



## Guidance for NETL's Carbon Capture R&D Program

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**Booz Allen Hamilton**

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U.S. DEPARTMENT OF  
**ENERGY**

National Energy  
Technology Laboratory

# Acknowledgements

- **Booz Allen Hamilton**

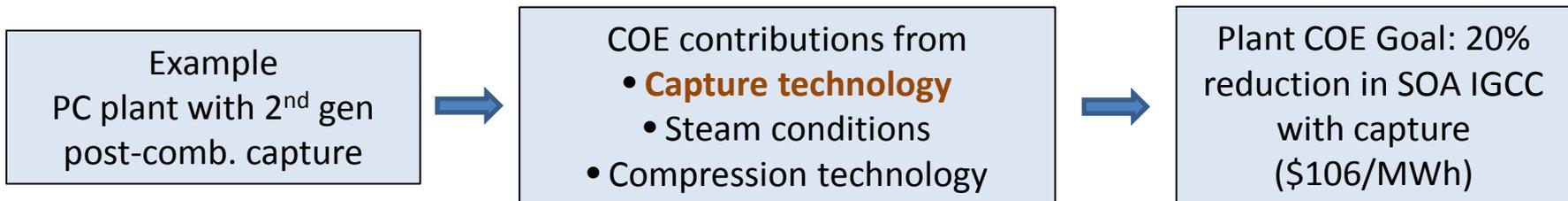
- Richard Newby
- Mark Woods

- **NETL**

- Jim Black
- Kristin Gerdes
- Mike Matuszewski
- Bob Stevens
- Capture and Adv. Combustion Technology Program Leadership

# Objectives

- **Devise a methodology to estimate power plant performance and cost using specific developer-provided characteristics of advanced CO<sub>2</sub> capture technology**
  - Ensure results on a consistent basis
  - Include diverse capture technologies: solvents, sorbents, adsorbents, membranes, phase change, cryogenic concepts
  - Reduce time and cost to assess advanced technology development status and guide development
- **Develop ‘COE’ and ‘cost of CO<sub>2</sub>’ metrics for an advanced capture technology that relate to the NETL advanced power plant R&D goals**



# Approach

NETL Baseline Study Reference Plants  
(PC post-combustion, PC oxy-combustion, IGCC pre-combustion)  
with Representation of Today's Capture Technology



Remove 'Conventional' CO<sub>2</sub> Capture Process;  
Insert Advanced Capture Technology

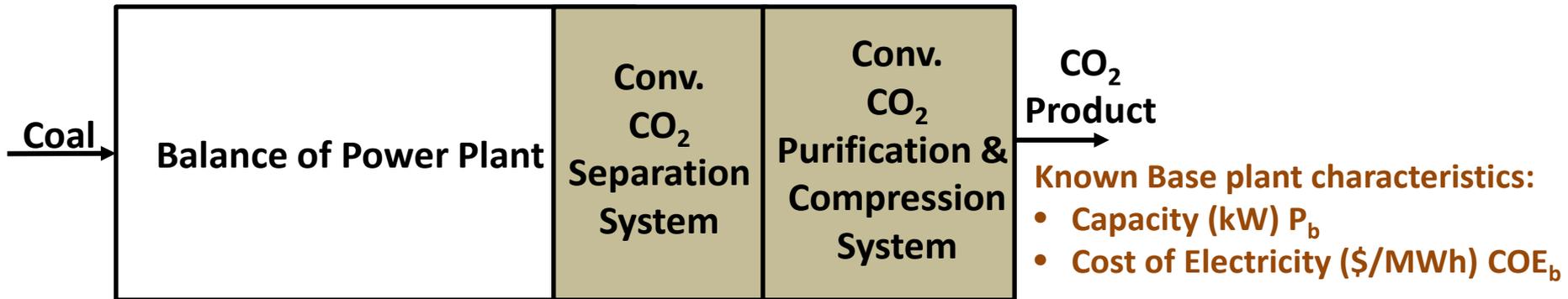
- Developer given plant design basis and boundary conditions
- Developer provides specific set of performance and cost estimate parameters for their process



Methodology Utilizes Adv. Technology Inputs to Project  
Integrated Plant Performance and Cost

# Methodology for Power Plant Performance and Cost Scaling

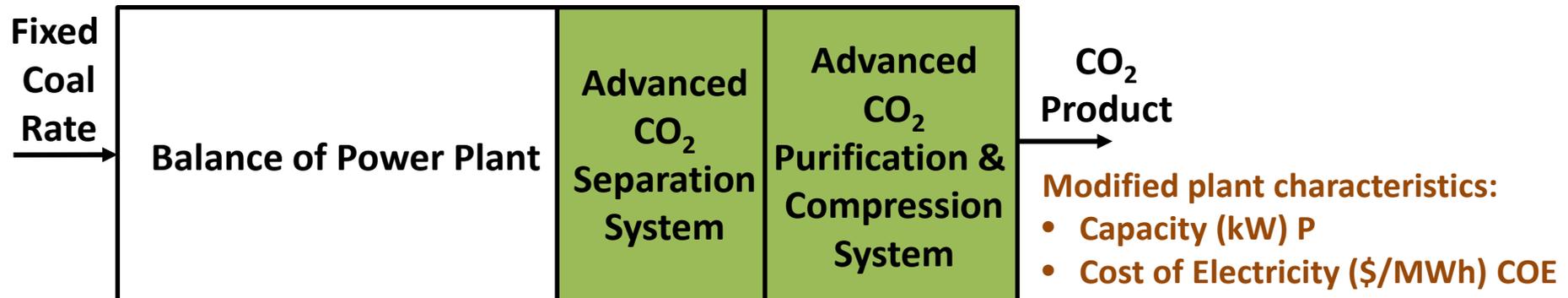
## BASE POWER PLANT WITH CONVENTIONAL CARBON CAPTURE



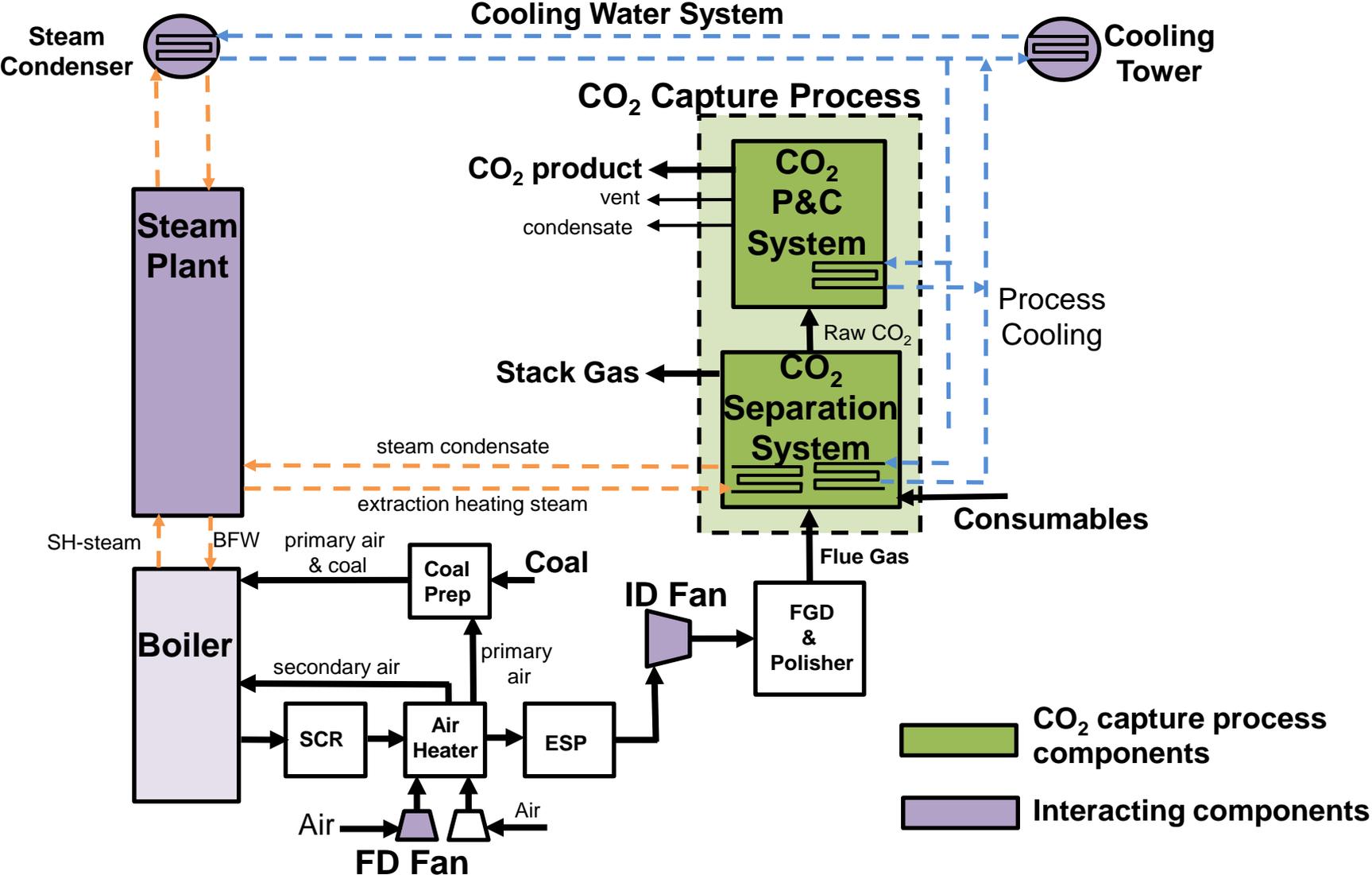
Direct Substitution

Direct Scaling

## MODIFIED POWER PLANT WITH ADVANCED CARBON CAPTURE

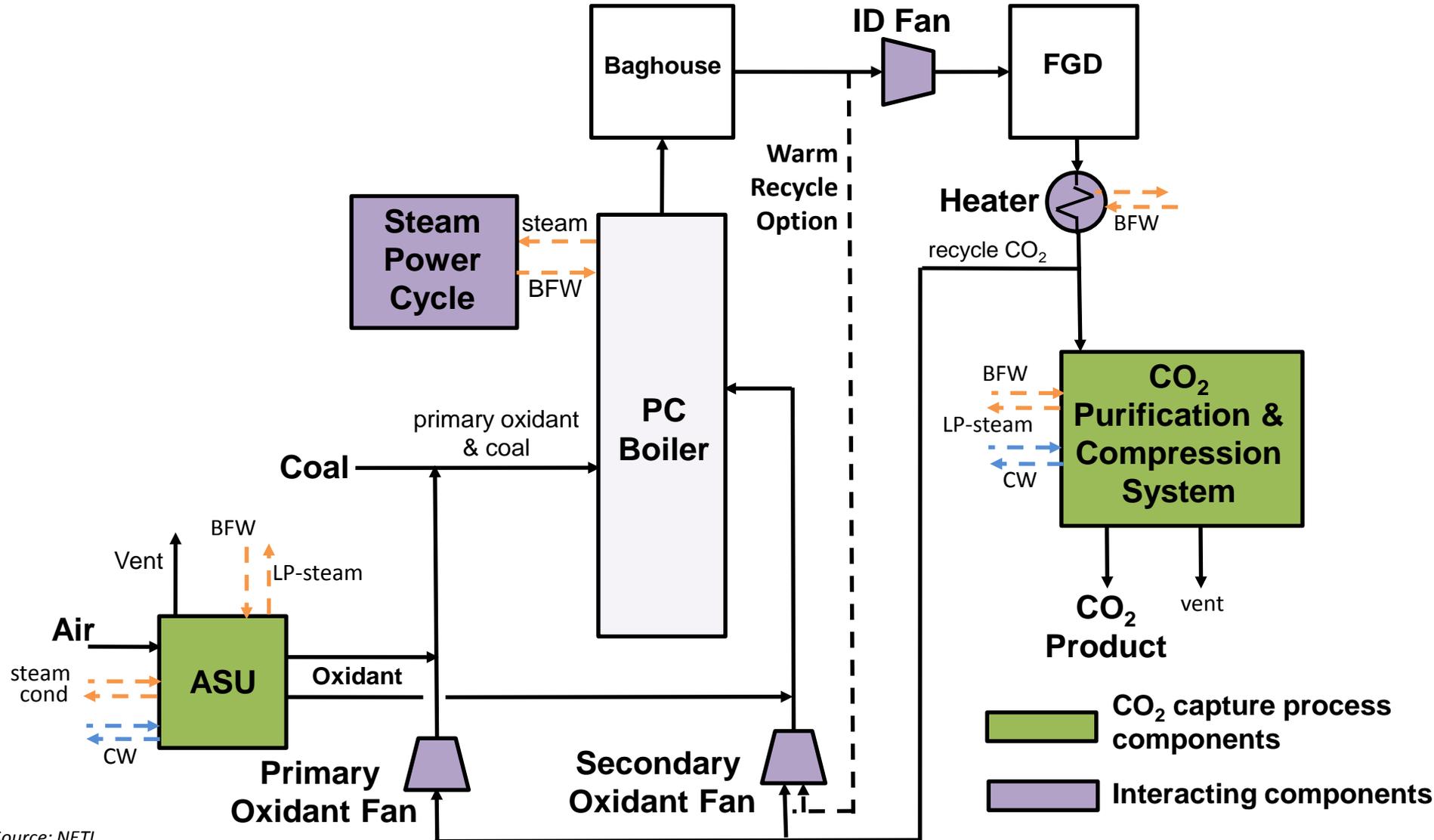


# PC Post-Combustion



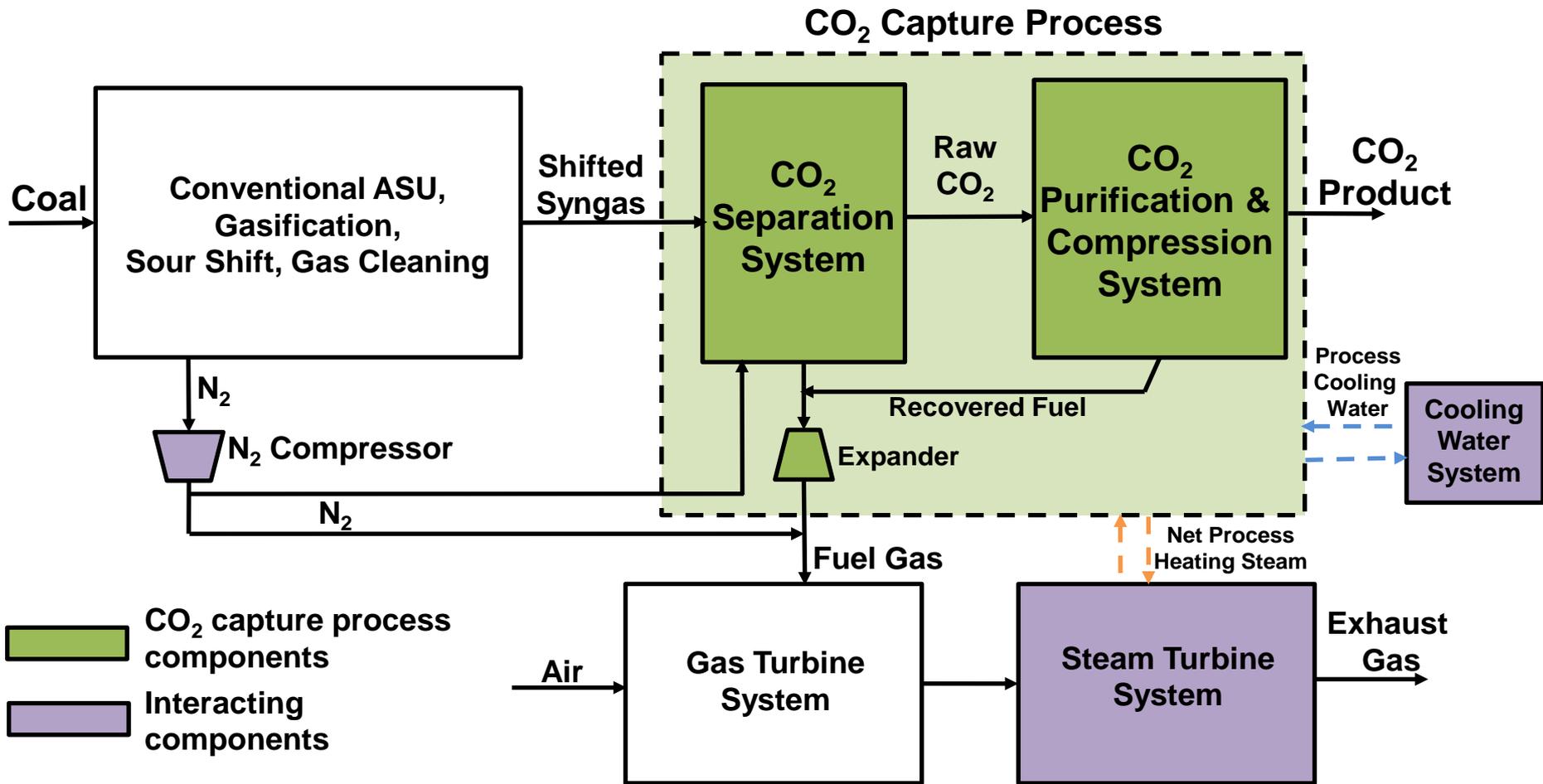
Source: NETL

# PC Oxy-Combustion



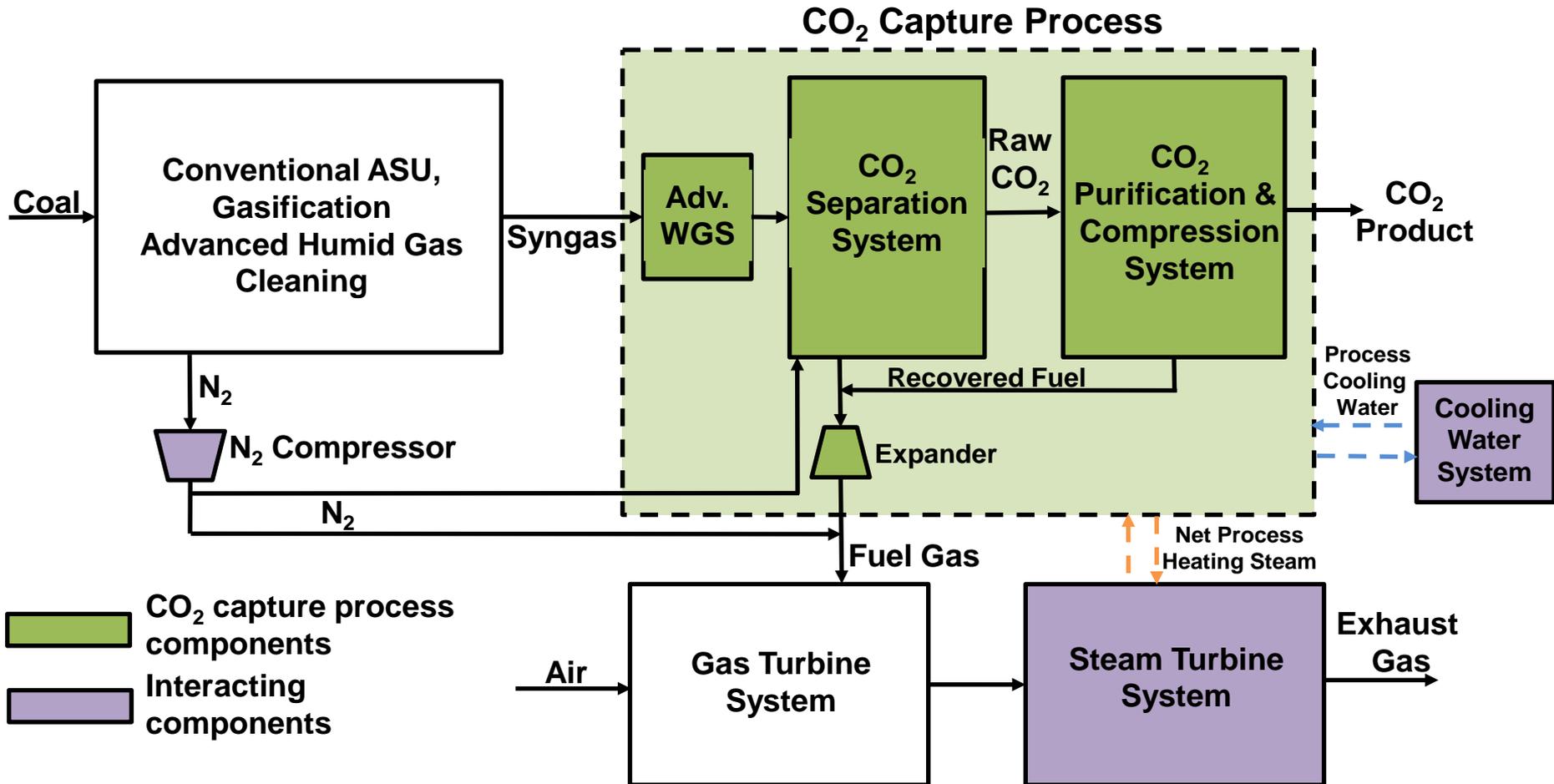
Source: NETL

# IGCC Pre-Combustion Conventional Gas Cleaning



Source: NETL

# IGCC Pre-Combustion Advanced Humid Gas Cleaning



Source: NETL

# Power Factor (PF)

## Associated with Advanced Capture Technology

- Represents the sum of the impacts of the advanced CO<sub>2</sub> capture process on the power plant generating capacity
- Form of the Power Factor (kW per tonne/hr CO<sub>2</sub>) is:

$$PF = \underline{A}_{CO_2} + \underline{A}_{P\&C} + (\underline{P}_{bST} - \underline{P}_{ST}) + \sum (\underline{A}_i - \underline{A}_{bi})$$

- $\underline{A}_{CO_2}$ : Advanced CO<sub>2</sub> separation system auxiliary power, kW/tonne/hr CO<sub>2</sub>
- $\underline{A}_{P\&C}$ : Purification & compression system auxiliary power, kW/tonne/hr CO<sub>2</sub>
- Interaction terms:
  - $(\underline{P}_{bST} - \underline{P}_{ST})$ : Difference between steam cycle power in advanced and base plant
  - $(\underline{A}_i - \underline{A}_{bi})$ : Difference between system “i” auxiliary power in advanced and base plant

# COE Factor (COEF)

- Represents all contributions of the advanced CO<sub>2</sub> Capture Process components to the power plant COE
- The form of the COE Factor (\$ per tonne/hr CO<sub>2</sub>) is:

$$\text{COEF} = \underline{C}_{\text{CO}_2} + \underline{C}_{\text{P\&C}} + (\underline{C}_{\text{ST}} - \underline{C}_{\text{bST}}) + \Sigma (\underline{C}_i - \underline{C}_{\text{bi}}) + K_c \cdot \underline{OC}_{\text{VarCO}_2}$$

- $\underline{C}_{\text{CO}_2}$ : Capital cost of the CO<sub>2</sub> separation system, \$/tonne/hr CO<sub>2</sub>
- $\underline{C}_{\text{P\&C}}$ : Capital cost of the CO<sub>2</sub> purification and compression system, \$/tonne/hr CO<sub>2</sub>
- $\underline{OC}_{\text{VarCO}_2}$ : Variable operating cost of the  
CO<sub>2</sub> separation and CPU systems, \$/yr per tonne/hr CO<sub>2</sub>
- $K_c$  is a constant based on financial assumptions
- Interaction terms:
  - $\underline{C}_{\text{ST}} - \underline{C}_{\text{bST}}$ : Change in capital cost of the steam turbine system, \$/tonne/hr CO<sub>2</sub>
  - $\underline{C}_i - \underline{C}_{\text{bi}}$ : Change in capital cost of the “I” system, \$/tonne/hr CO<sub>2</sub>

# Methodology for Power Plant Performance and Cost Scaling

- **Net power (P) and first-year COE (w/o T&S) Scaling Relationships:**

$$P = B_1 - B_2 \bullet \text{Power Factor}$$

$$\text{COE} = [B_3 + B_4 \bullet \text{COE Factor}] / P$$

- **The “B” terms are constants derived from the base plant performance and cost**
- **Power Factor and COE Factor are based on characteristics of the advanced CO<sub>2</sub> capture process**

Fixed Coal Feed Rate for Reference Plant and Advanced Capture Plant

# PC Post-Combustion Example

## Inputs for Membrane-Based CO<sub>2</sub> Capture Process

Required CO <sub>2</sub> Capture Process Input Data	
CO <sub>2</sub> process steam heating duty (MMBtu/hr)	0
Extracted steam heating temperature (F)	N/A
CO <sub>2</sub> process cooling duty (MMBtu/hr)	0
CO <sub>2</sub> separator pressure drop (psi)	2
FD fan boost pressure (psi)	1.5
CO <sub>2</sub> separation process auxiliary power (kW)	34,897
CO <sub>2</sub> purification & compression power (kW)	57,404
CO <sub>2</sub> separation process cost (\$1000)	307,311
CO <sub>2</sub> purification & compression cost (\$1000)	67,184
CO <sub>2</sub> capture process annual variable operating cost (\$1000)	5,215

These input data are based on a hypothetical membrane system concept with design, operating and performance parameters\* selected to meet the DOE goal.

\* Includes design concept, permeances (e.g. CO<sub>2</sub>, H<sub>2</sub>O, SO<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>), operating temperature, operating pressures, membrane surface area, pressure drop, membrane life, membrane cost, and module cost

# Example Results for PC Post-Combustion Membrane-Based CO<sub>2</sub> Capture Process

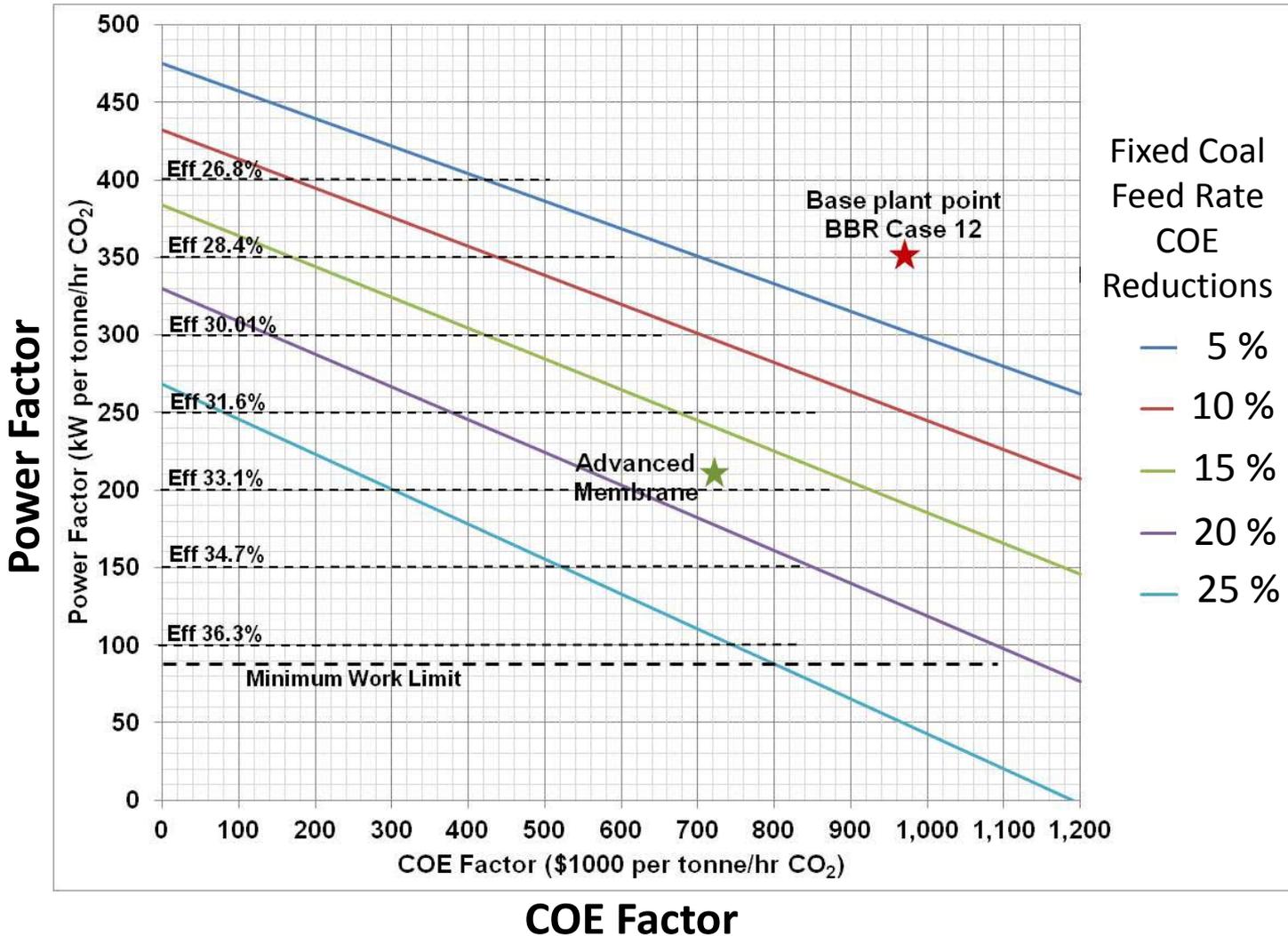
PC Power Plant Results	
<b>Power Factor (kW per tonne/hr flue gas CO<sub>2</sub>)</b>	<b>210.06</b>
<b>Plant net efficiency (% , HHV)</b>	<b>32.81</b>
<b>COE Factor (\$ per tonne/hr flue gas CO<sub>2</sub>)</b>	<b>721,849</b>
<b>COE (\$/MWh)</b>	<b>113.3</b>
<b>COE Reduction (%)</b>	<b>17.5</b>

These input data are based on a hypothetical membrane system concept with design, operating and performance parameters\* selected to meet the DOE goal.

\* Includes design concept, permeances (e.g. CO<sub>2</sub>, H<sub>2</sub>O, SO<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>), operating temperature, operating pressures, membrane surface area, pressure drop, membrane life, membrane cost, and module cost



# COE Reduction Plot for PC Post-Combustion Membrane Technology Example



This plot represents the COE reduction contribution for a plant with

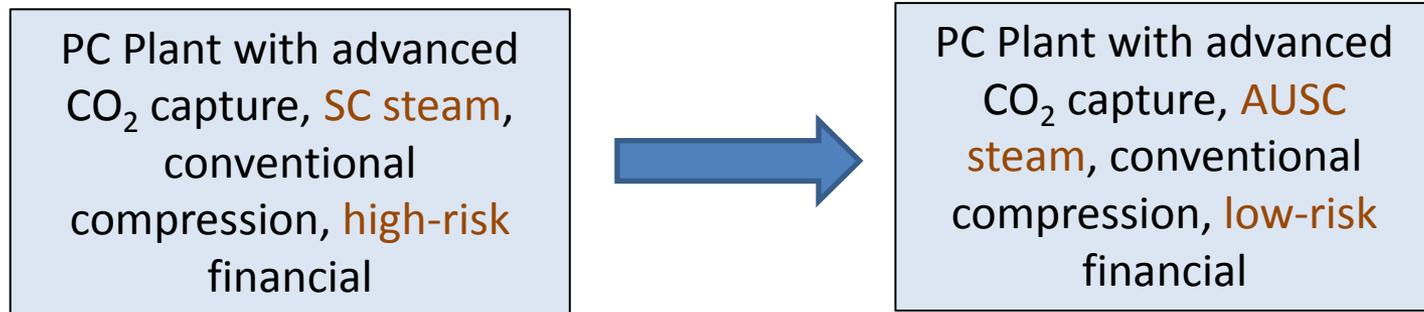
- Adv. capture tech.
- SC steam
- Conv. compression
- High-risk financial

Source: NETL



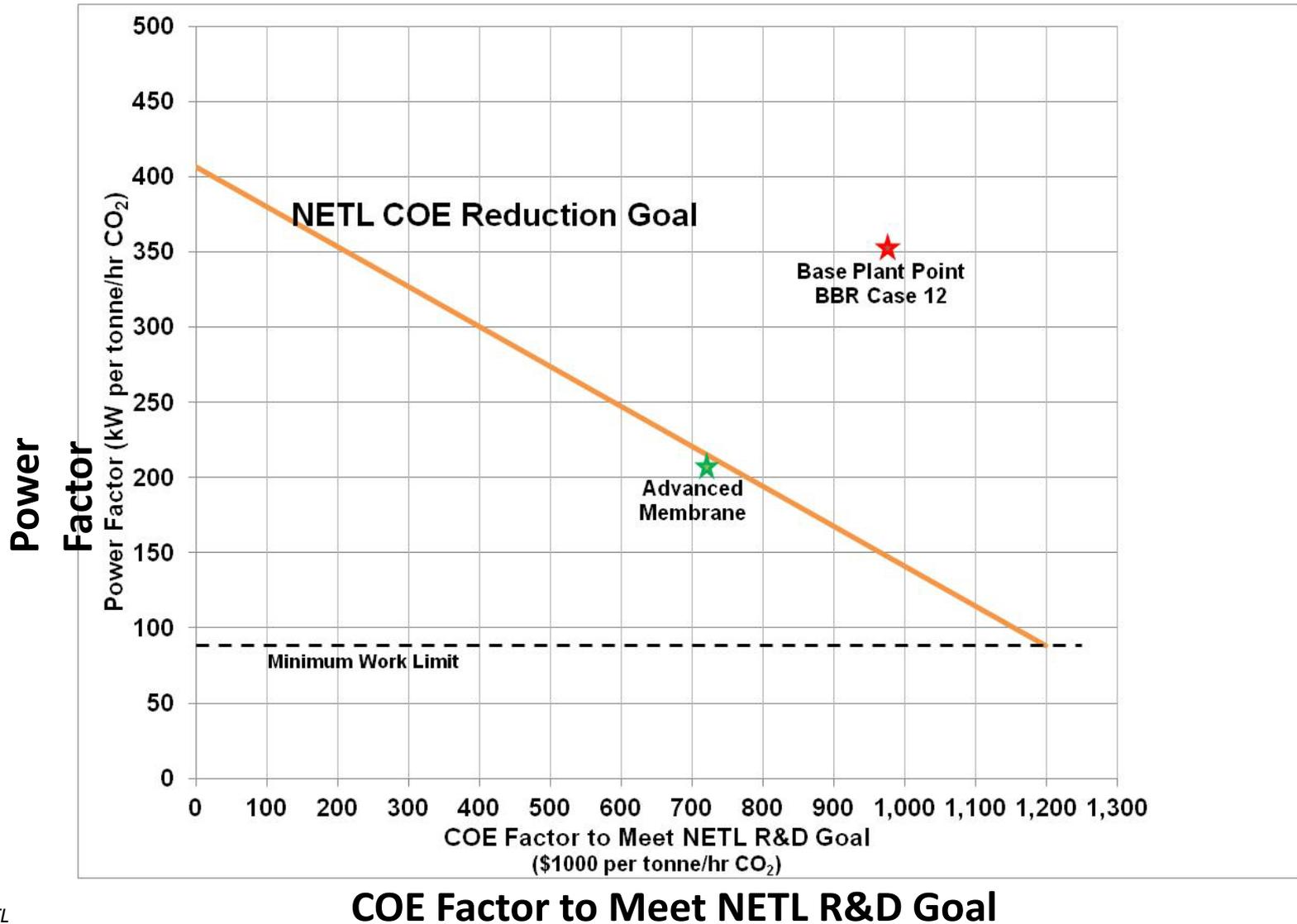
# Methodology for Power Plant Cost Metrics and Goals

- The PC Plant with the advanced CO<sub>2</sub> capture process is related to the NETL advanced power generation R&D goal of 20% reduction in the COE (\$106/MWh)



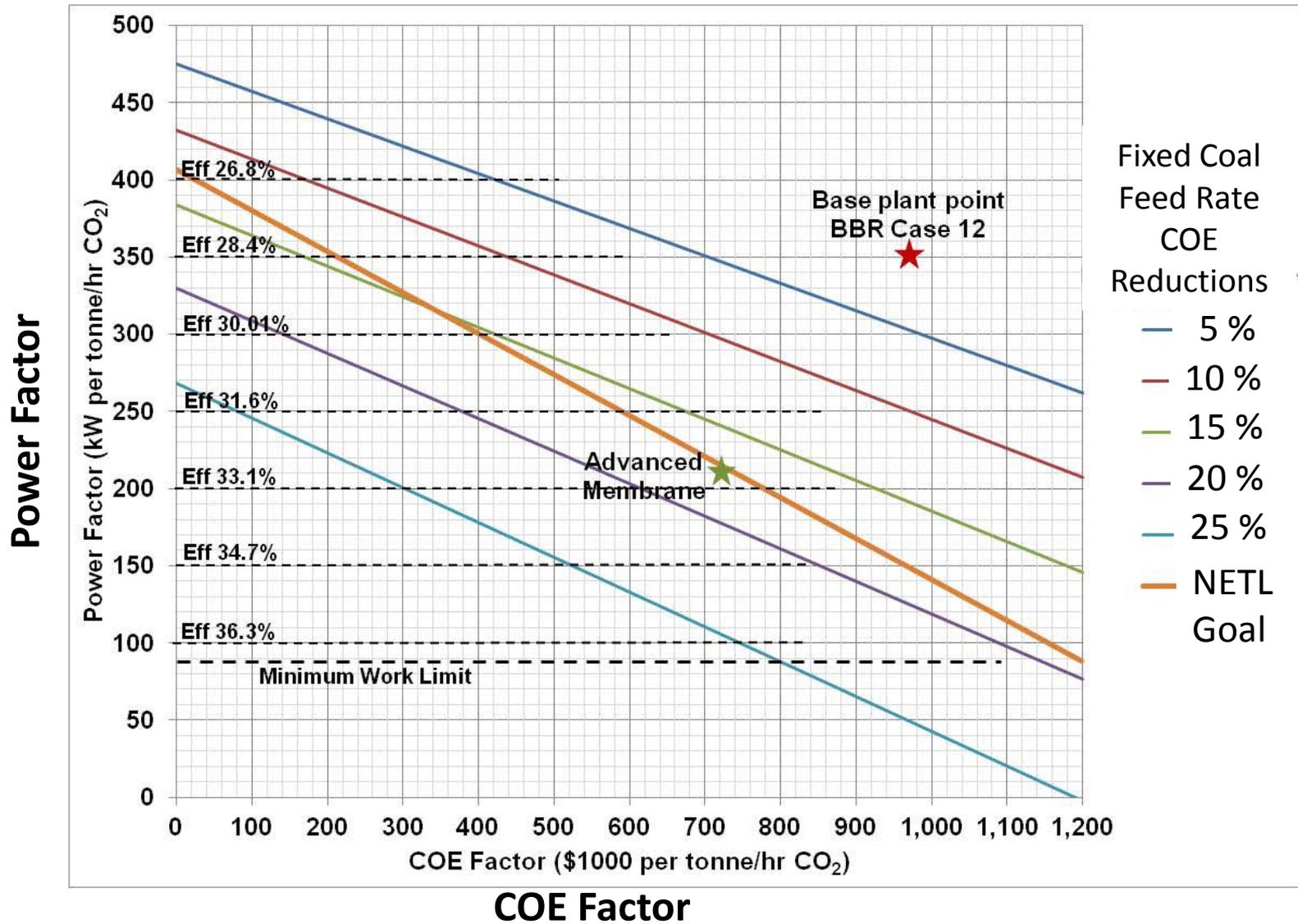
The methodology for an IGCC plant with advanced capture would include options for an advanced gas turbine, ASU, gas cleaning, gasification.

# COEF and PF to Meet NETL Advanced Power Generation R&D Goal



Source: NETL

# Relationship of Capture Technology Metrics to NETL R&D Program Goal for COE



# Methodology Tool Application

- A technology developer or evaluator can apply the methodology relationships to assess the feasibility, sensitivity, development requirements, and development progress of CO<sub>2</sub> separation technologies
- If the technology developer can estimate the PF for the CO<sub>2</sub> Capture Process, the COEF required to meet any given COE goal can be determined and assessed
- If the technology developer can estimate the PF and COEF for the CO<sub>2</sub> capture process, the COE for the resulting plant can be determined and assessed