

# Conversion of CO<sub>2</sub> to Alkyl Carbonates Using Ethylene Oxide as Feedstock

C.B. Panchal, Richard Doctor, Rachel Sturtz and John Prindle

E3Tec Service, LLC

2815 Forbs Avenue, Suite 107  
Hoffman Estates, Illinois 60192

[cpanchal@e3-tec.com](mailto:cpanchal@e3-tec.com)

[www.e3-tec.com](http://www.e3-tec.com)

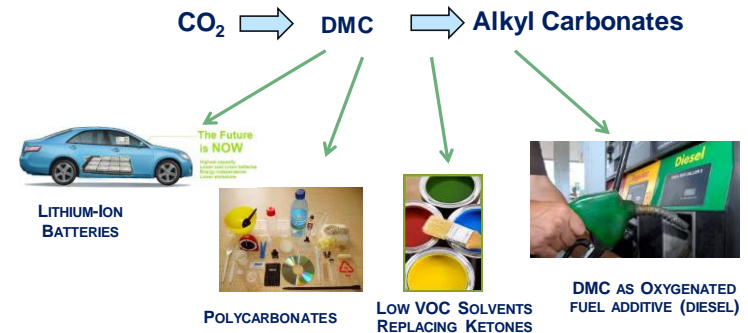
# SBIR Phase II Project Status

- **Technical**: Developed validated ASPEN Plus® design based on pilot-scale tests at Michigan State University
- **Economic Analysis**: CAPEX for a 50 kTA DMC plant, competitive selling price of DMC compared to syngas-based DMC production, *ProForma* based NPV & IRR
- **Intellectual Property**: Two patents on DMC process plus one patent on Differential Kinetic Test Unit (DKTU)
- **Industry Interactions**: Interactions with potential industrial organizations for feedback on TRL status and economic analysis
- **Path Forward**: Commercial demonstration (build and operate) to validate techno-economic merits

# Alkyl Carbonates - Ideal Candidates for Conversion of CO<sub>2</sub> to Value-Added Products

## Expanding Market Demands

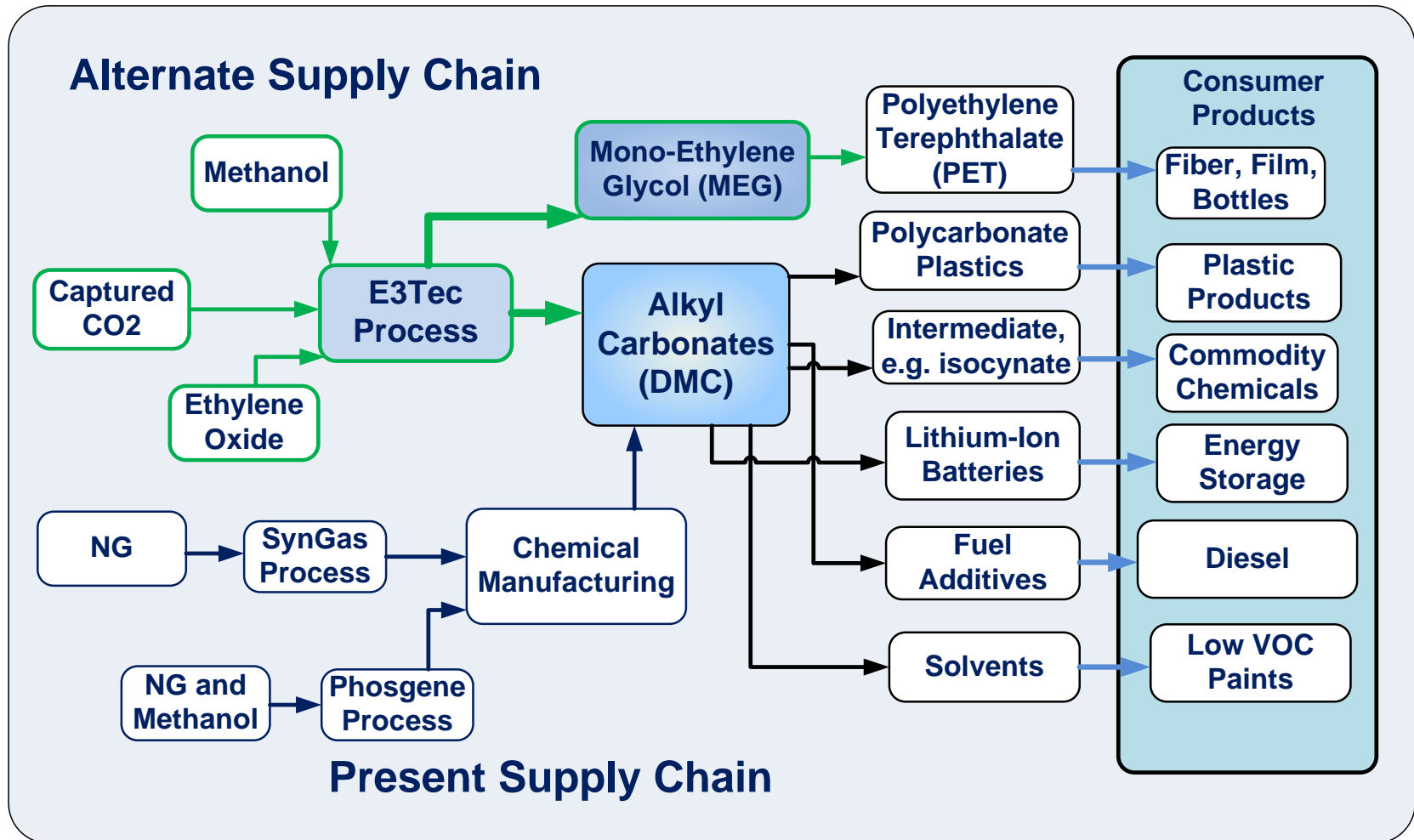
- High market growth considering replacement of phosgene based process and to meet expanding demands for polycarbonates and surging demand for Li-ion batteries
- E3Tec focus on high-purity 99.9%+ CO<sub>2</sub> based DMC
- MEG is one of the top 50 chemicals



Application	Global DMC Market Potential - kTA*	
	2017	2030
DMC in Polycarbonate Production	2,440	4,910
Li-Ion Battery Electrolyte	45	350
Solvents (replacing ketones)	1,430	1,820
Chemical Intermediate, e.g. Polyurethane	11,350	18,470
Potential diesel oxygenate additive**		1,580,000

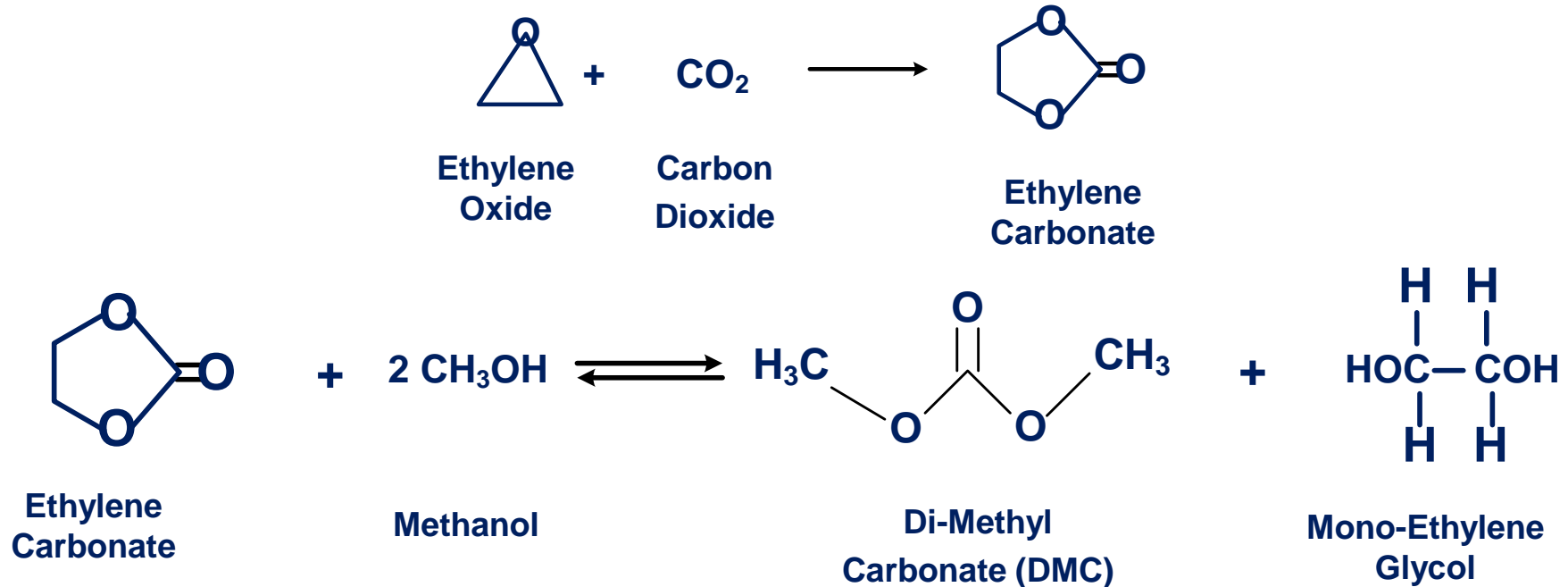
\*kTA - Thousand Tonnes Per Year \*\* Based on government approval for pollution control

# Alkyl Carbonate Supply Chain



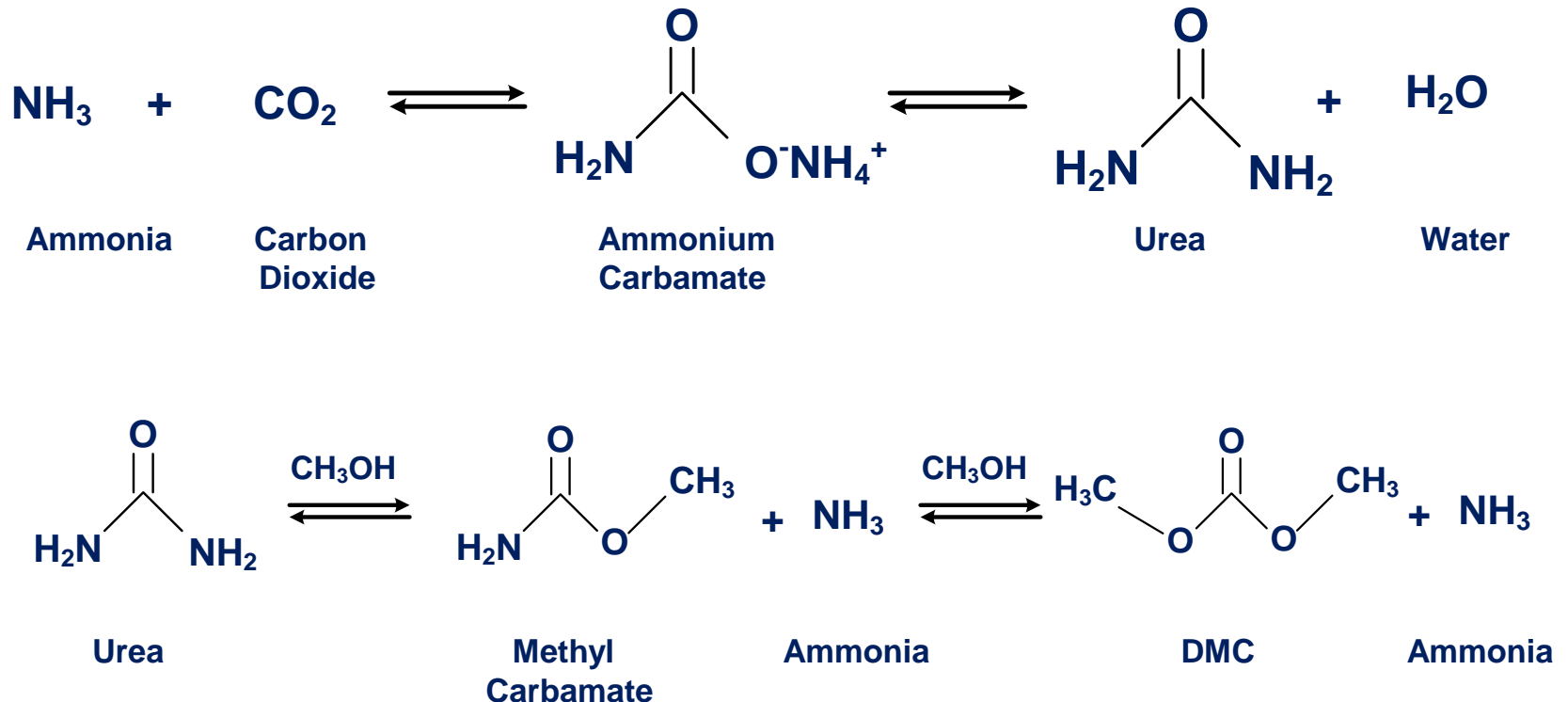
# E3Tec's Process Based on Two Chemical Pathways

## *Ethylene-Oxide-Based Process with Selective Co-Production of Mono-Ethylene Glycol (MEG)*

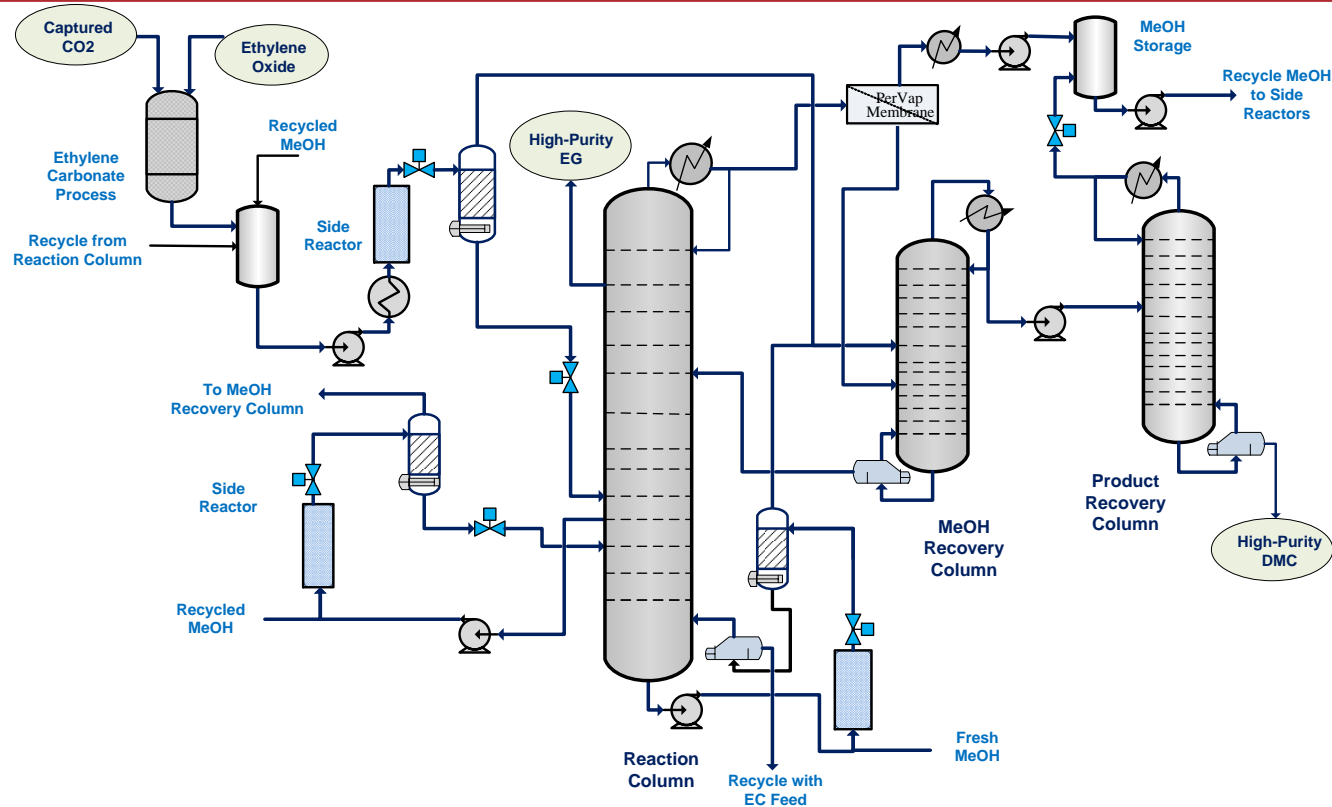


# E3Tec's Process Based on Two Chemical Pathways

*Urea-based Process with Ammonia Acting as a Chemical Carrier and for Breaking DMC/Methanol Azeotrope*



# Heat Integrated Reactive Distillation (HIRD) Process Equipped with Side Reactors & PerVap Membrane

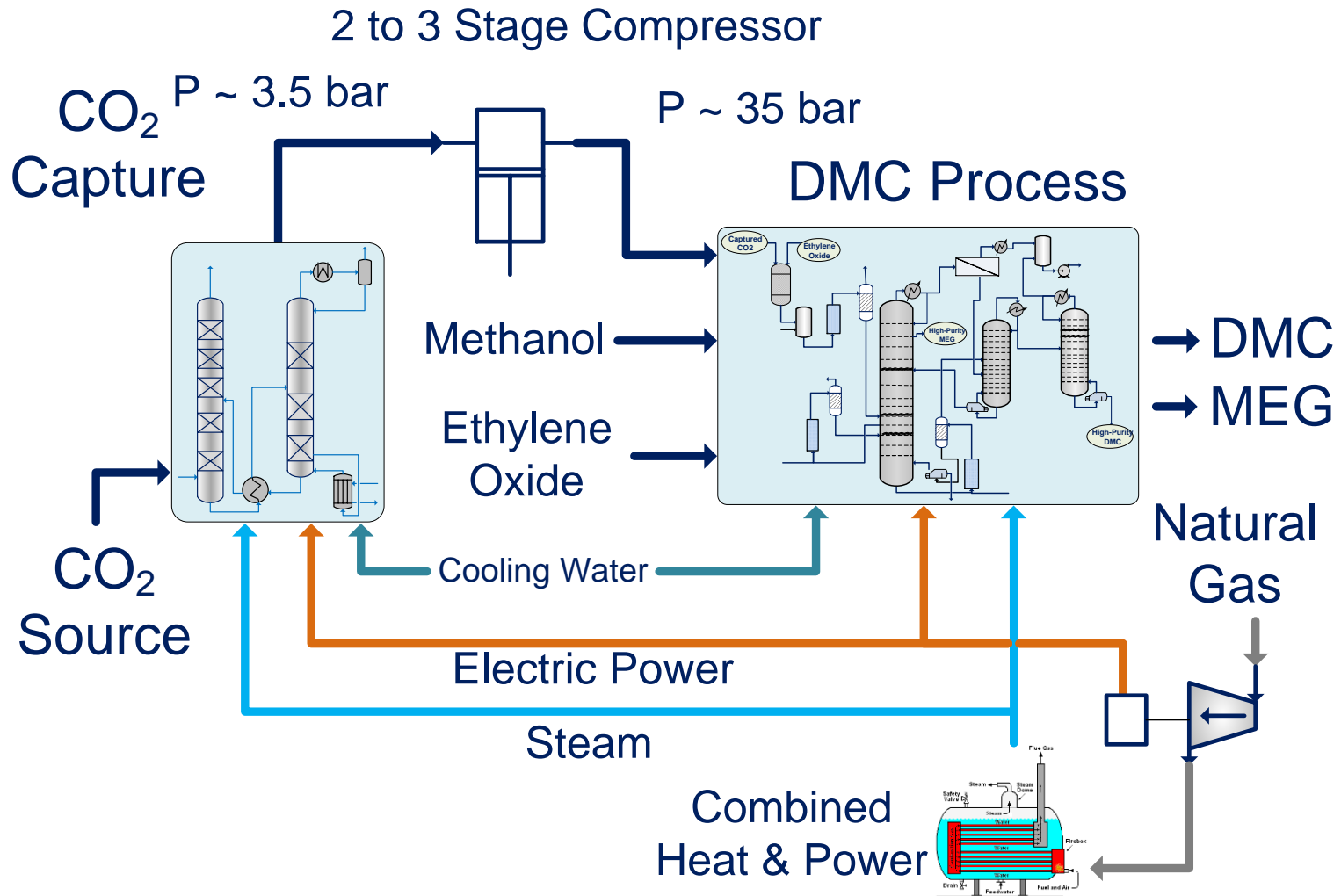


**DMC 51.7 kTA MEG 35.8 kTA CO<sub>2</sub> Consumption 25.6 kTA**

**Purity of Products: DMC 99.99% wt MEG 98.9% wt**

**US Patent 9,518,003 B1 December 2016 and 9,796,656 B1 October 2017**

# Integrated CO<sub>2</sub> Source DMC Process





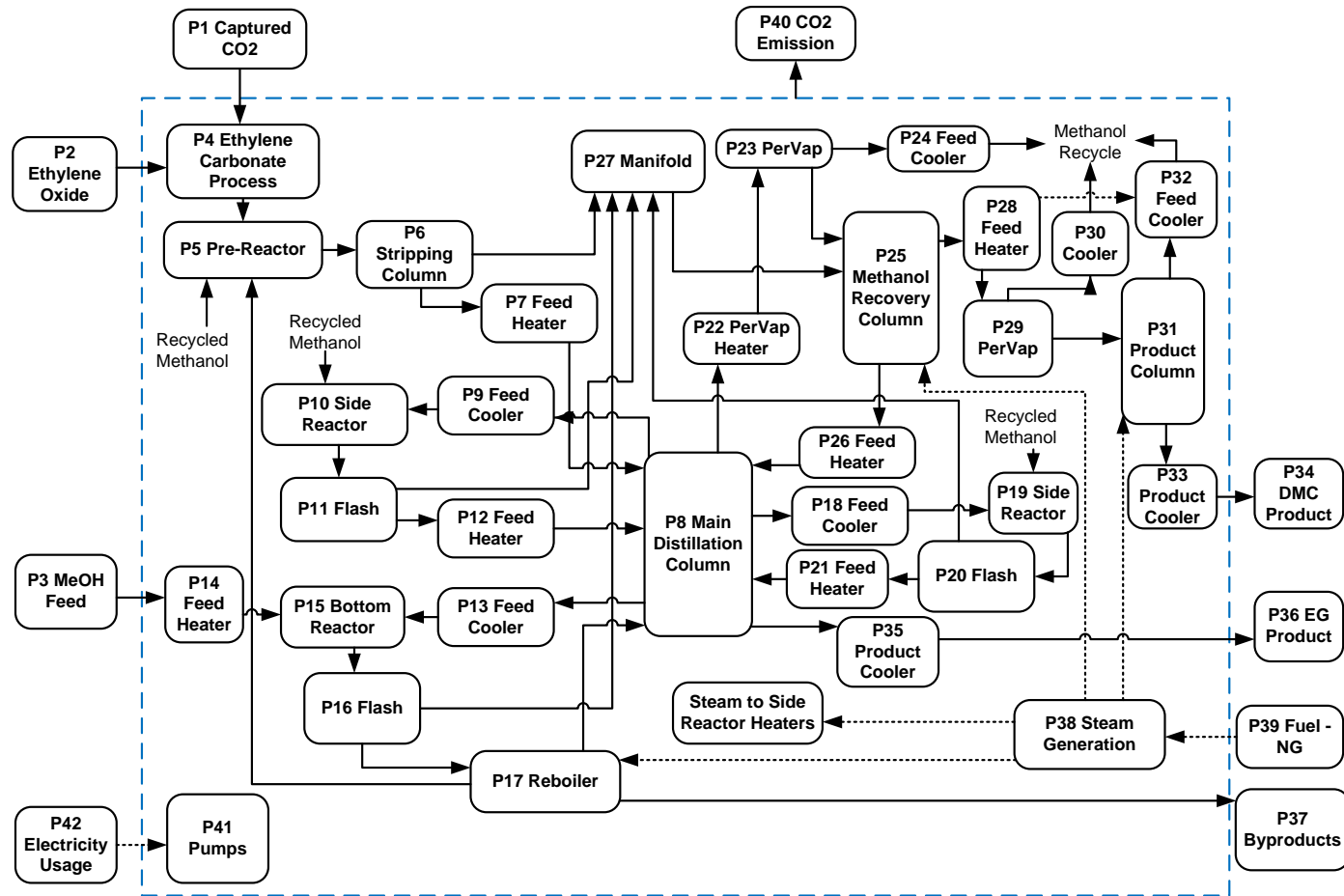
# Economic Analysis of Integrated Process

## Case Study: 15 MWe Coal Plant

<b>Baseline Case</b>	<b>UIUC 15 MW Coal Plant</b>	
<b>Power Generation</b>	<b>15</b>	<b>MWe</b>
<b>CO<sub>2</sub> Emission</b>	<b>300</b>	<b>Tonnes / day</b>
<b>CO<sub>2</sub> Capture &amp; Sequestration Costs</b>		
<b>CO<sub>2</sub> Capture Costs</b>	<b>\$56.2</b>	<b>\$ / Tonne CO<sub>2</sub></b>
	<b>\$16,860</b>	<b>\$ / day</b>
<b>Sequestration Costs</b>	<b>\$44.8</b>	<b>\$ / Tonne CO<sub>2</sub></b>
	<b>\$10,080</b>	<b>\$ / day</b>
<b>COE Impact (assuming 90% availability)</b>		
<b>CO<sub>2</sub> Capture</b>	<b>\$52</b>	<b>\$/MWe</b>
<b>CO<sub>2</sub> Sequestration</b>	<b>\$31</b>	
<b>Total</b>	<b>\$83</b>	
<b>DMC/MEG Production</b>		
<b>Fraction of CO<sub>2</sub> Emission Consumed in DMC</b>	<b>25%</b>	
<b>CO<sub>2</sub> Consumption</b>	<b>75</b>	<b>Tonnes / day</b>
<b>DMC Production</b>	<b>150</b>	
<b>MEG Production</b>	<b>105</b>	
<b>Annual DMC Production</b>	<b>50.0</b>	
<b>Annual MEG Production</b>	<b>35.0</b>	
<b>Product Margin Required for Offsetting CO<sub>2</sub> Costs</b>		
<b>CO<sub>2</sub> Capture &amp; Sequestration</b>	<b>\$180</b>	<b>\$ / Tonne DMC</b>
<b>Commercial Price of 99.99 wt % Purity DMC</b>	<b>\$1,789</b>	
<b>Production Costs of CO<sub>2</sub>-Based DMC</b>	<b>\$1,285</b>	
<b>Product Margin</b>	<b>\$504</b>	

# C-footprint Analysis

## ASPEN Plus® based process block diagram



Dimethyl Carbonate (DMC) / Ethylene Glycol (EG) Process Block Diagram

Mass Flow Energy Flow

# C-footprint Analysis

## Offsetting CO<sub>2</sub> Emissions

	CO <sub>2</sub> -Based Process	Syngas-Based Process
CO <sub>2</sub> Consumption, tonne CO <sub>2</sub> /tonne DMC	-0.51	0
CO <sub>2</sub> Emission Inside Battery Limits (ISBL)	0.58	1.29
Energy Consumption		
Thermal, MWh/Tonne DMC	2.87	4.41
Electric, MWh/tonne DMC	0.01	0.02
Cooling water, tonnes/tonne DMC	108.0	206.5
CO <sub>2</sub> emission Outside Battery Limits (OSBL)		
Methanol, tonne CO <sub>2</sub> /tonne DMC	0.39	0.47
Ethylene oxide, tonne CO <sub>2</sub> /tonne DMC	0.31	
Total CO <sub>2</sub> Emission, tonnes CO <sub>2</sub> /tonne DMC	1.28	1.76
Offsetting CO <sub>2</sub> Emission of MEG Production	-0.58	0
Net Emission tonne CO <sub>2</sub> /tonne DMC	0.19	1.76

# Potential Abatement of CO<sub>2</sub> Emissions

Application	Global CO <sub>2</sub> Abatement Potentials* kTA	
	2018	2030
<b>DMC in Polycarbonate Production</b>	<b>3,831</b>	<b>7,708</b>
<b>Li-Ion Battery Electrolyte</b>	<b>71</b>	<b>550</b>
<b>Solvents (replacing ketones)</b>	<b>2,245</b>	<b>2,857</b>
<b>Chemical Intermediate, e.g. Polyurethane</b>	<b>17,820</b>	<b>28,998</b>
<b>Potential diesel oxygenate additive**</b>		<b>2,480,600</b>

\*Based on offsetting CO<sub>2</sub> emissions by commercial production of DMC by syngas and MEG by hydration of ethylene oxide processes

\*\* Based on government approval for pollution control

# Economic Analysis

## *Competitive Product Margin*

	<b>E3Tec Process</b>	<b>Syngas Based Process</b>
<b>Plant Capacity, kTA</b>		
<b>DMC</b>	<b>51.7</b>	<b>50.0</b>
<b>MEG</b>	<b>35.0</b>	<b>0.0</b>
<b>Capital Costs (CAPEX), \$ Million</b>	<b>\$ 164</b>	<b>\$ 223</b>
<b>Costs \$/tonne DMC</b>		
<b>Total Variable</b>	<b>\$ 291</b>	<b>\$ 431</b>
<b>Total Fixed</b>	<b>\$ 196</b>	<b>\$ 254</b>
<b>Cash Cost of Production</b>	<b>\$ 487</b>	<b>\$ 685</b>
<b>Capital Charge</b>	<b>\$ 798</b>	<b>\$ 1,104</b>
<b>Selling Price</b>	<b>\$ 1,285 *</b>	<b>\$ 1,789</b>
<b>Product Margin</b>	<b>\$ 504</b>	

**\* Taking into credit for MEG as co-product**

# Economic Analysis

## *Proforma Based NPV and IRR*

### **Economic Parameters**

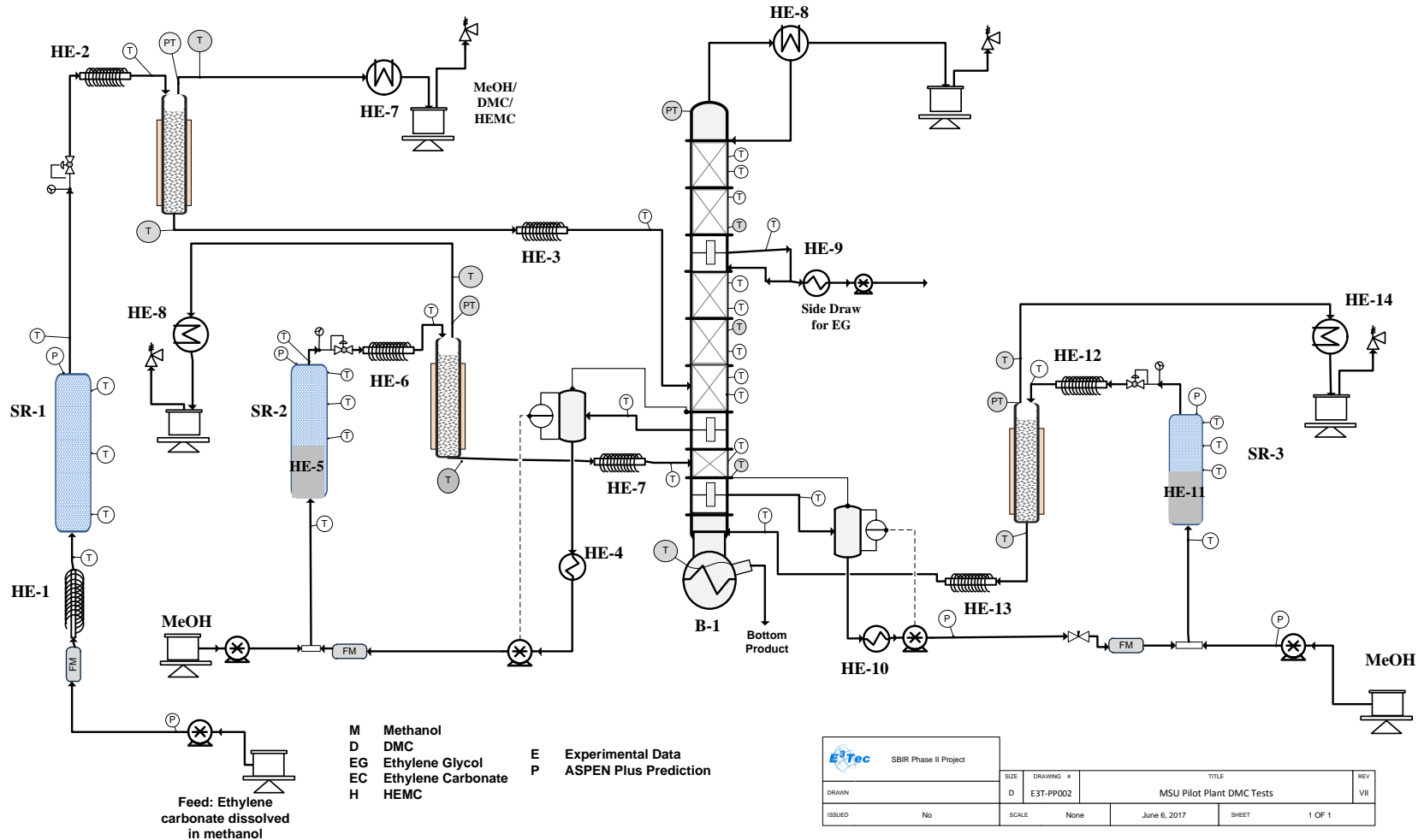
<b>Plant Service Life</b>	<b>30 Years</b>
<b>Normal Discount Rate</b>	<b>9 %</b>
<b>Corporate Income Tax</b>	<b>34 %</b>
<b>Inflation Rate</b>	<b>Between 2.2 % &amp; 3.0 %</b>
<b>Net Present Value (NPV)</b>	<b>\$ 249 million</b>
<b>Internal Rate of Return (IRR)</b>	<b>21%</b>

# Technology Demo Unit as Next Step

## Design Criteria

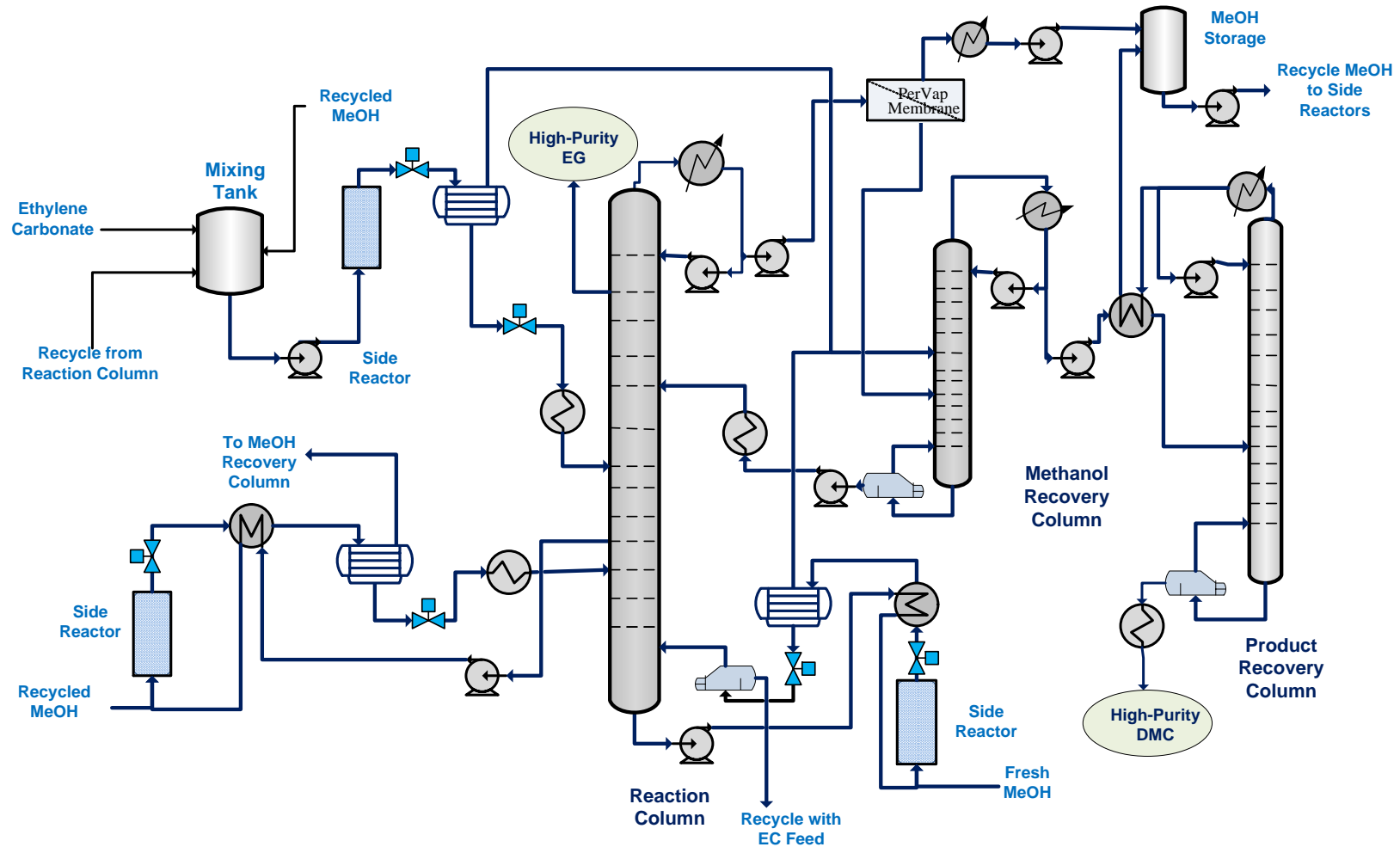
- **Skid-mounted unit with DMC capacity of one tonne per day**
- **Total Installed Cost (TIC) within \$10 million**
- **Continuous operation of fully integrated process, including recycle streams**
- **Catalyst activities for an extended period (12 months or more)**
- **Demonstrate product yield and purity – DMC and MEG**
- **Scale-up from MSU test unit → Demo Unit → Commercial plant**
- **Validation of the ASPEN Plus® design model as well as reactor models**

# MSU Test Unit





# Technology Demo Unit Scaled up from MSU Test Unit



# Path Forward

## *Partnership Opportunities*

- **Funding and Investment**: Pilot plant demonstration of the technology at a cost of \$10 million with a possibility of SBIR Phase III CRADA funding
- **Licensing Partners**: Licensing the patented technologies and/or strategic alliances for advancing TRL to commercialization stage
- **Facilities**: Industrial site for pilot plant demonstration
- **Collaboration for Marketing**: DMC Offtakes
- **Path Forward**: Commercial demonstration (build and operate) to validate techno-economic merits