

# *Improving the Economic Viability of Biological CO<sub>2</sub> Utilization by Improved Algae Productivity & Integration with Wastewater Treatment*

Cooperative Agreement No: DE-FE0030822

CO<sub>2</sub> Capture Technology  
Project Review Meeting  
August 17, 2018



# Basic Project Information



- **Title:** *Improving the Economic Viability of Biological Utilization of Coal Power Plant CO<sub>2</sub> by Improved Algae Productivity & Integration w/ Wastewater Treatment*
  - DOE Program Manager: Andy Aurelio
  - Lead Organization: University of Illinois - Illinois Sustainable Technology Center
  - PI: Lance Schideman, PhD, PE
  - Major Collaborating Organization: Helios-NRG
  - Project Cooperative Agreement Number: DE-FE0030822
- **DOE Funding Program DE-FOA-0001622:** *Applications for Technologies Directed at Utilizing Carbon Dioxide from Coal Fired Power Plants*
  - Total Project Value: \$ 1,249,873 Government: \$999,536 Cost Share: \$250,337
  - Budget Period 1 Total Value: \$ 414,242 Government: \$331,394 Cost Share: \$ 82,848
- **3-Yr Project Duration: Oct. 1, 2017 – Sept. 30, 2020 with Annual Budget Periods**
  - Currently in Budget Period 1(BP1) - October 1, 2017 – September 30, 2018

# Major Project Objectives

- *Improve Algal Productivity & CO<sub>2</sub> Capture by Improved Bioreactor Design & Oper.*
  - Proprietary reactor design and algal strains grown on simulated flue gas with key contaminants added
  - End of project performance goals
    - 35 g/m<sup>2</sup>·day biomass productivity
    - 70% carbon capture efficiency
- *Reduce Net Costs and Energy Inputs for Producing Algal Products*
  - Integrate use of low-cost or negative-cost wastewater nutrient inputs
    - Large quantity of sustainable nutrients available
  - Develop low-energy forward osmosis dewatering
  - Membrane separation & recycle of aqueous byproducts from hydrothermal biofuel processes
  - Algal biomass for animal feed
    - Large-volume stable markets with potential for higher net value than biofuels
  - Sanitary sewer distribution of flue gas
- *Evaluate Life-cycle and Techno-economic Impacts of Proposed System*

# Objectives in Context of Block Flow Diagram

*LCA & TEA of Proposed System*

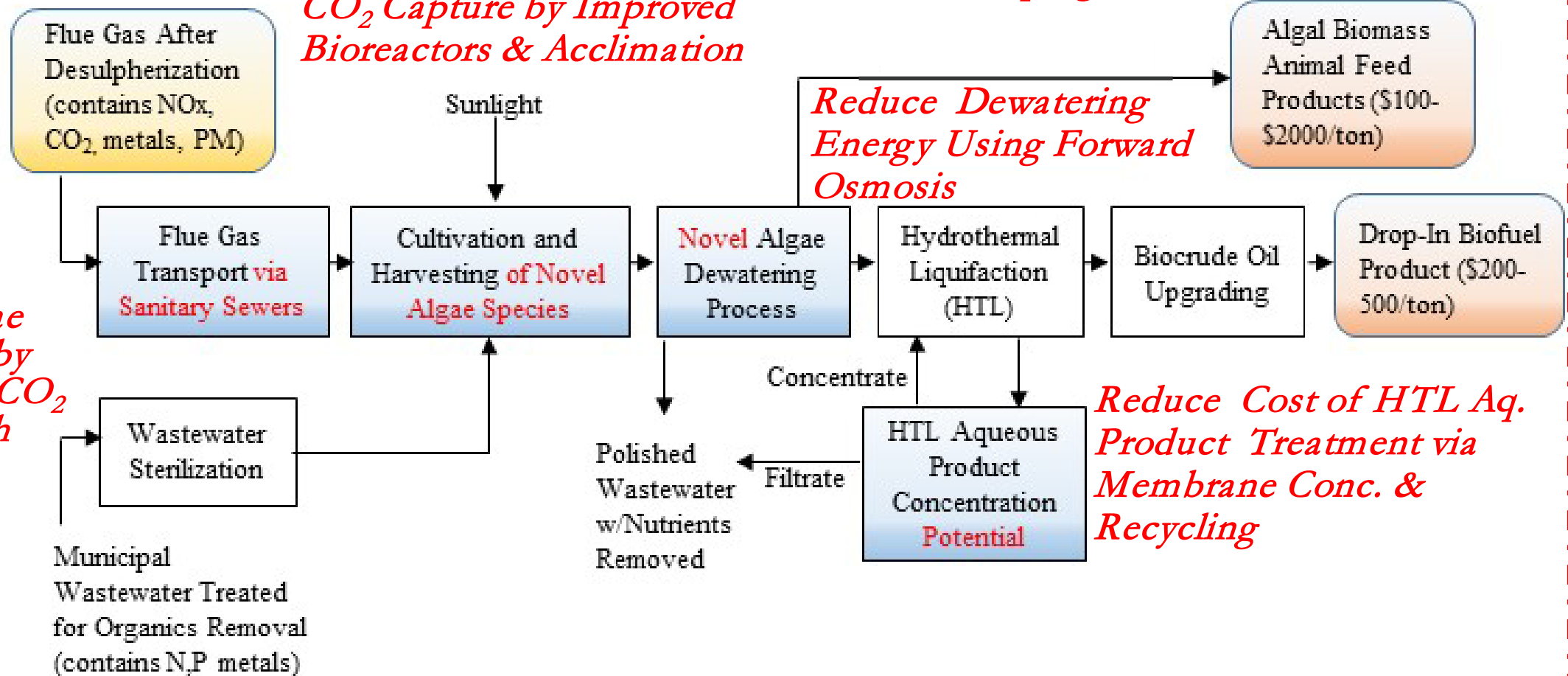
*Reduce Net Cost of Algae Production by Integrating CO<sub>2</sub> Capture with Wastewater Treatment*

*Improve Algae Productivity & CO<sub>2</sub> Capture by Improved Bioreactors & Acclimation*

*Increase Value of Algal Biomass by Developing Animal Feed Products*

*Reduce Dewatering Energy Using Forward Osmosis*

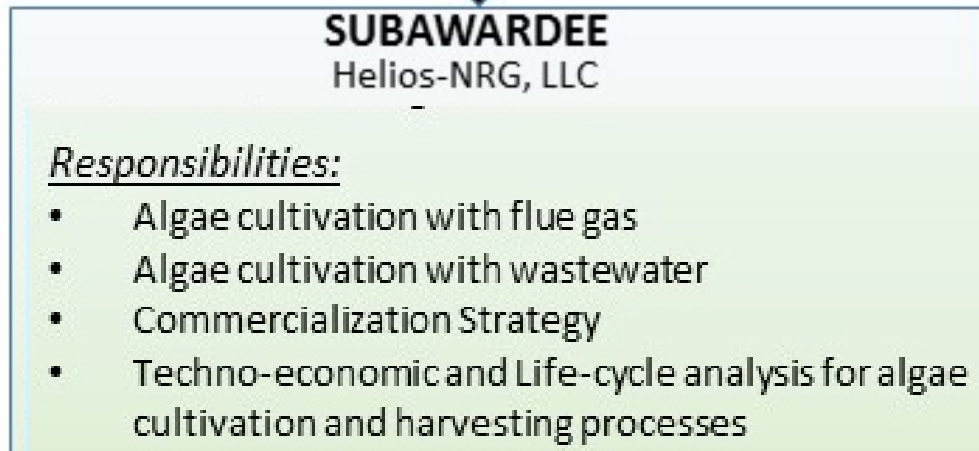
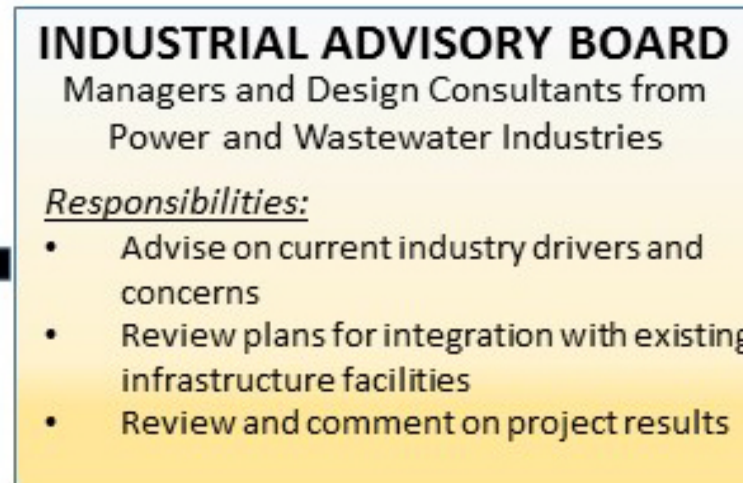
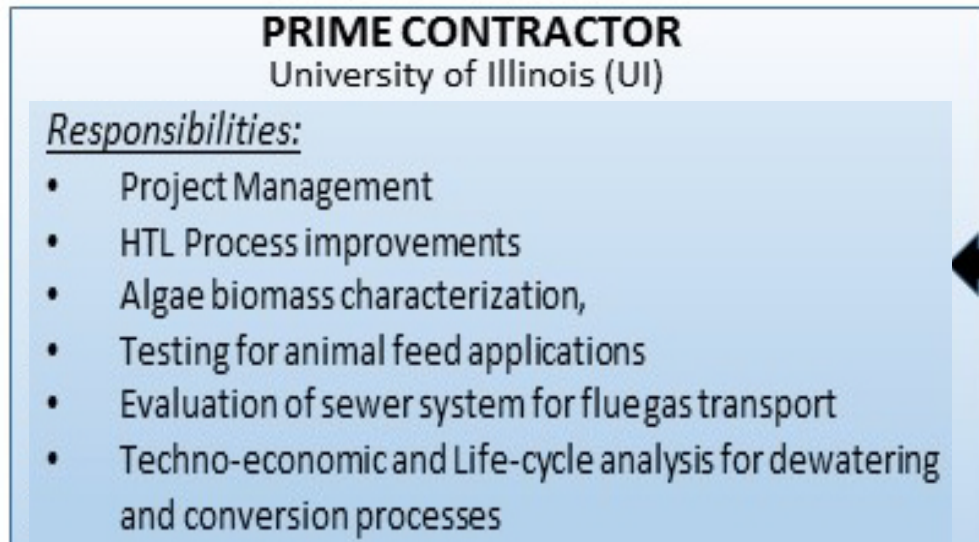
*Reduce Cost of HTL Aq. Product Treatment via Membrane Conc. & Recycling*



# Project Tasks

- *Task 1- Project Management* **B**
- *Task 2- Demonstrate Stable Algae Cultivation w/ Simulated Flue Gas* **P**
- *Task 3- Demonstrate Stable Algae Cultivation w/ Wastewater Nutrients* **1**
- *Task 4- Optimize CO<sub>2</sub> Capture Efficiency in the Algae Cultivation Process*
- *Task 5- Evaluate Novel Algae Dewatering Processes (forward osmosis)*
- *Task 6- Characterize algal biomass for HTL and animal feed applications*
- *Task 7- Demonstrate ability to concentrate & recycle HTL aqueous phase*
- *Task 8- Evaluate the potential of sewer network flue gas distribution*
- *Tasks 9- Techno-Economic Analysis*
- *Tasks 10- Techno-Economic Analysis*

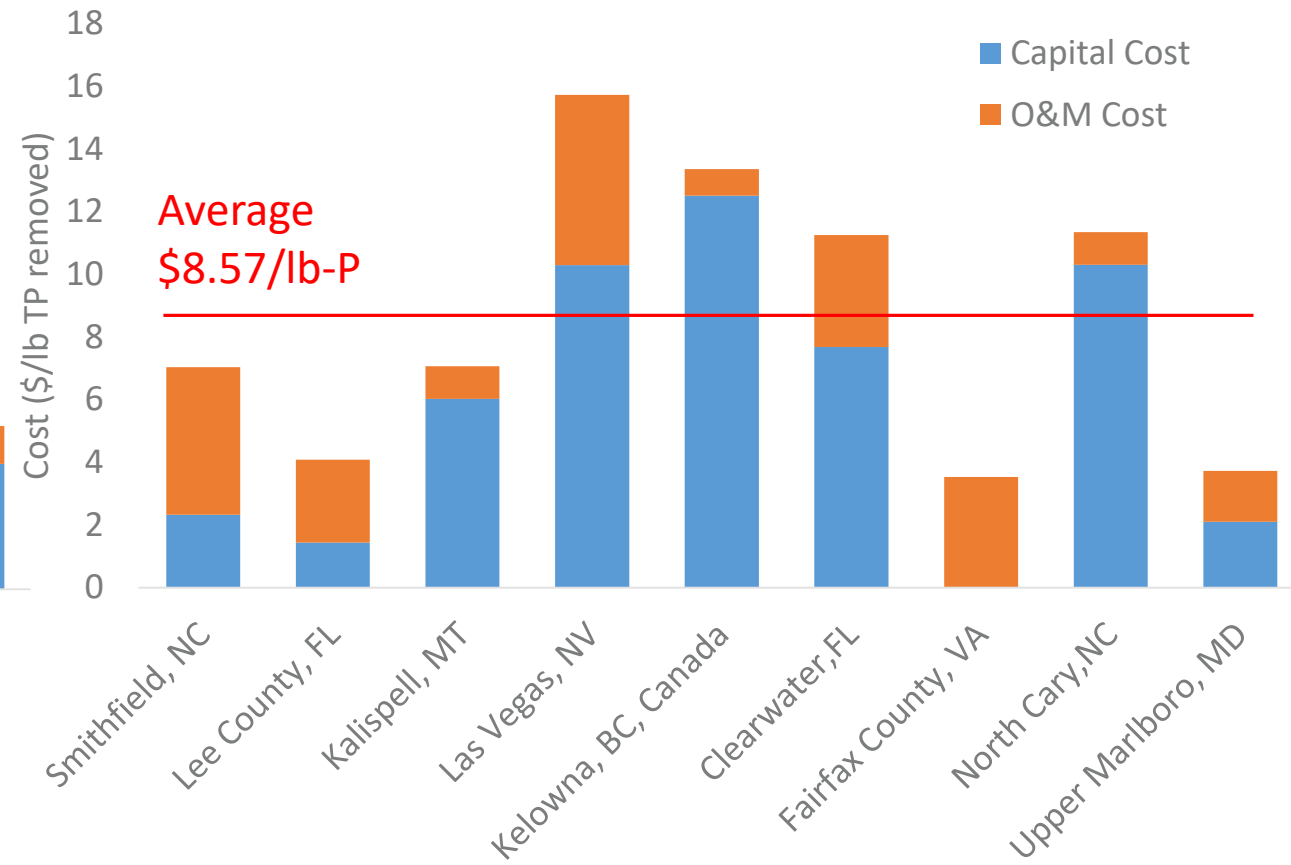
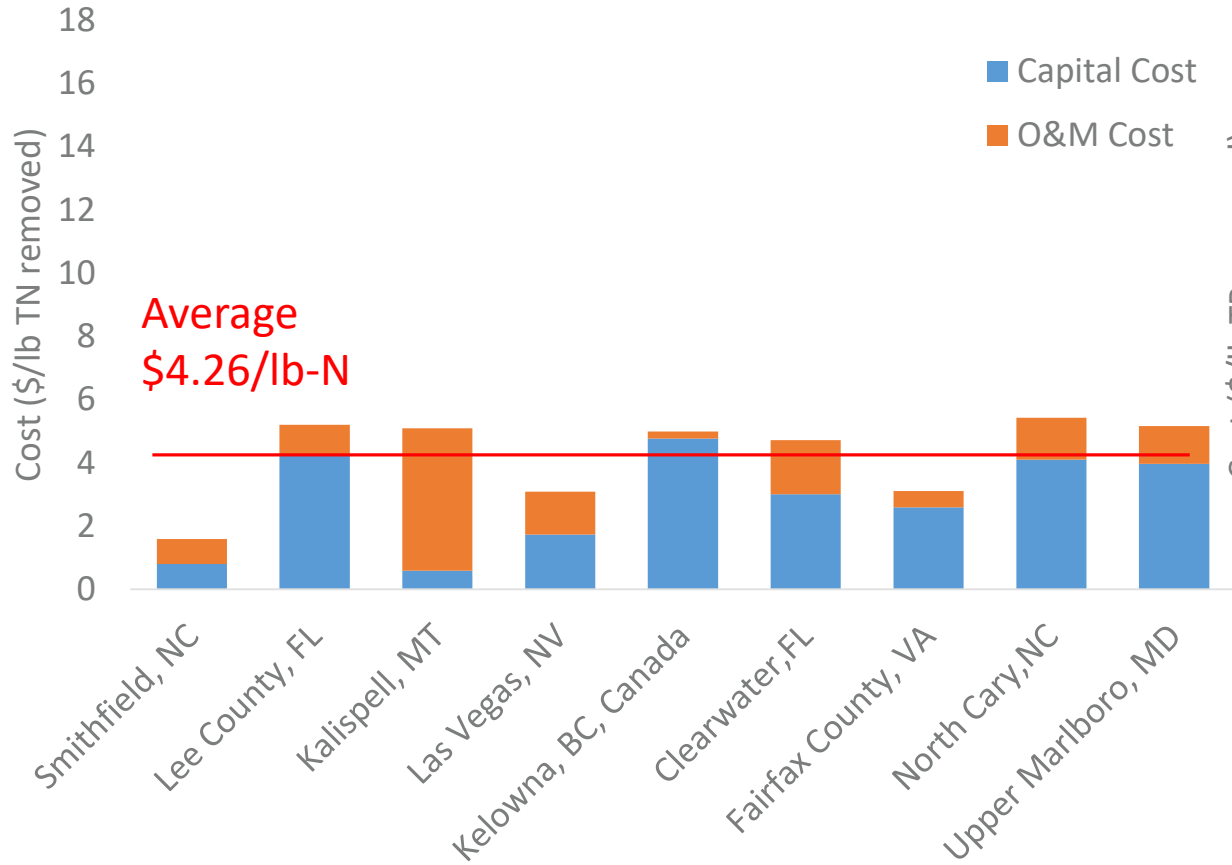
# Project Organizational Chart



- **Industrial Advisory Board Members**
  - Springfield City Water, Power & Light
    - 578 MW coal-fired steam turbine generators
  - Urbana-Champaign Sanitary District
    - 40 MGD Wastewater Treatment Plant Capacity
  - Fehr-Graham Engineering
    - Wastewater Design Consultant

# What is the Value of Wastewater Nutrient Removal?

Source: US-EPA Tech. Reference Document: 832-R-08-006, 2008



- Baseline Algae Elemental Mass Composition - 36%C, 7%H, 50%O, 6%N, 1%P
- Est. Wastewater Treatment Value of Algal Nutrient Uptake  $(0.06 * \$4.26 + 0.01 * \$8.57) * 2000 = \$680/ton$

**Economic Rationale:** Integrating wastewater treatment can make algal biofuels cost-effective  
*(Ref: C.T. Kuo PhD Thesis, Univ. of Illinois, 2017)*

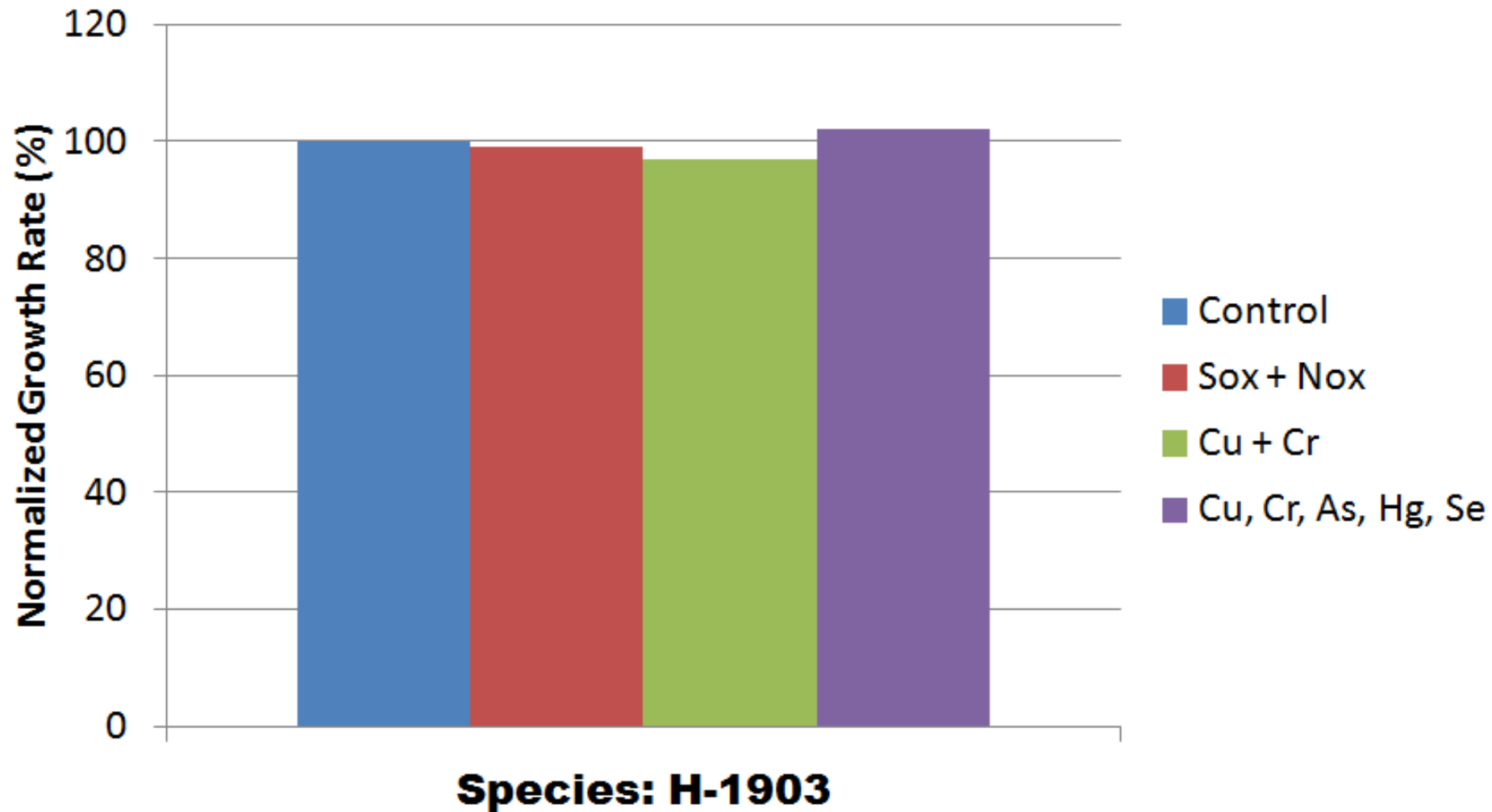


Cost Categories	2015 Current State of Technology w/ Algae Productivity of 8.5 g/m <sup>2</sup> /day	2022 DOE Projected Design Case w/ Algae Productivity of 25 g/m <sup>2</sup> /day
<b>Algal Biomass Production Costs (\$/ton)</b>		(Project Economic Impacts)
Ponds & Inoculum	\$ 1,359	\$ 289 (Raceway pond mods + \$44)
CO <sub>2</sub> Supply	\$ 99	\$ 97 (Carbon capture credit - \$60)
Dewatering Operations	\$ 82	\$ 52
Nutrient Supply	\$ 25	\$ 24 (WW credit -\$680)
Other Costs	\$ 76	\$ 32
<b>TOTAL Algae Biomass Prod</b>	<b>\$ 1,641 /dry ton (DT)</b>	<b>\$ 494 /DT (-\$202/DT)</b>
<b>Algal Biofuel Production Costs (\$/gge)</b>		
Algae Biomass Supply	\$ 15.15	\$ 3.18 (Sum of above -\$1.28)
Hydrothermal Liquefaction Conv.	\$ 1.18	\$ 0.49
Bio-oil Upgradation/Finishing	\$ 0.44	\$ 0.31
Aqueous product post-treatment	\$ 1.54	\$ 0.57 (Conc/recycle aq prod. \$0.28)
Balance of Plant	\$ 0.29	\$ 0.17
<b>TOTAL Biofuel Production Costs</b>	<b>\$ 18.60 / gal gasoline equiv (gge)</b>	<b>\$ 4.72/gge (-\$0.03/gge)</b>



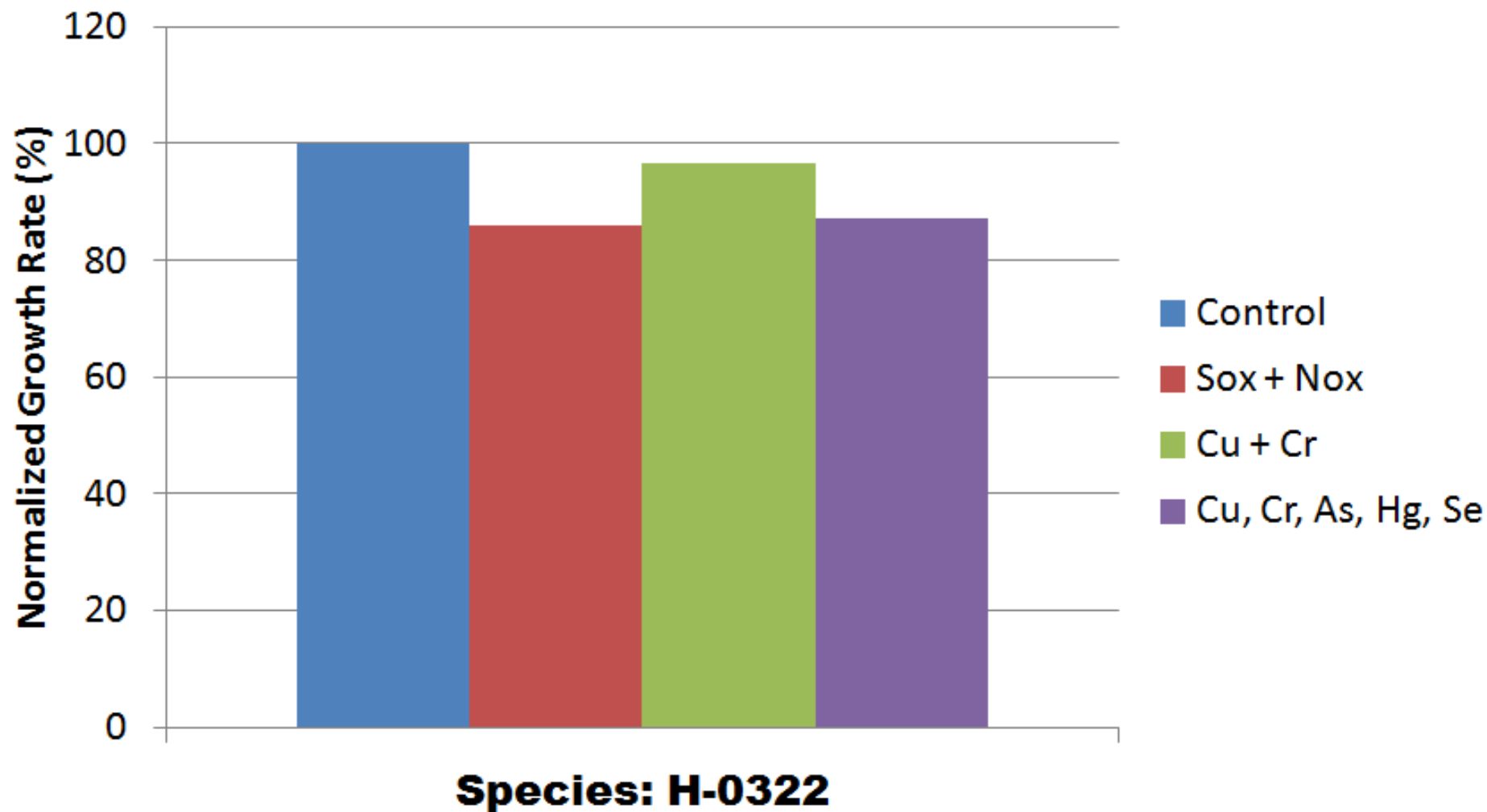
# Impact of flue gas contaminants on algae growth

Simulated post-FGD flue gas (all with 12% CO<sub>2</sub>)



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Simulated post-FGD flue gas (all with 12% CO<sub>2</sub>)



# Algae Heavy Metal Content after Combined Heavy Metal Tests

Compared with Animal Feed Maximum Tolerable Level (MTL) (National Research Council, 2005)

Minerals	H-1903 2 HM (ppm)	H-1903 5 HM (ppm)	Poultry Feed MTL (ppm)	Swine Feed MTL (ppm)	Cattle Feed MTL (ppm)	Fish Feed MTL (ppm)
As		2.18	30	30	30	5
Cd	सझ	सझ	10	10	10	10
Cr	2.93	1.16	100	100	100	3,000* as CrO
Co	सज़	सज़	25	100	25	
Cu	64.8	46.6	250	250	40	100
Pb	सड़	सड़	10	10	100	10
Ni	सड़	सड़	250	250	100	50
Se		7.7	3	4	5	2
Zn	10.3	11.3	500	1000	500	250

- Algal biomass over accumulated Cu, Se which could limit certain animal feed applications without management or mitigation

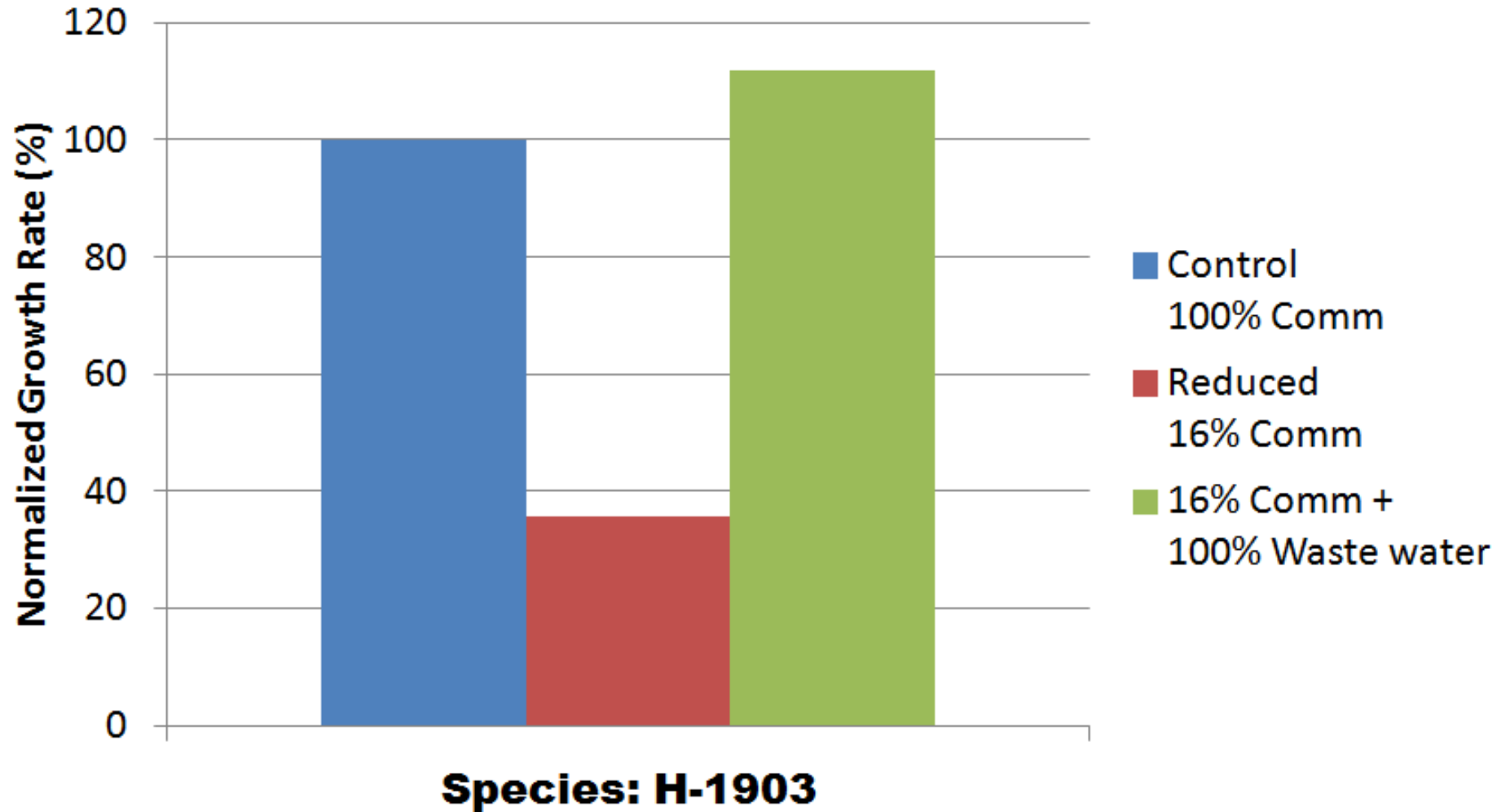
# Comparison of Wastewaters Used for Algae Cultivation

Sample Type & Treatments		TSS (mg/L)	COD (mg/L)	NH3-N (mg/L)	NO3-N (mg/L)	Total N (mg/L)	Total P (mg/L)	pH
Muni-WW Centrifuge Centrate	Filtered & Autoclaved	n/a	260 ±12	1021 ±8	22 ±17	1133 ±76	274 ±2	7.7
HTL Aq Product	Filtered & Autoclaved	n/a	44,177 ±326	7,206 ±66	360	10,944 ±1,237	2,108 ±7	5.6

- HTL aq product was significantly stronger than municipal wastewater dewatering centrate
  - Higher organics (~100x)
  - Higher nutrients (~10x)
  - HTL aq product has nitrogen-substituted organics and phenolics that have been shown to have inhibitory effects on microbial growth including algae

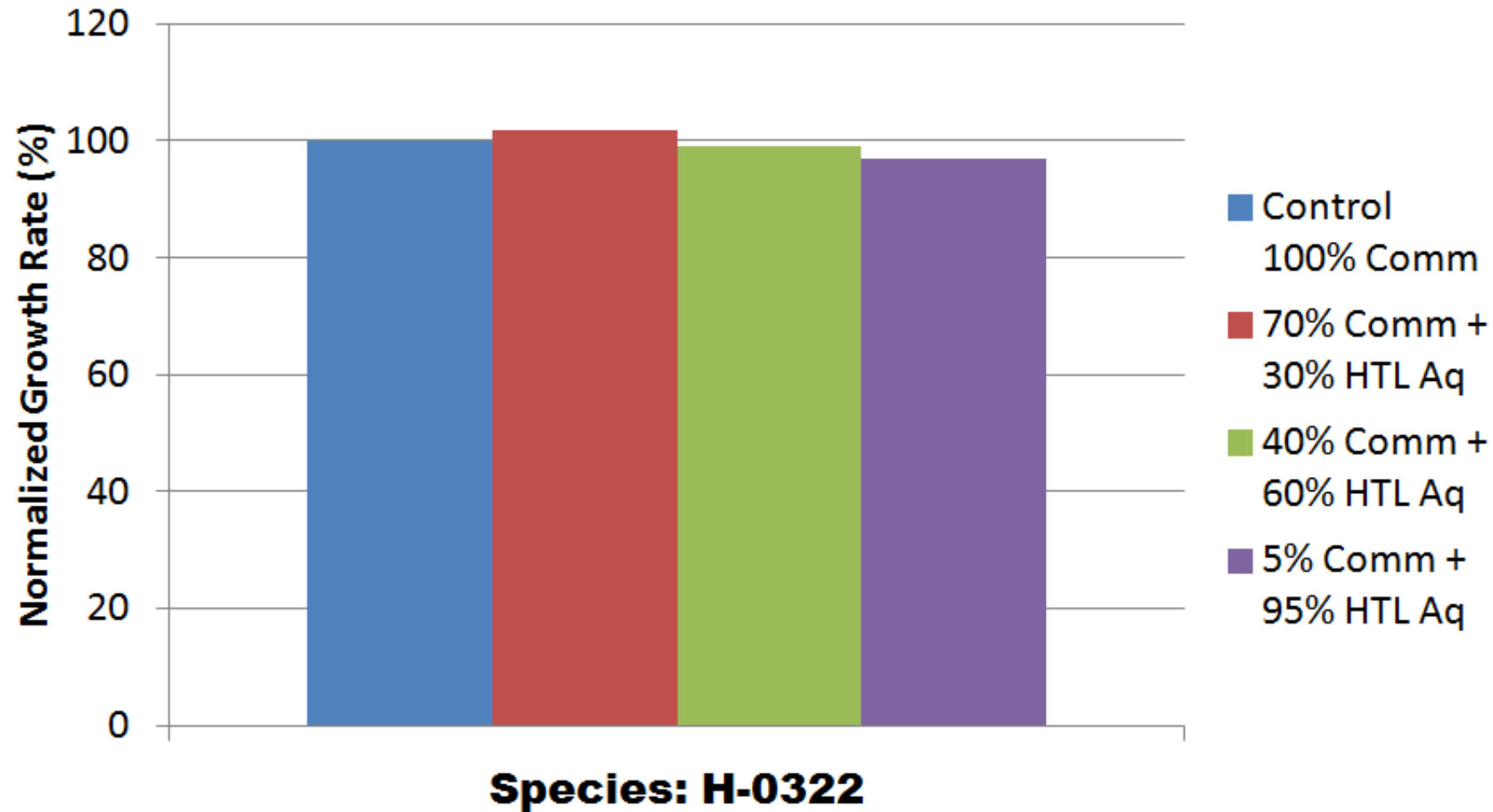
# Impact of wastewater nutrient replacement on algae growth

## Lower-strength centrate wastewater from biosolids dewatering

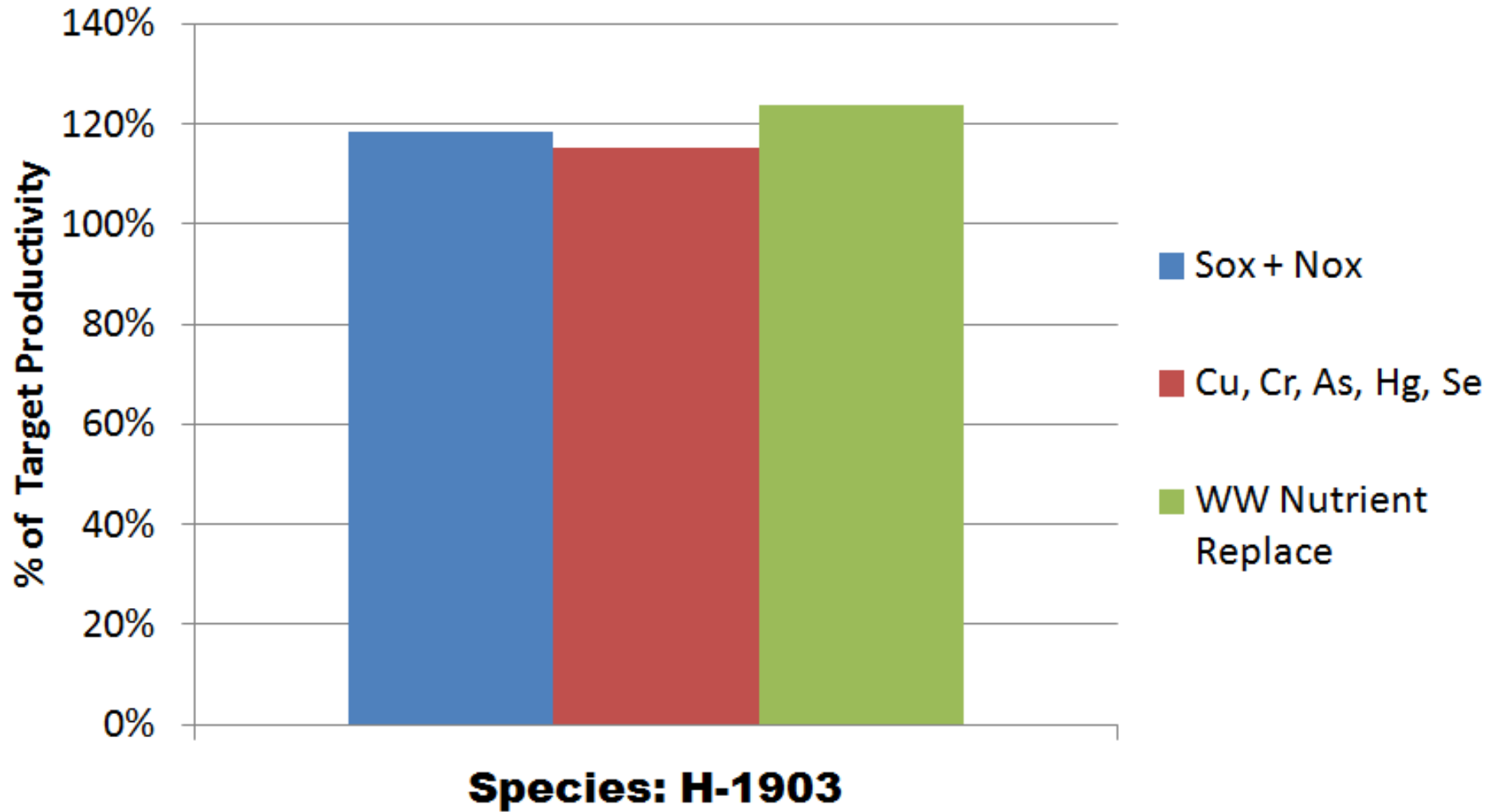


# Impact of wastewater nutrient replacement on algae growth

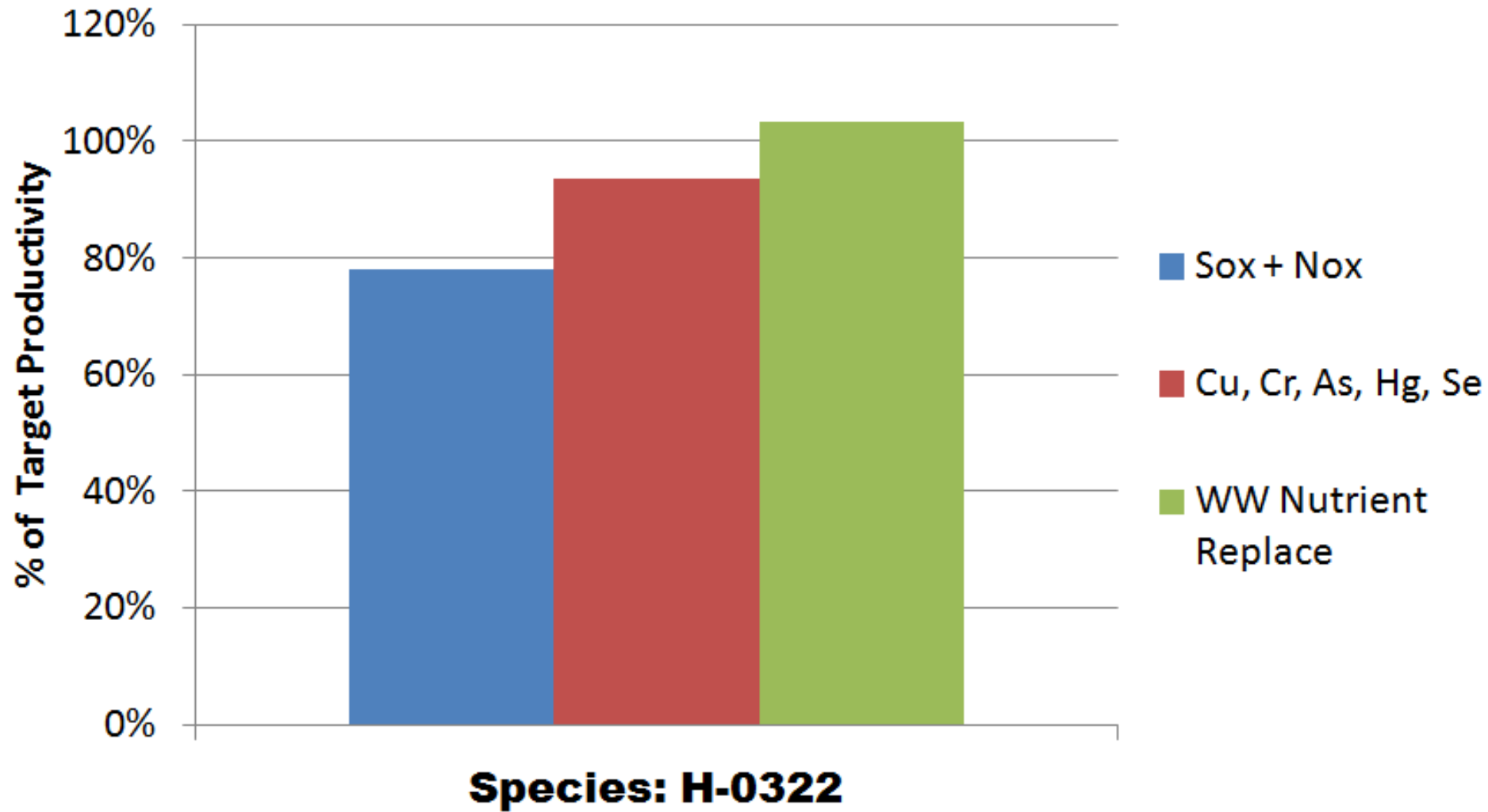
## Higher-strength HTL aq wastewater from biofuel production



# Weekly Avg. Productivity With Flue Gas & Wastewater Inputs



# Weekly Avg. Productivity With Flue Gas & Wastewater Inputs





# Project Milestones for Budget Period 1

Budget Period	Task #	Mile-stone #	Description	Planned Completion Date	Actual Completion Date	Verification Method
1	1	T1.1	Kickoff Meeting	Dec. 2017	Dec. 2017	Presentation file
1	1	T1.2	Updated Project Management Plan	Oct. 2017	Oct. 2017	Project Management Plan File
1	2	T2.1	Stable Algae Growth with simulated flue gas	Mar. 2018	Mar. 2018	Quarterly Progress Report
1	3	T3.1	Stable Algae Growth with wastewater nutrients	Sept. 2018		BP1 Annual Progress Report
1		G/N-1	Algal Productivity with Simulated Flue Gas > 25 g/m <sup>2</sup> /d	Sept. 2018		DOE Annual Review

# Project Success Criteria for Each Budget Period



Decision Point	Date	Success Criteria
G/N-1 Go/No-Go Budget Period 1	9/30/2018	Algal Productivity > 25 g/m <sup>2</sup> /d (weekly average) with Simulated Flue gas containing 12% CO <sub>2</sub> , SOX, NOX and representative levels of heavy metals Hg, Se, As, Cu and Cr
G/N-2 Go/No-Go Budget Period 2	9/30/2019	Algal Productivity > 25 g/m <sup>2</sup> /d (weekly average) and >70% CO <sub>2</sub> capture with Simulated Flue gas containing 12% CO <sub>2</sub> , SOX, NOX and representative levels of heavy metals Hg, Se, As, Cu and Cr
G/N-3 Go/No-Go Budget Period 3	9/30/2020	Integrated Application of Project Technologies w/ Projected Cost of Algal Biomass < \$470 /dry ton

# Technical Risks & Potential Mitigation Strategies

Description of Risk	Probability	Impact	Risk Management- Mitigation and Response Strategies
<b>Technical Risks:</b>			
Algae growth is inhibited by contaminants in post-FGD flue gas (SO <sub>x</sub> , NO <sub>x</sub> , metals)	Medium	Medium to High	<ul style="list-style-type: none"> <li>Use adsorbents in algal culture to sequester problem contaminants</li> <li>Problem contaminants can be removed from the simulated flue gas</li> <li>For future applications flue gas pre-treatment may be required</li> </ul>
Algae growth is inhibited by contaminants in nutrient-rich wastewater liquids	Low	Medium to High	<ul style="list-style-type: none"> <li>Use adsorbents to sequester problem contaminants</li> <li>Wastewater filtrate can be pre-treated to remove problem contam.</li> <li>Wastewater filtrate use for algae cultivation can reduced/eliminated</li> </ul>
Algal uptake of CO <sub>2</sub> is not fast enough for capture goal (70-90% removal in 3 stages)	Low	Low	<ul style="list-style-type: none"> <li>Provide fine bubble diffusers if it is a physical mass transfer limitation</li> <li>Add stages if it is a biological limitation</li> </ul>
Forward osmosis dewatering flux is too low to facilitate cost-effective applications	Low	Medium	<ul style="list-style-type: none"> <li>Pre-treat algal biomass with ultrasound to open cells and reduce resistance to water diffusion through the cell walls</li> <li>Use alternate dewatering methods</li> </ul>
Concentrated HTL aqueous product is not converted to bio-oil when recycled	Low	Low	<ul style="list-style-type: none"> <li>Use alternate methods for treatment of HTL aqueous product (anaerobic digestion, or catalytic hydrothermal gasification)</li> </ul>
Sewer conveyance of flue gas causes too much loss/dilution	Medium	Low	<ul style="list-style-type: none"> <li>Use a dedicated pipeline for transport of CO<sub>2</sub> from flue gas</li> </ul>

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P  
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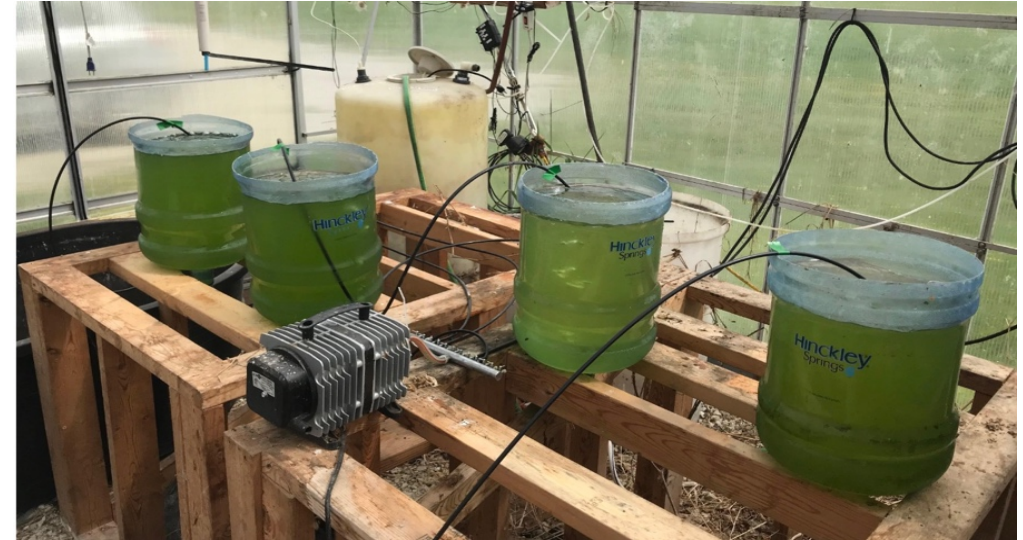
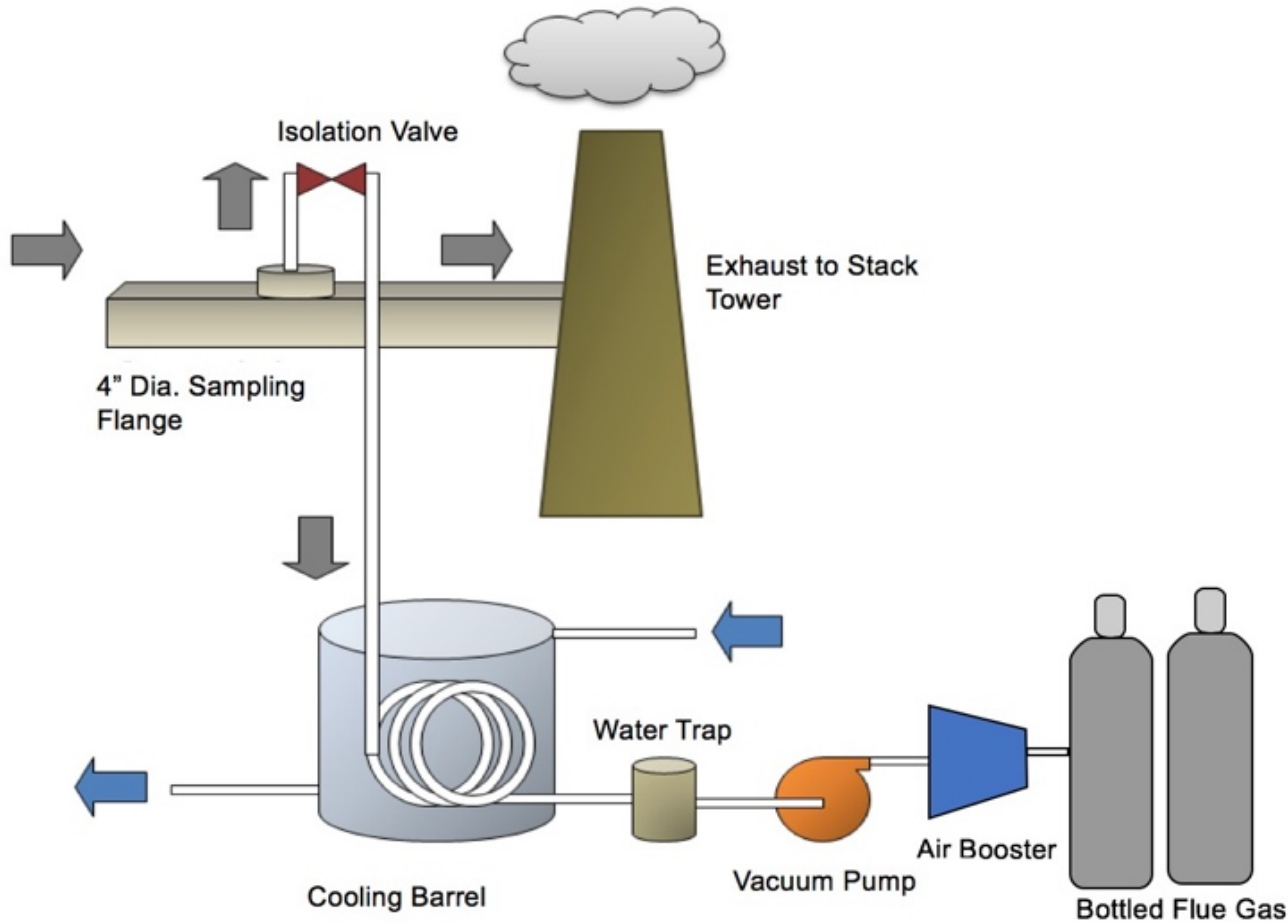
# Summary of Major Project Activities



- **Task 1- Project Management (Ongoing)**
  - Monthly Progress Conference Calls with DOE Program Manager
  - Three Quarterly Progress Reports Submitted
  - Individual Meetings with Three Industrial Advisory Board Members
- **Task 2- Algae Cultivation using Simulated Flue Gas w/Contaminants (Completed)**
  - Demonstrated acclimation & robust growth of 2 algal species w/ acid gasses (CO<sub>2</sub>, NO<sub>x</sub>, SO<sub>x</sub>)
  - Demonstrated acclimation & robust growth of 2 algal species w/ heavy metals (As, Se, Hg, Cr, Cu)
- **Task 3- Algae Cultivation w/ Wastewater Nutrients (Ongoing)**
  - Demonstrated acclimation & robust growth of 2 algal species with 2 wastewater sidestreams
    - Centrate from wastewater biosolids centrifuge dewatering
    - Raw hydrothermal liquefaction (HTL) aqueous product from conversion of biomass to biofuels
  - >50% nutrient replacement achieved with all combinations of wastewater nutrients & algal species
  - Full nutrient replacement achieved with several combinations of wastewaters & algal species
  - Ongoing testing to optimize productivity of algal cultures

# New Flue Gas Testing Capability

## Small-Scale Algae Cultivation w/ Bottled Flue Gas Samples



	LOW FLUE GAS	MEDIUM FLUE GAS
Flue Gas CO <sub>2</sub> concentration	6.01%	6.01%
Air pumping rate (L/min)	0.5	0.5
Flue gas Injection rate (L/min)	0.05	0.1
Influent CO <sub>2</sub> conc.	0.58%	1.04%
Exhaust CO <sub>2</sub> conc.	0.44%	0.85%
CO <sub>2</sub> removal efficiency	24%	18%
Carbon Capture (mg-C)	183.0	258.3
Assimilated Carbon (mg-C)**	178.6	243.7

# Questions and Comments...

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Lance Schideman  
[schidema@Illinois.edu](mailto:schidema@Illinois.edu)  
217-390-7070

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