the Energy to Lead

### ADVANCED GASIFIER AND WATER GAS SHIFT TECHNOLOGIES FOR LOW COST COAL CONVERSION TO HIGH HYDROGEN SYNGAS

#### **DOE/NETL Cooperative Agreement DE-FE0023577**

#### > Don Stevenson, Executive Director

 DOE Gasification and C&CBTL Workshop Morgantown, WV August 10, 2015



# **AGWGST Program Team**

- **gti** > Gas Technology Institute Compact gasifier technology



- >RTI International
  - Advanced Water Gas Shift reactor technology



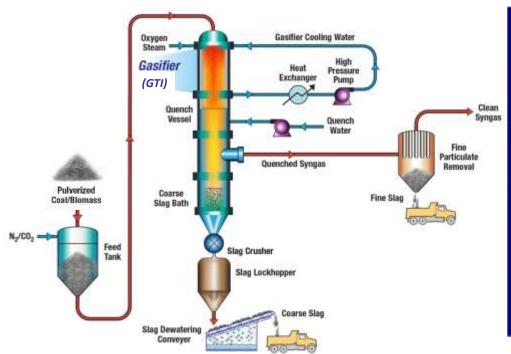
- Coanda > Coanda Research & Development
  - Cold flow simulation of gasifier quench zone

### *Nexant* > Nexant, Inc.

 Techno-economic analysis showing integrated benefits of GTI, RTI technologies



# **Compact Gasifier Overview**



#### **Compact Gasifier Attributes:**

- Dry feed for high efficiency, feedstock flexibility
- Rapid mix injector + plug flow reactor for 90% smaller volume
- Advanced cooling design for robust thermal margins, long component life
- Eliminates black water system
- Long MTBF, short MTTR for high availability

#### **Benefits:**

- High CGE: 2-4% > than other dry feed, 7%-9% > than slurry
- Lower capex: ~15-25% plant cost reduction vs. lowest cost entrained flow tech
- 15%-25% reduction in cost of product (power, chemicals, liquids)



# **Principles of Operation**

- > Dry feed system enables use of low rank coals
- > Multi-element feed splitter
  - Uniform splitting assures good O<sub>2</sub>/coal ratio at each element
  - Establishes "plug flow" to minimize recirculation, accelerate gasification
- > Advanced cooled liner design
  - Keeps metal temperatures < 550°C for long life</li>
  - High thermal margins enables operation on coals with high ash fusion temperature (AFT)
- > Rapid spray quench
  - Flexibility to provide dry syngas from 350°C to 800°C
  - High degree of flexibility for process optimization

# **Gasifier Development Needs**

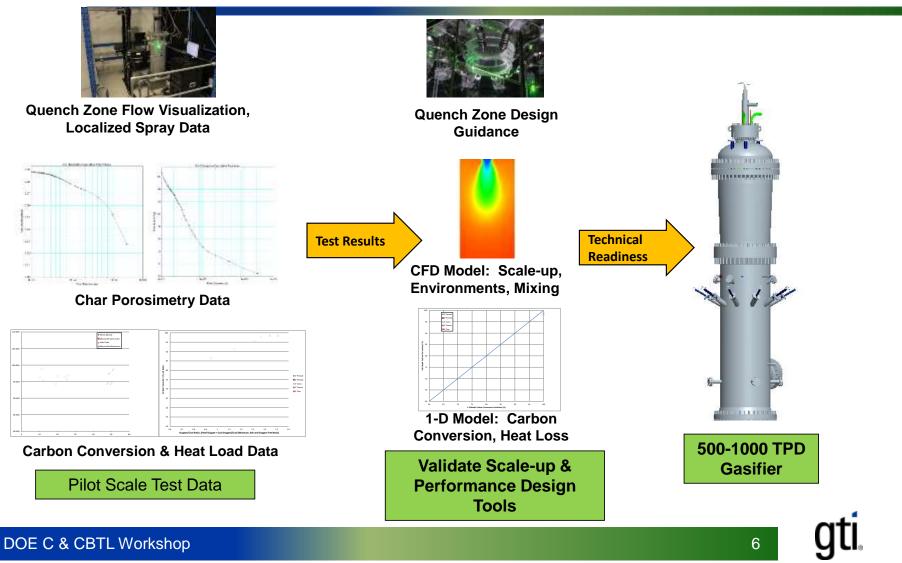
- > Quench Zone Modeling
  - Slag blockage, misdirected syngas flow
- > Highly Reactive Feedstocks
  - Potential for aggressive thermal environments near burner
- > High AFT + High Ash Coals
  - AFT >1500°C, >25% ash
  - Significant limitation for existing technologies
- > Carbon Conversion Kinetics
  - Need better data to address final ~5% carbon conversion
  - Study porosimetry, surface area per unit mass as function of conversion







### Test Program Matures Technology to Readiness for 500-1000 TPD Demonstration



# Advanced Water Gas Shift Technology

Primary reaction pathway is the Water Gas Shift (WGS) reaction

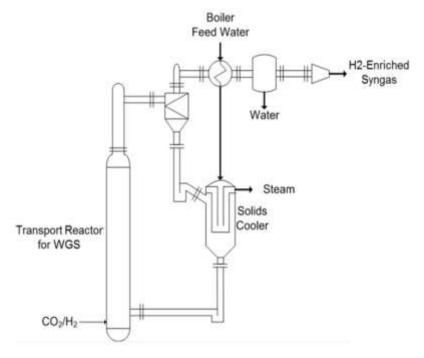
 $CO + H_2O = CO_2 + H_2$   $\Delta H = -41 \text{ kJ/mol}$ 

#### Challenges

- Proactive reactor temperature control required
  - WGS reaction is exothermic
  - Coal-derived syngas has high CO concentration
- WGS reaction is equilibrium limited
  - Lower temperatures maximize H<sub>2</sub> production
  - High-activity lower-temperature catalysts are poisoned by syngas contaminants

#### **Conventional solutions**

- Large additions of steam
- Multiple reactor stage with inter-stage cooling



#### **Proposed solution**

- Leveraging commercial FCC technologies (transport reactor with solids cooler)
- RTI's expertise in developing attrition-resistant fluid-bed materials

# **AWGS Technology Road Map**

#### **Critical technical challenges**

- Development of attrition-resistant WGS catalyst formulation
- Successfully leveraging existing commercial technologies

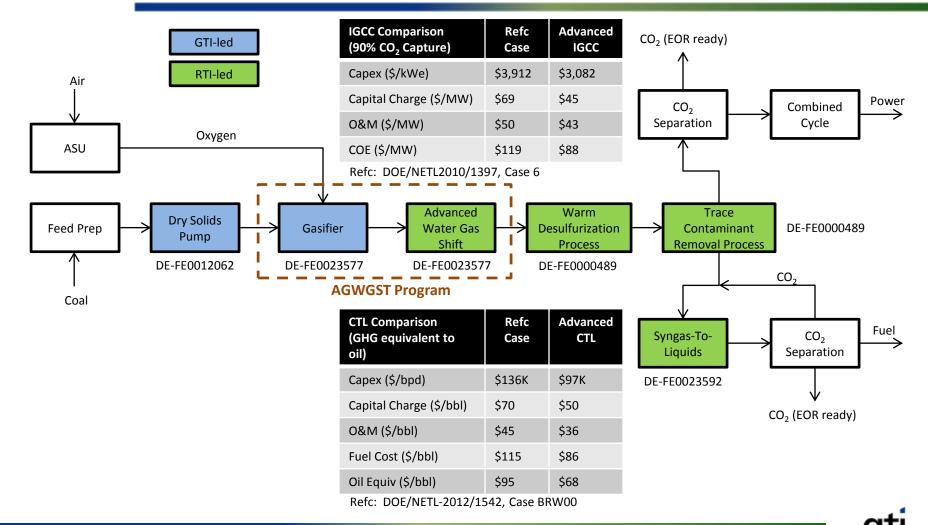
Stage	Research Objectives	Status
Technical feasibility	<ul> <li>Demonstrate fluidizable WGS catalysts that possess attrition resistance and WGS activity.</li> <li>Perform preliminary techno-economic analysis to assess cost and efficiency benefits</li> </ul>	Completed by 12/31/2014 (DE-FE0012066)
Catalyst Development	<ul> <li>Optimize fluidizable WGS catalyst for attrition resistance and WGS activity</li> <li>Complete lab-scale testing of catalyst performance using simulated syngas mixtures at typical operating conditions to determine catalytic performance (activity, stability and selectivity)</li> <li>Update preliminary TEA to assess cost and efficiency benefits</li> </ul>	In Progress (DE-FE0023577)
Pilot-plant Testing	<ul> <li>Demonstrate performance of fluidized-bed catalyst in a pilot-scale transport reactor with a solids cooler using real coal-derived syngas.</li> </ul>	Optional Task (DE-FE0023577)
Demonstration	<ul> <li>Demonstrate expected commercial performance in demonstration-scale equipment with real commercial syngas and a commercially produced catalyst.</li> </ul>	Future project



# **Integration with Balance of Plant**

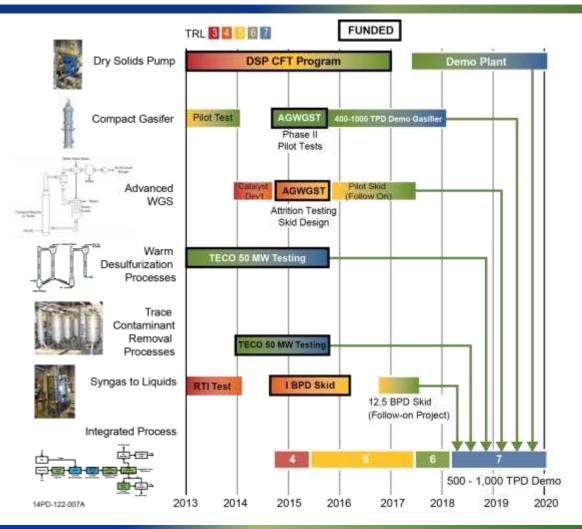
- Standard coal pulverization equipment
- Ultra-dense phase feed system, fed by conventional lock hoppers or Dry Solids Pump
- Standard oxygen, steam supply to gasifier
- Reactant supply skid for high pressure torch igniter (GTI supplied equipment)
- High pressure BFW in closed loop gasifier cooling system
- Recycled process condensate for quench
- Standard slag bath process
- Cyclone/candle filters for fines removal (dry recovery)

## Integration With Other DOE Projects – 25% Reduction in Cost of Products



DOE C & CBTL Workshop

### Technologies on Path for 2020 FOAK Commercially Relevant Demo



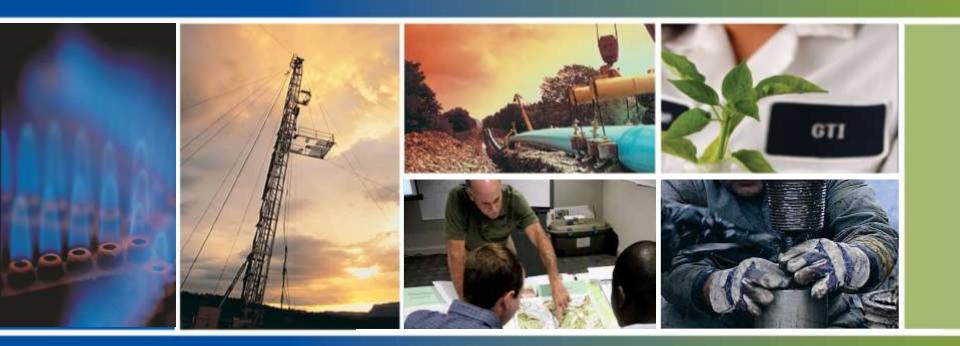
DOE C & CBTL Workshop



# Conclusion

- GTI and RTI technologies offer potential for >25% reduction in cost of power, fuels
- GTI compact gasifier is ready for demonstration plant scale up after program
- RTI AWGS technology ready for pilot plant test after program
- Techno-economic analysis will assess integrated benefits of these technologies
- Technologies on track for 2020 demonstration

# Turning Raw Technology into Practical Solutions



don.stevenson@gastechnology.org

www.gastechnology.org | @gastechnology

DOE C & CBTL Workshop



qti