

### RTI Warm Syngas Cleanup Operational Testing at Tampa Electric Company's Polk 1 IGCC Site

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### Energy Technologies at RTI International

delivering the promise of science **ENERGY TECHNOLOGIES** Production for alobal aood Industry **Developing advanced process** Pilot technologies for energy applications **ORTI** by partnering with industry leaders \$885 M III Bench FY2016 Revenue Clean Coal / **Industrial Water** University Lab **Syngas Processing** Treatment **TECHNICAL MATURITY** 5,032 Staff Members 3,064 📋 1,102 Research Development Deployment Projects Clients Worldwide Advanced (fiscal year 2016 **Carbon Capture &** Materials for **Focused on Applied** Utilization / 90 250 105 Catalysis & Research **Gas Separations Degree Fields** Languages Nationalities **Separations** (concept to demonstration) Natural Gas in Partnership with 13 10 **Biomass** Government Agencies, Extraction & U.S. Offices Internationa Conversion Offices Conversion Academia, and Industry ENERGY Energy Efficiency & Renewable Energy Energy Efficiency & ENERGY Energy Efficiency & Benewable Energy .S. DEPARTMENT OF NATIONAL NERGY CASALE BASF GASSNOVA CLARIANT TECHNOLOGY BIOENERGY TECHNOLOGIES OFFICE ADVANCED MANUFACTURING OFFICE mm NC STATE STANFORD UNIVERSITY Duke CRIVERSITY OF CALIFORNIA SINTEF HALDOR TOPSOE I OVEOLIA Masdar  $\mathcal{L}$ BERKELEY LA THE LINDE GROU





## Integrated Gasification Combined Cycle – Syngas Cleanup



# RTI Warm Syngas Cleanup Technology Platform

#### RTI PILOT PLANT TEST UNITS AT EASTMAN COAL GASIFICATION PLANT



RTI has developed a platform of warm syngas cleanup technologies that:

- Increase efficiency and lower costs,
- Operate at 250-600°C (maximum temperature varies with specific contaminants),
- Have been tested on actual coal-based and petcoke-based syngas,
- Are fully compatible with CO<sub>2</sub> capture technologies, and
- Enable specific syngas purity needs to be met via a flexible modular approach.





### RTI Warm Gas Desulfurization Process (WDP) - Overview

Enables high removal of total sulfur ( $\geq$ 99.9%) from syngas at temperatures as high as 600°C.

A unique process technology based on dual transport reactor loops (similar to FCC reactor designs)...



... and on a regenerable, high-capacity, rapid acting, attrition-resistant sorbent.



RTI Proprietary Desulfurization Sorbent

- R&D 100 Award
- Unique highly-dispersed nanostructures
- Developed in long-term cooperation with Clariant (~100 tons to date)
- Covered by extensive US & International patents, including several recent improvements





**RTI Warm Gas Desulfurization Process (WDP)** 

### Successful WDP Scale-up from Lab to Large-Scale Pre-Commercial Testing







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# RTI Warm Syngas Desulfurization: 50-MW $_{\rm e}$ Pre-Commercial Testing Project at Tampa Electric Company's Polk 1 IGCC Site







# Integration of Warm Syngas Cleaning and Carbon Capture Systems at Tampa Site



20% slipstream test (~50 MW<sub>e</sub>) enables direct commercial scale-up from this demonstration scale. The demonstration plant cleans ~2MMscfh of raw syngas from the TECO gasifier.





# CO<sub>2</sub> Capture: BASF OASE<sup>®</sup> Activated Amine Process





OASE<sup>®</sup> has the lowest specific energy consumption of any standard amines for acid gas removal.
OASE<sup>®</sup> 's higher absorption kinetics and capacity reduce equipment size resulting in lower capex and opex.
OASE<sup>®</sup> is chemically and thermally stable, non-corrosive, non-toxic, and readily biodegradable.
But, exploiting OASE<sup>®</sup> for CCS in IGCC requires upstream selective sulfur removal technology for syngas.

Design rate ~1200 tpd of carbon dioxide captured by RTI demonstration plant





## **RTI WDP Pre-commercial Demonstration Project Team**

### **Project Team**







## RTI WDP Demonstration Project Performance – Construction and Initial Operation Period (ARRA Funding)



DOE/RTI/TECO/Clariant Team

- Construction achieved <u>on</u> schedule & <u>under</u> budget
- >500,000 total labor hours with <u>no</u> significant injury
- Unit performed as expected
- ~99.9% total sulfur removal from RTI WDP step
- Up to 99.999% total sulfur removal with WDP + aMDEA<sup>®</sup> (sub-ppmv levels of total sulfur in syngas)
- Sorbent attrition rate in line with design expectations
- Sorbent sulfur capacity steady no deactivation
- Successful operation below and above design rate
- Unit was down for an unexpectedly long period of time in 2015 due to host site problems, resulting in need for extension of the operational testing period.





### Need:

- Testing through ARRA funding showed that WDP technology had great potential to provide clean syngas from coal and petcoke-based gasification at increased efficiency and at lower capital and operating costs than conventional syngas cleanup technologies.
- The unexpectedly long host site outage in spring/summer of 2015 sacrificed operational time needed to fully address all critical technical risks before the technology could be deemed ready for scale-up to a full commercial demonstration.

### Goals of Extended Operational Testing:

- Operate the WDP unit up to an additional 3,000 hours to allow adequate time to mitigate remaining technical risks for WDP scale-up.
- Target achieving 1,000 of those hours via continuous operation of the integrated pre-commercial demonstration system (WDP+WGS+aMDEA) to mitigate any risks of integrating WDP with WGS and carbon capture.





### RTI WDP Pre-Commercial Testing Project Performance -Post-ARRA Operations Summary Results



- WDP consistently reduced inlet total sulfur ~99.9%.
- Clean syngas exiting the carbon capture block was as low as 99.999% total sulfur removal (< 0.5 ppmv total sulfur).</li>
- Post operation inspections demonstrated that acceptable materials of construction had been ultimately identified for heat exchangers and refractory.
- Microreactor testing of the cleaned syngas showed no significant signs of methanol or F-T catalyst deactivation.
- Achieved >3,500 total syngas operation hours on WDP, >2,000 hrs on WDP+aMDEA<sup>®</sup>, and ~700 total integrated hours on WDP+WGS+aMDEA<sup>®</sup> (had to stop testing in April, 2016 due to host site cooling water system switchover).
- We achieved ~7,000 hours of total syngas operations from the combined pilot and pre-commercial demonstration testing programs.
- WDP availability at the end of testing was as high as 93%, with identified new design improvements that should enable availabilities in the high 90's% for future commercial units.

 $aMDEA^{(e)} = activated amine carbon capture process of BASF WGS = water gas shift process$ 





### Pre-commercial Demonstration Test Plant Results: Consistently High Total Sulfur Removal from WDP Alone (both H<sub>2</sub>S and COS)

#### Data from Four Months of WDP Operations







### Effluent Syngas Concentrations







### 90% Carbon Capture Goal Was Achieved







### Follow-up Testing Needs Identified

A few data gaps were identified from the lessons learned workshops, particularly related to operation and control when using low sulfur coals (about half of coal reserves in the U.S.). These data gaps can and should be addressed by additional hot and cold flow testing.

#### Hot Flow Test Unit



Cold Flow Test Unit







# Operational Testing Summary

- The operational phase of this project was very successful in its primary goal of reducing technical risks associated with commercial deployment of WDP:
  - Demonstrated that available knowledge and expertise for transport reactor systems from fluid catalytic crackers could be effectively leveraged for high-pressure operations and WDP. This eliminated a number of technical risks for scale-up and deployment.
  - Stable and continuous desulfurization was achieved in just two reactors using near commercial-scale equipment.
  - The desulfurization sorbent consistently demonstrated ability to remove 99.8%-99.9% of both  $H_2S$  and COS from syngas.
  - Attrition resistance of the sorbent actually improved with use and actual attrition losses were substantially below design estimates.
  - Sorbent capacity was stable, showing no significant loss in sulfur capacity over >3,500 hours of operation.





# Operational Testing Summary (continued)

- Stable, continuous desulfurization of syngas was demonstrated during extended integrated runs with an availability of >90% for the WDP block.
- No evidence was observed of deterioration of new metallurgy installed in the syngas interchanger and the regenerator heat exchanger.
- Refractory remained in good shape in spite of multiple start/stop events with maintenance limited to field installed sections. Refractory is expected to achieve satisfactory commercial lifetimes.
- The aMDEA<sup>®</sup> system, when coupled with WDP, enabled highly selective removal of both sulfur and CO<sub>2</sub> achieving up to 99.999% total sulfur removal (sub-ppmv levels) and ~98% CO<sub>2</sub> removal. AECOM stream analysis showed essentially no trace contaminants in final syngas.
- WDP, WGS, and aMDEA<sup>®</sup> were successfully integrated and operated for extended hours while generating a H<sub>2</sub>-rich syngas stream and capturing >90% of the system carbon.

This project has been one of the most successful DOE-NETL projects.





# Value Drivers of RTI Warm Syngas Cleanup Technology



RTI Technology Reduces Cost and Improves Efficiency!





## Benefits of RTI WDP Technology

- RTI WDP is a unique differentiated warm-temperature, solidsorbent based syngas cleanup system that <u>simultaneously</u> offers:
  - Lower capital costs (20-50% less),
  - Lower non-labor, non-feedstock operating costs (up to 30-50+% less),
  - Improved overall process efficiency (up to 10+% better),
  - Improved process flexibility by decoupling sulfur removal and CO<sub>2</sub> capture, and
  - A capable and economic syngas cleanup option for all applications:

| Typical/Suitable<br>Applications        | Amines        | Selexol™      | Rectisol®       | RTI WDP + CC<br>(e.g., aMDEA <sup>®</sup> ) | CC = Carbor<br>Capture |
|---|---------------|---------------|-----------------|---|------------------------|
| IGCC (without CC)                       | V             | ×             | (too expensive) | <b>V</b>                                    |                        |
| IGCC (with CC)                          | 1             | V             | (too expensive) | ~   |                        |
| H <sub>2</sub> or NH <sub>3</sub> /Urea | (not capable) | V             | ×               | ×   | -                      |
| Chemicals (e.g.,<br>MeOH, F-T, SNG)     | (not capable) | (not capable) | 1               | <b>~</b>                                    |                        |



### WDP Pre-commercial Testing Video (optional)

# RTI's Unique Breakthrough Warm Gas Cleanup Technology





### **RTI** Team



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  - CH2M Hill
  - BASF
  - Clariant





### QUESTIONS?





