Numerical Modeling for the Performance of Reversible Solid Oxide Fuel Cell

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Introduction

Background & Motivation

- Different phenomena are observed in various Solid Oxide Electrolysis Cells (SOEC) experiments with different testing conditions.
- A global minimum resistance exists under different working bias conditions.
- Severe performance degradation caused by Ni migration was also reported in the literature.

> Purpose of the study

The performance of solid oxide cells (SOCs) under both electrolysis mode and fuel cell mode is investigated via in-house developed high fidelity multiphysics simulations.

Methodology

> Multiphysics modeling



basic physical/electrochemical processes:

- Electrochemical reactions
- Chemical reactions
- Charge transport
- Double layer capacitor
- Species consumption/production
- Gas phase diffusion within porous media
- Surface/Bulk diffusion within electrodes
- Gas transport in the channel
- Heat transfer
- Phase change/formation
- Microstructure evolution
- * * * * * *

* based on the MSRI anode-supported button cell

Mathematically, these highly coupled processes are formulated by sets of partial differential equations

Charge conservation

domain	phase	governing equations
Cathode	LSM	$a_{int,c}C_{DL,c}\frac{\partial}{\partial t}(\varphi_c-\varphi_i)+\nabla\cdot(-\sigma_c\nabla\varphi_c)=i_{Fc}$
	YSZ	$a_{int,c}C_{DL,c}\frac{\partial}{\partial t}(\varphi_i-\varphi_c)+\nabla\cdot(-\sigma_i\nabla\varphi_i)=-i_{Fc}$
Electrolyte	YSZ	$\nabla \cdot (-\sigma_i \nabla \varphi_i) = 0$
Anode	YSZ	$a_{int,a}C_{DL,a}\frac{\partial}{\partial t}(\varphi_i-\varphi_a)+\nabla\cdot(-\sigma_i\nabla\varphi_i)=-i_{Fa}$
	Ni	$a_{int,a}C_{DL,a}\frac{\partial}{\partial t}(\varphi_a - \varphi_i) + \nabla \cdot (-\sigma_a \nabla \varphi_a) = i_{Fa}$

Species transportation

$$\varepsilon \frac{\partial \phi}{\partial t} = \nabla \cdot \left(D_{\phi}^{eff} \nabla \phi \right) - S_{\phi}$$

Exchange current densities (i_{Fc}, i_{Fa}) and species consumption/production rate (S_{ϕ}) are coupled via the electrochemical model (i.e., Butler-Volmer model).

References

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- T. Yang et al., International Journal of Hydrogen Energy, 43(32), pp 15445-15456, 2018.
- T. Yang et al, Physical Chemistry Chemical Physics, 19(45), pp 30464 30472, 2017.
- T. Yang et al., International Journal of Electrochemical Science, 12, pp 6801-6828, 2017.



agency thereof.

> Parametric study of cell performance under practical working conditions (fuel/steam supply conditions & working loads) OCV SOEC mode SOFC mode 0.225 0.200 0.175 0.150 0.125 0.200 0.175 0.200 0.200 0.175 0.150 0.125 0.175 0.150 0.150 75% 25% 25% 75% 25% 25% 75% 🔪 *iment I* (H₂:N₂=1:4) H₂O H₂O H₂O H₂O H₂O eriment II (15% H₂) 50% 50% 50% 50% $ation I (H_2:N_2=1:4)$ Simulation II (15% H₂) 25% 25% 25% 25% ○ (global minimum) 0% 0%

Performance Degradation due to Ni Redistribution microstructural properties change



Multiphysics simulations are developed for the performance investigation of solid oxide cells under both SOFC and SOEC operation mode. The full parameter space (various fuel/steam supply conditions) is explored to better understand the trends of cell performance under practical working conditions. For each specific working loads, a global minimum resistance is found, but the conditions for the global minimum resistance shift for different working loads under different working modes. The performance degradation due to the Ni redistribution is predicted and investigated based on the changes of reaction sites and

microstructural properties. The charge transfer processes in the hydrogen/steam electrode are mainly affected by Ni redistribution. This study can provide guidance for the design of efficient reversible solid oxide fuel cell (r-SOFC) systems.

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Results



Mapping of impedance behavior under different working loads and fuel/steam supply conditions

	anode active layer	ca act
ϵ	0.2	
f_{Ni} or f_{LSM}	0.34	
f_{YSZ}	0.45	
$l_{tpb} \ (m/m^{-3})$	5.97×10^{12}	6.7
D_{pore} (μm)	0.44	
$D_{Ni} or D_{LSM} (\mu m)$	0.57	
D_{YSZ} (μm)	0.35	
$A_{Ni/YSZ} \ or A_{LSM/YSZ}$ (m^2/m^{-3})	1.0×10^{6}	0.9

• T. Hsu et al., Journal of Power Sources, 386, pp. 1-9, (2018) • R. Mahbub et al., ECS Transactions, 78, pp. 2159-70, (2017)

Main performance degradation occurs on the high frequency range (> 1000 Hz), indicating that the Ni redistribution inside the active layer mainly affects the charge transfer processes hydrogen/steam electrode.

Impedance behavior

Summary

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