Pilot Plant Testing of Piperazine (PZ) with High T Regeneration

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Objective is to demonstrate PZ with advanced regeneration at 150°C in coal-fired flue gas



Phased testing at UT SRP and NCCC to optimize PZ absorption/regeneration



Budget Period 1

\$1.65 M Federal Share\$0.92 M Cost Share\$ 2.57 M Total BP1

Cost share by CO₂ Capture Pilot Plant Project (C2P3)



5m Piperazine is a Superior Solvent

Solubility Window for 5 m & 8 m PZ



Piperazine: Superior Energy Performance

Amine	m	kg'avg*1e7	μ	ΔC_{μ}	T _{max}
		mol/s·Pa·m ²	сР	mol/kg	С
PZ	8	8.5	11	0.84	163
	5	11.3	4	0.81	163
AMP/PZ	4_2	8.6	5	0.90	128
MEA	7	4.3	3	0.67	121
MDEA/PZ	5_5	8.5	13	0.91	117

Absorber Performance

40°C Intercooling

	5 m PZ	8 m PZ
Lean Ldg at solid limit (mol CO ₂ /mol alk)	0.22	0.26
Rich Loading (mol CO₂/mol alk.)	0.40	0.40
L/G (mol/mol)	3.03	2.55
Equivalent Work (kJ/mol CO ₂)	36.0	36.3
Packing Required (m ² /mol CO ₂)	126	298

PZ: superior solvent management

Resistant to oxidation

• Cyclic : PZ (160C)) = 1.3 MEA (120C) = 4.7 mM/hr

Volatility just right

- At lean absorber: PZ = 8 MEA=30 ppm
- Thermal reclaiming removes nonvolatile impurities
- PZ & MEA may condense out as aerosols in absorber

Nitrosamine manageable

- $PZ + NO_2/NO_2^- \rightarrow mononitrosopiperazine (MNPZ)$
- Decomposes at 150°C giving 1 mM MNPZ at SS

The Advanced Flash Stripper (AFS) minimizes Energy Use and Capital Cost.

Irreversibility of simple stripper using 5 m PZ



Advanced flash stripper using 5 m PZ



Irreversibility of AFS using 5 m PZ



Total Annualized Cost of Regeneration (Does not include absorber)



Total Energy



AFS saves 10% over SS (\$/metric ton CO₂ Captured, not rigorous DOE method) (593 MWe Gross)

	MEA-SS	PZ-SS	PZ-AFS
Energy Derating (MW_e)	145	97.5	90.1
CAPEX	22	22.1	19.4
OPEX	37	25.1	23.2
Cost of CO ₂ Capture	59.5	47.2	42.6
(excluding IS&IVI)	(1.00)	(0.79)	(0.72)

Amine Aerosols can be measured by FTIR and Phase Doppler Interferometer (PDI).

Amine aerosols cause high amine emissions

Nucleation sites in flue gas

- SO₃/H₂SO₄
- Submicron fly ash
- SO₂/amine
- + Amine condensation
 - Amine/CO₂/H₂O from solvent to aerosol
- + Poor collection of small drops in water wash
- = Unacceptable amine emissions

Effect of H2SO4 Injection FTIR Absorber out



Effect of 25 ppm SO₂ on PZ Aerosol



Phase-Doppler Interferometer (PDI) Size & concentration: 0.5 – 10 µm up to 10⁶ particle/cm³ 2G Bypass Extractive Sampler (tested 11/13)



PDI at Absorber Outlet – Startup (11/22/2013)



Absorber Outlet – Steady-State (LVI H₂SO₄: 11/22/2013)



Modifications for 3G PDI

- Use custom transmitter/receiver
 - to see down to 0.1 μm
- Use sapphire heated windows
 - to prevent liquid sheeting
- Set windows in flow body
 - To minimize wall geometry effects

Aerosol and AFS Test Plans for SRP 2014

- Energy performance of AFS
- Energy performance of 5 m PZ vs. 8 m PZ
- Aerosol formation
 - Add SO_2 and H_2SO_4 to the inlet gas
 - Use 3G PDI purchased by NCCC
 - Manual and FTIR measurements of amines
 - Impingement tray at top of the absorber

Conclusions

- 5 m PZ is a superior, demonstrated solvent.
- The advanced flash stripper provides 10% better energy performance for PZ and other solvents.
- Aerosol measurements by FTIR and PDI will quantify aerosol emissions for further control.

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