

Liquid Fuels and Electricity from IT-Fuel Cells

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Project Objective:

To develop a cell technology capable of direct conversion of methane to liquid product, methanol or formaldehyde, by electrochemical partial oxidation at intermediate temperatures (<500°C), to provide means for an economic utilization of stranded gas.



Value Proposition





Western ND

Population ~100,000



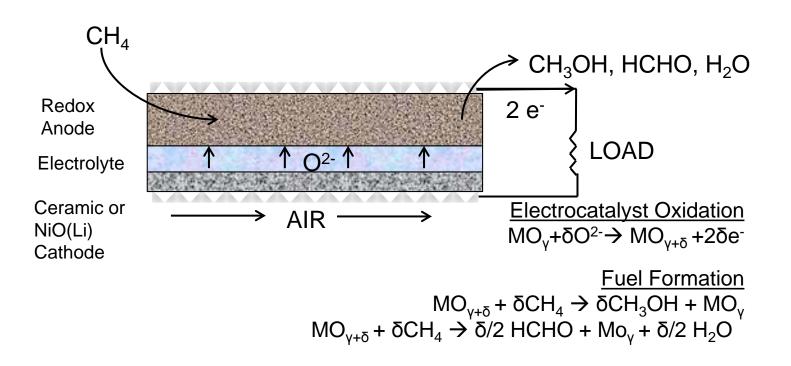
Eastern NY, CT, MA & RI Population ~25,000,000

Satellite image of visible light sources in US, demonstrating level of natural gas flaring Image – NASA Earth Observatory

- Electrochemical Gas-to-Liquid (EC-GTL) offers a cost effective method for reducing emissions impact of stranded gas sources
- Scalability, modular nature, and transportability of electrochemical system also provide the means to economically utilize associated gas at low production wellheads
- The EC-GTL technology will meet ARPA-E's Mission Areas:
 - Enhance the economic and energy security of the United States
 - Ensure that the United States maintains a technological lead in developing and deploying advanced energy technologies







Electrochemical Gas-to-liquid cell utilizes a metal/metal oxide redox couple, which serves as the anode electrocatalyst, to partially and indirectly oxidize CH_4 to CH_3OH and HCHO.



- University of Connecticut Cell manufacturing technology development
- Pacific Northwest National Laboratory GTL catalyst development
- Energy and Environmental Research Center at the University of North Dakota – GTL catalyst evaluation and pressurized testing
- Massachusetts Institute of Technology Electrode interface characterization



Massachusetts Institute of Technology



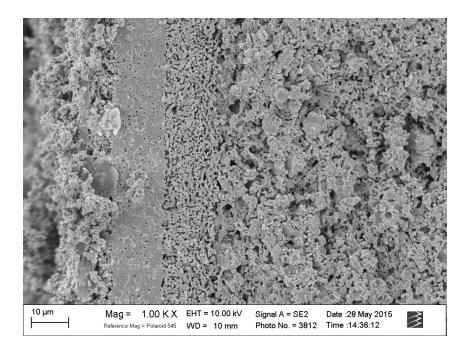






Development Approach

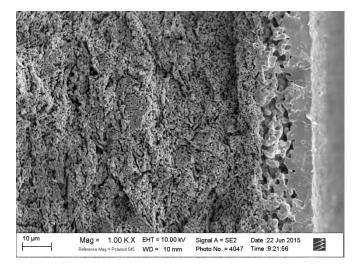
- Development of a novel EC-GTL cell presents an opportunity for top-down approach
- Incorporation of the catalyst within the EC-GTL anode requires ability to withstand constant redox cycling
- Chosen cathode and electrolyte must provide sufficient electrode activity and O²⁻ ionic conductivity to support the Redox reaction with the EC-GTL anode
- Institutional experience with MCFC commercialization can be leveraged to facilitate pathway to commercialization



SEM micrograph of potential EC-GTL cell under development at FCE



Cell Materials - Support



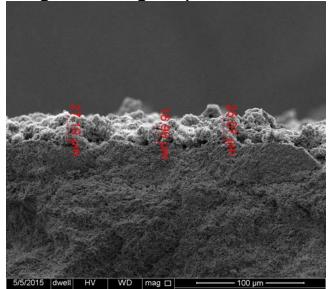
SEM micrograph of ceramic anode support with functional layer and electrolyte

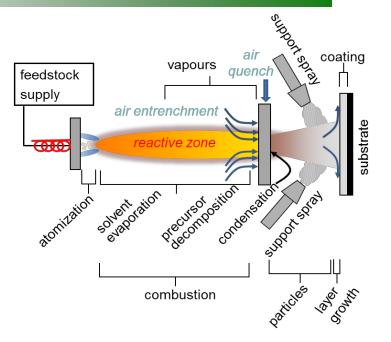
- Initial investigation focused on modified NiO as cathode side support, including production line MCFC cathode, but was found to have insufficient mechanical strength
- Anode side ceramic support was chosen, with desirable conductivity and mechanical properties



Cell Manufacturing

- To reduce future cell cost and streamline commercialization, advanced manufacturing techniques, that can be readily scaled to high volume are being investigated as primary source of laboratory sample testing
- Reactive Spray Deposition Technology (RSDT) is employed to produce cell functional layers, in both porous and dense forms, with minimal to no post deposition processing/sintering required





Economically viable RSDT for fabrication of the EC-GTL cell components and thin film layers



GTL Catalyst Development

- Development of GTL catalyst that favors the production of methanol/al with high selectivity as opposed to reformation to hydrogen
- Catalyst selection using candidate materials tested in batch-reactor mode
- Over twenty catalyst compositions have been evaluated, with multiple promising candidates identified
- Promising catalysts, based on selectivity and activity in ideal cell operation range, to be incorporated into button cells, then large area anodes

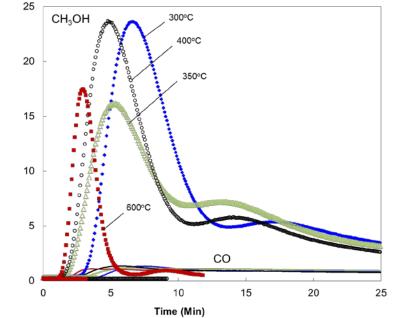


Batch mode reactor for catalyst evaluation.





GTL Catalyst Development



Catalyst screening has identified candidates with promising selectivity over desired range of temperatures

- Less than 1% CO observed, no CO₂
 - >90% Selectivity up to 600 °C

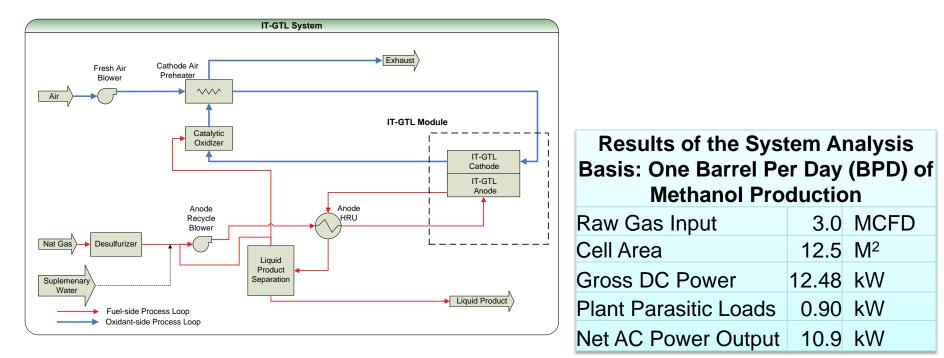
Continued development will focus on increased activity and conversion, while preserving selectivity





EC-GTL System Modeling

- System Process Flow Sheet Identifying the balance-of-plant processing requirements developed
- Performed system simulations based on thermodynamics first principle methods
- Focus on low-volume (~100 MCFD) associated gas systems
- Cost estimate based on prior fuel cell system development





EC-GTL System Cost

PILOT EC-GTL SYSTEM ANNUAL OPERATING COST

Case Study for 40 BPD Plant

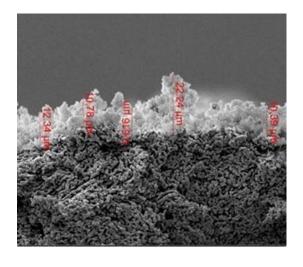
- Cell performance assumptions based on end of project milestones
- Equipment and Stack cost estimated based on SOFC systems of comparable scale
- Gas composition based on Bakken associated gas

ANNUAL OPERATING COST ITEMS							
	FUEL CELL STACK REPLACEMNT(3 RPLCMNTS)				\$	11,459	
FUE	L (FLAR	ED GAS)					0
	· ·	,	10% UNIT C	OST)	\$	29,883	
SYS	TEM OP	ERATION(C	D&M)				
	2 TECHS ,\$50/HR, 2200HR/YR)				\$	220,000	
				TOTAL	\$	261,342	
ANNUAL REVEN	UES						
POWER SALE (486.4 KW) (6 CENTS/KWHR)					\$	229,050	
MET	HANOL	SALES (1.1	4GPM)(\$1.3	3/GAL)	\$	716,909	
				TOTAL	\$	945,959	
ANNUAL COST							
ANN COS		D CAPITAL	@ 8%		\$	173,000	
ANNUAL OPERATING COST				\$	261,342		
	ANNUALIZED INSTALLATION COST				\$	153,000	
				TOTAL	\$	587,342	
			ANNUAL				
PAYBACK PERIOD, YRS			COST/REVENUES			0.	62
RATE OF RETURN,%		ANNUAL REVENUES -			21	%	
	ANNUAL COST/INITIAL COST						





- Material selection parallel path development of multiple cell designs show promise to meet project performance milestones
- Fabrication RSDT parameters have been refined to new material sets to deposit layers with desired characteristics
- Catalyst development Multiple catalysts have shown very high selectivity to desired products
- System analysis has shown the EC-GTL has the potential of co-generating 10 kw net electricity while producing one Barrel of methanol per day (BPD), with promising economics



RSDT Fabricated Anode Functional Layer for EC-GTL cell



- Continued development of GTL catalyst
- Incorporation of GTL catalyst to anode layer for electrochemical evaluation
- Continued fabrication development of RSDT for materials
- Refined Techno-economic analysis with actual cell performance





- DOE/ARPA-E: Ping Liu, John Lemmon, John Tuttle, Mark Pouy
- PNNL: Olga A. Marina
- EERC: Ted Aulich
- UCONN: Radenka Maric, Mark Aindow, Na Li
- MIT: Bilge Yildiz
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