



Integrating the PNNL SOFC Multi-Physics Model into the NETL Aspen System Model as a Reduced Order Model

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Outline



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Motivation



PROBLEM STATEMENT: NETL analysis of SOFC systems is limited to what can be described as a "black box" SOFC module within the current Aspen system model

- Consists of two reactors w/ heat and oxygen transfer
- Limited input/output
- Specific overpotential estimates
- Limited optimization from a system perspective

OBJECTIVE: To improve the accuracy and capability of NETL's Aspen-based SOFC system analyses

Produce a variety of optimization and what-if studies to guide the SOFC program

Motivation



SOLUTION: Integrate the PNNL SOFC-MP model into NETL's system model as a reduced-order model (ROM) to replace the current "black box" approach to:

- Increase the accuracy of SOA SOFC analysis
- Reduce computational time and complexity versus full model
- Allow for additional optimization studies (COE, etc.)
- Allow for the ease of incorporation of other models
 - Such as degradation models, etc.
- Facilitate development of a high fidelity SOFC tool for system analysis
 - An NETL/DOE/PNNL vision
 - SOFC industry team use



- SOFC-MP 2D is a numerical model for the efficient computation of parameters in planar SOFC stacks
 - Current density
 - Species concentration
 - Temperature distributions

• Capabilities

- Co- or counter-flow geometry
- Mixed fuel compositions (H_2 , H_2O , CO, CO_2 , CH_4 , N_2)
- User-defined electrochemistry and CH₄ reforming models
- Analysis of large area cells, multi-cell stacks
- Calibrated with state-of-the-art SOFC performance data from industry



SOFC ROM Generation





- Initial SOFC ROM generation was completed by PNNL
 - ROM generation had to be constrained to cover only limited SOFC scenarios with a small range of validity to get viable data points
 - Fixed inlet gas composition (natural gas)
 - Fixed fraction of pre-reforming
 - Counter-flow SOFC configuration w/ no heat loss
 - Single cell at atmospheric conditions
 - ROM validated against full model to be consistent with SOA SOFC technology
 - The accuracy of the ROM was verified by extensive error analysis by PNNL, with key metrics having error of < 3%

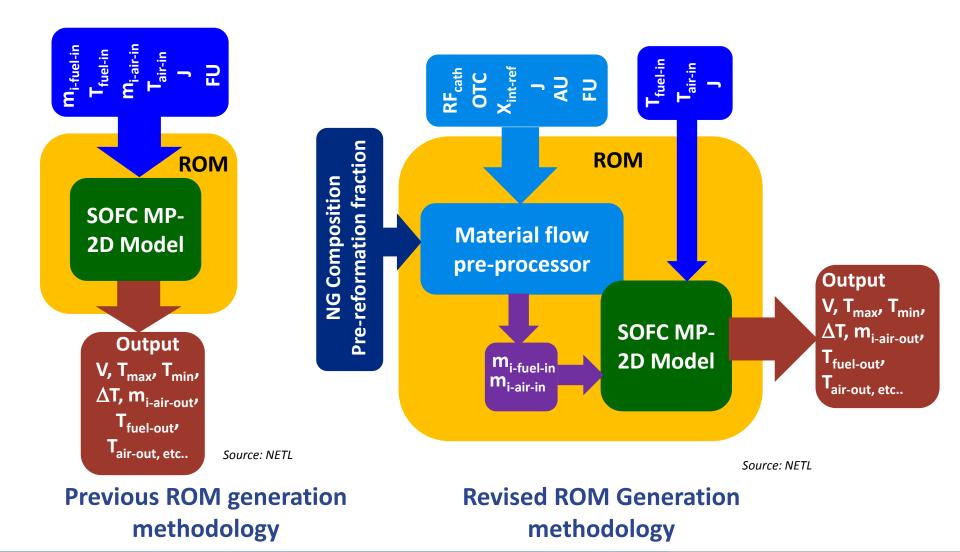


- Methodology used for ROM generation
 - A spreadsheet material flow model developed for an NGFC system was integrated into the ROM generation process
 - The spreadsheet model ensured that the inputs to the SOFC MP 2D model were physically consistent resulting in an efficient ROM

| ROM Input Parameters | Salient ROM Output Parameters |
|--|---|
| Average current density (J) | Cell voltage (V) |
| Fuel utilization (FU) | Cell temperature profile (T _{max} , T _{min} , and Δ T) |
| Inlet NG composition (FIXED) | Stack air outlet conditions |
| Inlet air composition | Air outlet temperature (T _{air-out}) |
| Fuel inlet temperature (T _{fuel-in}) | Species (N ₂ , O ₂ , Ar, CO ₂ , H ₂ O) mole flows (m _{i-air-out}) |
| Air inlet temperature (T _{air-in}) | Stack fuel outlet conditions |
| Anode inlet gas oxygen to carbon ratio (OTC) | Fuel outlet temperature (T _{fuel-out}) |
| Cathode gas recirculation fraction (RF _{cath}) | Species (CH ₄ , H ₂ , CO, H ₂ O, CO ₂ ,N ₂) mole flows (m _{i-fuel-out}) |
| Internal reformation fraction (X _{int-ref}) | Current density profile (J _{max} , J _{min} , J _{avg}) |
| Air utilization (AU) | |

Current Status Overview SOFC ROM Generation





ENERGY National Energy Technology Laboratory



- PNNL generated ROM based on the revised methodology
 - Supplied ranges for the new input parameters identified
 - SOFC electrochemical model calibrated to SOA SOFC technology was used
 - NG composition is the same as used in the Bituminous Baseline NGCC cases [1]
 - The methane pre-reformation fraction was set to 20 percent (to completely reform higher hydrocarbons, a typical value)

| ROM Input Parameters | Ranges |
|--|--|
| Average current density (J) | 2000 – 6000 A/m ² |
| Fuel utilization (FU) | 0.4 – 0.95 |
| Inlet NG composition | Fixed (as in Bituminous Baseline NGCC Cases) |
| Inlet air composition | Fixed: Standard air (Midwest ISO) |
| Fuel inlet temperature (T _{fuel-in}) | 550 – 800 °C |
| Air inlet temperature (T _{air-in}) | 550 – 800 °C |
| Anode inlet gas oxygen to carbon ratio (OTC) | 1.5 - 3.0 |
| Cathode gas recirculation fraction (RF _{cath}) | 0.0-0.8 |
| Air utilization (AU) | 0.125 – 0.833 |
| Internal reformation fraction (X _{int-ref}) | 0.0 - 1.0 |





Integration of SOFC ROM into Aspen System Model





- Integration of ROM into system model:
 - The outputs of the ROM integrated into Aspen were checked against ROM output values generated independently (non-Aspen) using the same input parameter values
 - The airflow, air inlet temperature, fuel outlet temperature, and cell voltage resulting from the routine were specified in the Aspen model
 - The air outlet temperature calculated by the Aspen model was checked against the value of air outlet temperature calculated using the ROM to confirm consistency of energy flows between the models
 - Aspen and ROM species mole flows were confirmed and checked for consistency

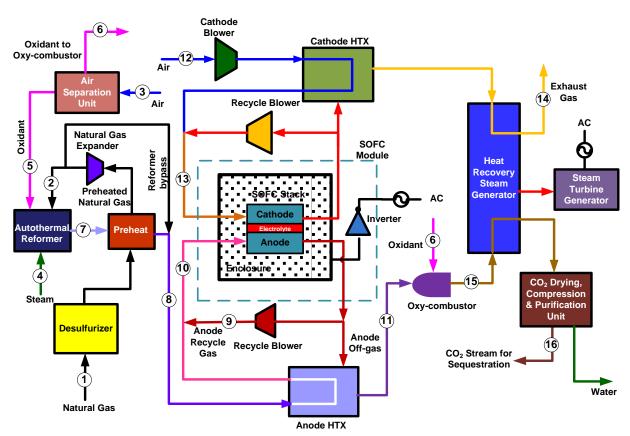


- PNNL generated ROM was integrated into the Aspen model of an NGFC utility-scale system
 - ROM translation FORTRAN routine is hardwired as a calculation block in the Aspen model
 - PNNL supplied ROM translation routine was modified to seek minimum air flow rate and air inlet temperature combination for a specified cell $T_{\rm MAX}$ and cell ΔT
 - Export/import links to key parameters in the Aspen file established
 - Needs external FORTRAN compiler configured to run with Aspen

Current Status Overview SOFC ROM Integration

NETL

- NGFC System with CCS
 - 550 MWe
 - Atmospheric SOFC
 - Auto-thermal O₂
 blown reformer
 - Steam bottoming cycle
 - Oxy-combustor
 - Cryogenic ASU provides O₂
 - CO₂ purification unit with autorefrigeration



Source: NETL



- Two sample NGFC cases considered to demonstrate ROM Integration
 - ROM Case 1 conditions were based on NGFC Case 1-2 [1], which represents
 SOA technology operating under high fuel utilization conditions
 - ROM Case 2 conditions were chosen to be generally reflective of typical operating conditions for SOA technology

| Parameters | Measurement | Case 1-2 NGFC Study (not ROM based) | ROM Based Case 1 | ROM Based SOA Case 2 | |
|------------------------------------|--------------------|---|---------------------|-------------------------|--|
| Average current density | mA/cm ² | | 400 | | |
| Fuel utilization | | 0.9 | | 0.8 | |
| Cell maximum temperature | | 750 | 750 | 775 | |
| Cell ∆T | °C | 100 | 100 | 75 | |
| Fuel inlet temperature | L | 650 | 627 | 688.5 | |
| Air inlet temperature | | 650 | 550 | 550 | |
| Oxygen to carbon ratio | | 2.6 2.1 | | | |
| Cathode gas recirculation fraction | | 0.5 | | | |
| Air stoichs (Air utilization) | | 2.9 (0.345) | 3.61 (0.277) | 4.34 (0.230) | |
| Internal reformation fraction | | | 0.6 | | |



 1. NETL - National Energy Technology Laboratory. " Cost and Performance Baseline for Fossil Energy Plants Volume 1: Bituminous Coal and Natural Gas to Electricity, "Revision 2a, DOE/NETL -2010/1397, September 2013.

Current Status Overview SOFC ROM Integration



- The outputs of the ROM runs within Aspen were confirmed to be identical to stand-alone ROM runs with the same input parameters
- The air outlet temperature was calculated using Aspen and was found to be nearly the same value as that predicted by the ROM
 - Confirms consistency of energy flows and heat balance between the ROM and Aspen model

| Parameters | Unit | ROM Based Case 1 | | ROM Based SOA Case 2 | |
|--------------------------|--------------------|------------------|----------|----------------------|----------|
| | | Aspen | External | Aspen | External |
| Cell voltage | V | 0.788 | 0.788 | 0.844 | 0.844 |
| Cell average temperature | °C | 729.0 | 729.0 | 700.0 | 700.0 |
| Cell max temperature | °C | 750.0 | 750.0 | 775.4 | 775.4 |
| Cell min temperature | °C | 649.5 | 649.5 | 700.0 | 700.0 |
| Cell ∆T | °C | 100.5 | 100.5 | 75.4 | 75.4 |
| Fuel outlet temperature | °C | 687.0 | 687.0 | 727.5 | 727.5 |
| Air outlet temperature | °C | 739.4 | 739.6 | 757.3 | 757.5 |
| Max current density | | 568.8 | 568.8 | 499.1 | 499.1 |
| Min current density | mA/cm ² | 205.5 | 205.5 | 218.9 | 218.9 |



Current Status Overview SOFC ROM Integration



- The stack fuel and air inlet flows in the Aspen model were compared to the corresponding flows used in the SOFC-MP model for the same ROM input parameters
 - The flows were found to be the same within practical limits
 - Serves a check of the consistency of flows between the material flow preprocessor of the ROM and the Aspen model

| Parameters | ROM Based Case 1 | | ROM Based SOA Case 2 | |
|-----------------------------------|------------------|---------|----------------------|---------|
| | Aspen | SOFC-MP | Aspen | SOFC-MP |
| Air inlet species mole-fractions | | | | |
| 0 ₂ | 0.1842 | 0.1842 | 0.1883 | 0.1883 |
| N ₂ | 0.7950 | 0.7951 | 0.7911 | 0.7911 |
| Ar | 0.0096 | 0.0097 | 0.0096 | 0.0096 |
| Fuel inlet species mole-fractions | | | | |
| H ₂ | 0.2384 | 0.2409 | 0.3263 | 0.3297 |
| СО | 0.0856 | 0.0831 | 0.1170 | 0.1140 |
| CH4 | 0.0639 | 0.0639 | 0.0827 | 0.0828 |
| H ₂ O | 0.4169 | 0.4145 | 0.3175 | 0.314 |
| CO ₂ | 0.1896 | 0.1922 | 0.1508 | 0.1542 |

Current Status Overview

SOFC ROM Integration



| Parameters | Measurement | Case 1-2 NGFC Study (not ROM based) | ROM Based Case 1 | ROM Based SOA Case 2 | |
|--------------------------------|---------------------------|--|---------------------|-------------------------|--|
| Internal Reformation Fraction | % | | | | |
| Average Current Density | mA/cm ² | <u> </u> | | | |
| Fuel Utilization | in Aveni | 90 8 | | | |
| Cell Maximum Temperature | | 750 | 750 | 775 | |
| Cell DT | | 100 | 100 | 75 | |
| Oxygen to Carbon Ratio | - ! | 2.6 | | 2.1 | |
| Air Stoichs | | 2.9 | 3.61 | 4.34 | |
| Cell Voltage | N | 0.791 | 0.788 | 0.844 | |
| Inlet Nernst Voltage | V | 0.941 | 0.958 | 0.966 | |
| In Stack Fuel Utilization | % | 80 | 80 | 69 | |
| Plant Output | | | | | |
| SOFC Power | | 525,700 | 516,708 | 515,495 | |
| Natural Gas Expander Power | kWe | 18,400 | 18,200 | 19,000 | |
| Steam Turbine Power | күүе | 79,000 | 78,300 | 89,000 | |
| Fotal Gross Power | | 623,100 | 613,208 | 623,495 | |
| Auxiliary Load | | | | | |
| ASU Auxiliaries | | 321 | 318 | 464 | |
| ASU Main Air Compressor | | 15,090 | 14,680 | 21,460 | |
| CO ₂ Compressor | | 18,570 | 22,451 | 23,535 | |
| CO ₂ Refrigeration | | 14,499 | 0 | 0 | |
| Boiler Feedwater Pumps | | 1,371 | 1,359 | 1,545 | |
| Condensate Pump | | 102 | 101 | 115 | |
| Circulating Water Pump | | 2,090 | 2,180 | 2,400 | |
| Cooling Tower Fans | | 1,080 | 1,120 | 1,240 | |
| Steam Turbine Auxiliaries | kWe | 33 | 33 | 37 | |
| Cathode Air Blower | | 7,610 | 8,222 | 9,224 | |
| Cathode Recycle Blower | | 7.690 | 8,273 | 9.541 | |
| Anode Recycle Blower | | 2,110 | 1,955 | 1,368 | |
| Viscellaneous Balance of Plant | | 398 | 394 | 413 | |
| Fransformer Losses | | 2.070 | 2,011 | 2,072 | |
| Total Auxiliary Load | | 73,035 | 63.097 | 73.414 | |
| Net Plant Power | | 550.065 | 550,111 | 550,081 | |
| Net Plant Efficiency (HHV) | % | 55.9* | 56.5 | 53.9 | |
| Net Plant Heat Rate (HHV) | kJ/kWhr (Btu/kWhr) | 6,441 (6,105) | 6,372 (6,039) | 6,681 (6,332) | |
| Condenser Duty | GJ/hr (MMBtu/hr) | 464 (440) | 454 (430) | 517 (490) | |
| Natural Gas Feed Flowrate | kg/hr (lb/hr) | 67,551 (148,925) | 66,828 (147,330) | 70,069 (154,475) | |
| Thermal Input | kWth | 984,164 | 973,623 | 1,020,841 | |
| Raw Water Consumption | m ³ /min (gpm) | 4.1 (1,071) | 4.29 (1,132.4) | 4.84 (1,278.1) | |



National Energy Technology Laboratory * The NGFC case 1-2 uses externally refrigerated CPU unlike the ROM based cases, which use autorefrigerated CPU; the HHV efficiency of the case 1-2 can be projected to be ~57.4% (1.5 percentage points higher than listed) if an autorefrigerated CPU was employed.



Conclusions





- Developed a methodology for ROM generation
 - Results in an efficient ROM generation process
 - The resultant ROM input parameters closely mimic the design and operational parameters of a typical SOFC system
 - Enables the ultimate vision of the development of a tool that is useful for SOFC system calculations since the methodology can be extended to ROM representation of high fidelity SOFC-MP 3D models
- Successfully generated a ROM based on the revised methodology
 - Utilized the SOFC electrochemical model that was calibrated to be consistent with SOA SOFC technology
 - Range of input parameters covered the gamut of values encountered in a typical NGFC system
 - The accuracy of the ROM was verified by extensive error analysis and was found to be acceptable (<3%) for the key parameters



- The ROM was successfully into the Aspen model of NGFC system
 - The outputs of the ROM integrated into Aspen were checked against ROM outputs values generated independently (external to Aspen) using the same input parameter values
 - A routine that iterated the ROM calculations to find the lowest air flow and the corresponding air inlet temperature for specified values of cell maximum temperature and cell ΔT was developed
 - Aspen and ROM species mole flows were confirmed and checked for consistency
 - Two sample NGFC cases were analyzed using the ROM based and compared to a previous NGFC case



- The next phase of the ROM development will focus on:
 - Modifications to the SOFC-MP 2D model to include:
 - Cathode and anode recirculation
 - Cathode and anode heat exchangers representations
 - Pre-reformer routine
 - Pressure drop calculations
 - Extension to other fuel compositions
 - Other natural gas compositions
 - Syngas compositions (for IGFC system analyses)
 - Extension to pressurized SOFC operation
 - Inclusion of cross-flow SOFC configuration



- The next step of ROM integration into the Aspen system model is to develop a custom user SOFC model based on the ROM that can be easily called within the Aspen model
 - Enables ROM customization without affecting the Aspen model
 - Enables user-friendliness and portability of the ROM model
- Application of the ROM integrated Aspen model to different systems-level optimization
 - COE, based on voltage/current operating point
 - Re-visitation of SOFC pathway based on new capability and accurate SOA analysis
 - Guide SOFC program with meaningful and achievable goals, such as a reduction in ASR rather than overpotential

Acknowledgments



- Arun Iyengar, Booz Allen Hamilton
- Brian Koeppel and Kevin Lai, PNNL
- Dale Keairns, BAH
- Briggs White, NETL
- Travis Shultz, NETL
- Heather Quedenfeld, NETL
- Shailesh Vora, NETL

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