New Options in the IECM Power Plant Simulation Model

Edward S. Rubin

Department of Engineering and Public Policy Department of Mechanical Engineering Carnegie Mellon University Pittsburgh, Pennsylvania

Presentation to the DOE/NETL

CO₂ Capture Technology Meeting Pittsburgh, Pennsylvania

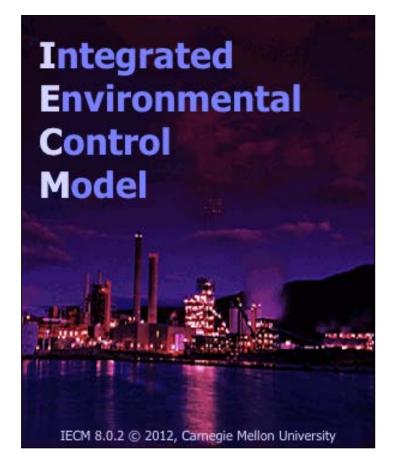
June 23, 2015

Outline of Talk

- Overview of the IECM
- Recent developments
- Future developments

IECM: A Tool for Analyzing Power Plant Design Options

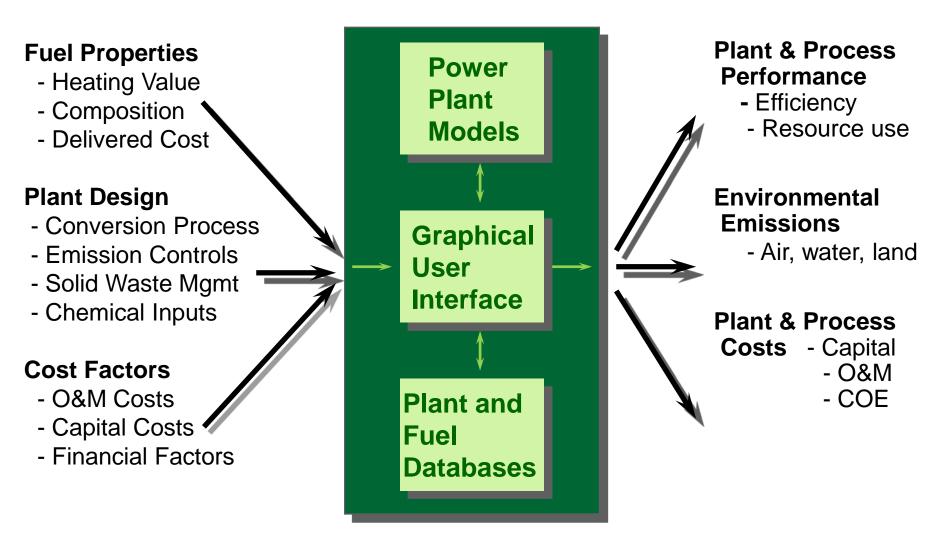
- A versatile computer simulation model developed for DOE/NETL (runs quickly on a laptop or desktop)
- Provides systematic estimates of performance, emissions, costs and uncertainties for preliminary design of:
 - PC, IGCC and NGCC plants
 - All flue/fuel gas treatment systems
 - CO₂ capture and storage options (pre- and post-combustion, oxycombustion; transport, storage)
- Free and publicly available at: <u>www.iecm-online.com</u>



IECM Modeling Approach

- Systems Analysis Approach
- Process Performance Models
- Engineering Economic Models
- Advanced Software Capabilities
 - Probabilistic analysis capability
 - User-friendly graphical interface
 - Versatile input/output features

IECM Software Package



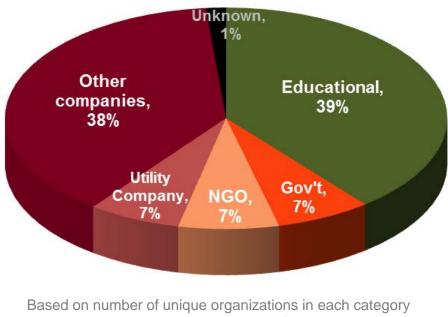
Inputs and results can be either deterministic or probabilistic

Technologies in IECM v.8.0.2

CO ₂ Capture & Storage Systems*	Coal Com	bustion Plants	Gasification Plants (IGCC)	IGCC and NGCC Plants
Post-Combustion Capture	Boiler/Turbine	Particulate Removal	Air Separation Unit	Gas Turbine
Conv. Amine; Adv. amines	<u>Systems</u>	Cold-side ESP; Fabric	Cryogenic	GE 7FA; GE 7FB
(FG+); Chilled ammonia;	Subcritical;	filter (Reverse air;		
Membrane systems; Aux.	Supercritical;	Pulse jet)	Slurry Preparation	Heat Recovery
NG steam or power gen.	Ultra-supercritical		& Coal Pretreatment	Steam Generator
(optional)		<u>SO₂ Removal</u>		
	Furnace Firing	Wet limestone (Conv.;	Gasification	Steam Turbine
Oxy-Combustion Capture	Tangential; Wall;	F. oxidation;	Slurry-fed gasifier	
Flue gas recycle; ASU;	Cyclone	Additives); Wet lime;	(GE-Q); Dry-fed	Boiler Feedwater
Chemical processing units		Lime spray dry	gasifier (Shell)	<u>System</u>
	Furnace NOx			
Pre-Combustion Capture	<u>Control</u>	Solids Management	Syngas Cooling and	Process Condensate
Water gas shift + Selexol	LNB; SNCR;	Ash pond; Landfill;	Particulate Removal	Treatment
Chemical looping	SNCR+LNB;	Co-mixing; useful		
	Gas reburn	byproducts	Mercury Removal	Cooling Water
CO ₂ Compressor			Activated carbon	<u>System</u>
	Flue Gas NOx	Cooling and		Once-through; Wet
CO ₂ Transport	<u>Removal</u>	Wastewater Systems	<u>H₂S Removal</u>	cooling tower; Dry
Pipelines (6 U.S. regions);	Hot-side SCR	Once-thru cooling;	Selexol; Sulfinol	cooling
Other (user-specified)		Wet cooling tower;		
	Mercury Removal	Dry cooling;	Sulfur Recovery	Aux. Equipment
<u>CO₂ Storage</u>	Carbon/sorbent	Chemical treatment;	Claus plant; Beavon-	
Deep saline formation;	injection	Mech. treatment	Stretford unit	
Geol.Storage w/ EOR;				
Other (user-specified)				

IECM Users and Uses

- ~ 2000 Individuals
- ~ 600 Organizations
- ~ 60 Countries



(as of March 24, 2015)

IECM IS USED FOR:

- Process design
- Technology evaluation
- Cost estimation
- R&D management
- Risk analysis
- Environmental compliance
- Marketing studies
- Strategic planning
- Teaching/Education

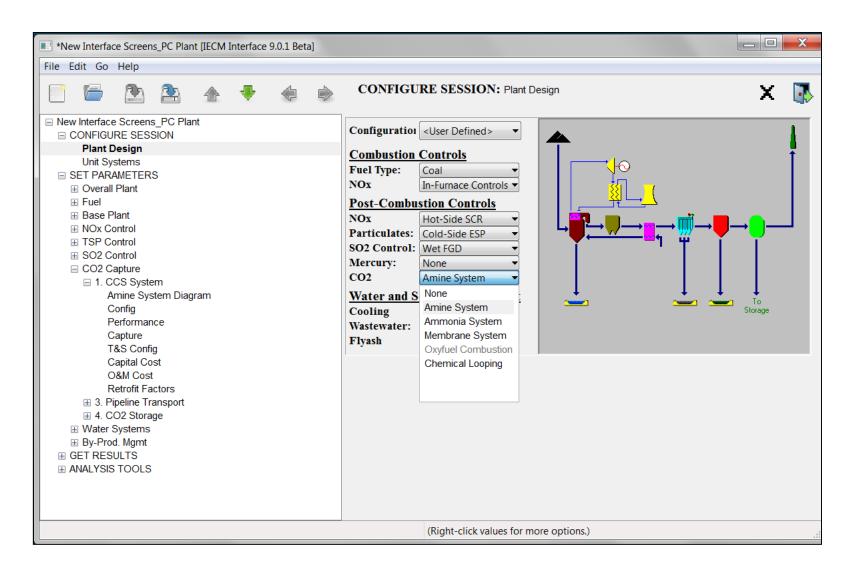
Recent Developments

New IECM Options and Features (v.9.0 beta)

NEW SOFTWARE FEATURES

- A new collapsible menu for navigation (instead of "tabs")
- A "Configure Session" menu, including unit conversion options
- An "Analysis Tools" menu with cool new analytical options
- Addition of process flow diagrams to Set Parameters screens
- Adjustments to GUI screens for better readability and consistency

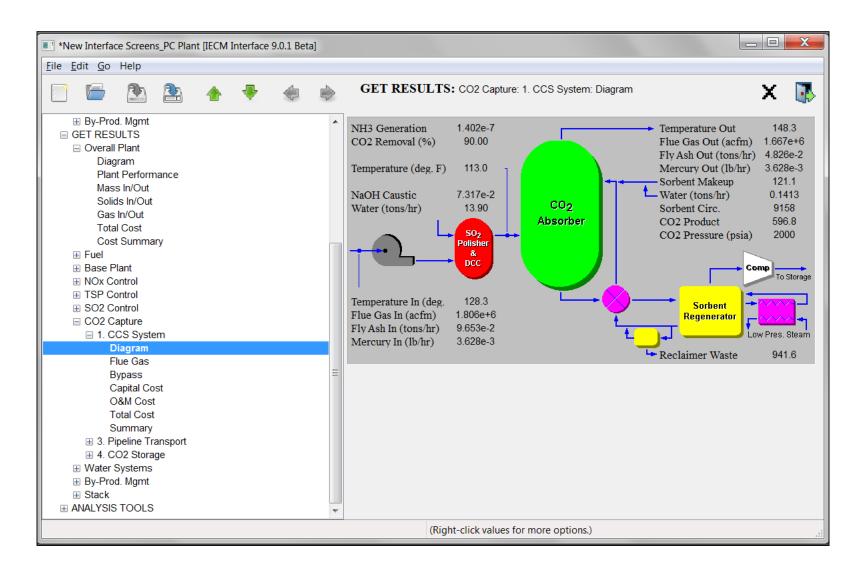
New Interface: Configure Session



New Interface: Set Parameters

e <u>E</u> dit <u>G</u> o Help								
🗋 🗁 🖭 🏝 🔶 🔶	1	SET PARAMETERS: CO2 Capture:	1. CCS	System: Capt	ure		3	× 🛯
New Interface Screens_PC Plant CONFIGURE SESSION Plant Design		<u>Title</u> Absorber	<u>Unc</u>	<u>Value</u>	<u>Calc</u>	<u>Min</u>	<u>Max</u>	<u>Defaul</u>
Unit Systems		Sorbent Concentration (wt %)		30.00	✓	15.00	40.00	Calc
		Lean CO2 Loading (mol CO2/mol sorb)		0.1900	V	0.0	0.3000	Calc
⊞ Overall Plant ⊞ Fuel		Sorbent Losses (excluding acid gasses) (lb/		0.6002		0.0	10.00	Calc
⊞ Base Plant		Sorbent Recovered (lb/ton CO2)		0.3970		0.0	10.00	Calc
NOx Control		Liquid-to-Gas Ratio (ratio)		3.090		0.0	10.00	Calc
TSP Control SO2 Control		Ammonia Generation (mol NH3/mol sorb)		1.000		0.0	2.000	Calc
		Gas Phase Pressure Drop (psia)		1.000		0.0	5.000	Calc
☐ 1. CCS System		ID Fan Efficiency (%)		75.00	= -	50.00	100.0	75.00
Amine System Diagram		Makeup Water for Wash Section (% raw flue		0.8000	_	0.0	10.00	0.8000
Config Performance		Regenerator						
Capture		Regenerator Heat Requirement (Btu/lb CO2)		1519		500.0	5000	Calc
T&S Config		Regenerator Steam Heat Content (Btu/lb ste		1373		500.0	1500	Calc
Capital Cost O&M Cost		Heat-to-Electricity Efficiency (%)		18.70		0.0	40.00	Calc
Retrofit Factors		Solvent Pumping Head (psia)		30.00		0.0	80.00	30.00
		Pump Efficiency (%)		75.00	_	50.00	100.0	75.00
⊕ 4. CO2 Storage		Percent Solids in Reclaimer Waste (%)		40.00	v	0.0	100.0	Calc
Water Systems By-Prod. Mgmt		Capture System Cooling Duty (t H2O/t CO2)		90.87	v	0.0	200.0	Calc
		, , ,						
ANALYSIS TOOLS								

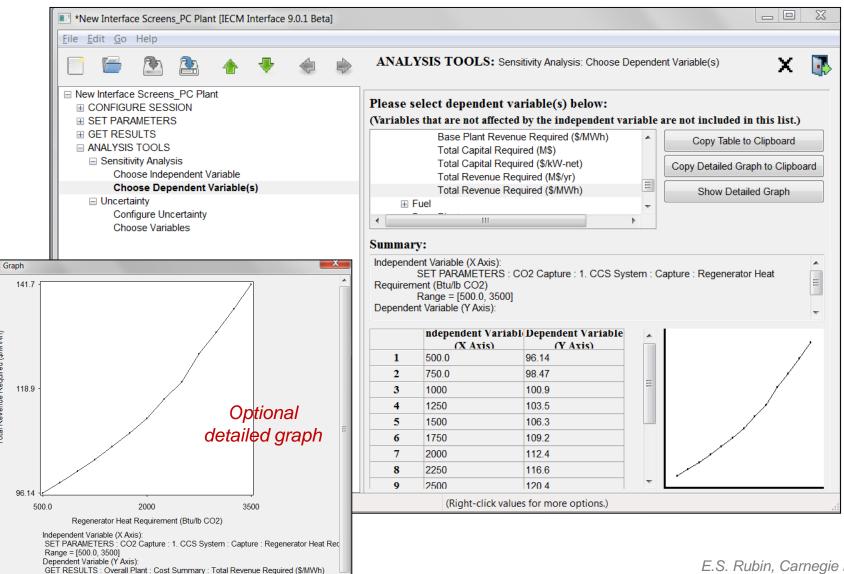
New Interface: Get Results (diagram)



New Interface: Get Results (table)

<u>E</u> dit <u>G</u> o Help						
🖆 🖄 🏝 🛧 🔻 🚸 🔿	(GET RESULTS: Overall Plant:	Cost Summ	ary		
By-Prod. Mgmt GET RESULTS		A	В	С	D	E
Overall Plant Diagram Plant Performance	1	Technology	Capital Required (M\$)	Capital Required (\$/kW-net)	Revenue Required (M\$/yr)	Revenue Required (\$/MWh)
Mass In/Out	2	Combustion NOx Control	9.429	17.84	1.205	0.3468
Solids In/Out	3	Post-Combustion NOx Control	33.99	64.32	7.012	2.018
Gas In/Out	4	Mercury Control	0.0	0.0	0.0	0.0
Total Cost	5	TSP Control	26.61	50.36	5.861	1.687
Cost Summary	6	SO2 Control	170.1	321.9	41.60	11.97
	7	Combined SOx/NOx Control	0.0	0.0	0.0	0.0
Base Plant	8	CO2 Control	537.2	1016	114.2	32.86
NOx Control	9	Subtotal	777.4	1471	169.9	48.89
TSP Control	10	Cooling Tower	79.86	151.1	21.33	6.139
SO2 Control	11	Wastewater Control	0.0	0.0	0.0	0.0
□ CO2 Capture	12	Base Plant	1006	1903	178.8	51.45
□ 1. CCS System	13	Emission Taxes	0.0	0.0	0.0	0.0
Diagram Flue Gas	14	Total	1863	3525	370.0	106.5
Bypass =	15	6				
Capital Cost	16	1				
O&M Cost	<u> </u>					
Total Cost	1					
Summary						
Water Systems						
By-Prod. Mgmt						
⊞ Stack						
ANALYSIS TOOLS						

New Interface: Analysis Tools (sensitivity)



Total Revenue Required (\$/MWh)

Range = [96.14, 141.7]

E.S. Rubin, Carnegie Mellon

New IECM Options and Features (v.9.0 beta)

NEW TECHNOLOGY OPTIONS

For PC Plants:

- Calcium looping system model for post-combustion CO₂ capture
- Enhanced oxy-combustion system performance and cost models

For IGCC Plants:

- Updated chemical looping system cost model for pre-combustion capture
- Ability to specify custom fuels and syngas composition for IGCC plants
- Updated direct capital cost default values for IGCC plants

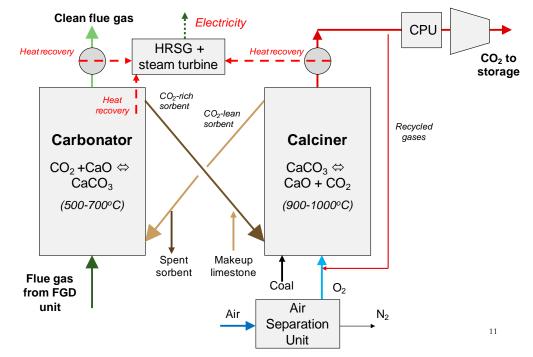
For All Plant Types:

- Updated process and project contingency cost factor default values (based on current level of maturity and cost estimating basis)
- Site-specific CO₂ storage cost model and geological reservoir database

Post-Combustion CaL Process Model



Calcium looping pilot plant at La Pereda coal-fired station, Asturias, Spain (March 2015)



Post-Combustion CaL Process Model

				4	SET PARAMET	ERS: COS	Capture: 1. C	nemical L	poping: Ca	rbonator				×
	E TSP Control			~	I	tle		Linc	Value		Calc	Min	Max	Default
	CO2 Capture				Carbonator Temperature (de	eg.C)		Tol .	650.0			600.0	700.0	650.0
	😑 1. Chemical L				Degree of Carbonation (frac	tion)			0.8000			0.0	1.000	0.800
	Air Separa		g Diagram Ioram		Makeup Limestone/Recircul	Makeup Limestone/Recirculating Sorbent (mol/mol) Maximum CaO Conversion (traction)			2.500e-	2	1	000e-2	1.000	2.500+
	Heat Reci	overy Sy	stem Diagr	an	Maximum CaO Conversion				0.2083			0.0	1.000	Calc
	Chemical Air Separa				Actual CaO Conversion (frac	tion)		I STATE	0 1683		1	0.0	1.000	Calc
	Performan		cey.		Residence Time of Solids (s	seconds)			267.1			0.0	None	Calc
	Carbonab	or			Cas Bhace Brecove Drop	00000000			0.4404	-	12	0.0	5.000	Calc
(B)	2 4 4		ф S	ET PA	RAMETERS: 002 Capture	1. Chemical i	Looping Calcin	er .			x	30	100.0	75.00
	1 🔶 🌩	4	φ s	ET PA									100.0 None	- 223
SP Contro 02 Contro	rol	+			Title	1. Chemical i	Salae	er Calc	Min	Max	Def	anit 10	100.0 None	- 1233
SP Contro 02 Contro 02 Contro	rol bure	+							Min 850.0	Max 950.0		anit 10		- 1233
SP Contro 02 Contro 02 Contro 02 Contro 02 Contro	rol ture mical Looping	+	Caloner 1	lempera	Title		Salae				Def 900	andz 10		- 1233
SP Contro 02 Con	rol bure	+	Caloner 1 Degree of	Tempera (Calcina	Tide shure (deg. C)		Xalae 900.0		850.0	950.0	Def 900	mit 10 0.0 500		- 1233
SP Contro IO2 Contro IO3 Contro I	rol Imical Looping emical Looping Diagram Separation Diagram at Recovery System Dia		Catoner 1 Degree of CaCO3 C	Tempera (Calcinu onversio	Title store (deg. C) ation (fraction)		Xabae 900.0 0.9500	Cale	850.0 0.1000	950.0	Def 900 0.95	anda 40 0.0 5000 44c		- 1233
SP Contro 102 Contro 102 Capts 0 1 Cher Air 1 Hea Che	rol tare emical Looping emical Looping Diagram Separation Diagram at Recovery System Dia emical Looping Config		Caloner 1 Degree of CaCO3 C Residence	fempera (Calcina onversio a Time (Title ature (deg. C) ation (fraction) on in Calciner (fraction)		Xalas 900.0 0.9500 8.415e-3	Cale	850.0 0.1000 0.0	950.0 0.9900 1.000	Ded 900 0.95 Ca	10 0.0 500 4c		- 1233
SP Canter 02 Conter 02 Capto 02 Capto 0	rol Imical Looping emical Looping Diagran Separation Diagram at Recovery System Dia emical Looping Config Separation Config dormance		Caloner 1 Degree of CaCO3 C Residenc Gas Phas	Tempera (Całonu onversk a Time (a Press	Title ature (deg. C) ation (traction) on in Calciner (traction) of Solids (seconds)		Xabae 900.0 0.9500 8.4154-3 132.3	Cale	850.0 0.1000 0.0 50.00	950.0 0.9900 1.000 500.0	Ded 901 0.91 Ca Ca	10 0.0 500 4c 4c 4c		- 1233
SP Contro 02 Con	rol Imical Looping emical Looping Diagram Separation Diagram at Recovery System Dia emical Looping Config Separation Config ritomance ritomator		Caloner 1 Degree of CaCO3 C Residenc Gas Phas Fradion o	fempera f Calcina onversik a Time i a Press f Gas R	Title store (deg. C) ation (fraction) on in Calciner (fraction) of Solids (seconds) sure Drop (bar)		Xabae 900.0 0.9500 8.415e-3 132.3 9.015e-2	Cale	850.0 0.1000 0.0 50.00 0.0	950.0 0.9900 1.900 500.0 5.000	Ded 901 0.91 Ca Ca	10 10 10 10 10 10 10 10 10 10		- 1233
SP Contro IO2 Contro IO2 Contro IO2 Copts IO2 Copts IO2 Copts IO2 Contro IO2	rol Imical Looping emical Looping Diagran Separation Diagram at Recovery System Dia emical Looping Config Separation Config dormance		Caloner 1 Degree of CaCO3 C Residenc Gas Phas Fraction o Caloner F	Tempera (Całcinu onversik a Time (a Press f Gas R Recyclin	Title store (deg. C) ation (fraction) on in Calciner (traction) of Solids (seconds) sure Drop (bar) ecycling (traction)		Xidae 900.0 0.9500 8.415e-3 132.3 9.015e-2 0.6000	Cale	850.0 0.1000 0.0 50.00 0.0 0.0	950.0 0.9900 1.900 5.000 1.900 1.900	Ded 901 0.92 Ca Ca Ca Ca 0.61	Image: Name Image: Name		75.00

Post-Combustion CaL Process Model

		, 												
-	TSP Control			^		Title		Unc	Value		Calc <u>N</u>	lin	Max	Default
_	SO2 Control			Carbona	ator Temperat	ure (deg. C)			650.0		60	0.0	700.0	650.0
	I. Chemical	Loc	pping		of Carbonatio				0.8000	_			1.000	0.8000
	Chemica	al Lo	oping Diagram											
			on Diagram	Makeup	Limestone/R	ecirculating Sorbe	ent (mol/mol)		2.500e-2	2	1.00	0e-2	1.000	2.500e-2
			ery System Diagram ooping Config	Maximu	m CaO Conve	rsion (fraction)			0.2083		✓ 0	.0	1.000	Calc
			on Config	Actual C	aO Conversio	on (fraction)			0.1683		v 0	.0	1.000	Calc
	Perform		-	Resider	nce Time of So	olids (seconds)			267.1		v 0	.0	None	Calc
	Carbona	ator			aco Broccuro				0.4400				5.000	Calc
	🔊 🔺 🕀	4	🔶 🏟 SET 🛙			apture: 1. Chemical	I Looping: Calcin	er			x	r		
			~ ~ ~		2100.002.00		a zooping. oaion					' 00	100.0	75.00
			^	Tit	le	Unc	Value	Calc	Min	Max	Default	ne	None	100.0
GO2 Control GO2 Capture			Calciner Temp	perature (deg.)	C)		900.0		850.0	950.0	900.0			
□ 1. Chemic			Degree of Cal	cination (fraction	on)		0.9500	_	0.1000	0.9900	0.9500			
	ical Looping Diagra	am	CaCO3 Conve				8.415e-3		0.0	1.000	Calc			
	paration Diagram Recovery System Di	ianra												
	ical Looping Confid	_	Residence Tin				132.3	✓	50.00	500.0	Calc			
Chemi	ical Looping Coning	9												
Air Sep	paration Config	9	Gas Phase Pr				9.015e-2	v	0.0	5.000	Calc			
Air Sep Perform	paration Config mance	9	Gas Phase Pr Fraction of Gas	essure Drop ((bar)				0.0 0.0	5.000 1.000	Calc 0.6000			
Air Sep	paration Config mance nator	9	Fraction of Gas	essure Drop (s Recycling (fr	(bar)	eg. C)	9.015e-2							
Air Sep Perforn Carbor	paration Config mance nator er	-	Fraction of Gas Calciner Recy	essure Drop (s Recycling (fr	bar) action) Temperature (de		9.015e-2 0.6000		0.0 100.0	1.000 200.0	0.6000 120.0		am	
Air Sep Perforn Carbor Calcine	paration Config mance nator er	-	Fraction of Gas Calciner Recy	essure Drop (s Recycling (fr	bar) action) Femperature (de) GET	9.015e-2 0.6000 120.0 F RESULTS: C (tonne/hr)	02 Capture:	0.0 100.0	1.000 200.0	0.6000 120.0	ping Diagr	am roduct (tor	nne/hr)
Air Sep Perforn Carbor Calcine GET RESULTS: CO2 Capture: 1	paration Config mance nator er 1. Chemical Looping	-	Fraction of Gas Calciner Recyc	essure Drop (s Recycling (fr. cling Stream T	ibar) raction) Femperature (de) 🔿 GET	9.015e-2 0.6000 120.0 F RESULTS: C (tonne/hr)	O2 Capture: 2270 50.00	0.0 100.0	1.000 200.0	0.6000 120.0	ping Diagr		nne/hr)
Air Sep Perforn Carbor Calcine GET RESULTS: CO2 Capture: 1 A CO2 Capture Process Area Costs	paration Config mance nator er 1. Chemical Looping B Capital Cost	r: Cap	Fraction of Gas Calciner Recyc	essure Drop (s Recycling (fr cling Stream T nt Costs	bar) (action) Femperature (de X B Capital Cost) GET	9.015e-2 0.6000 120.0 F RESULTS: C (tonne/hr)	O2 Capture: 2270 50.00	0.0 100.0 1. Chemical	1.000 200.0 .ooping: C	0.6000 120.0 hemical Loo	ping Diagr		nne/hr)
Air Sep Perforn Carbor Calcine GET RESULTS: CO2 Capture: 1 A CO2 Capture Process Area Costs Carbonator	baration Config mance nator er 1. Chemical Looping B Capital Cost (\$/kW-net)	r: Cap	Fraction of Gas Calciner Recyn bital Cost A CO2 Capture Plan	essure Drop (s Recycling (fr cling Stream T nt Costs	bar) reaction) Femperature (de B Capital Cost (SrkW-net)) GET	9.015e-2 0.6000 120.0 F RESULTS: C (tonne/hr)	O2 Capture: 2270 50.00	0.0 100.0 1. Chemical	1.000 200.0 .ooping: C	0.6000 120.0 hemical Loo 5674	ping Diagr		une/hr)
Air Sep Perforn Carbor Calcine GET RESULTS: CO2 Capture: 1 A CO2 Capture Process Area Costs Carbonator Calciner	aration Config mance nator er 1. Chemical Looping Capital Cost (\$/kW-net) 501.1 279.9 233.8	r: Cap 1 2 F 3 C 4 F	Fraction of Gas Calciner Recytoital Cost A CO2 Capture Plan Process Facilities Capital General Facilities Capital Engineering & Home Offi	essure Drop (s Recycling (fr cling Stream T nt Costs ice Fees	bar) reaction) Femperature (de B Capital Cost (\$/kW-net) 1980 198.0 138.7) GET	9.015e-2 0.6000 120.0 F RESULTS: C (tonne/hr)	02 Capture: 2270 50.00	0.0 100.0 1. Chemical ich Sorbent (t emperature (d	1.000 200.0 .ooping: C onne/hr) eg. C)	0.6000 120.0 hemical Loo 5674 650.0	ping Diagr		ane/hr)
Air Sep Perforn Carbor Calcine GET RESULTS: CO2 Capture: 1 A CO2 Capture Process Area Costs Carbonator Calciner ASU Blowers	aration Config mance nator er 1. Chemical Looping Capital Cost (S'kW-net) 501.1 279.9 233.8 6.317	r: Cap 1 2 F 3 C 4 E 5 F	Fraction of Gas Calciner Recyt Dital Cost A CO2 Capture Plan CO2 Capture Plan Process Facilities Capital General Facilities Capital Engineering & Home Offi Process Contingency Cos	essure Drop (s Recycling (fr cling Stream T nt Costs ice Fees st	bar) reaction) Temperature (de B Capital Cost (\$/kW-net) 1980 198.0 138.7 438.3) GET	9.015e-2 0.6000 120.0 F RESULTS: C (tonne/hr)	02 Capture: 2270 50.00	0.0 100.0 1. Chemical	1.000 200.0 .ooping: C onne/hr) eg. C)	0.6000 120.0 hemical Loo 5674	ping Diagr		ine/hr)
Air Sep Perforn Carbon Carbon GET RESULTS: CO2 Capture: 1 A CO2 Capture Process Area Costs Carbonator Calciner ASU Blowers CO2 Product Compressor	aration Config mance nator er 1. Chemical Looping Capital Cost (\$'kW-net) 501.1 279.9 233.8 6.317 105.8	r: Cap 1 2 F 3 C 4 F 5 F 6 F	Fraction of Gas Calciner Recyt Dital Cost A CO2 Capture Plan Process Facilities Capital General Facilities Capital Engineering & Home Offi Process Contingency Cos Project Contingency Cost	essure Drop (s Recycling (fr cling Stream T nt Costs ice Fees st t	bar) remperature (de B Capital Cost (\$/kW-net) 1980 1980 198.0 138.7 438.3 516.7	GET Flue Gas Out (Temperature (c	9.015e-2 0.6000 120.0 T RESULTS: C (tonne/hr) (deg. C)	02 Capture:	0.0 100.0 1. Chemical ich Sorbent (t emperature (d	1.000 200.0 .cooping: C onne/hr) eg. C) nne/hr)	0.6000 120.0 hemical Loo 5674 650.0	ping Diagr	roduct (tor	
Air Sep Perforn Carbor Calcine GET RESULTS: CO2 Capture: 1 A CO2 Capture Process Area Costs Carbonator Calciner ASU Blowers CO2 Product Compressor CO2 Cryogenic Purification Unit	aration Config mance nator er 1. Chemical Looping Capital Cost (\$'kW-net) 501.1 279.9 233.8 6.317 105.8 236.7	1 2 3 4 5 5 6 7 7	Fraction of Gas Calciner Recyc bital Cost A CO2 Capture Plan CO2 Capture Plan CO2 Capture Plan Process Facilities Capital Engineering & Home Offi Process Contingency Cost interest Charges (AFUDO	essure Drop (s Recycling (fr cling Stream T nt Costs ice Fees st t	bar) action) Temperature (de B Capital Cost (5/kW-net) 1980 1980 1980 138.7 438.3 516.7 237.5	Flue Gas Out (Temperature (Steam	9.015e-2 0.6000 120.0 T RESULTS: C (tonne/hr) (deg. C) Carbonato	02 Capture:	0.0 100.0 1. Chemical ich Sorbent (t emperature (d fakeup LS (to	1.000 200.0 .ooping: C onne/hr) eg. C) nne/hr) conne/hr)	0.6000 120.0 hemical Loo 5674 650.0 185.5	ping Diagr		red
Air Sep Perforn Carbor Calcine GET RESULTS: CO2 Capture: 1 A CO2 Capture Process Area Costs Carbonator Calciner ASU Slowers CO2 Product Compressor CO2 Cryogenic Purification Unit Heat Recovery Steam Generator	Daration Config mance nator er 1. Chemical Looping Capital Cost (SrkW-net) 501.1 279.9 233.8 6.317 105.8 236.7 152.1	r: Cap 1 2 F 3 C 4 E 5 F 6 F 7 E 8 F	Fraction of Gas Calciner Recyc bital Cost A CO2 Capture Plan CO2 Capture Plan CO2 Capture Plan CO2 Capture Plan Process Facilities Capital Engineering & Home Offi Process Contingency Cost Project Contingency Cost interest Charges (AFUDO Royalty Fees	essure Drop (s Recycling (fr. cling Stream T nt Costs ice Fees st t C)	bar) reaction) remperature (def B Capital Cost (5/kW-net) 1980 198.0 199.0 19	GET Flue Gas Out (Temperature (c	9.015e-2 0.6000 120.0 T RESULTS: C (tonne/hr) (deg. C) Carbonato	02 Capture:	0.0 100.0 1. Chemical ich Sorbent (t emperature (d fakeup LS (to ean Sorbent (1.000 200.0 .ooping: C onne/hr) eg. C) nne/hr) conne/hr)	0.6000 120.0 hemical Loo 5674 650.0 185.5 4773	ping Diagr	oduct (tor	red
Air Sep Perforn Carbor Carbor Calcine GET RESULTS: CO2 Capture: 1 A CO2 Capture Process Area Costs Carbonator Calciner ASU Blowers CO2 Product Compressor CO2 Cryogenic Purification Unit Heat Recovery Steam Generator Coal Handling Equipment for ASU	Daration Config mance nator er 1. Chemical Looping Capital Cost (\$/kW-net) 501.1 279.9 233.8 6.317 105.8 236.7 152.1 76.45	r: Cap 1 2 F 3 C 4 F 5 F 6 F 7 F 8 F 9 F	Fraction of Gas Calciner Recyc bital Cost A CO2 Capture Plan CO2 Capture Plan CO2 Capture Plan Process Facilities Capital Engineering & Home Offi Process Contingency Cost interest Charges (AFUDO	essure Drop () s Recycling (fr cling Stream T nt Costs ice Fees st t c) Cost	bar) action) Temperature (de B Capital Cost (5/kW-net) 1980 1980 1980 138.7 438.3 516.7 237.5	Flue Gas Out (Temperature (Steam	9.015e-2 0.6000 120.0 T RESULTS: C (tonne/hr) (deg. C) Carbonato	02 Capture:	0.0 100.0 1. Chemical ich Sorbent (t emperature (d fakeup LS (to ean Sorbent (emperature (d	1.000 200.0 cooping: C onne/hr) eg. C) nne/hr) eg. C)	0.6000 120.0 hemical Loo 5674 6550.0 165.5 4773 900.0	ping Diagr	oduct (tor	red
Air Sep Perforn Carbon Carbon Carbon Carbonator Calciner A CO2 Capture Process Area Costs Carbonator Calciner ASU Blowers CO2 Product Compressor CO2 Cryogenic Purification Unit Heat Recovery Steam Generator Coal Handling Equipment for ASU Solids Handling Equipment	Daration Config mance nator er 1. Chemical Looping Capital Cost (\$'kW-net) 501.1 279.9 233.8 6.317 105.8 236.7 152.1 76.45 114.7	1 2 3 4 5 7 5 7 8 8 7 9 9 10 10	Fraction of Gas Calciner Recyc bital Cost A CO2 Capture Plan CO2 Capture Plan CO2 Capture Plan CO2 Capture Plan Process Facilities Capital Engineering & Home Offi Process Contingency Cost Project Contingency Cost Interest Charges (AFUDO Royalty Fees Preproduction (Startup) O	essure Drop (s Recycling (fr cling Stream T nt Costs ice Fees st t c) Cost cost	bar) reaction) remperature (de B Capital Cost (\$/kW-net) 1980 1980 1980 1980 138.7 438.3 516.7 237.5 9.904 83.74	Flue Gas Out (Temperature (Steam	9.015e-2 0.6000 120.0 T RESULTS: C (tonne/hr) (deg. C) Carbonato	02 Capture:	0.0 100.0 1. Chemical ich Sorbent (t emperature (d fakeup LS (to ean Sorbent (1.000 200.0 cooping: C onne/hr) eg. C) nne/hr) eg. C)	0.6000 120.0 hemical Loo 5674 650.0 185.5 4773	ping Diagr	oduct (tor	red
Air Sep Perform Carbor Calcine GET RESULTS: CO2 Capture: 1 A CO2 Capture Process Area Costs Carbonator Calciner ASU Blowers CO2 Product Compressor CO2 Cryogenic Purification Unit Heat Recovery Steam Generator CO2 Handling Equipment for ASU Solids Handling Equipment Steam Turbine for Power Generation	Daration Config mance nator er 1. Chemical Looping B Capital Cost (S'kW-net) 501.1 279.9 233.8 6.317 105.8 236.7 152.1 76.45 114.7 273.4 1980	1 2 3 4 5 5 7 4 5 7 4 8 7 10 11 11 12	Fraction of Gas Calciner Recyc bital Cost A CO2 Capture Plan CO2 Capture Plan CO2 Capture Plan Process Facilities Capital Engineering & Home Offi Process Contingency Cost Project Contingency Cost Project Contingency Cost Project Contingency Cost Project Contingency Cost Project Contingency Cost Project Contingency Cost Properties (AFUDO Royalty Fees Preproduction (Startup) C inventory (Working) Cap	essure Drop (s Recycling (fr cling Stream T nt Costs ice Fees st t c) Cost cost	bar) Femperature (de	Flue Gas Out (Temperature (Steam	9.015e-2 0.6000 120.0 T RESULTS: C (tonne/hr) (deg. C) Carbonato	02 Capture:	0.0 100.0 1. Chemical ich Sorbent (t emperature (d fakeup LS (to ean Sorbent (emperature (d	1.000 200.0 .ooping: C onne/hr) eg. C) onne/hr) eg. C) onne/hr)	0.6000 120.0 hemical Loo 5674 6550.0 165.5 4773 900.0	ping Diagr	oduct (tor	red
Air Sep Perforn Carbor Calcine GET RESULTS: CO2 Capture: 1 A CO2 Capture Process Area Costs Carbonator Calciner ASU	Daration Config mance nator er 1. Chemical Looping Capital Cost (\$/kW-net) 501.1 279.9 233.8 6.317 105.8 236.7 152.1 76.45 114.7 273.4 1980	1 2 3 4 5 5 7 10 8 8 9 9 7 10 11 12 13	Fraction of Gas Calciner Recyc bital Cost A CO2 Capture Plan CO2 Capture Plan CO2 Capture Plan Process Facilities Capital Engineering & Home Offi Process Contingency Cost Project Contingency Cost Project Contingency Cost Project Contingency Cost Project Contingency Cost Project Contingency Cost Project Contingency Cost Properties (AFUDO Royalty Fees Preproduction (Startup) C inventory (Working) Cap	essure Drop (s Recycling (fr cling Stream T nt Costs ice Fees st t c) Cost cost	bar) Femperature (de	Flue Gas Out (Temperature (Steam	9.015e-2 0.6000 120.0 F RESULTS: C (tonne/hr) deg. C)	02 Capture:	0.0 100.0 1. Chemical ich Sorbent (t emperature (d fakeup LS (to ean Sorbent (emperature (d olids Purge (t	1.000 200.0 .ooping: C onne/hr) eg. C) onne/hr) eg. C) onne/hr)	0.6000 120.0 hemical Loo 5674 650.0 165.5 4773 900.0	ping Diagr	oduct (tor	red
Air Sep Perform Carbor Calcine GET RESULTS: CO2 Capture: 1 A CO2 Capture Process Area Costs Carbonator Calciner ASU Blowers CO2 Product Compressor CO2 Product Compressor CO2 Product Compressor CO2 Product Compressor CO2 Product Compressor CO2 Cryogenic Purification Unit Heat Recovery Steam Generator COal Handling Equipment for ASU Solids Handling Equipment Steam Turbine for Power Generation	Daration Config mance nator er 1. Chemical Looping Capital Cost (\$'kW-net) 501.1 279.9 233.8 6.317 105.8 236.7 152.1 76.45 114.7 273.4 1980	1 2 3 4 5 5 7 4 5 7 4 8 7 10 11 11 12	Fraction of Gas Calciner Recyc bital Cost A CO2 Capture Plan CO2 Capture Plan CO2 Capture Plan Process Facilities Capital Engineering & Home Offi Process Contingency Cost interest Charges (AFUDO Royalty Fees Preproduction (Startup) C inventory (Working) Cap	essure Drop (s Recycling (fr cling Stream T nt Costs ice Fees st t c) Cost cost	bar) Femperature (de	GET Flue Gas Out (Temperature (c Steam Generator	9.015e-2 0.6000 120.0 F RESULTS: C (tonne/hr) deg. C) Carbonato	02 Capture:	0.0 100.0 1. Chemical ich Sorbent (t emperature (d fakeup LS (to ean Sorbent (emperature (d olids Purge (t	1.000 200.0 .ooping: C onne/hr) eg. C) onne/hr) eg. C) onne/hr)	0.6000 120.0 hemical Loo 5674 650.0 165.5 4773 900.0	ping Diagr	oduct (tor	red

Oxy-Combustion Process Model

- New detailed models for performance and cost of:
 - Air separation unit (ASU)
 - Direct contact cooler/polishing scrubber(DCC/PS)
 - Carbon Processing Unit (CPU)
 - System integration (overall mass & energy balances)

Three system configurations (High/med/low %S; cool or warm recycle)

Configuration:	Oxyfuel High S (>1.5%) 💌	•
Combustion C	ontrols	
Fuel Type:	Coal	
NOx Control:	In-Furnace Controls	SSI / Recycle
Post-Combust	ion Controls	
NOx Control:	None 💌	
Particulates:	Fabric Filter	
SO2 Control:	Wet FGD 💌	T T T T T T T T T T T T T T T T T T T
Mercury:	None 💌	to Atm.
CO2 Capture:	Oxyfuel High S (>1.5%) 💌	
		Storage
Water and Sol	ids Management	
Cooling System:	Wet Cooling Tower	

Oxy-Combustion Process Model

- New detailed models for performance and cost of:
 - Air separation unit (ASU)
 - Direct contact cooler/polishing scrubber(DCC/PS)
 - Carbon Processing Unit (CPU)
 - System integration (overall mass & energy balances)

Three system configurations (High/med/low %S; cool or warm recycle)

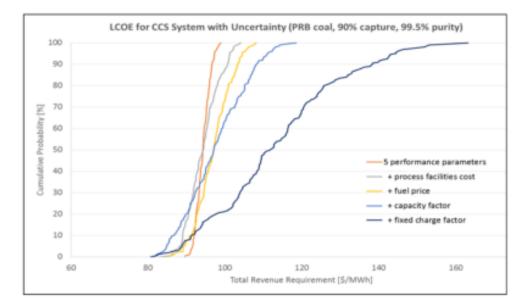
Configuratio	n: Oxyfuel High S (>1.5%) 💌	•
Configuration:	Oxyfuel Med S (0.5%-1.5	
Combustion C	Controls	
Fuel Type:	Coal	
NOx Control:	In-Furnace Controls	Recycle
Post-Combust	tion Controls	
NOx Control:	None	
Particulates:	Fabric Filter 💌	
SO2 Control:	Lime Spray Dryer	
Mercury:	None 💌	to Atm.
CO2 Capture:	Oxyfuel Med S (0.5%-1.5 -	📥 📩 📩
	_	Storage
Water and So	lids Management	
Cooling System:	Wet Cooling Tower	

Oxy-Combustion Process Model

- New detailed models for performance and cost of:
 - □ Air separation unit (ASU)
 - Direct contact cooler/polishing scrubber(DCC/PS)
 - Carbon Processing Unit (CPU)
 - System integration (overall mass & energy balances)
- Three system configurations (High/med/low %S; cool or warm recycle)

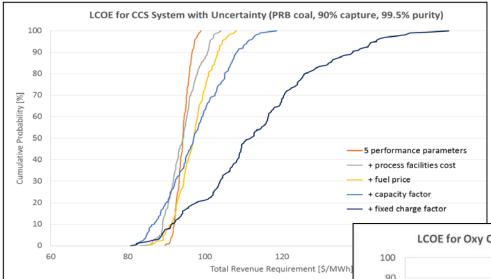
Configu	uration: Oxyfuel High S (>1.5%)	
Configurati	ion: Oxyfuel Med S (0.5%-1.5	
Configuration:	Oxyfuel Low S (<0.5%)	
Combustion C	Controls	
Fuel Type:	Coal	
NOx Control:	In-Furnace Controls 🔻	
	,	Recycle
Post-Combust	tion Controls	
NOx Control:	None	
Particulates:	Fabric Filter 💌	
SO2 Control:	Lime Spray Dryer 💌	
Mercury:	None	to Ătm. 🍟
CO2 Capture:	Oxyfuel Low S (<0.5%) 🔻	
	,	Storage
Water and So	lids Management	
Cooling System:	Wet Cooling Tower	

Oxy-Combustion Process Model: Examples of uncertainty analysis, LCOE



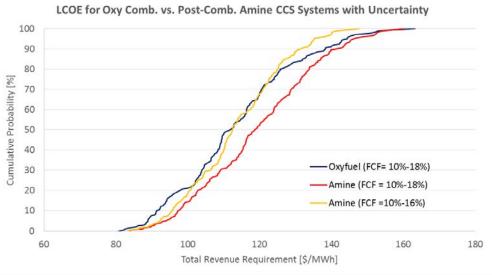
Decomposition of probability distribution function to show contributions from different sources of uncertainty

Oxy-Combustion Process Model: Examples of uncertainty analysis, LCOE



Decomposition of probability distribution function to show contributions from different sources of uncertainty

Comparative analysis of oxyvs. post-combustion CCS for two uncertainty ranges of FCF for amine-based system

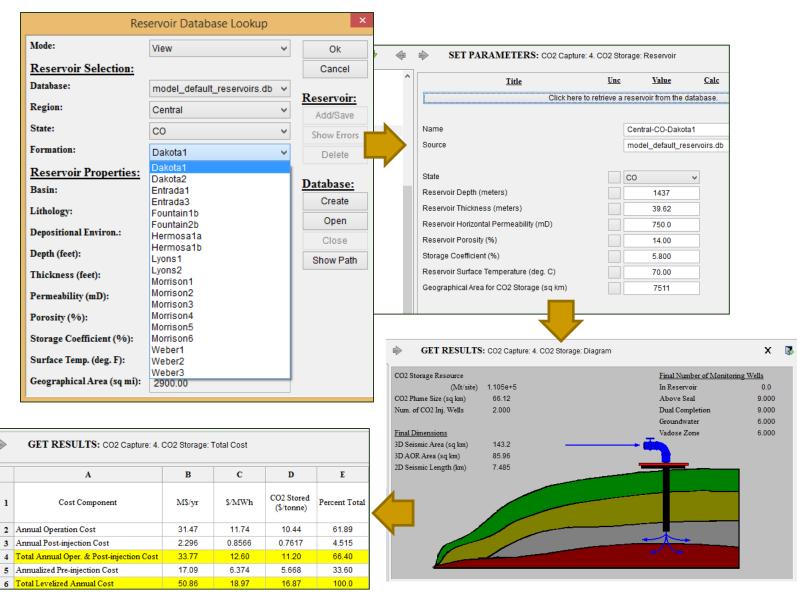


CO₂ Storage Cost Model

 Detailed site-specific models and geological database developed by DOE/NETL are now in IECM v.9.0

Edit Go Help		
E 🖻 🖹 🛧 🦊 🤿 🖈	SET PARAMETERS: CO2 Capture: 4. CO2 Storage: Pe	erformance
Performance Regulations & Taxes	^ <u>Title</u>	<u>Unc Value Calc</u>
Financing	Performance Model	Law & Bachu 🗸
Fuel Cost O&M Cost	Project Average Injection Rate (Mt CO2/yr)	Advanced Research Ir
Reference Plant	Design Maximum Injection Rate per Well (Mt CO2/y	r) 3.768 🗸
Fuel		
🗄 Base Plant	Manifestine Well Describe	
NOx Control	Monitoring Well Density	
TSP Control	Wells in Reservoir (sq km/well)	10.36
SO2 Control	Wells Above Seal (sq km/well)	5.180
CO2 Capture		5.180
	Wells that are Dual Completed (sq km/well)	10.36
∃ 3. Pipeline Transport	Wells Groundwater (Wells/Inj. Well)	3.000
4. CO2 Storage	Wells Vadose Zone (Wells/Inj. Well)	
CO2 Storage Diagram Financing	wens vadose zone (wenshinj. wen)	3.000
Reservoir	Dual Completed Wells in Reservoir (%)	100.0
Performance		
Pre-injection Cost	Maraina	
Operations Cost	Margins	
Post-injection Cost	AOR Margin 3D (% of Plume)	30.00
Water Systems		
By Brod Mamt		

CO₂ Storage Cost Model



Future Developments

New Process Models Nearing Completion

- Advanced membranes system (post-combustion)
- Ionic liquid systems (pre- and post-combustion)
- Metal organic framework systems (post-combustion)
- Carbon-based sorbent systems (post-combustion)
- Other solid sorbent systems (post-combustion)
- Enhanced water-gas shift reactor (pre-combustion)
- Hybrid water cooling systems (wet/dry)
- Life cycle analysis capability

Visit: www.iecm-online.com

Welcome to the

Carnegie Mellon Integrated Environmental Control Model



Home «

Download IECM

Video Tutorials

About IECM Documentation **IECM Publications** Other Publications People Links Contact Us

A tool for calculating the performance, emissions, and cost of a fossil-fueled power plant

Developed by

Carnegie Mellon University (CMU) Department of Engineering & Public Policy (EPP)

With Support from

United States Department of Energy's National Energy Technology Laboratory (NETL)

Contact us if you have questions or comments.

Thank You

rubin@cmu.edu