	#	4.04	2.02	0.66	0.33	1.25	1.17	0.86135	
Averages	#	4.02	2.01	0.67	0.34	1.26	1.17	0.00.00	
51	#	4.59	1.85	0.9	0.32	1.42	1.21		
52	#	4.51	1.85	0.91	0.34	1.42	1.21		
53	#	4.44	1.86	0.89	0.35	1.4	1.21		
54	#	4.59	1.86	0.9	0.32	1.42	1.2		
Averages	#	4.53	1.86	0.9	0.33	1.42	1.21		
55	#	5	1.73	1.04	0.32	1.6	1.23		
56	#	5.06	1.71	1.05	0.31	1.64	1.22		
57	#	5.07	1.71	1.05	0.35	1.62	1.22		
58	#	5.08	1.71	1.05	0.34	1.65	1.23		
59	#	5.01	1.7	1.05	0.33	1.63	1.22		
53	π	5.01	1.7	1.00	0.55	1.03	1.44		

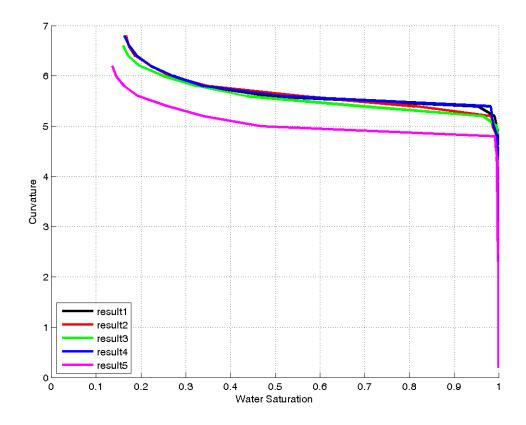
Averages	#	5.04	1.71	1.05	0.33	1.63	1.22		
60	#	4.56	1.84	0.91	0.32	1.43	1.21		
61	#	4.82	1.77	1	0.31	1.53	1.22	0.752922	
62	#	4.85	1.76	1	0.35	1.53	1.23	0.749431	
63	#	4.81	1.76	1	0.33	1.53	1.22	0.752072	
64	#	4.82	1.77	0.99	0.33	1.51	1.22	0.75331	
65	#	4.88	1.76	1	0.34	1.54	1.23	0.752684	
Averages	#	4.79	1.78	0.98	0.33	1.51	1.22		
66	#	5.36	1.6	1.15	0.33	1.89	1.24	0.711901	
67	#	5.38	1.61	1.14	0.32	1.85	1.24	0.712101	
68	#	5.44	1.6	1.15	0.33	1.94	1.23	0.708131	
69	#	5.43	1.6	1.14	0.33	1.91	1.24	0.704996	
70	#	5.32	1.59	1.14	0.33	1.9	1.25	0.704055	
Averages	#	5.39	1.6	1.14	0.33	1.9	1.24		
71	#	5.46	1.54	1.19	0.33	2.12	1.23	0.693023	
72	#	5.47	1.53	1.2	0.33	2.2	1.23	0.692432	
73	#	5.49	1.52	1.2	0.32	2.27	1.24		
74	#	5.64	1.53	1.2	0.33	2.18	1.24	0.690997	
75	#	5.65	1.53	1.19	0.33	2.13	1.26	0.688666	_
76	#	5.52	1.53	1.2	0.32	2.23	1.24	0.692512	
Averages	#	5.54	1.53	1.2	0.32	2.19	1.24		

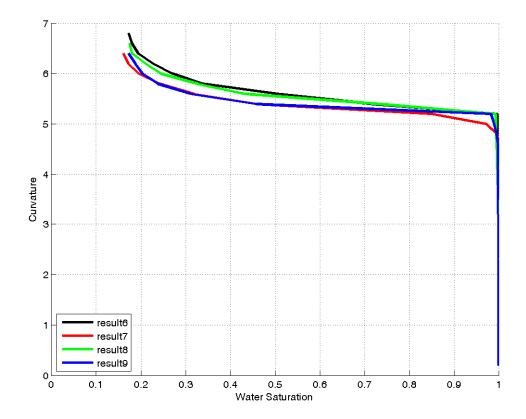
[#] indicates packings in which small grains were removed. Here "small" means less than one tenth the average grain size. In the following graphs packings with "_reduced" in their names show that we have eliminated these grains.

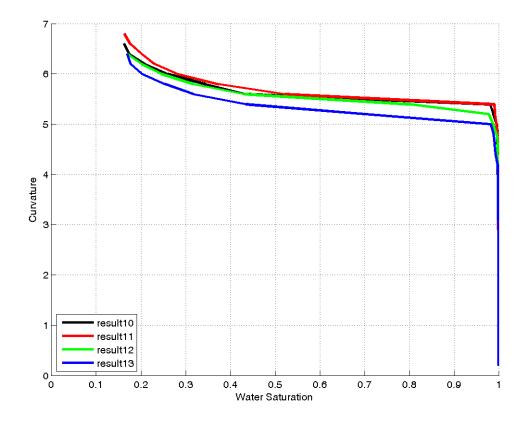
Appendix B: Drainage in All Model Sediments

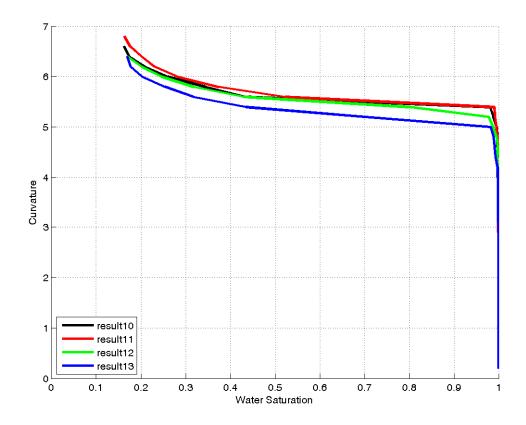
Drainage curves based on MSP critical curvatures along with the graphs of water/gas interfacial area for several packings are shown in the following graphs. The curves are labeled as "resultXX" where XX indicates the number of the model sediment in the table in Appendix A. Packings with "_reduced" in their names show that we have eliminated grains of size less than one tenth of the average grain size. This removes artifacts (very large nominal throat sizes) without affecting the essential physics so that the overall drainage behavior is consistent.

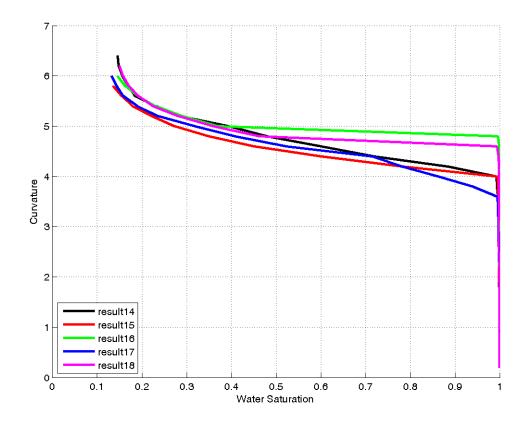
B.1 Drainage capillary pressure curves

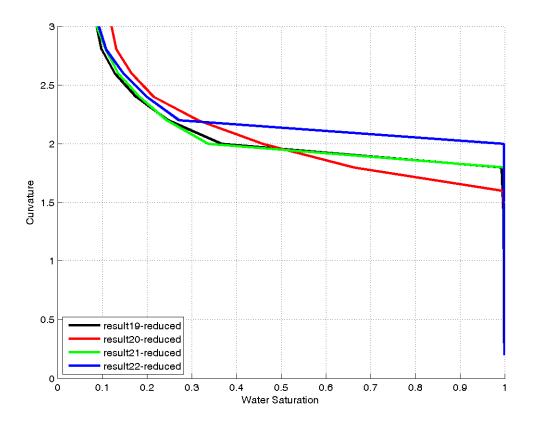


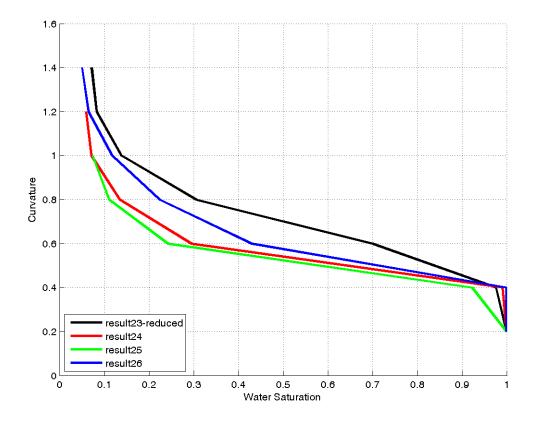


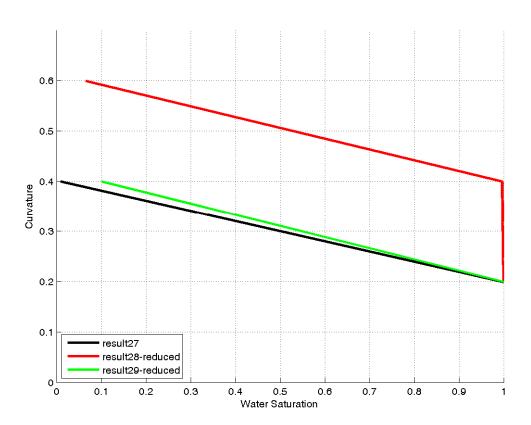


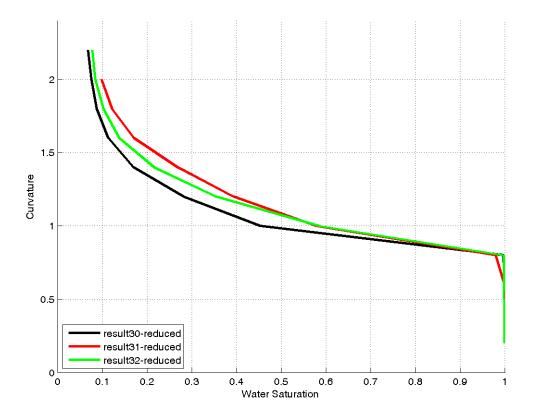


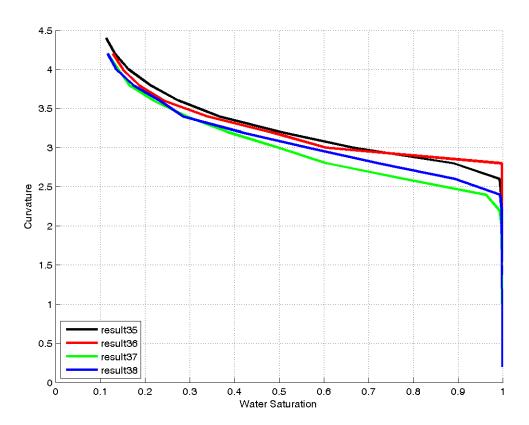


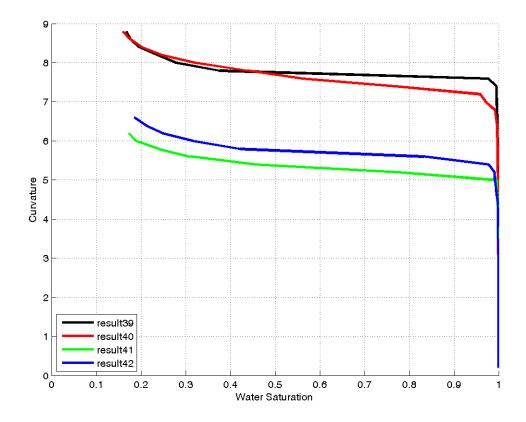


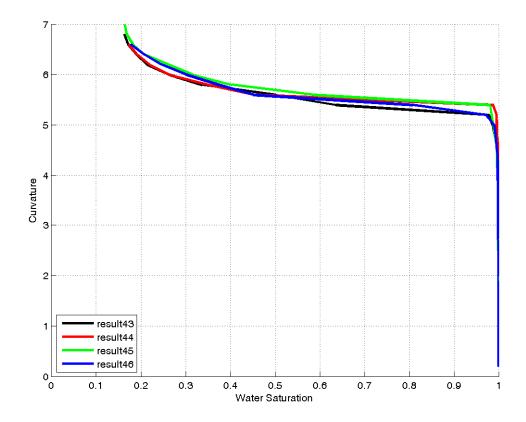


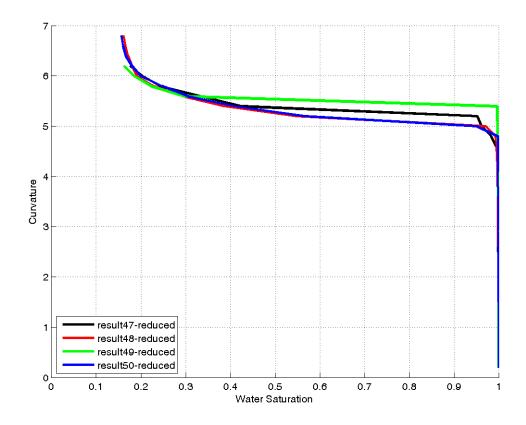


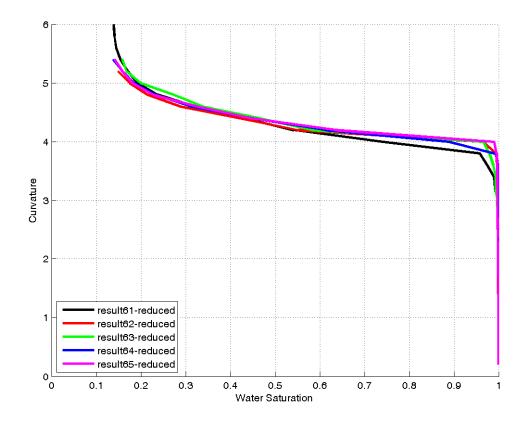


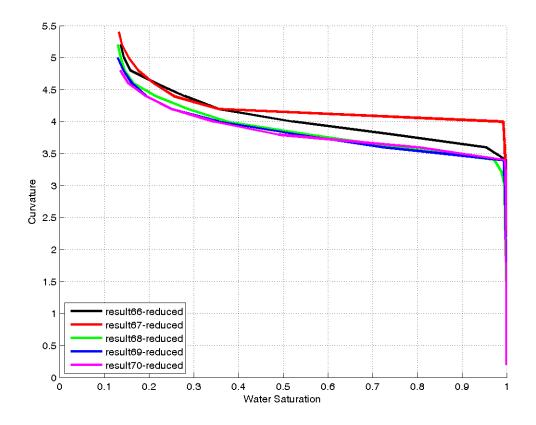


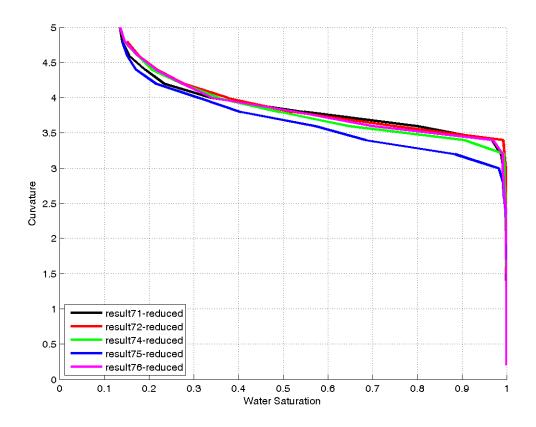






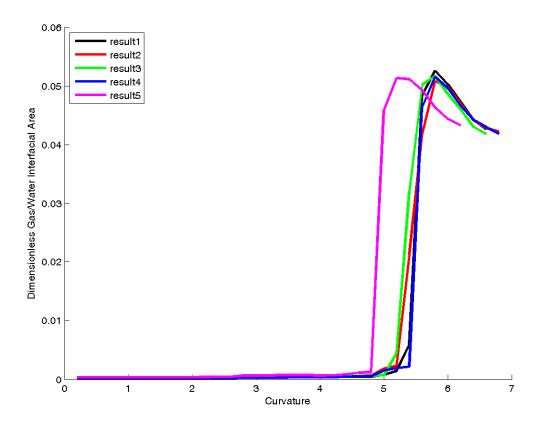


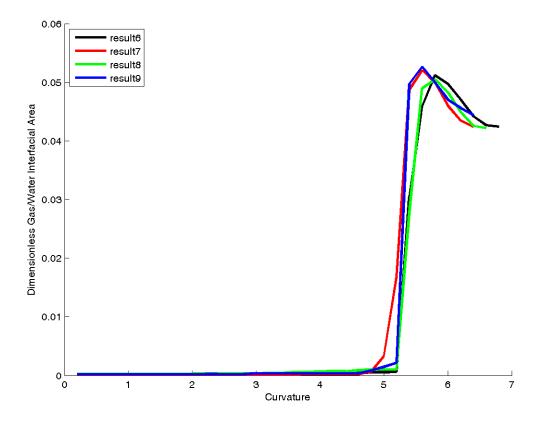


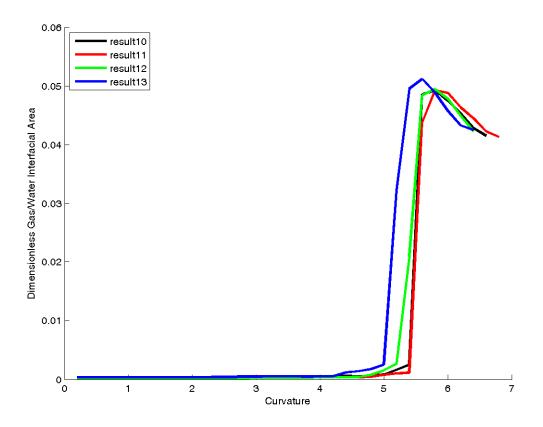


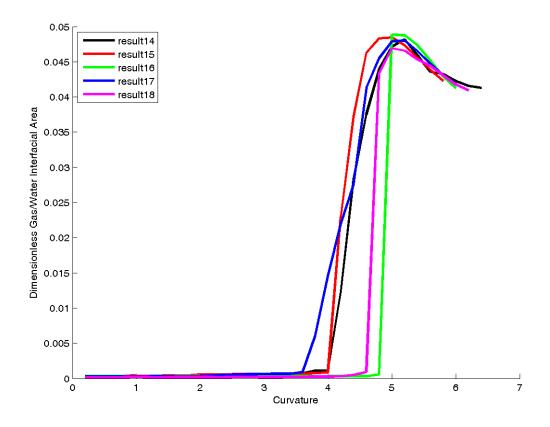
B.2 Normalized gas/water interfacial area during drainage.

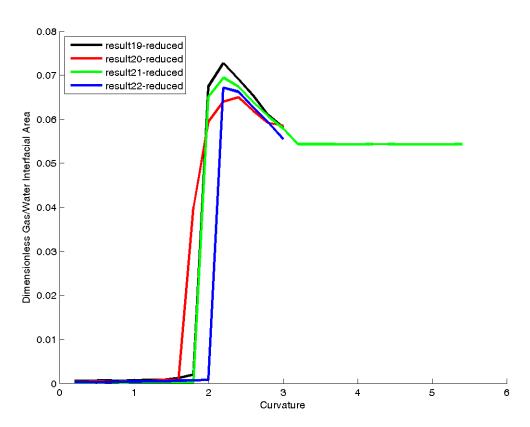
The interfacial area between gas and water was determined during drainage. The values have been normalized to the total grain surface area in the packing. The naming convention in the figure legends is same as in previous section.

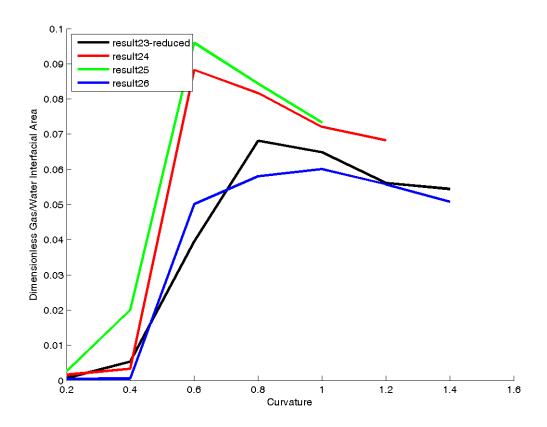


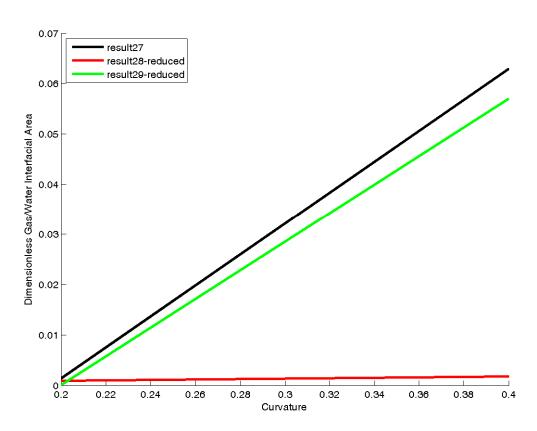


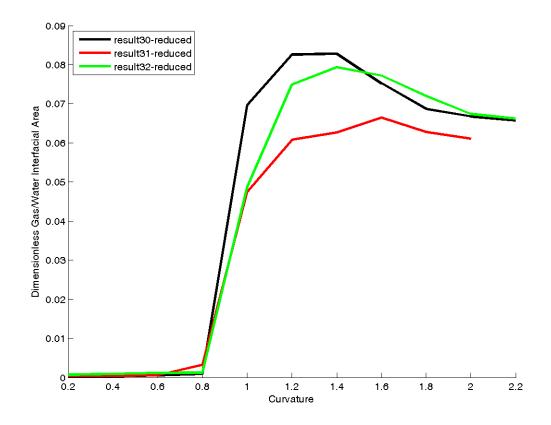


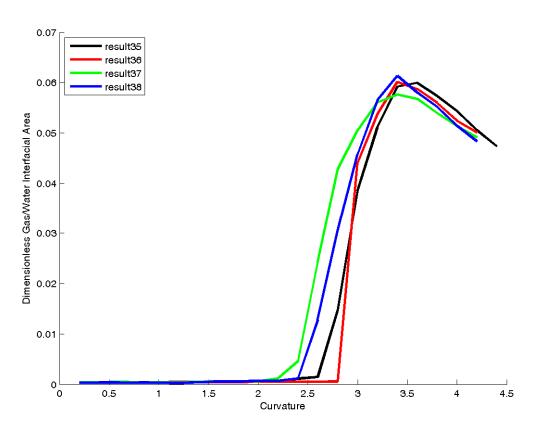


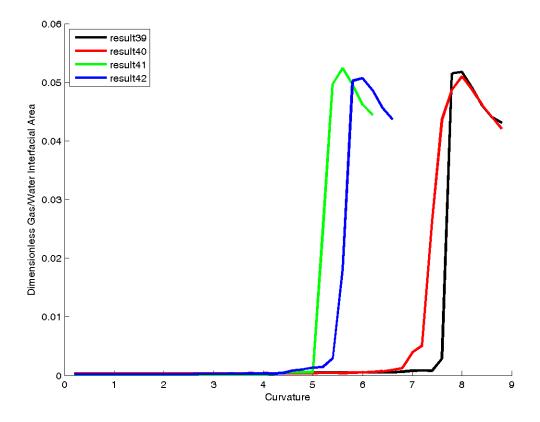


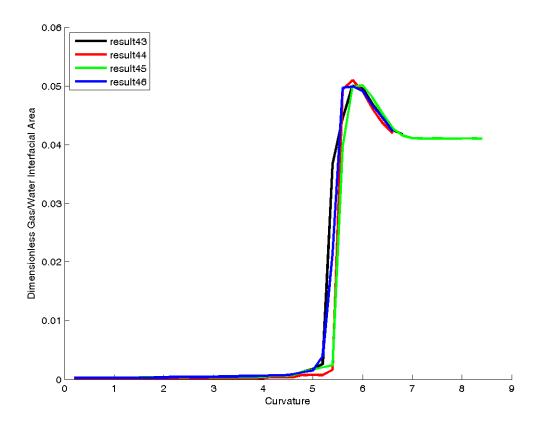


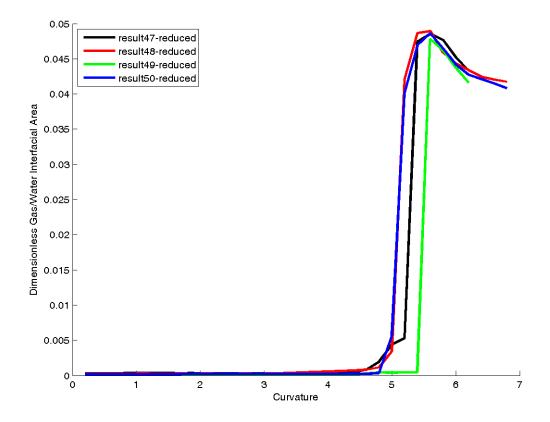


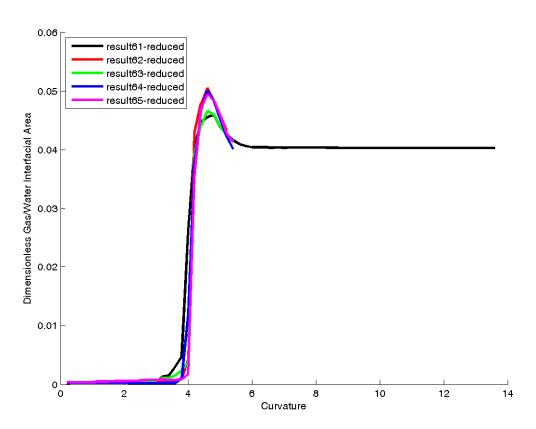


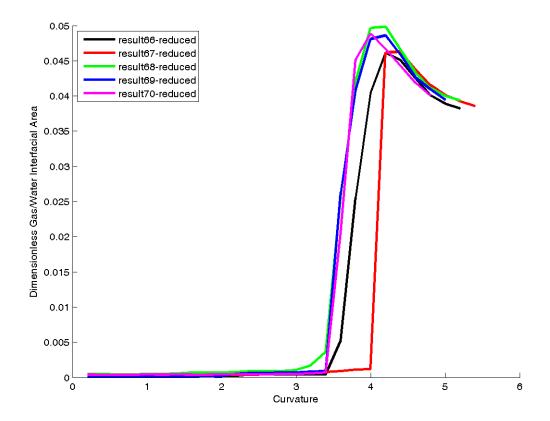


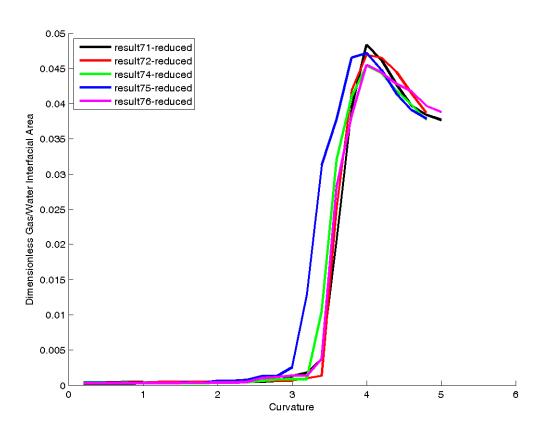






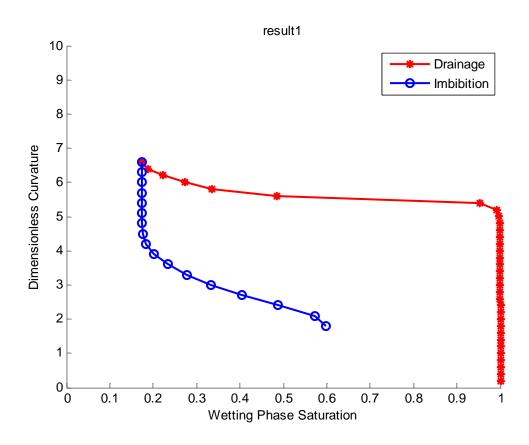


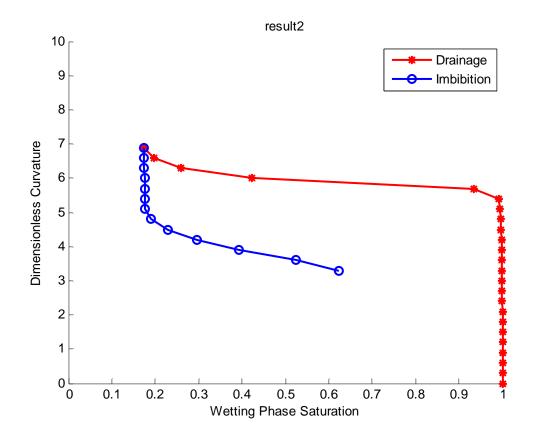


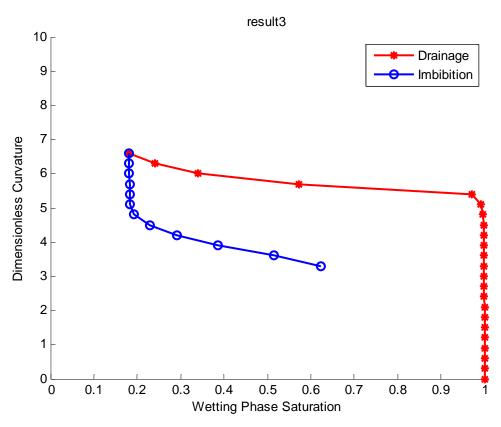


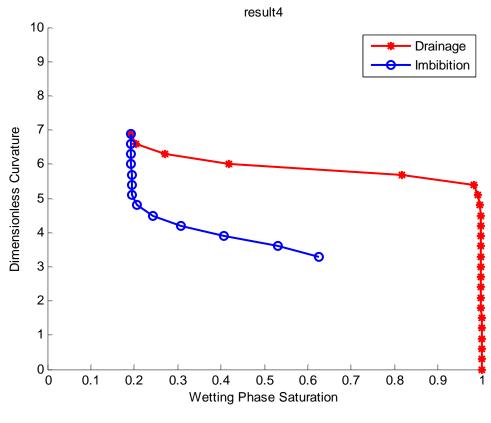
Appendix C: Imbibition in All Model Sediments

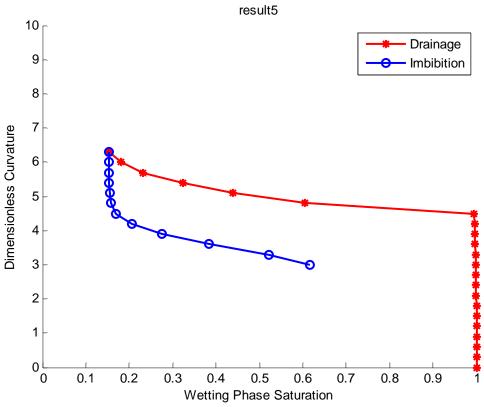
Imbibition curves based on the criterion for critical curvature in a pore reported previously are shown in the following graphs. The curves are labeled as "resultXX" where XX indicates the number of the model sediment in the table in Appendix A.

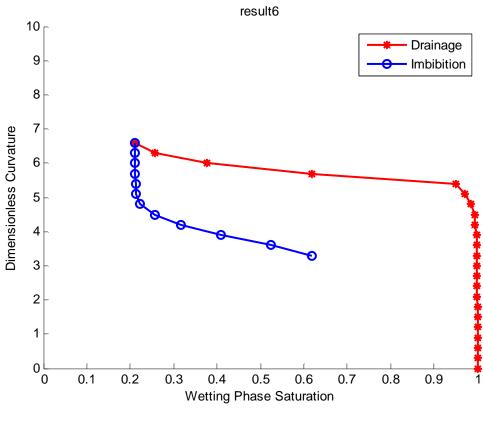


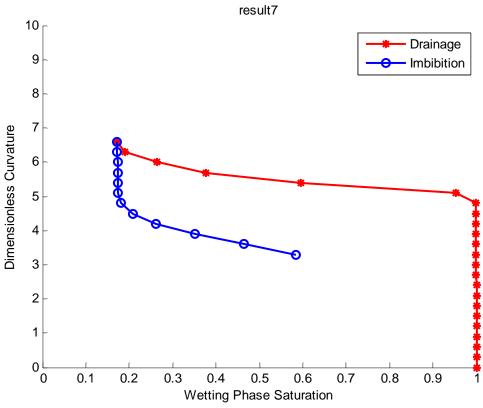


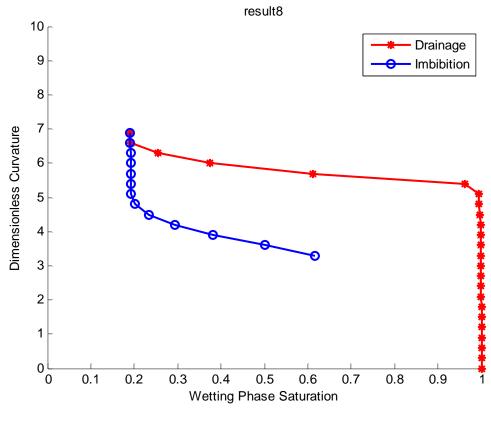


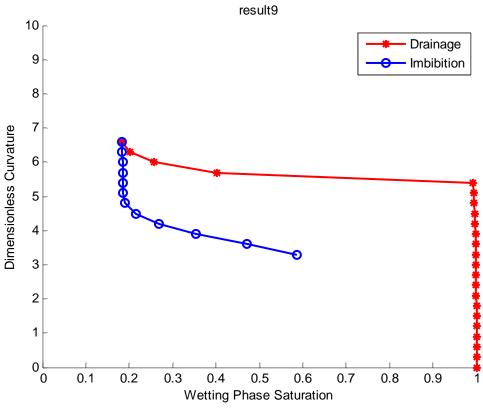


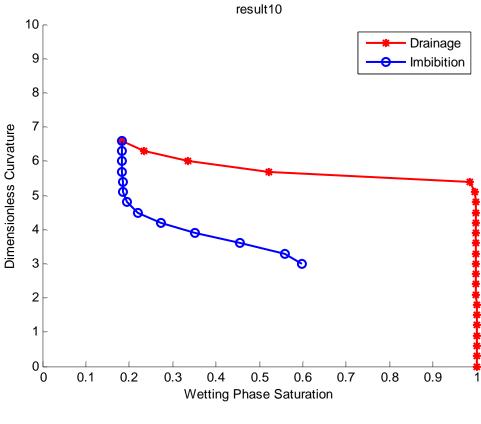


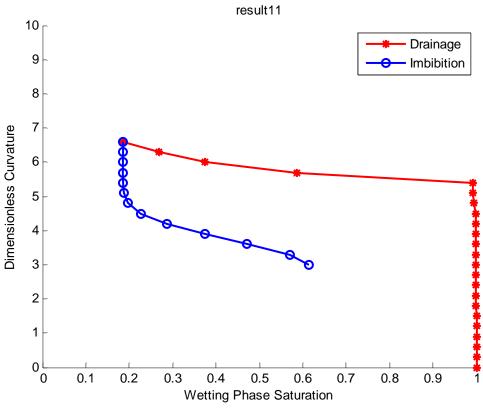


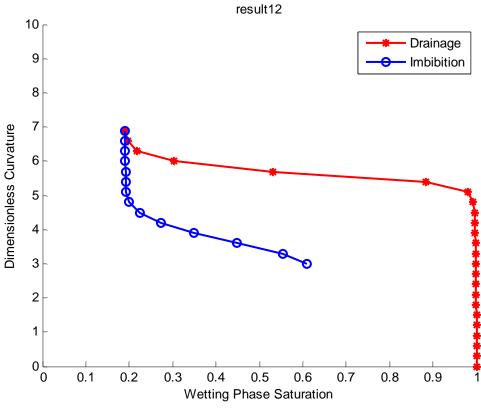


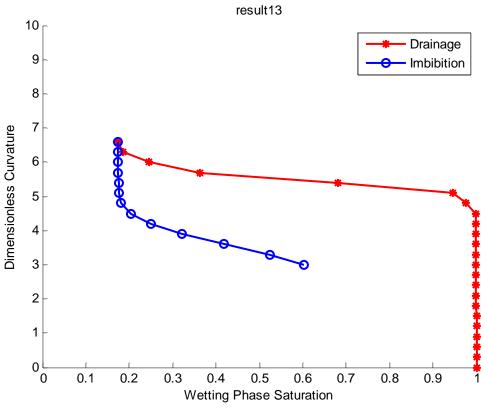


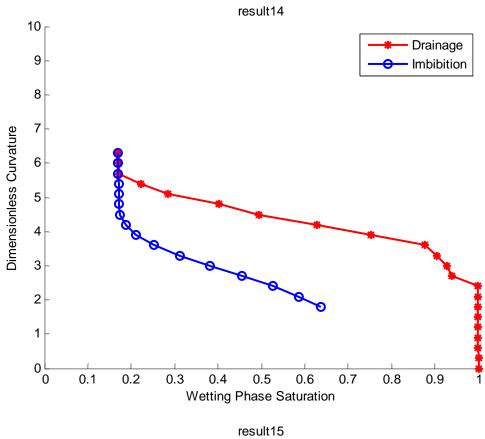


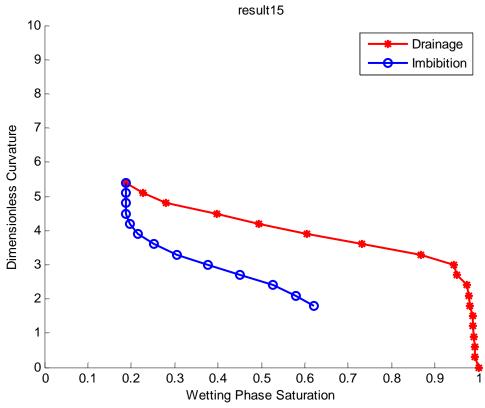


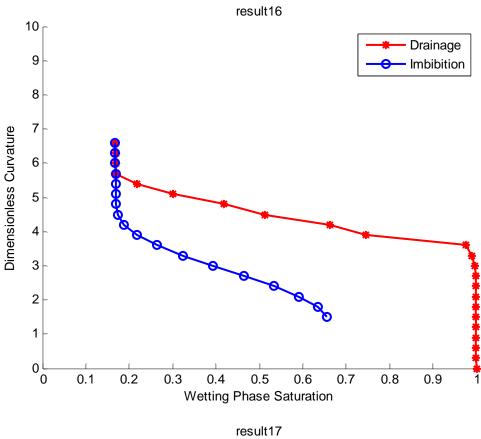


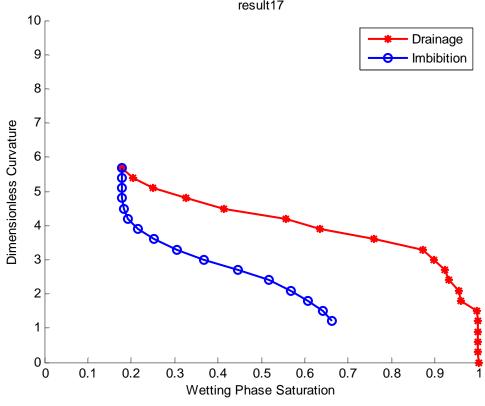


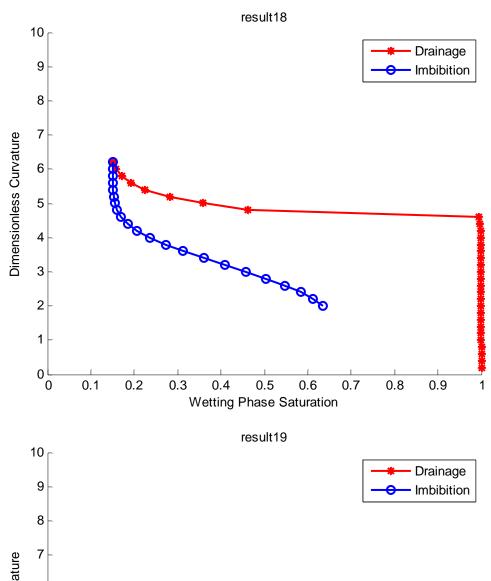


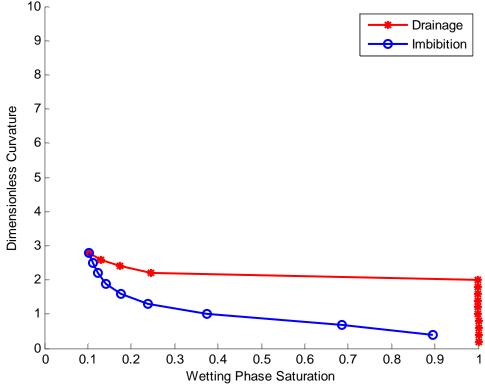


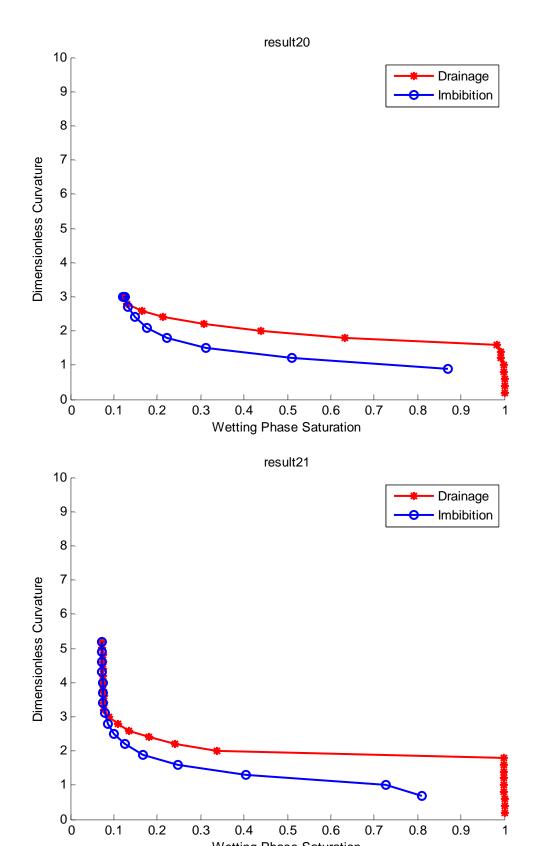




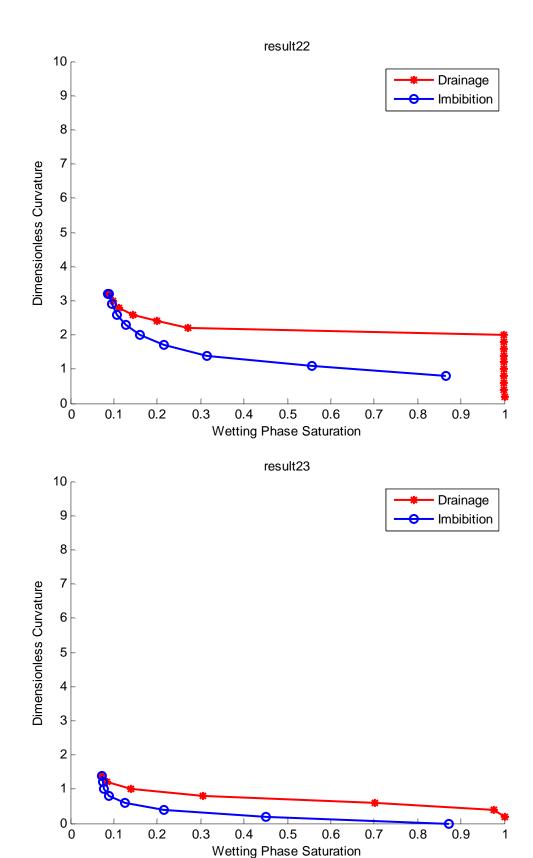


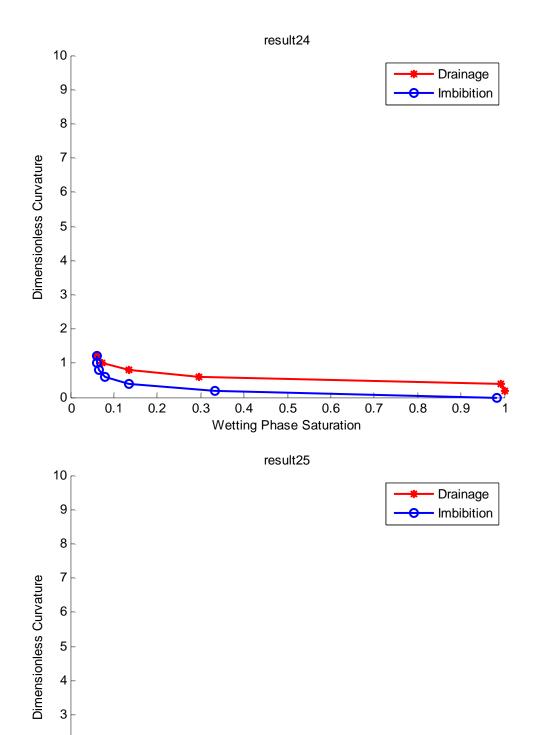






Wetting Phase Saturation





2

1

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0.3

0.2

0.1

0.4

0.5

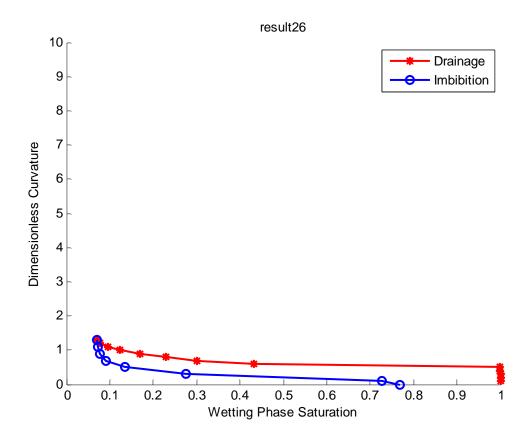
Wetting Phase Saturation

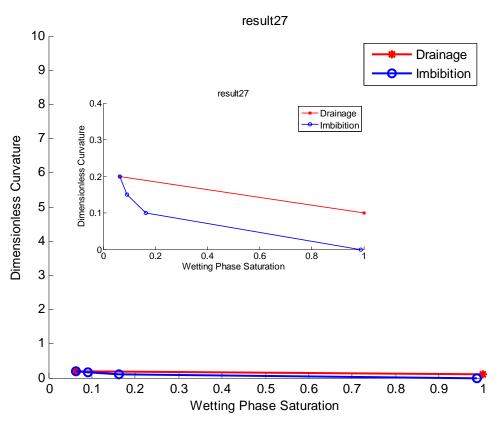
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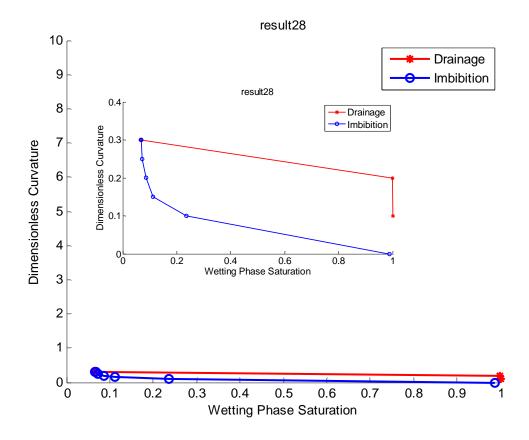
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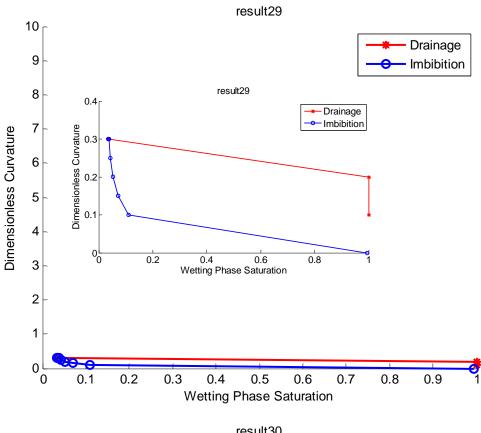
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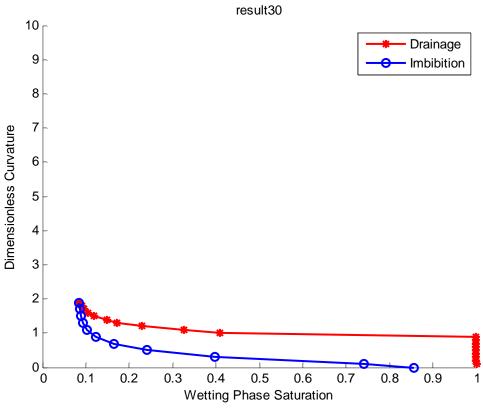
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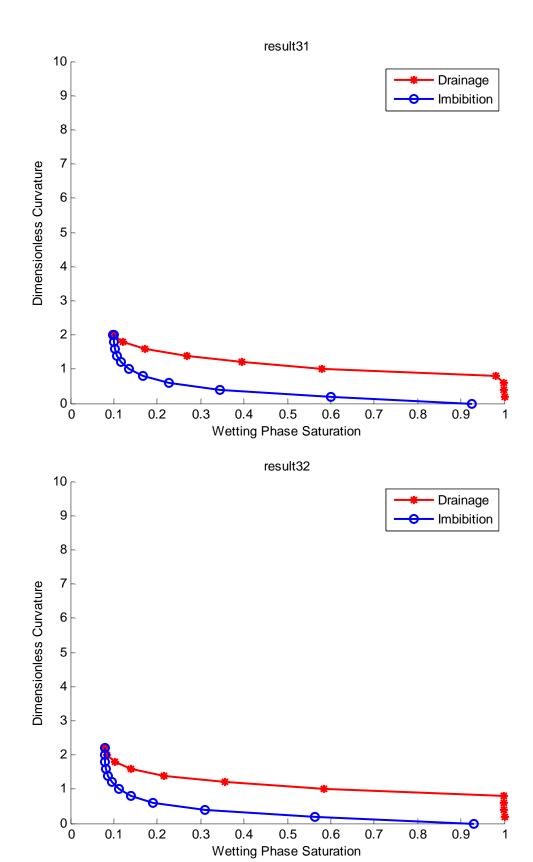


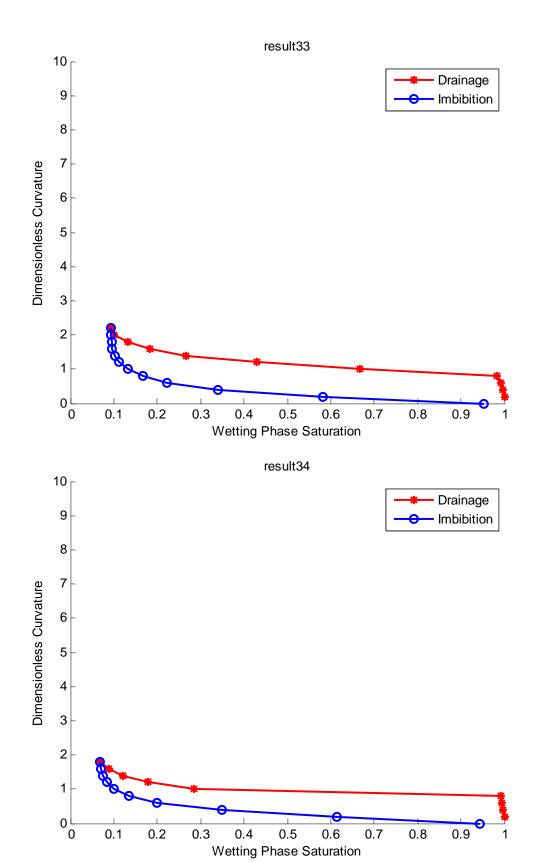


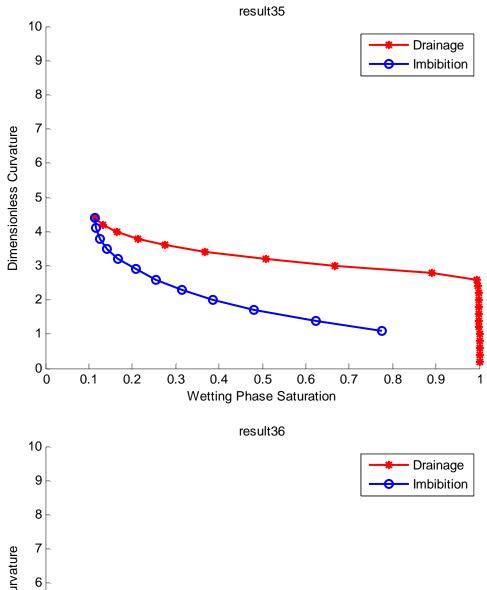


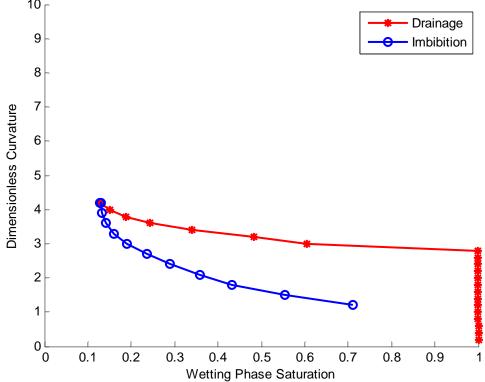


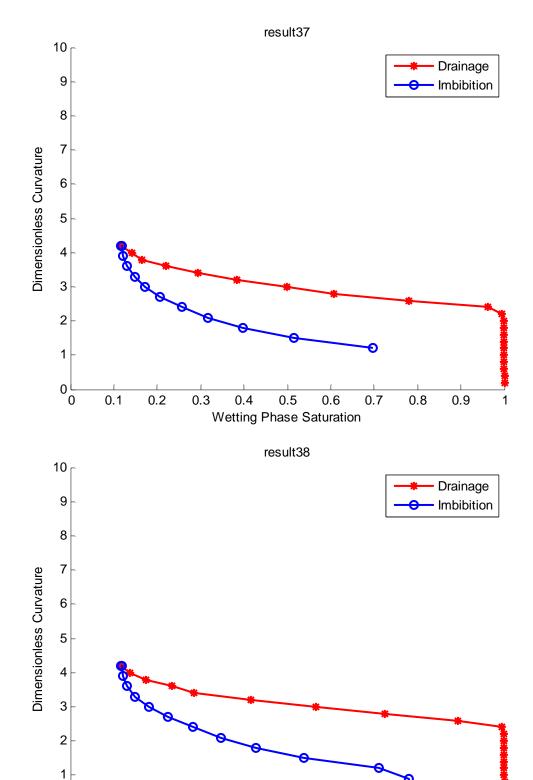












0 0

0.2

0.1

0.3

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0.5

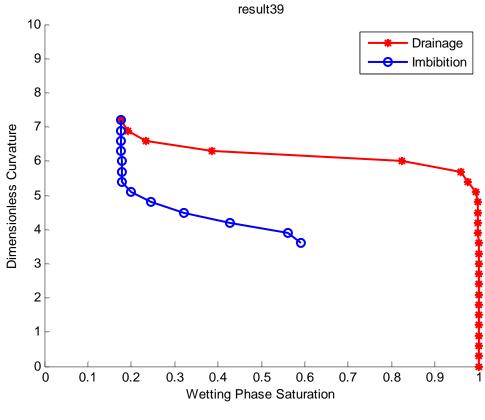
Wetting Phase Saturation

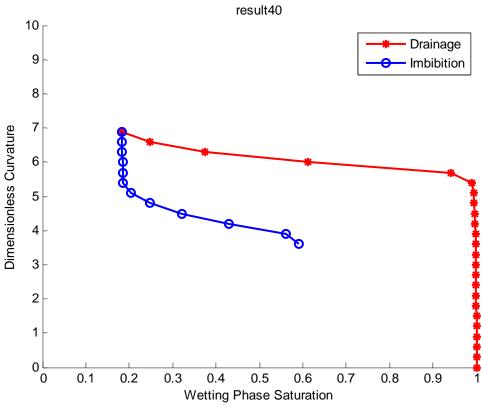
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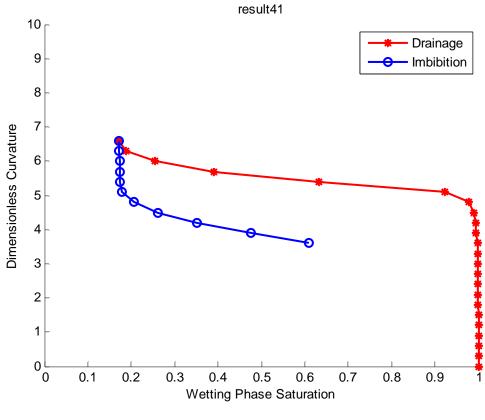
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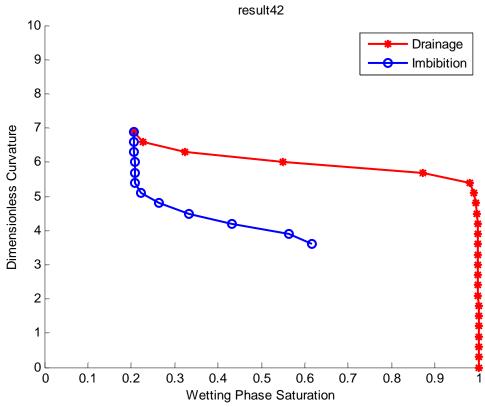
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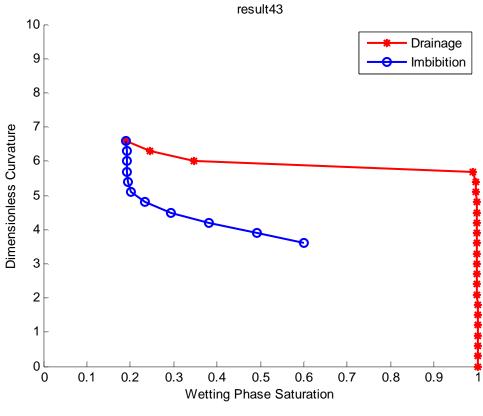
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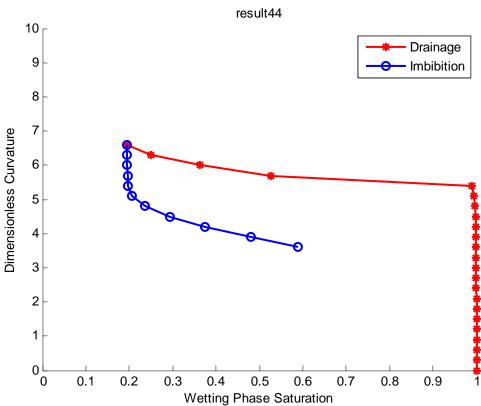


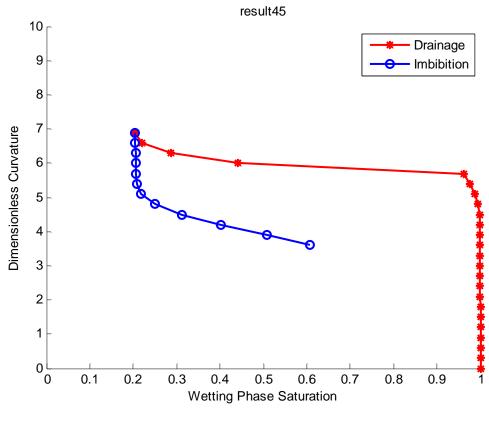


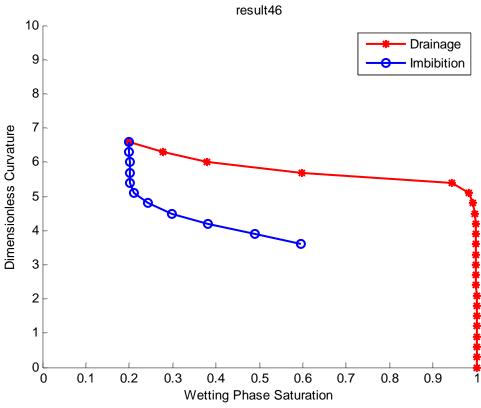


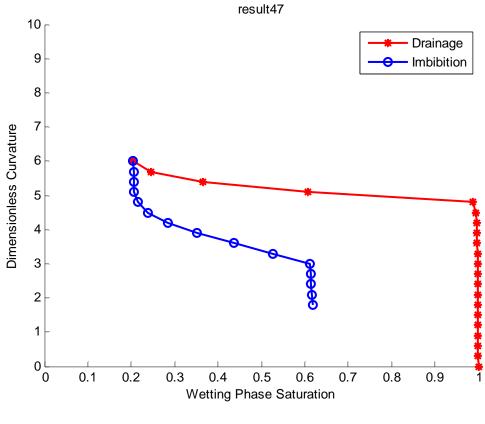


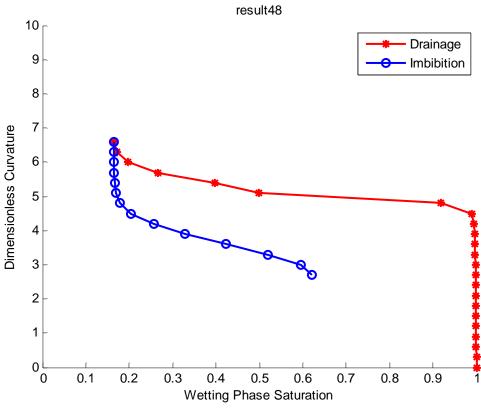


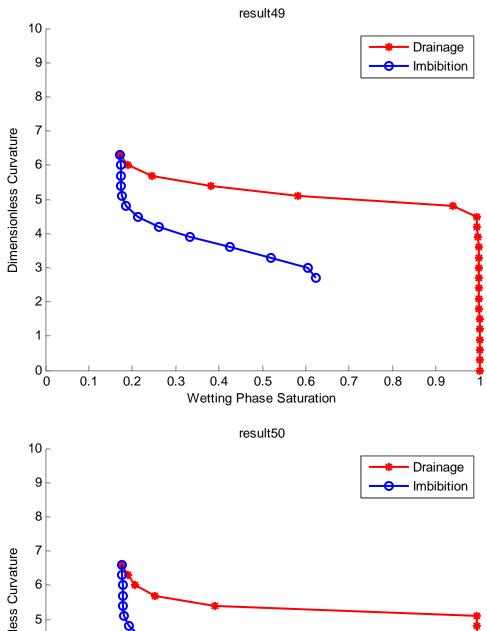


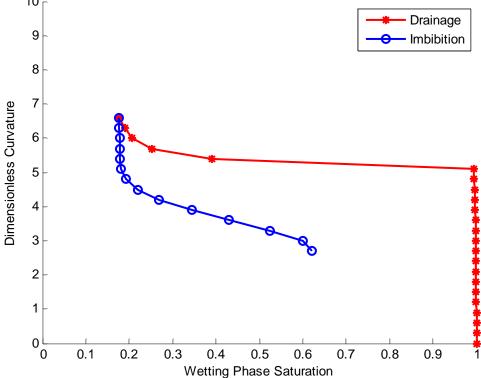


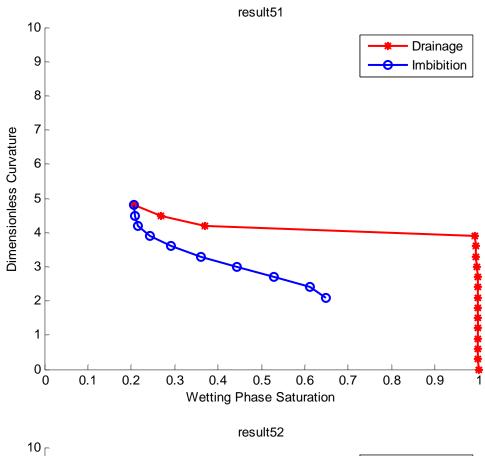


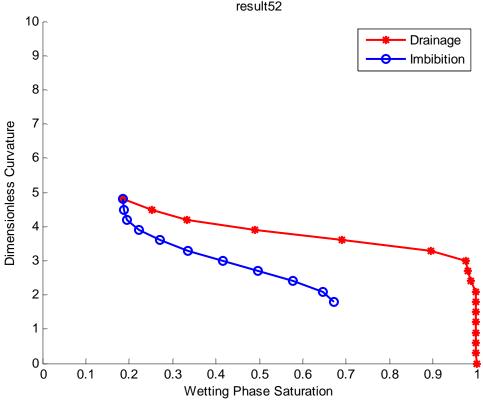


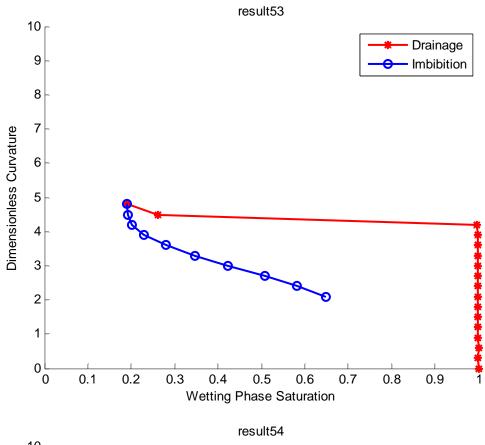


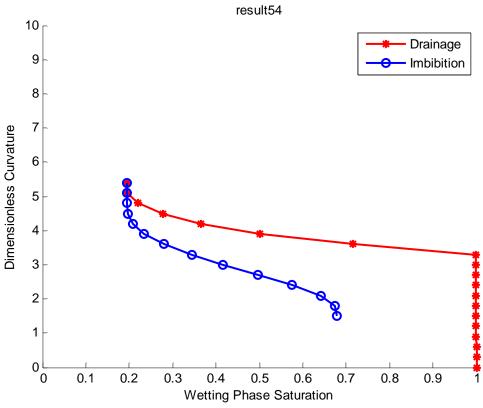


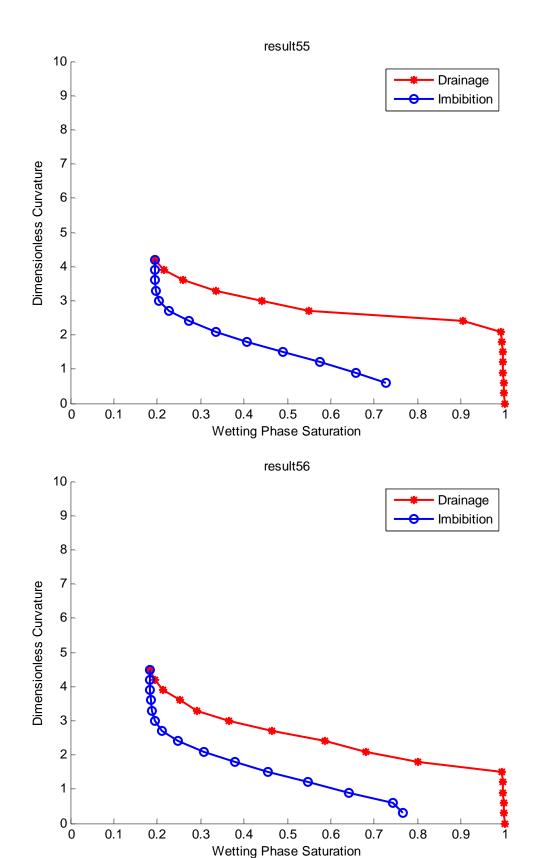


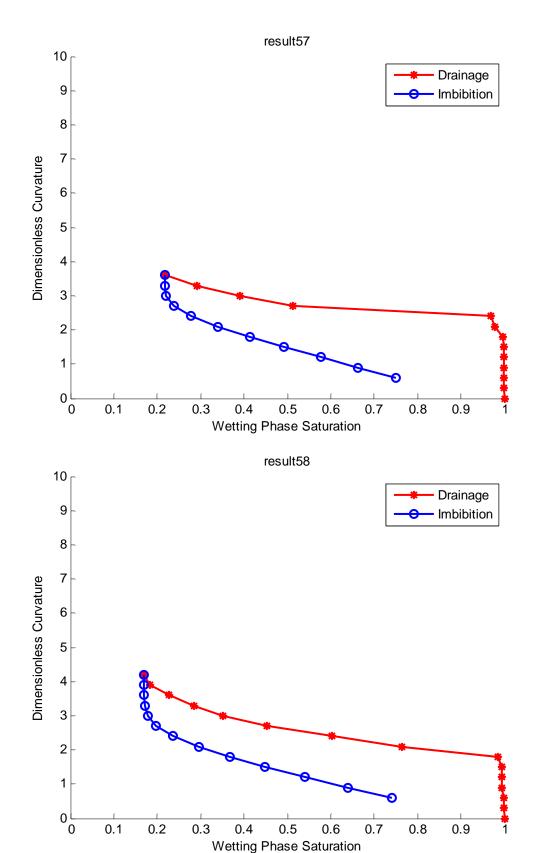


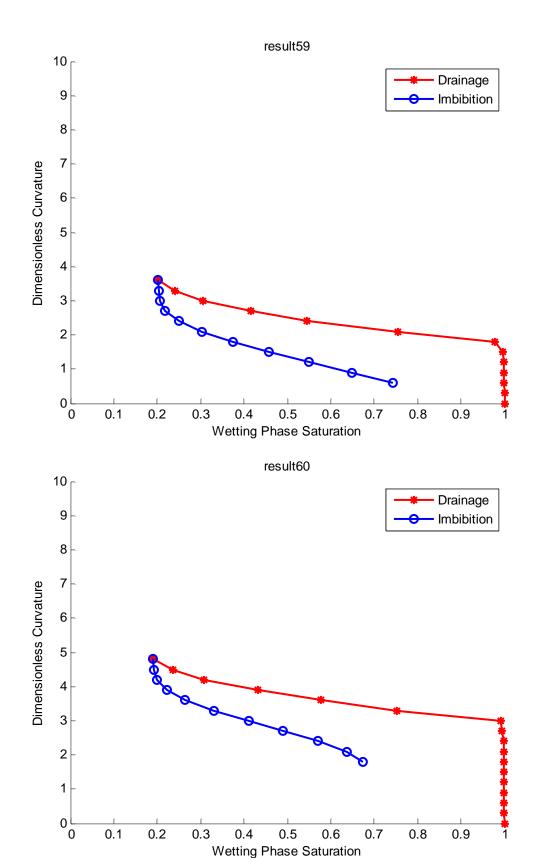


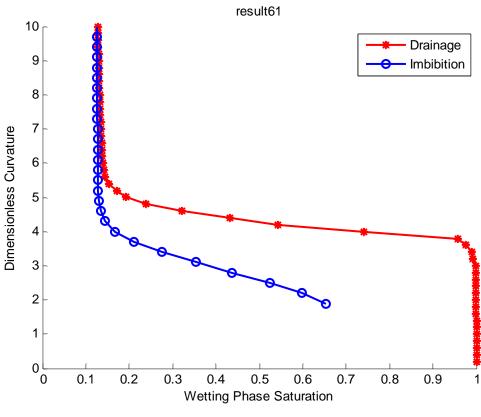


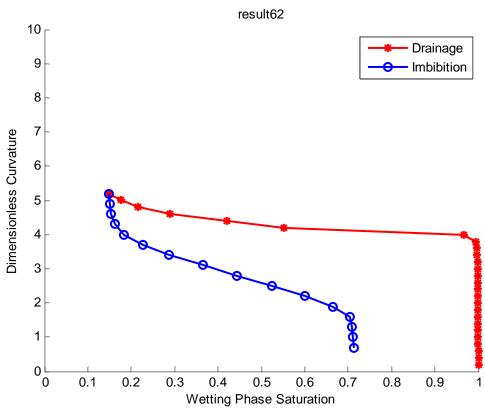


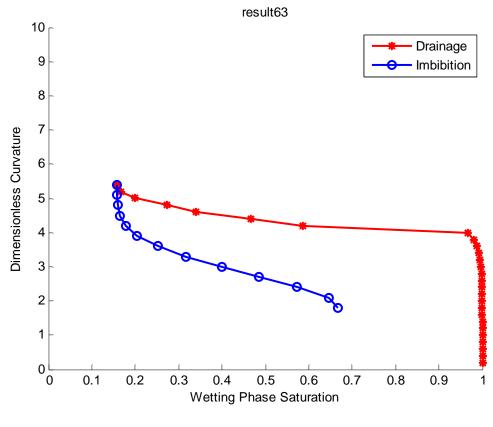


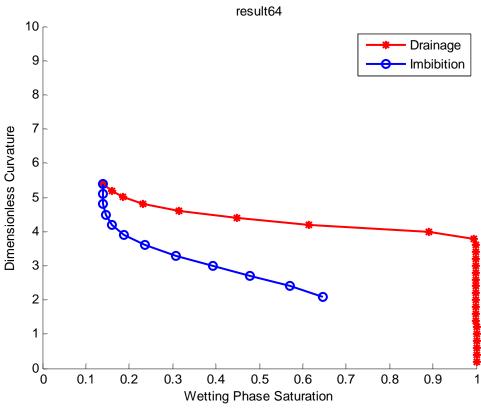


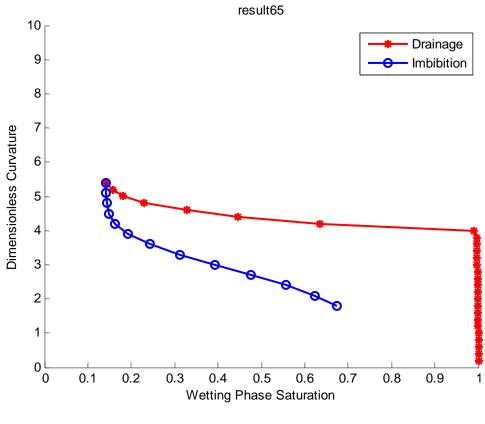


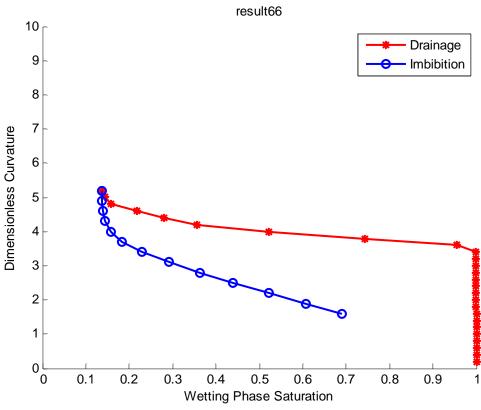


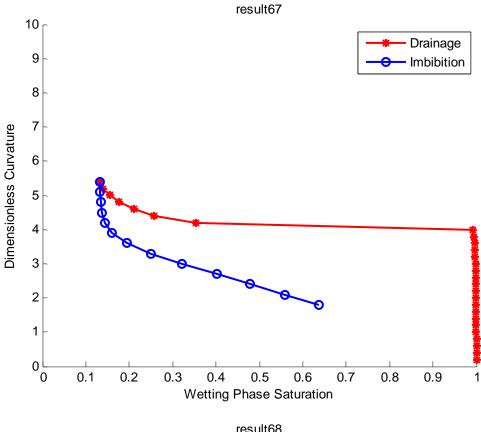


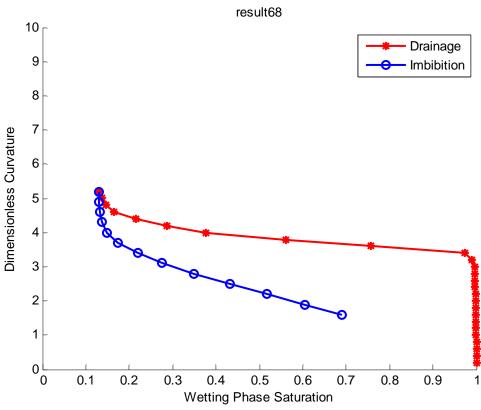


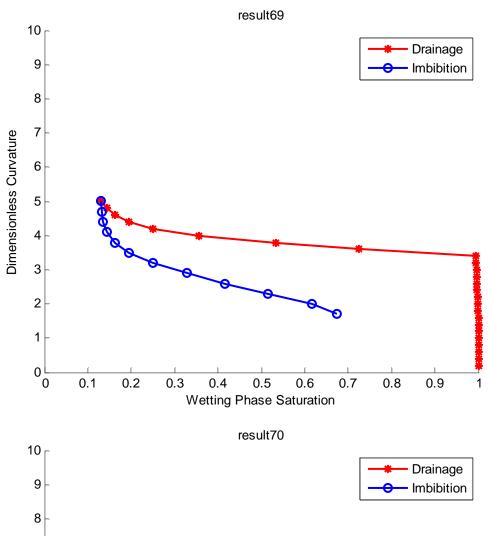


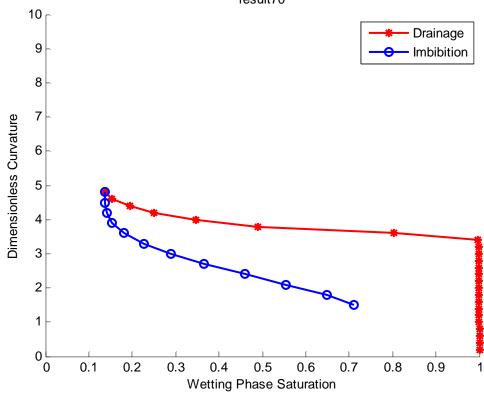


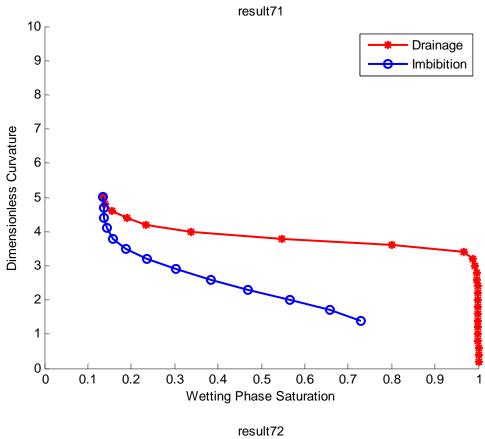


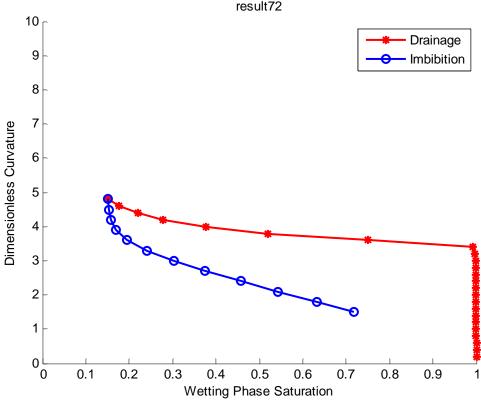


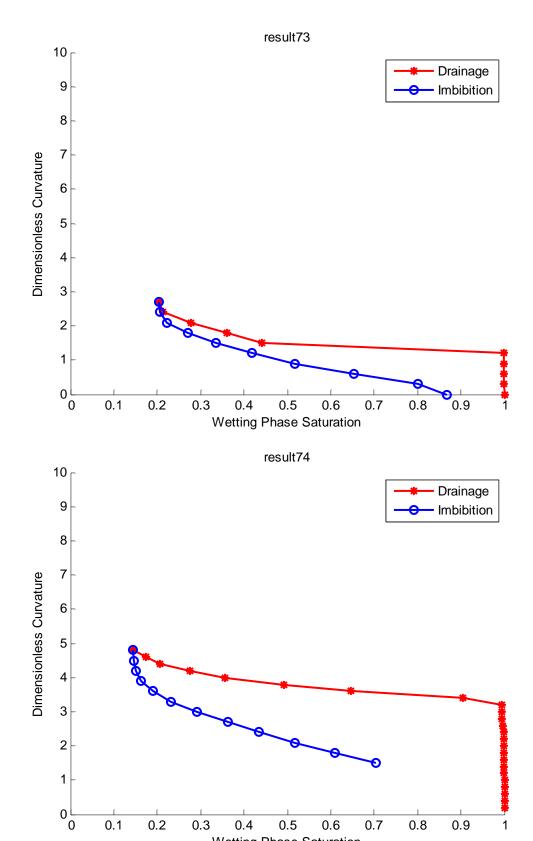












0.2

0.1

0.4

0.3

0.5

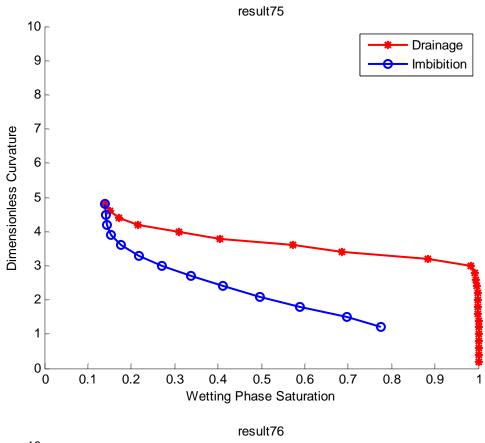
Wetting Phase Saturation

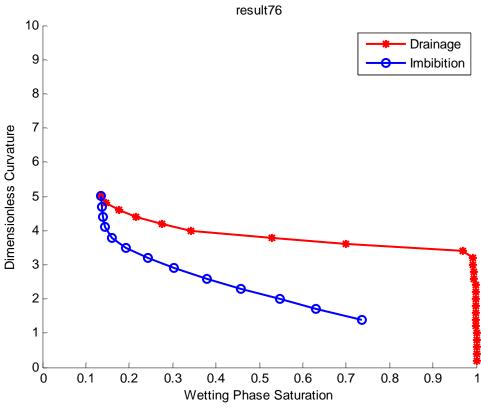
0.6

0.7

0.8

0.9





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