



# Development of Self-Powered Wireless-Ready High Temperature Electrochemical Sensors for In-Situ Corrosion Monitoring of Boiler Tubes

**Naing Naing Aung, Xingbo Liu**

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# Project Objectives

- To develop in-situ corrosion monitoring sensors for corrosion of USC boiler tubes in next generation coal-based power systems
- To develop thermal-electric based energy harvesting and telecommunication devices for the self-powered wireless ready sensor system

# Current Milestones

## July to September 2011

- Initiate preliminary high-temperature electrochemical corrosion rate (ECR) probe design

## October to December 2011

- To complete the design and construction of (ECR) probe for lab scale corrosion experiments and to complete laboratory test configuration

## January to March 2012

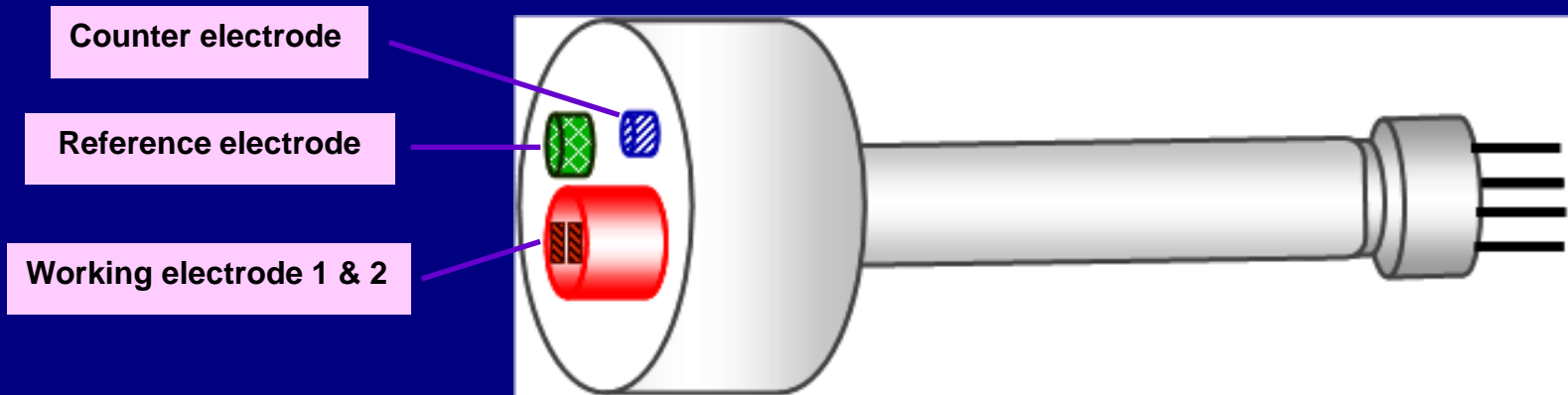
- To demonstrate the results of the corrosion tests as a function of exposure time, temperature and various simulated boiler exposure environments in lab-scale setting

# Project Milestone Status

July to September 2011

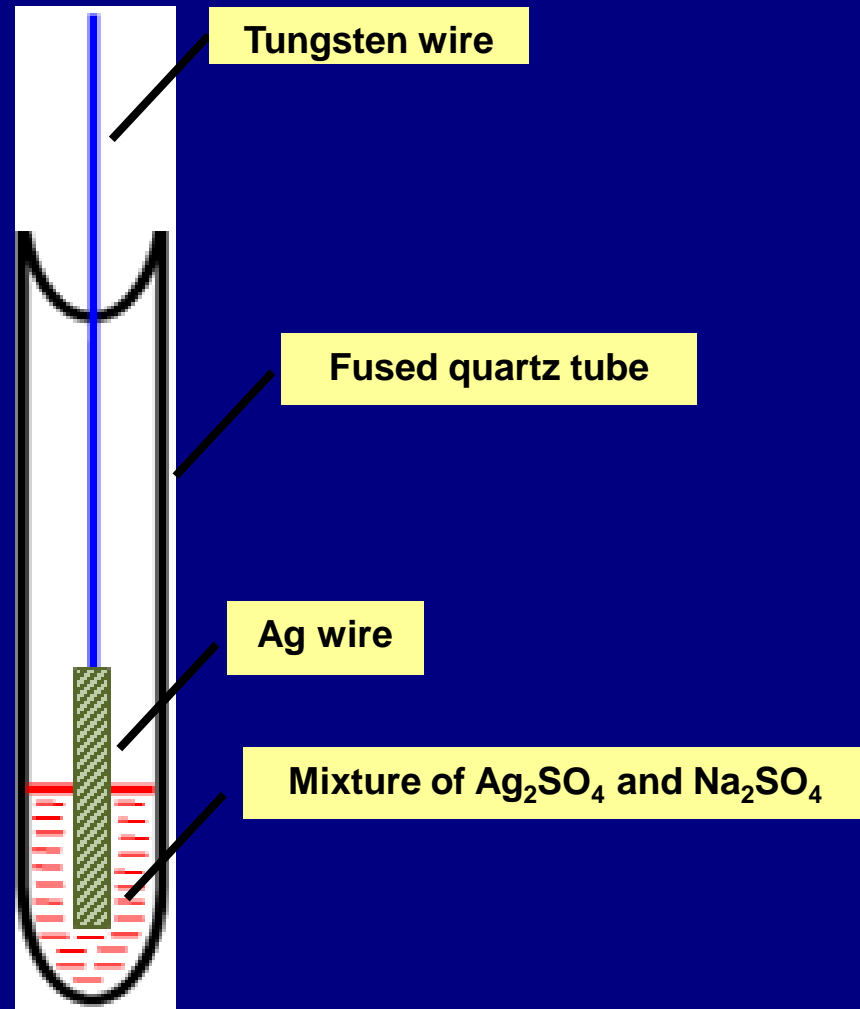
- High temperature electrochemical corrosion rate (ECR) probe for lab scale corrosion experiments has been designed and constructed.

# Developed High Temperature Corrosion Sensor

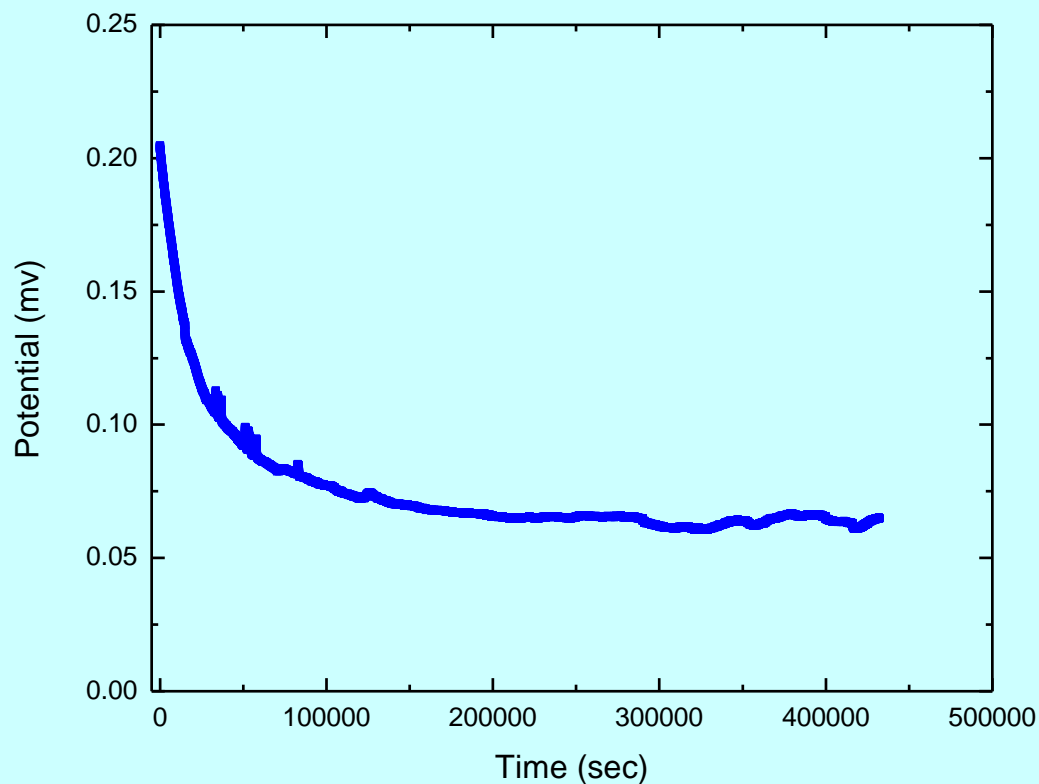


# Ag/Ag<sup>+</sup>/Fused-Quartz Reference Electrode

Stability  
Reproducibility  
Reusability



# Time Dependency of the Potential of Ag/Ag<sup>+</sup>/fused-quartz Reference Electrode in Synthesis Coal Ash Mixture at 800 °C



# Project Milestone Status

October to December 2011

- Construction of custom-designed coal ash exposure unit for lab-scale corrosion experiments has been completed in WVU.



# Laboratory Test Configuration



# Project Milestone Status

January to March 2012

- Coal ash corrosion behaviour of nickel- based Superalloy IN740-1 in synthetic coal ash mixture at 800 °C as a function of exposure time

# Corrosion in Coal-Fired Boilers

## In the Upper Furnace

Higher Steam Temperature and Pressure  
Deposit-induced Liquid Phase Corrosion



**Coal Ash Corrosion** in Superheater/Reheater alloys

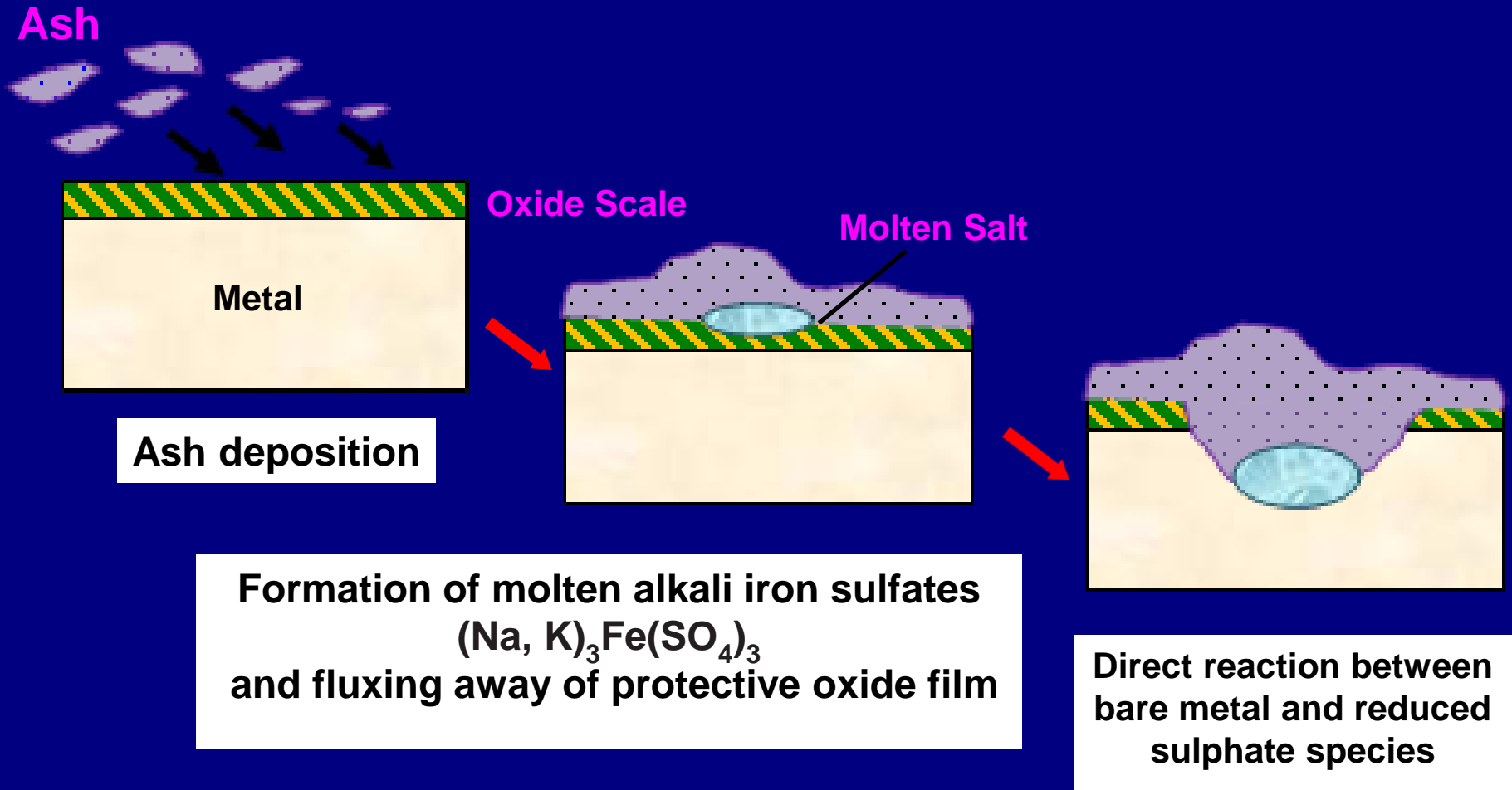
## In the Lower Furnace

Low- $\text{NO}_x$  combustion produces  $\text{H}_2\text{S}$  in the flue gas and  $\text{FeS}$  in the deposit due to incomplete combustion of the sulfur-bearing species in coal



**Furnace Wall Corrosion** on Waterwalls of the Boiler Tubes

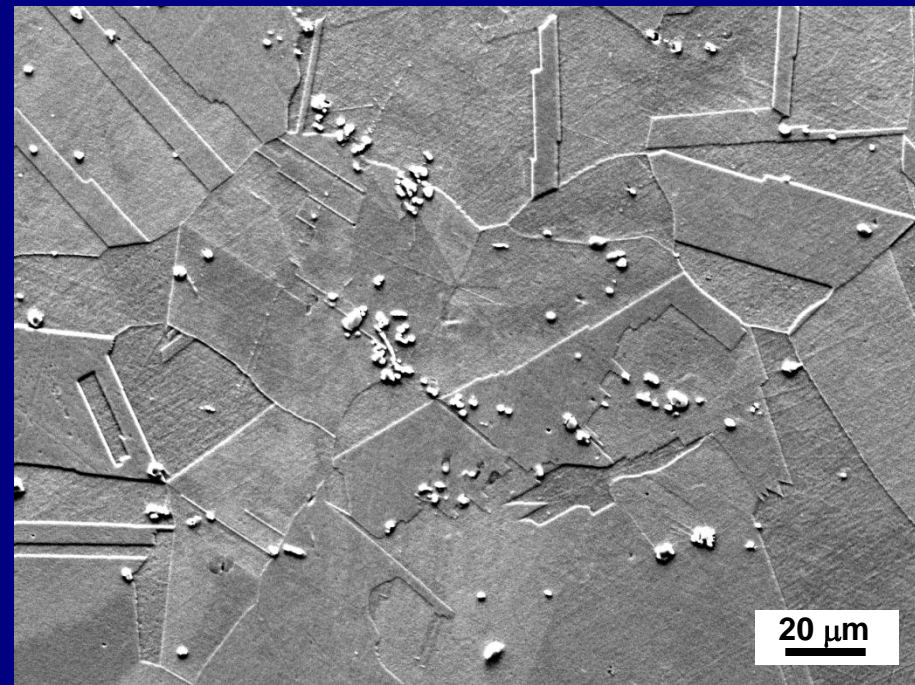
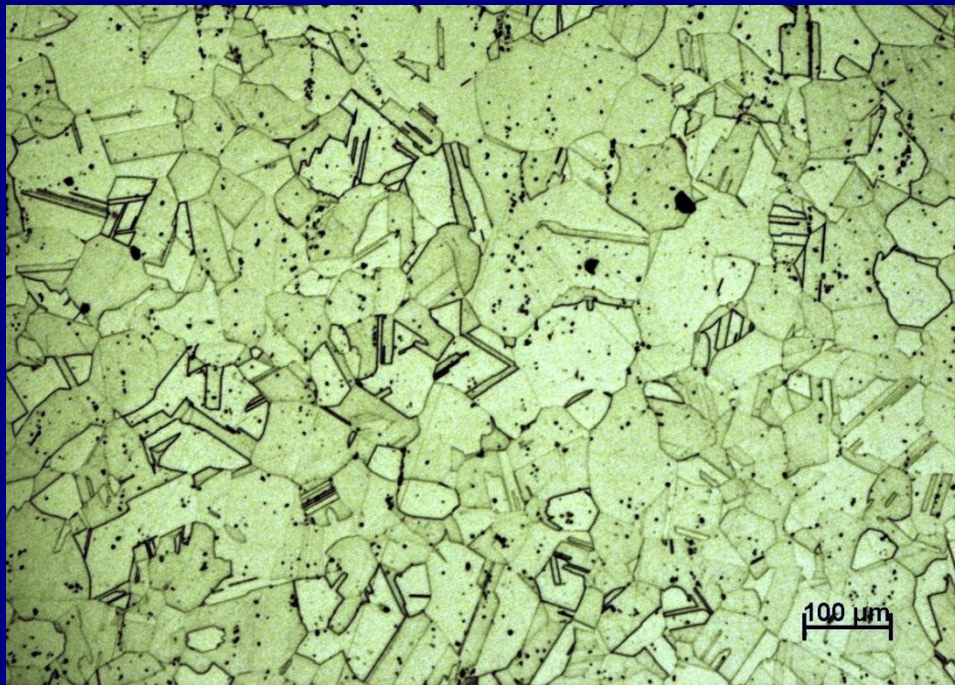
# Coal Ash Corrosion Mechanism



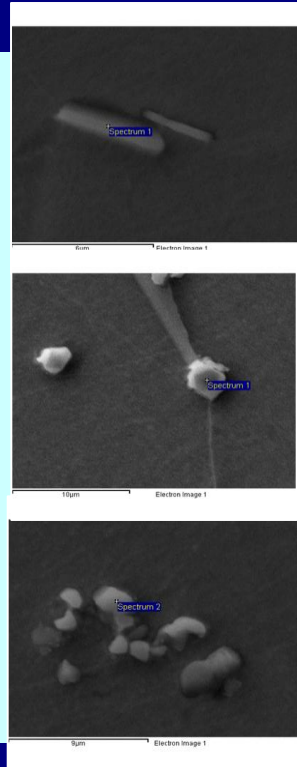
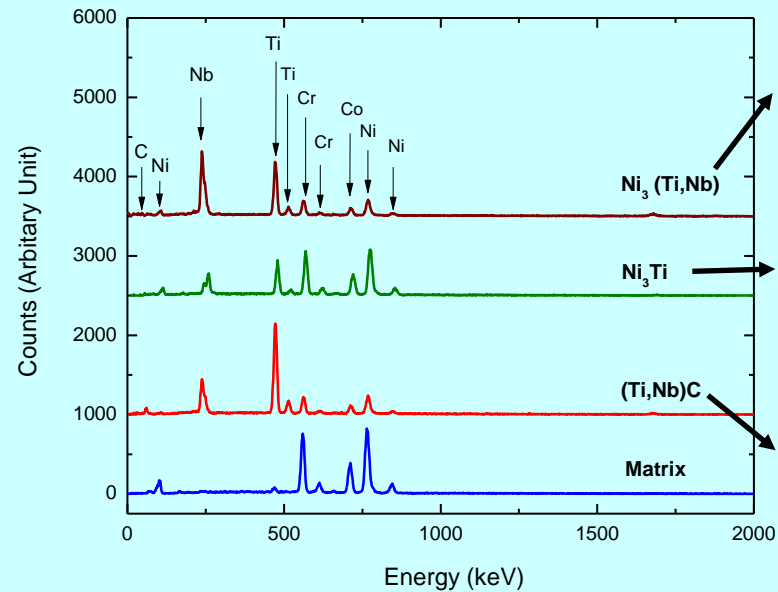
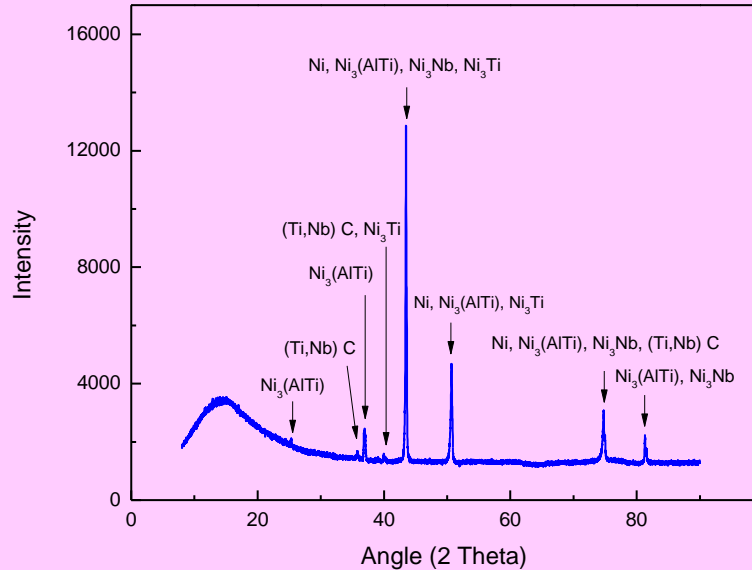


# IN 740-1 Ni-Base Superalloy

Ni	Cr	Fe	Cu	Co	Mo	Nb	Al	Mn	Ta	Ti	W	Si	C	Sn
35–80	5–25	<42	<35	<30	<17	<6	<5	<5	<5	<5	<5	<1	0	0



# Intermetallic Phases in IN 740-1 Ni-Base Superalloy



# Corrosive Media For Coal Ash Corrosion

Synthetic Flue Gas



Coal Ash Mixture

Ash+10% Alkali Sulfates+1% NaCl

Ash -  $\text{SiO}_2$ ,  $\text{Al}_2\text{O}_3$ , and  $\text{Fe}_2\text{O}_3$  in the ratio of 1:1:1 by weight  
mp=1600 °C mp=2027 °C mp=1566 °C

mp=800 °C

Alkali sulfate mixture -  $\text{Na}_2\text{SO}_4$  and  $\text{K}_2\text{SO}_4$  in the ratio of 1:1  
by weight mp= 880 °C mp= 1067 °C

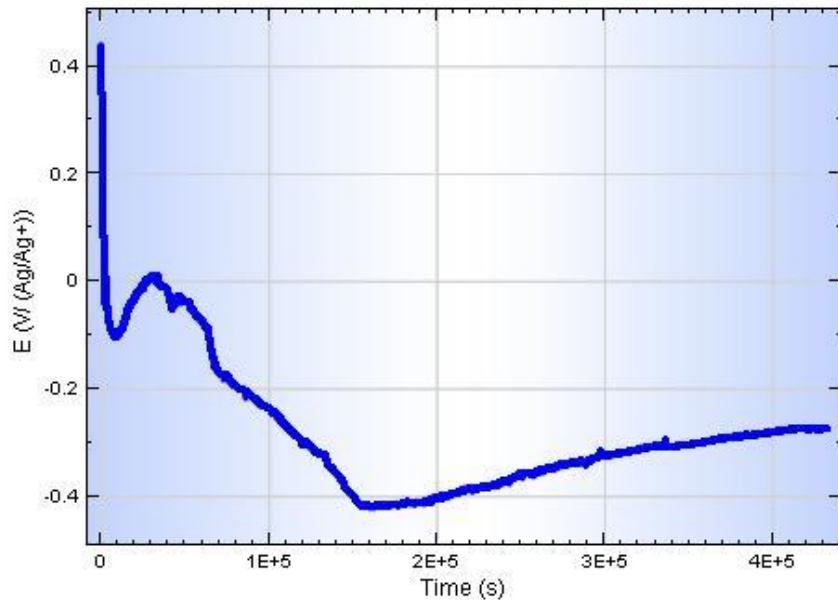
# Electrochemical Techniques Used to Study Corrosion

- Open Circuit Potential (OCP) Measurement
- Linear Polarization Resistance (LPR)
- Electrochemical Impedance Spectroscopy (EIS)
- Electrochemical Noise Analysis (ENA)



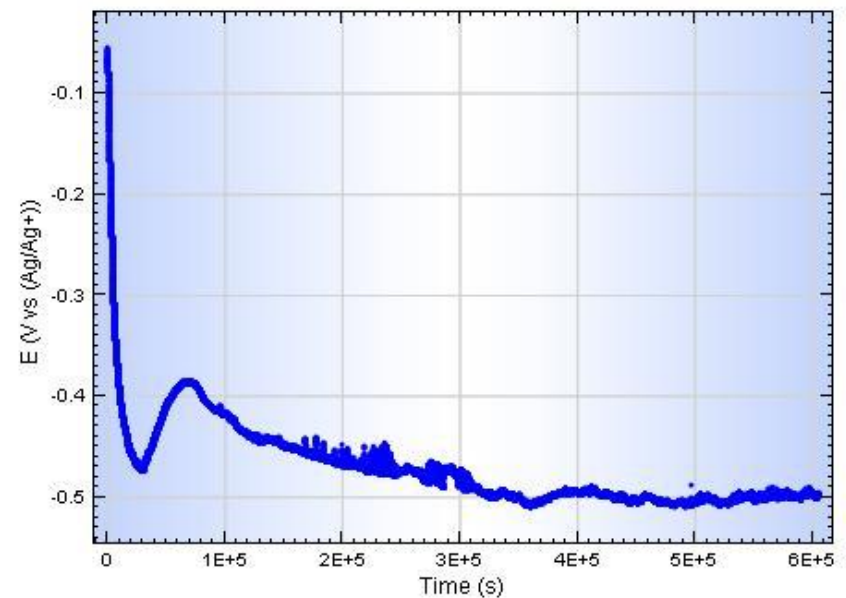
# OCP for Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C

Without Synthetic Flue Gas



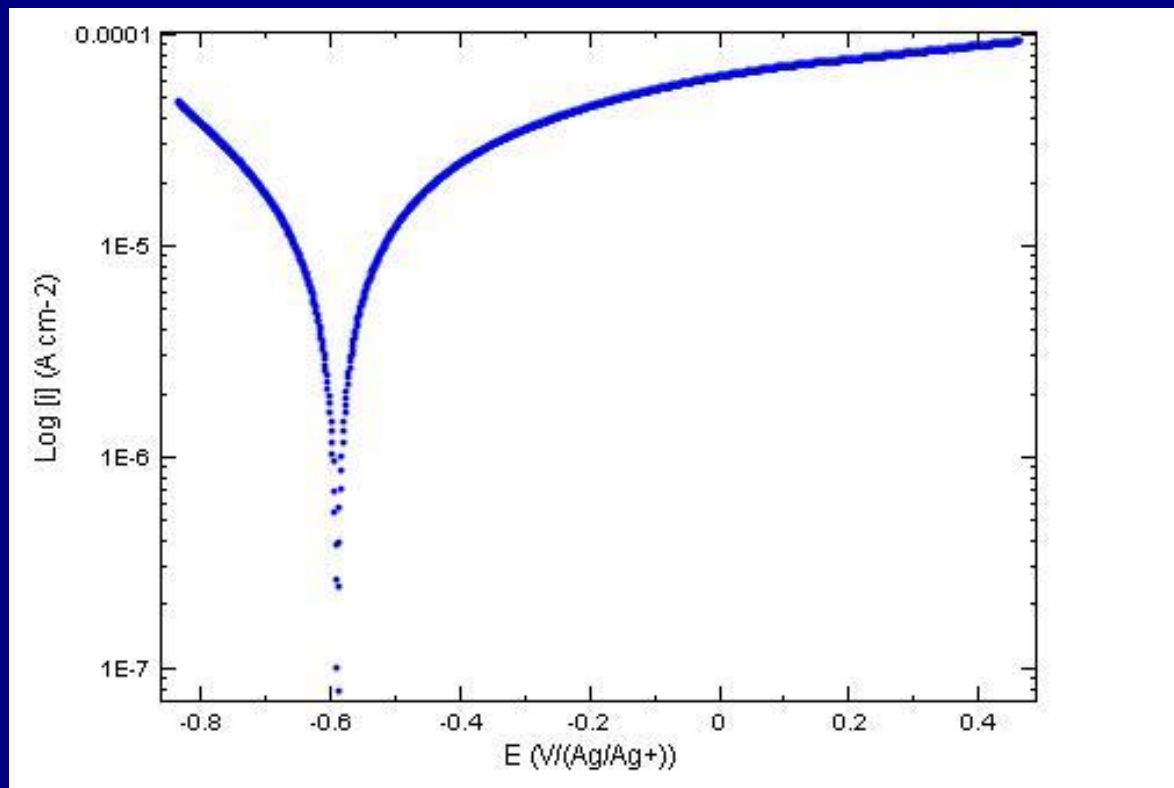
OCP = - 274 mV vs. Ag/Ag<sup>+</sup>

With Synthetic Flue Gas



OCP = -497 mV vs. Ag/Ag<sup>+</sup>

# $E_{\text{corr}}$ and $i_{\text{corr}}$ Values for Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C



OCP  
(mV vs. Ag/Ag<sup>+</sup>)

$E_{\text{corr}}$   
(mV vs. Ag/Ag<sup>+</sup>)

$i_{\text{corr}}$   
( $\mu\text{A cm}^{-2}$ )

$\beta_a$   
mV dec<sup>-1</sup>

$\beta_c$   
mV dec<sup>-1</sup>

Corrosion rate  
(mm y<sup>-1</sup>)

-538

-592

4.71

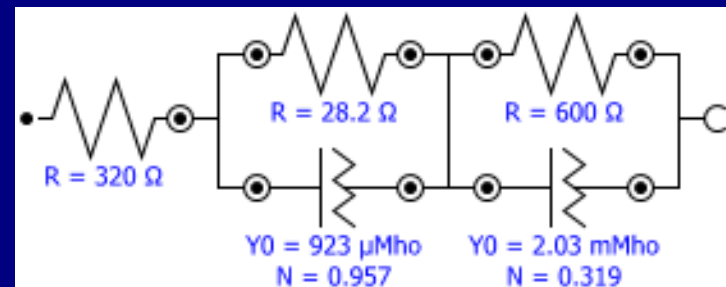
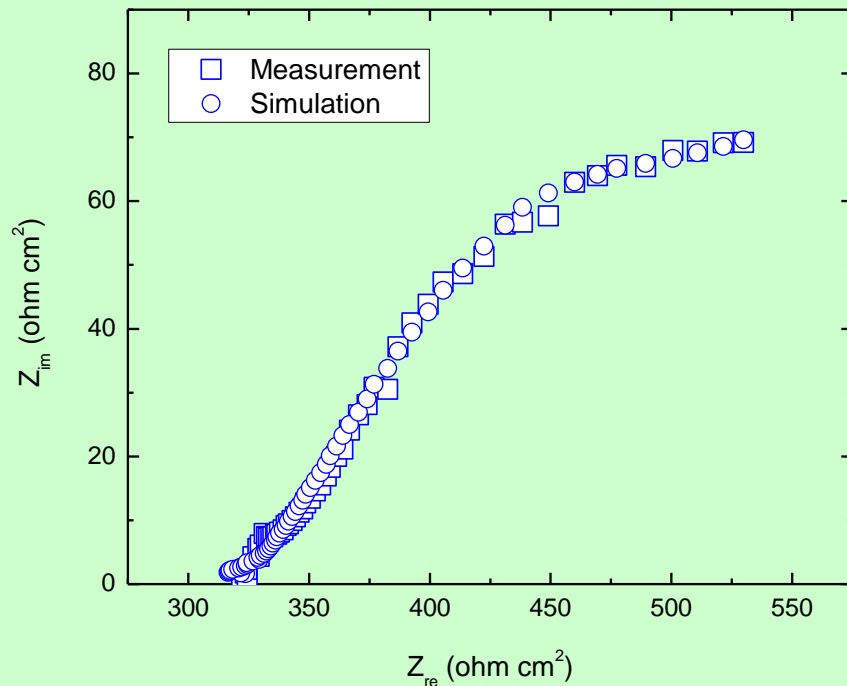
198

217

0.11

# Electrochemical Impedance for Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C

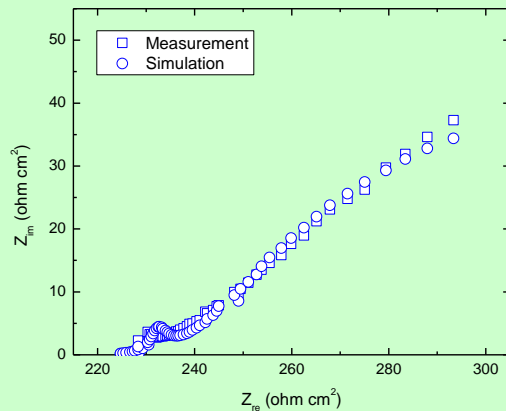
After 2 h



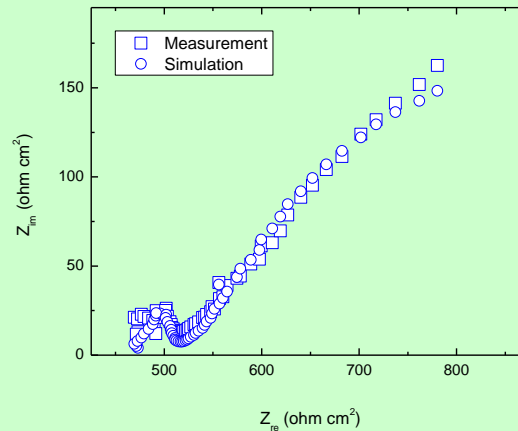
The transport of the oxygen to the alloy surface and the formation of a oxide scale

# Electrochemical Impedance for Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C

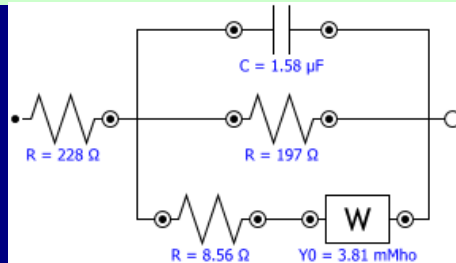
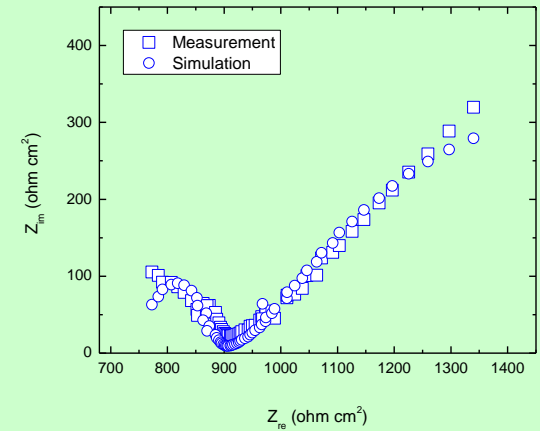
After 24 h



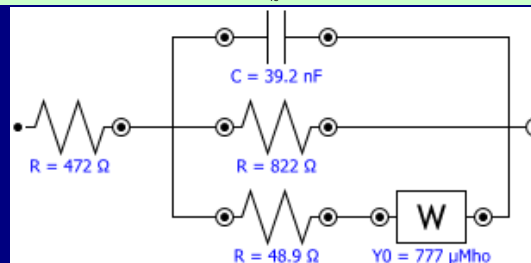
After 48 h



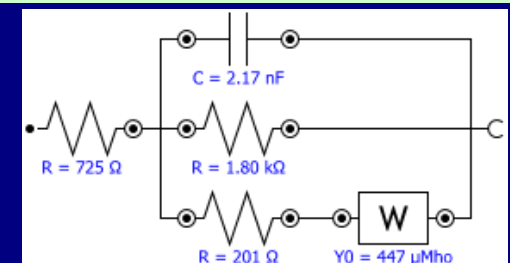
After 72 h



$$\bar{Z}(\omega) = \left\{ \frac{1}{Y_0 \sqrt{j\omega}} \right\} \tanh[B\sqrt{j\omega}]$$



$$\bar{Y}(\omega) = \left\{ Y_0 \sqrt{j\omega} \right\} \coth[B\sqrt{j\omega}]$$

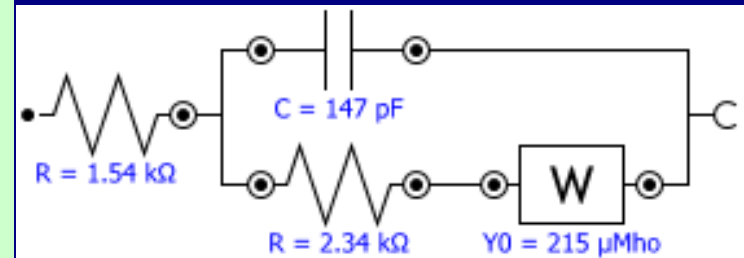
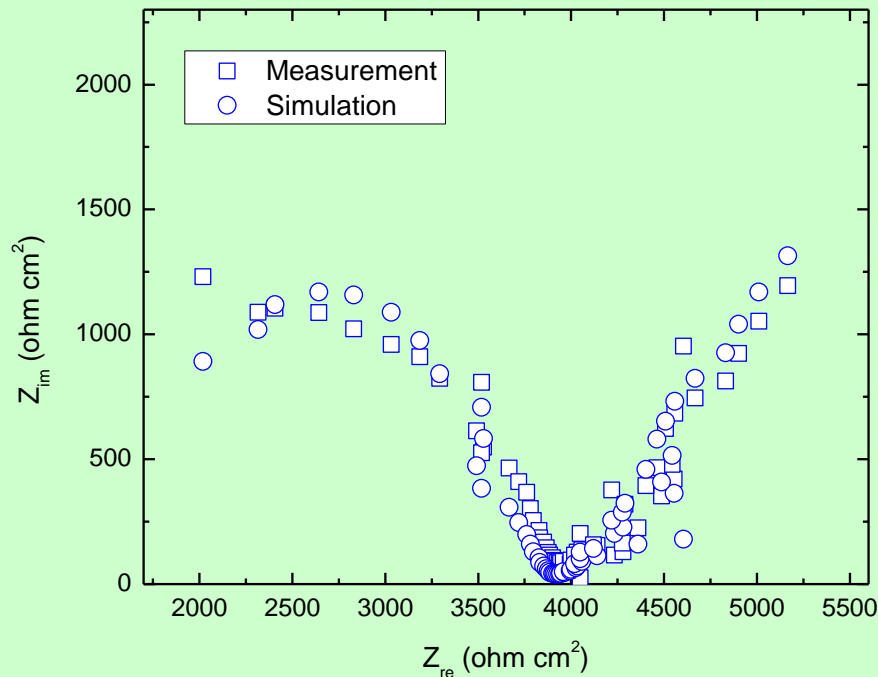


$$Z = A(i\omega)^{-\alpha}$$

Forming a porous scale in molten salts and the corrosion of the alloy is controlled by diffusion of the oxidant in the melt

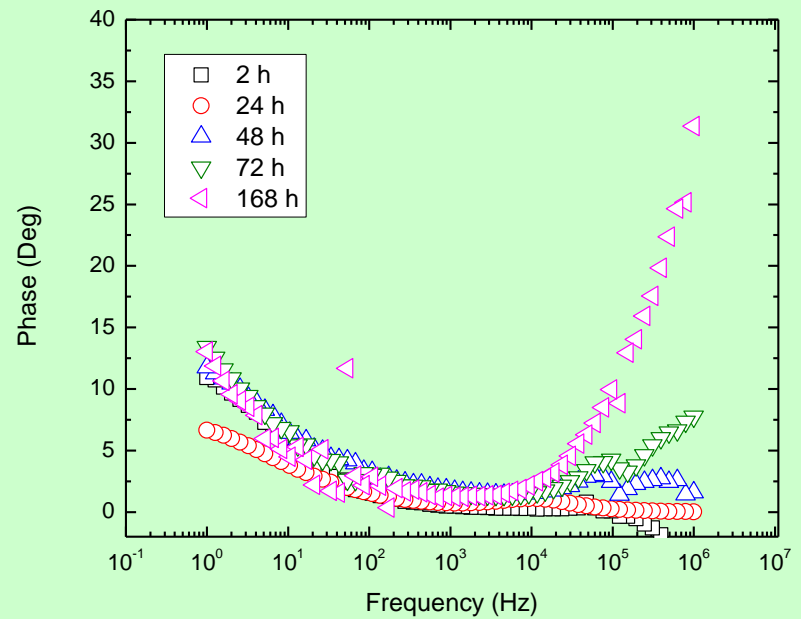
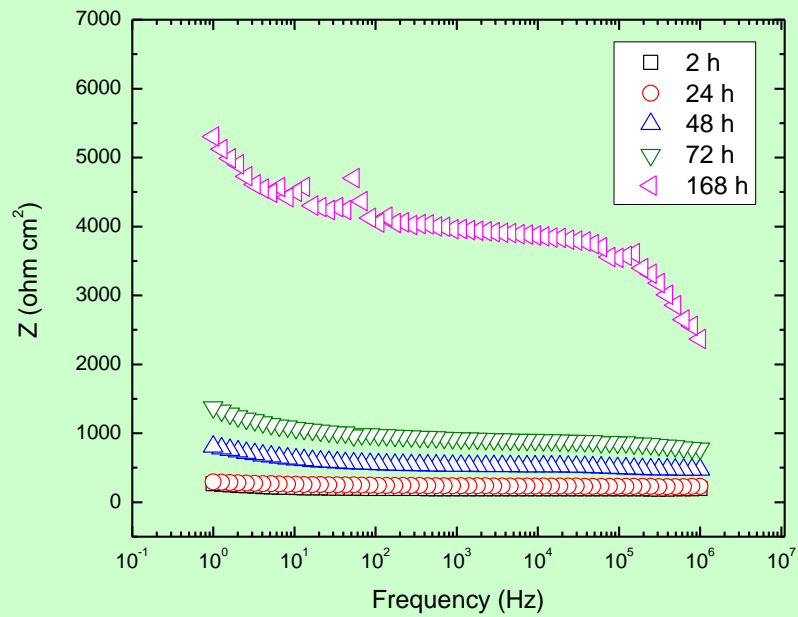
# Electrochemical Impedance for Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C

After 168 h



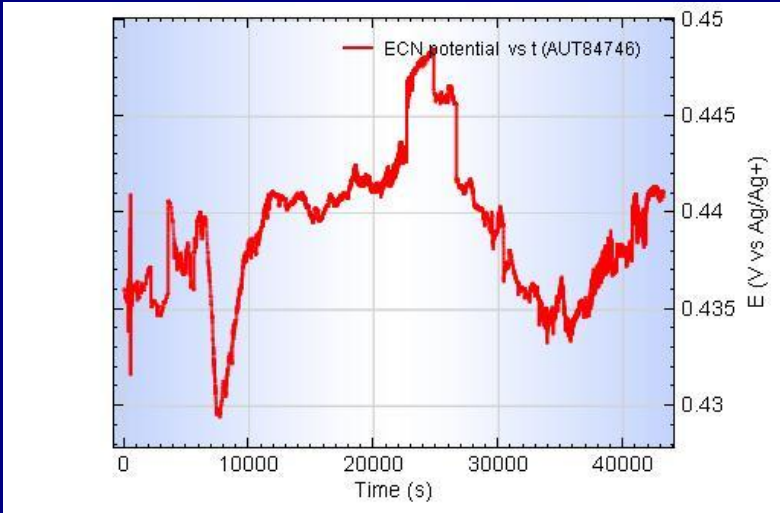
The corrosion of the alloy is controlled by diffusion of the ions through the scale after forming a compact scale

# Bode Plots for Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C

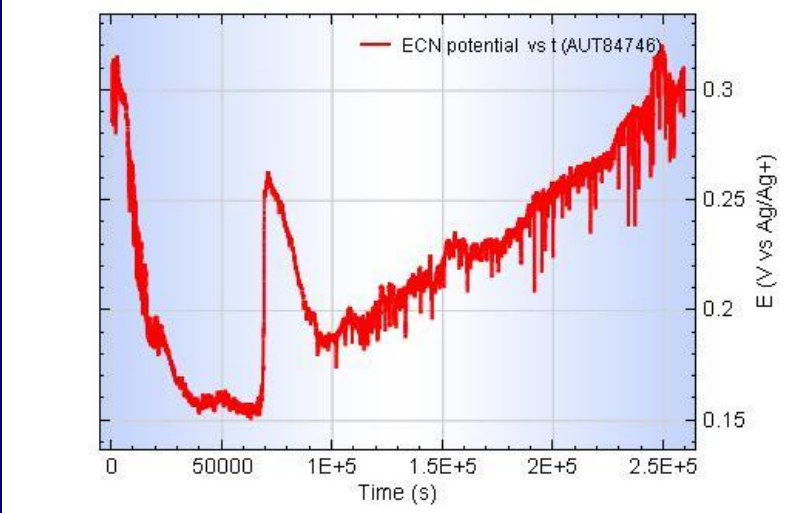


# Typical Potential Noise Signatures from Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C

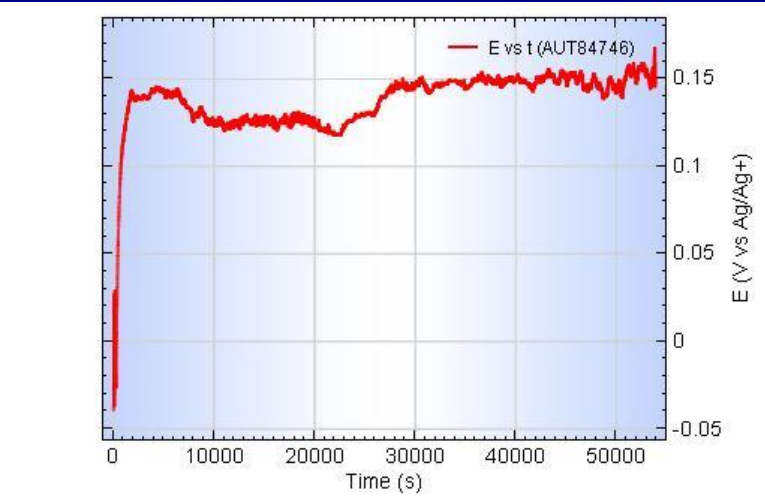
After 24 h



After 72 h

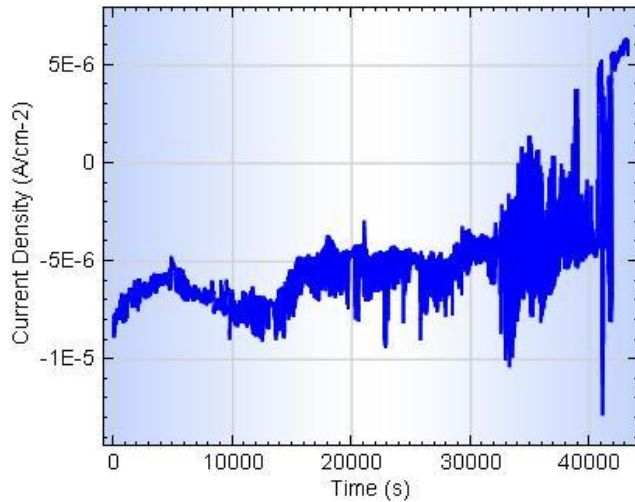


After 168 h

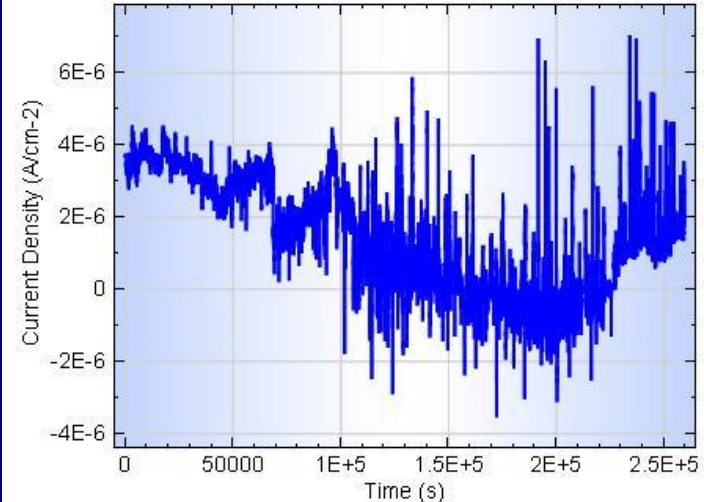


# Typical Current Noise Signatures from Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C

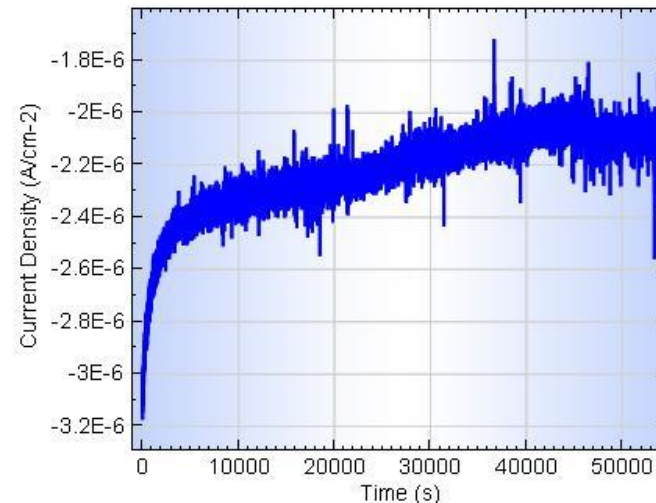
After 24 h



After 72 h



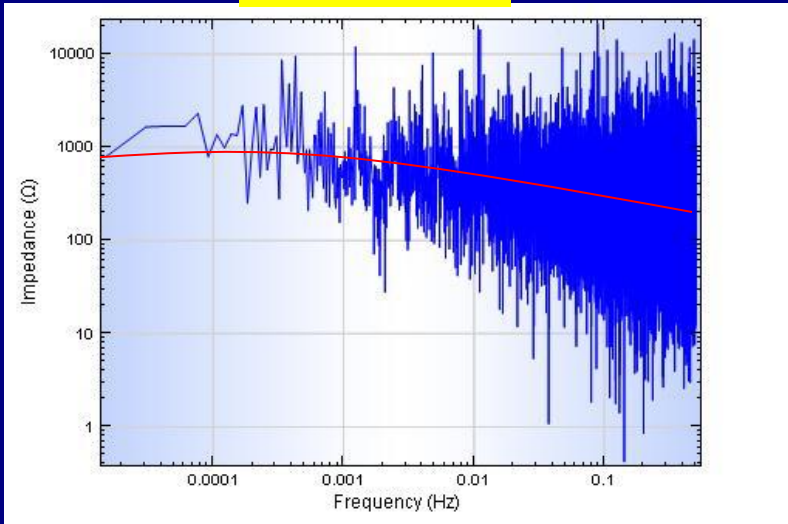
After 168 h



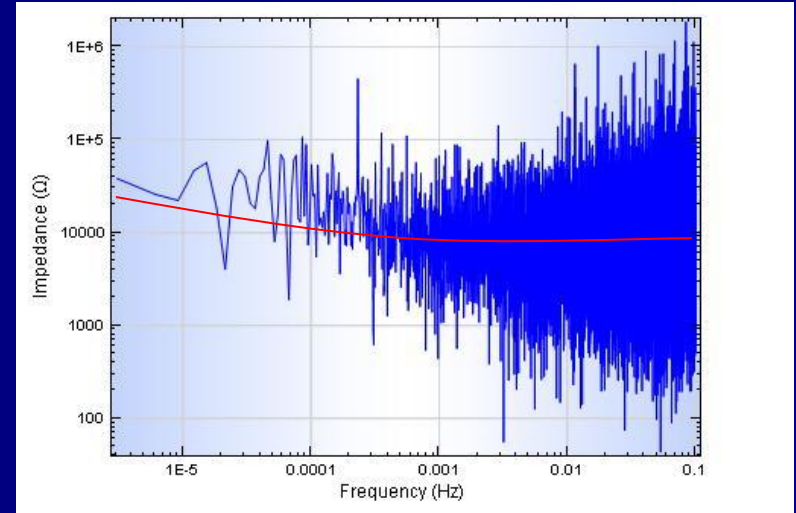


# Typical Noise Impedance from Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C

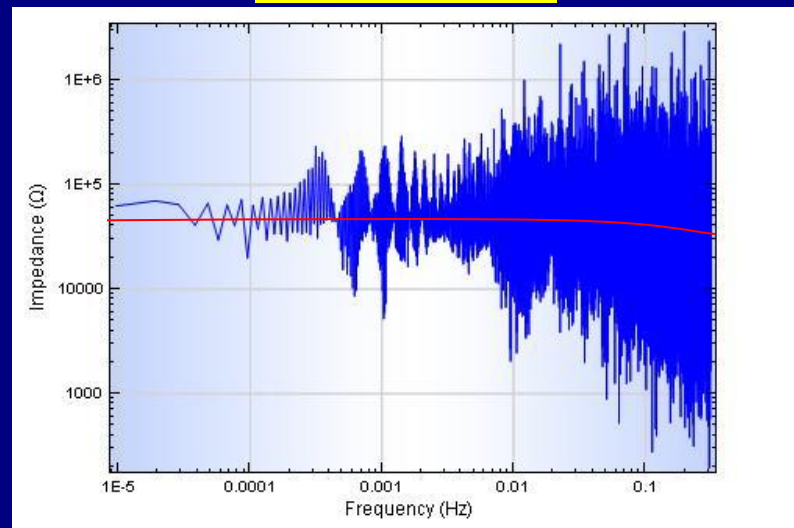
After 24 h



After 72 h



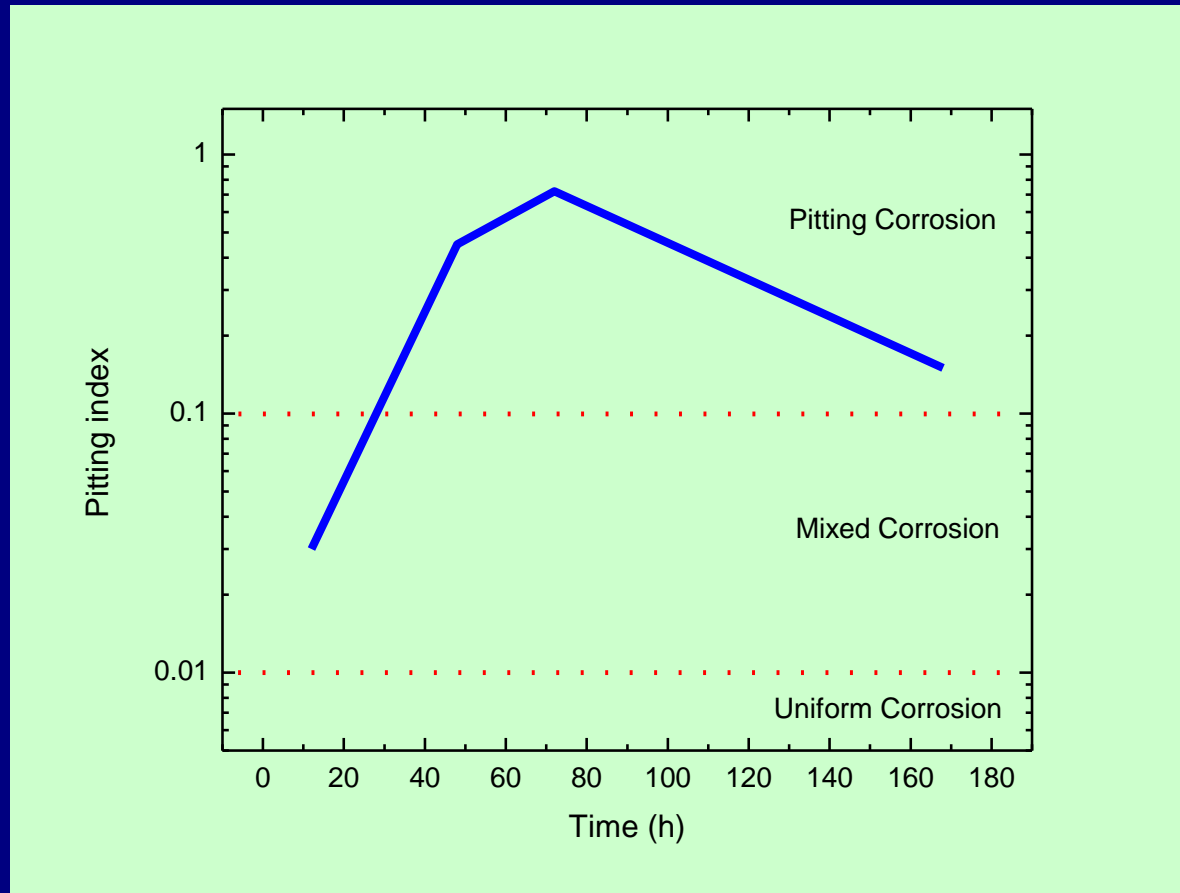
After 168 h



# Noise Resistance for Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C

	Exposure Time (h)	Noise Resistance ( $R_n$ ) (k $\Omega$ )
Pit initiation	24	1.46
Pit propagation	72	30.13
Stable pit formation	168	112.183

# Pitting Index for Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C



PI = 0 , the individual current  $x_i$  show only small deviations from the mean value of current

PI = 1 ,  $x_i \gg$  than the mean value of current

# Stern-Geary Linear Approximation



$R_p$  = Resistance obtained from the LPR and EIS techniques

$R_n$  = Resistance obtained from the EN

$B$  = Stern-Geary constant

$\beta_a$  = Anodic Tafel constant

$\beta_c$  = Cathodic Tafel constant

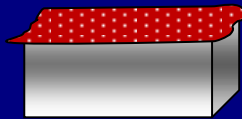
$i_{corr}$  = Corrosion current density

$$\text{Corrosion rate (mm y}^{-1}\text{)} = \frac{3.28M}{n\rho} i_{corr}$$

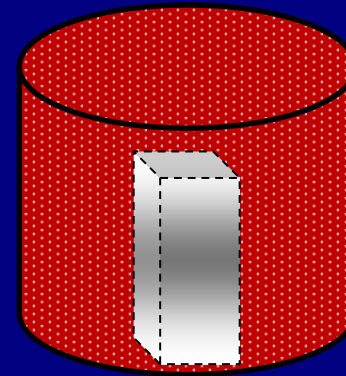
$n$  = Number of electrons freed by the corrosion reaction

$M$  = Atomic mass

# Weight Loss Measurement



For thin coal ash film corrosion



For deep molten coal ash corrosion

$$\text{Corrosion rate (mm y}^{-1}\text{)} = \frac{1}{0.274 \times \rho} \left[ \frac{W_b - W_a - B}{A \cdot t} \right]$$

$W_b$  = Weight of test sample before test, g

$W_a$  = Weight of test sample after test, g

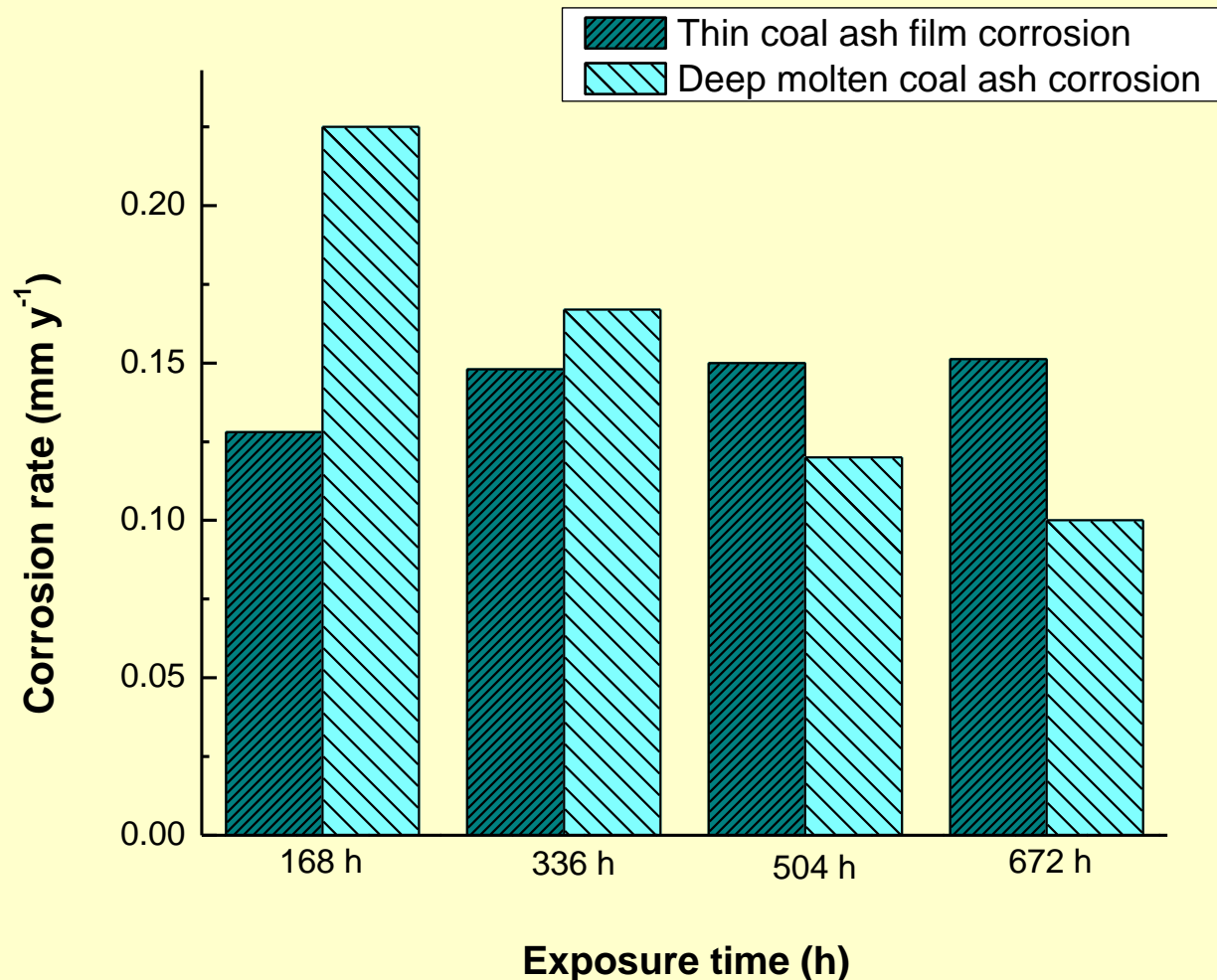
$B$  = Weight loss of blank, g (the average weight loss from 3 unused and clean sample was used as the blank correction)

$A$  = Surface area of sample, cm<sup>2</sup>

$t$  = Exposure time, day

$\rho$  = Density of alloy

# Weight Loss Rates for Deep Molten Coal Ash Corrosion and Thin Coal Ash film Corrosion of IN740-1 Alloy at 800 °C





# Corroded Surfaces for Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C

Before Corrosion



Without Synthetic Flue Gas

After 1 weeks



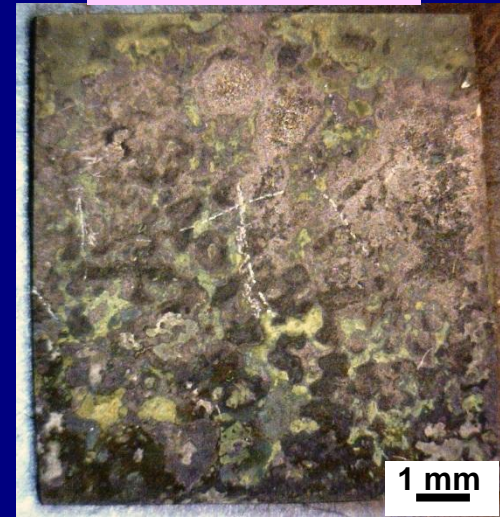
After 2 weeks



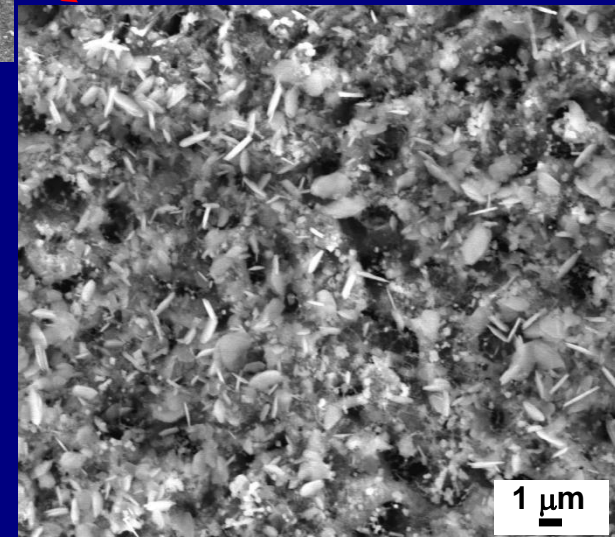
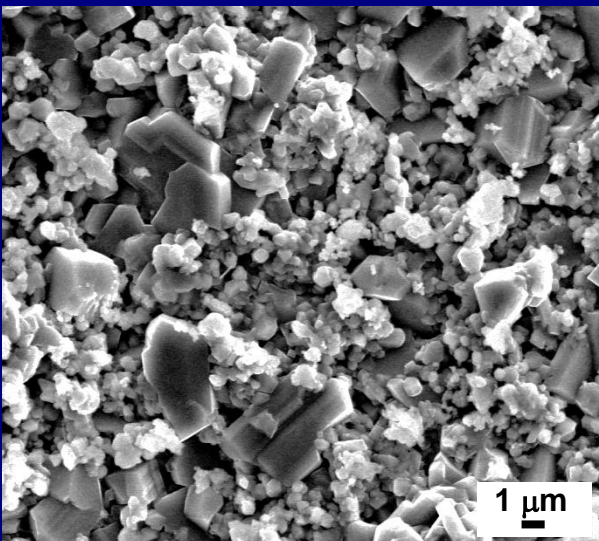
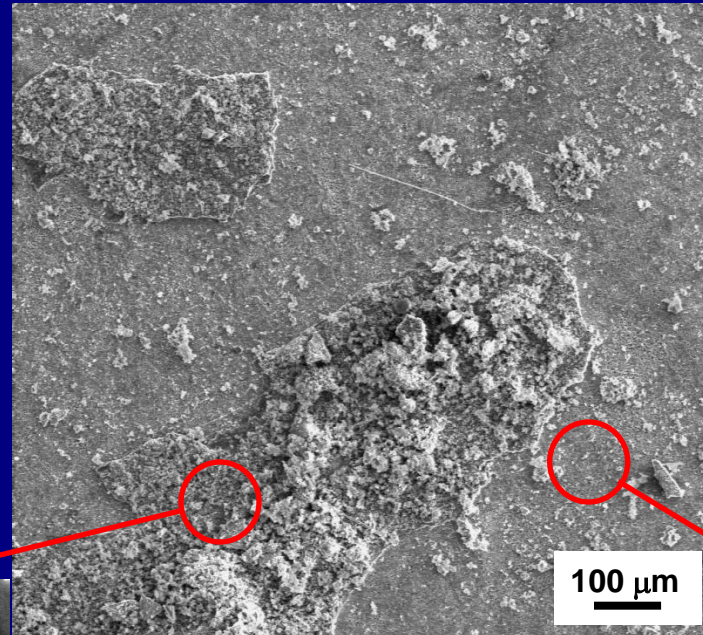
After 3 weeks



After 4 weeks

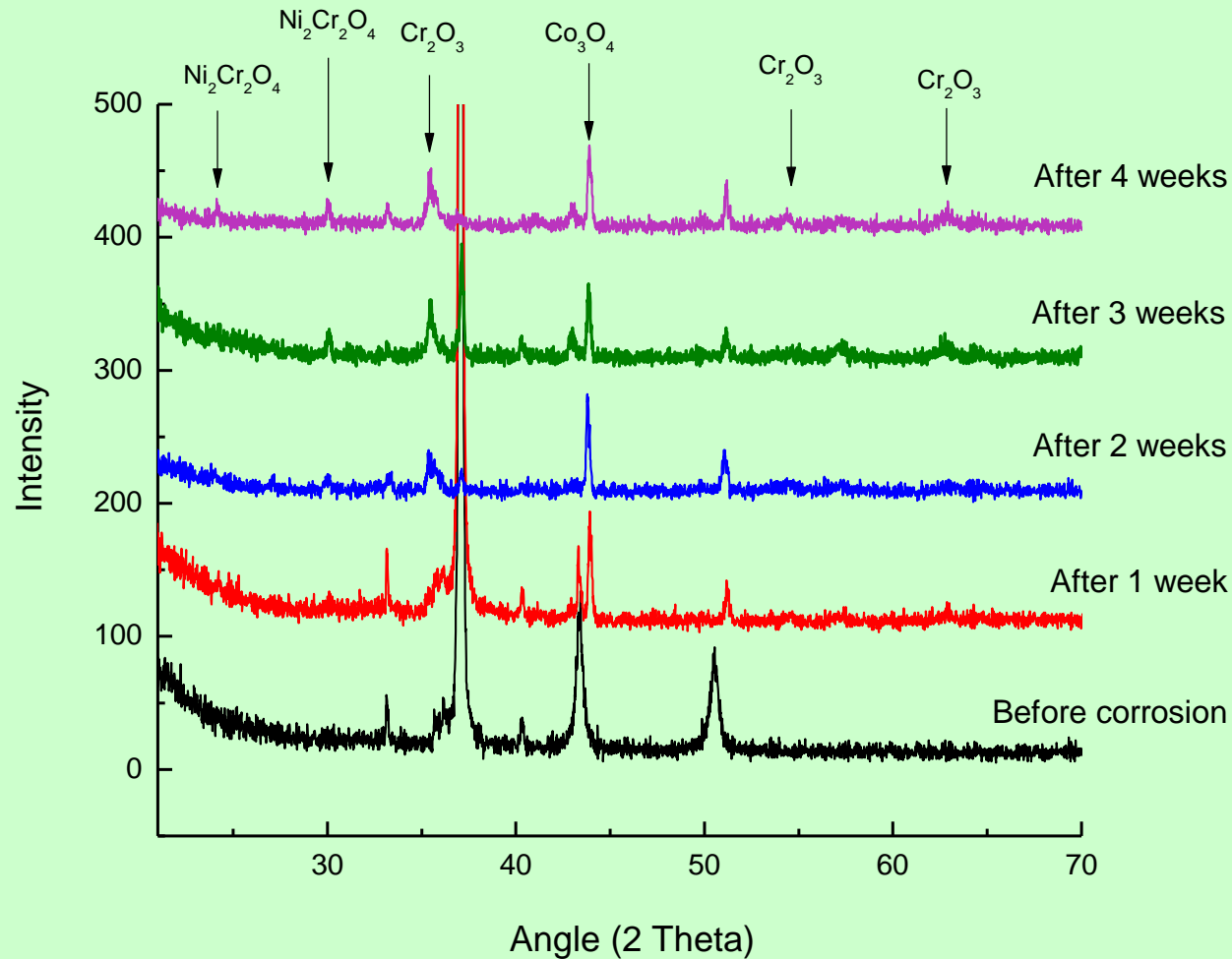


# Oxide Layer Formation on Corroded Surfaces for Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C





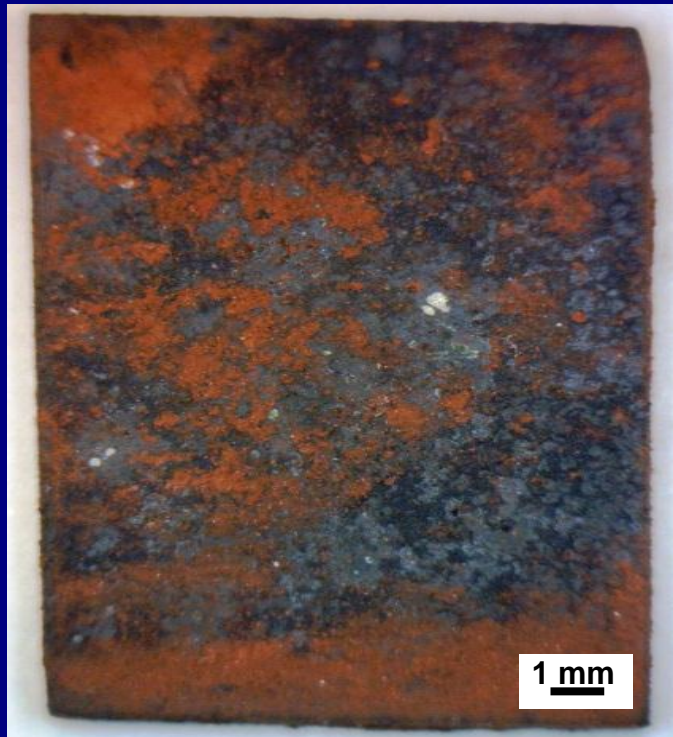
# Oxides Formation on Corroded Surfaces for Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C



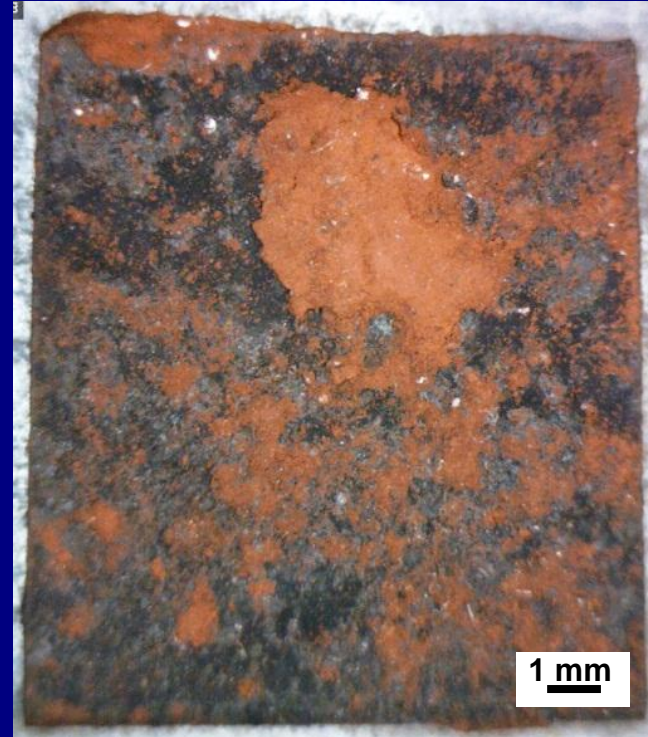
# Corroded Surfaces for Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C

With Synthetic Flue Gas

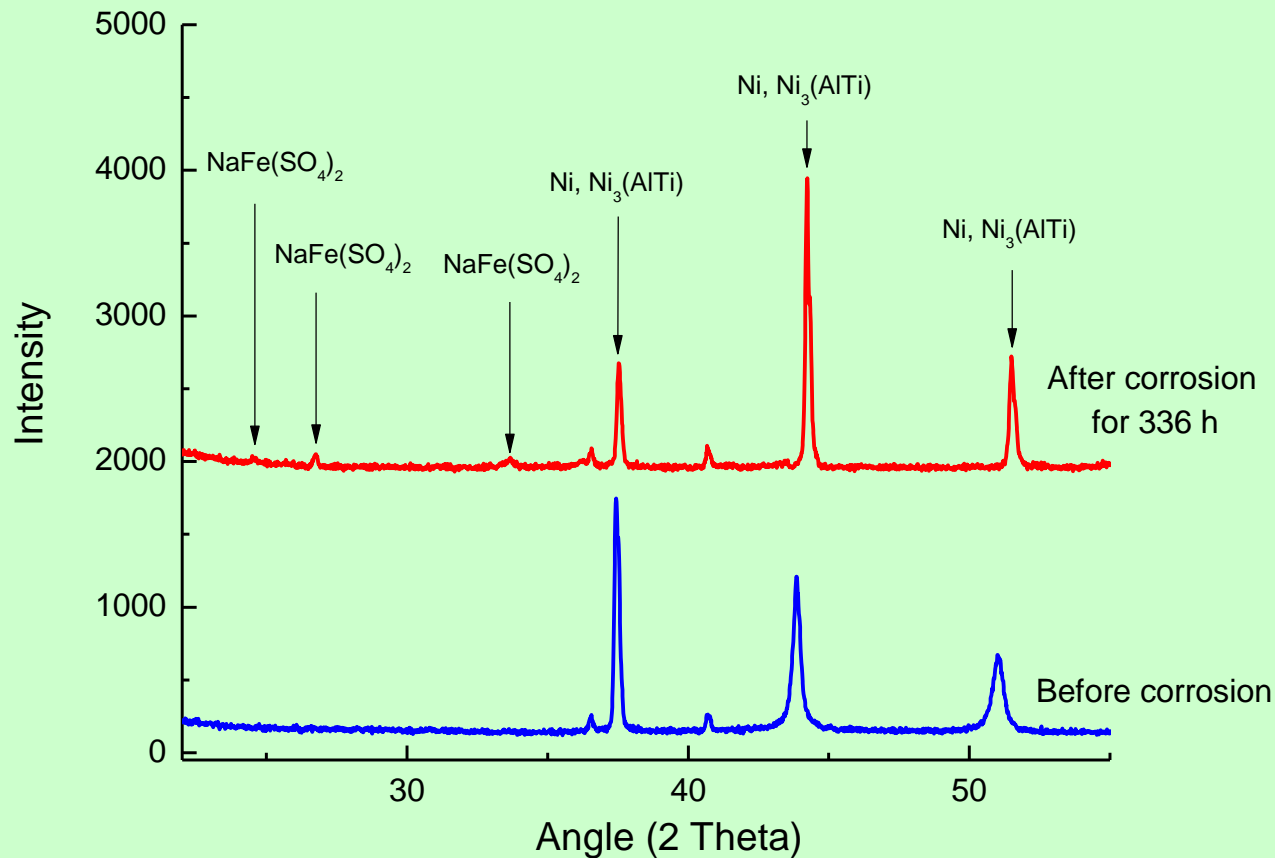
After 1 weeks



After 2 weeks



# Molten Alkali Iron Sulfate Formation During Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C



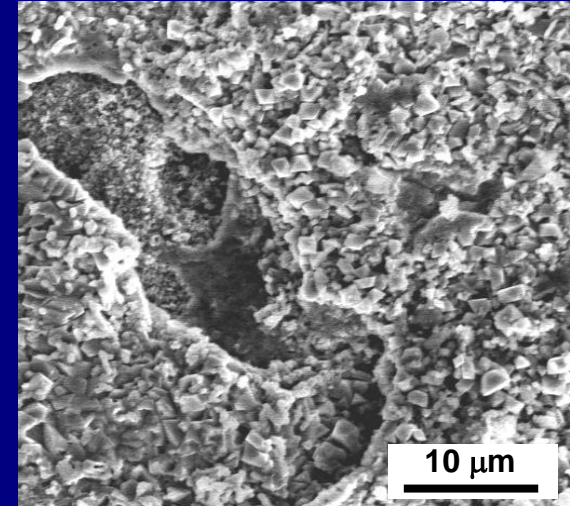
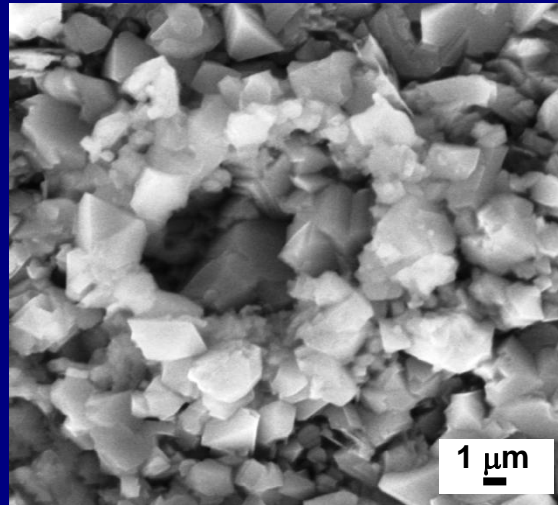
# Pits Formation

## on Corroded Surfaces for Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C

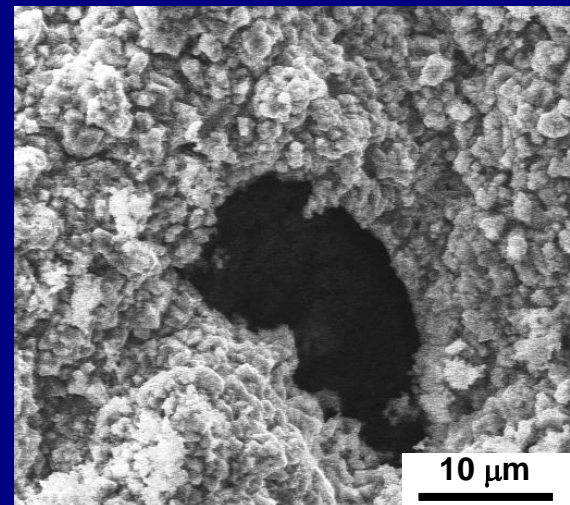
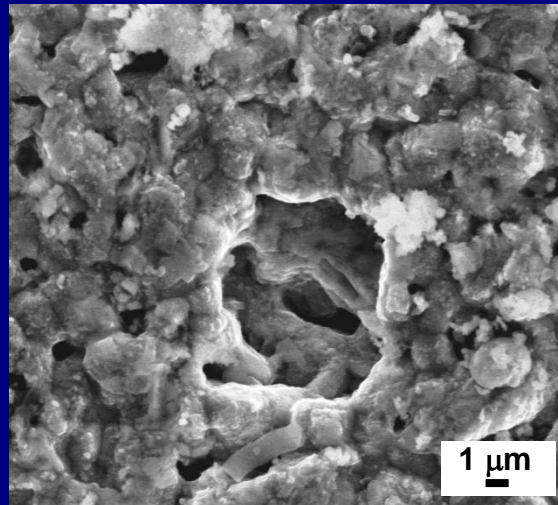
After 1 week

After 2 weeks

Without Synthetic Flue Gas

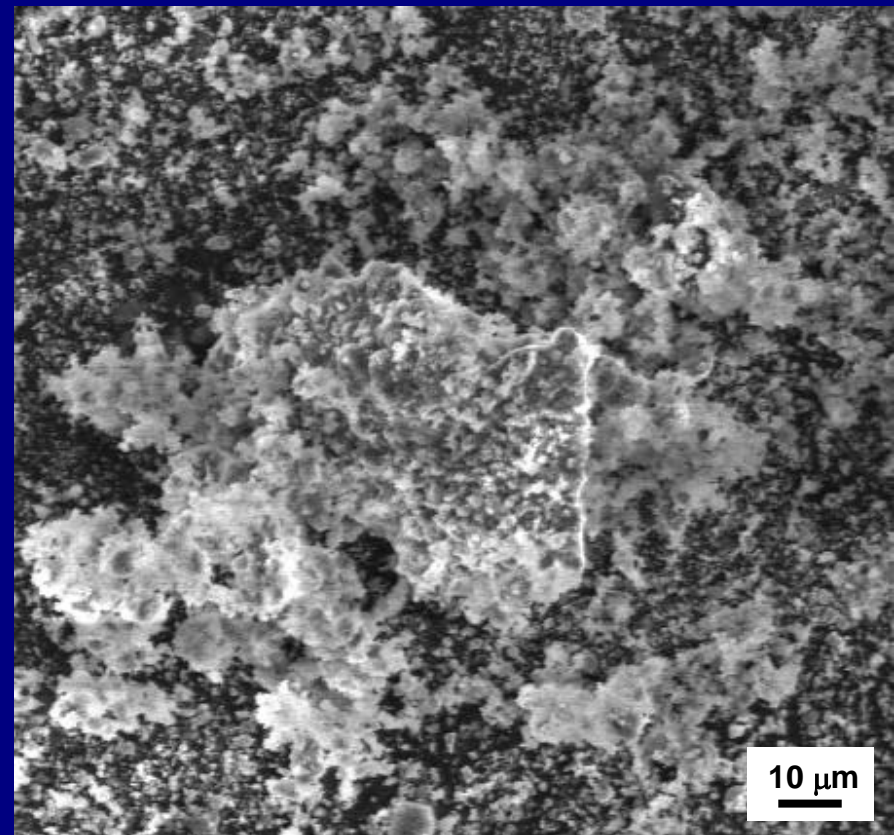
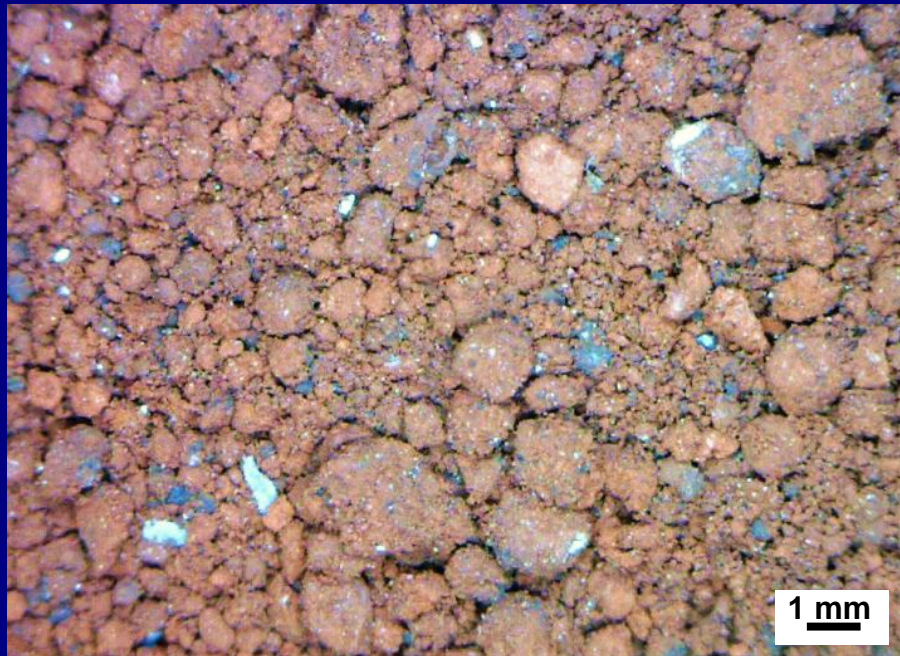


With Synthetic Flue Gas



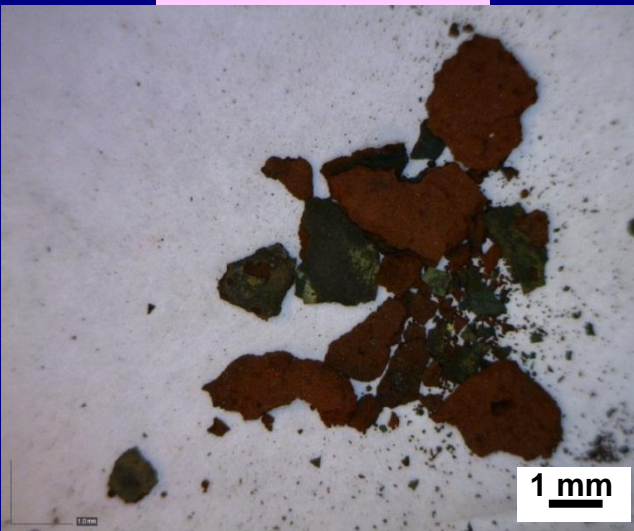


# Corrosion Products in Coal Ash from Deep Molten Coal Ash Corrosion of IN740-1 Alloy at 800 °C

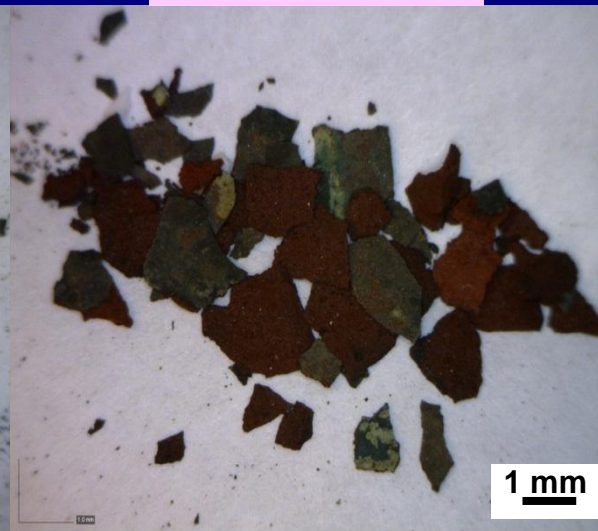


# Corrosion Products in Coal Ash from Thin Coal Ash Film Corrosion of IN740-1 Alloy at 800 °C

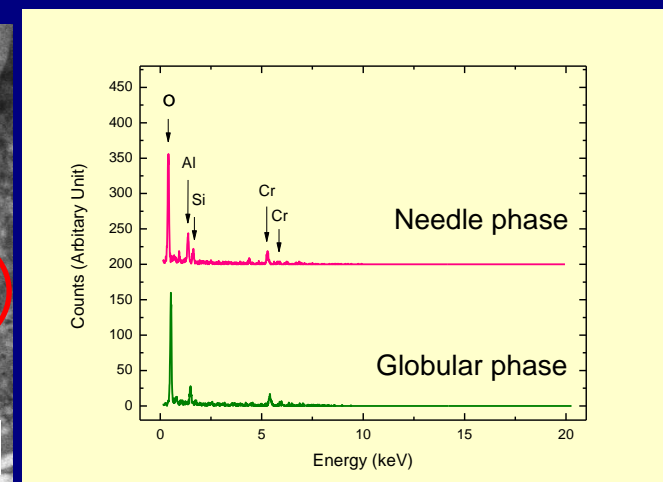
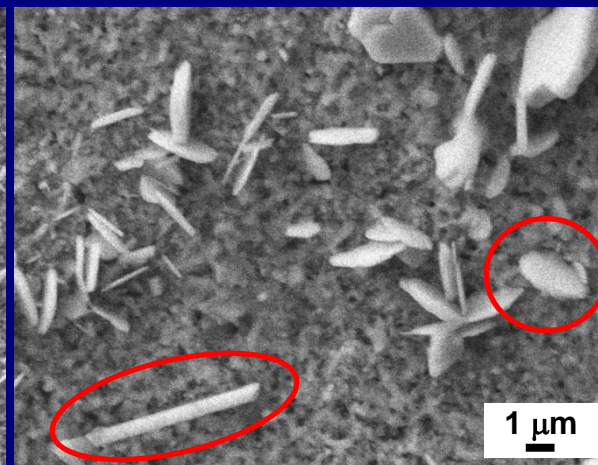
After 2 weeks



After 3 weeks



After 4 weeks





# Coal Ash Corrosion Mechanism

## Initiation Stage

The transport of the oxygen to the alloy surface and the formation of an oxide scale



## Propagation Stage

Formation of porous scale in molten salts and corrosion is controlled by soluble diffusion of the oxidant in the melt



## Stabilization Stage

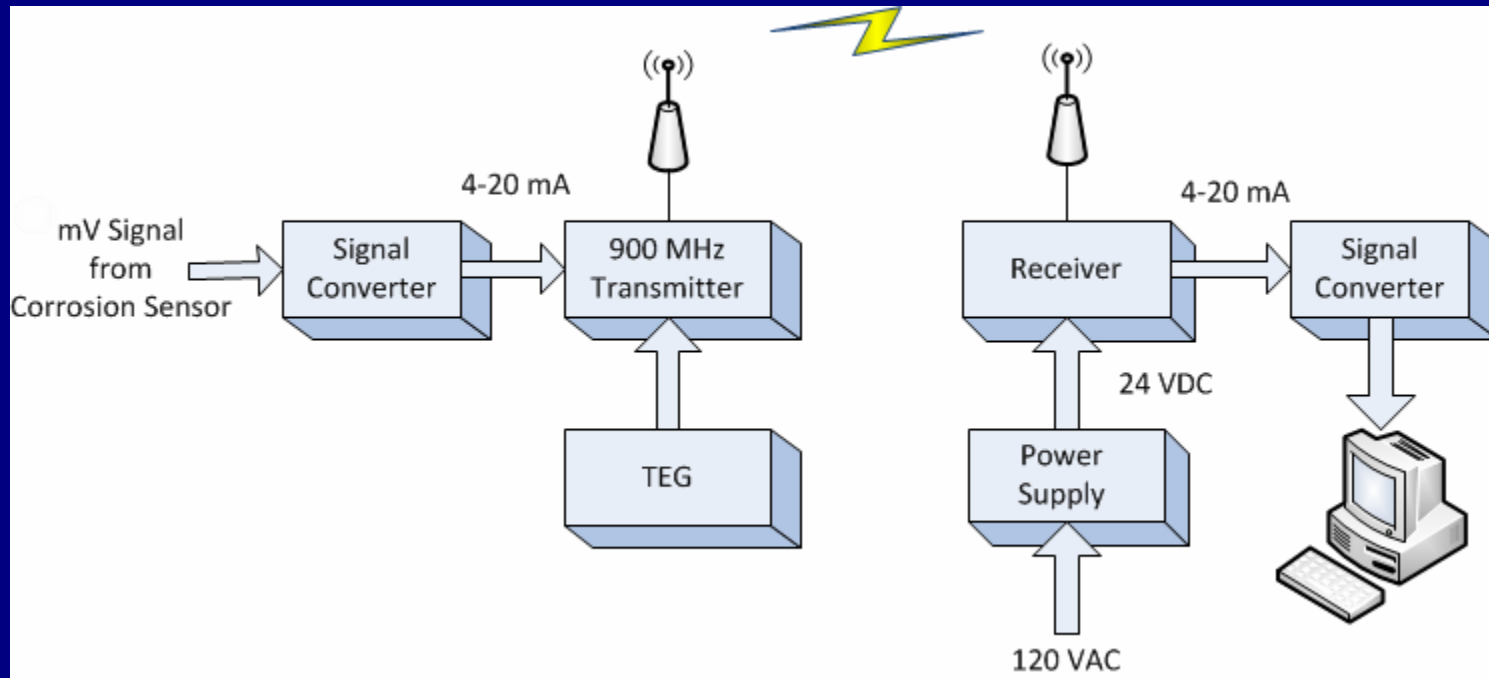
Corrosion is controlled by diffusion of the ions through the scale after forming a compact scale

# Conclusions

- The preliminary results suggest that the developed high temperature corrosion sensor allows accurate analysis of the sample material via several electrochemical techniques.
- Electrochemical and weight loss measurements show that corrosion of IN740-1 alloy in synthesis coal ash mixture at 800 °C was due to localized or pitting corrosion behavior.
- Three different stages of deep molten coal ash corrosion of IN740-1 alloy in synthesis coal ash mixture at 800 °C have been proposed.



# Self-Powered Wireless Communication



## Commercially available hardware

- 1 Watt transmitter - frequency-hopping, spread spectrum technology in the 902-928 MHz ISM band
- Preliminary testing of the thermoelectric generator (TEG) shows a 5 Watt output potential when contacting a surface temperature in the 300° C to 350° C range



## Completed:

- Purchased off-the-shelf TEG and wireless transmitter & receiver
- Demonstrated bench scale feasibility of TEG

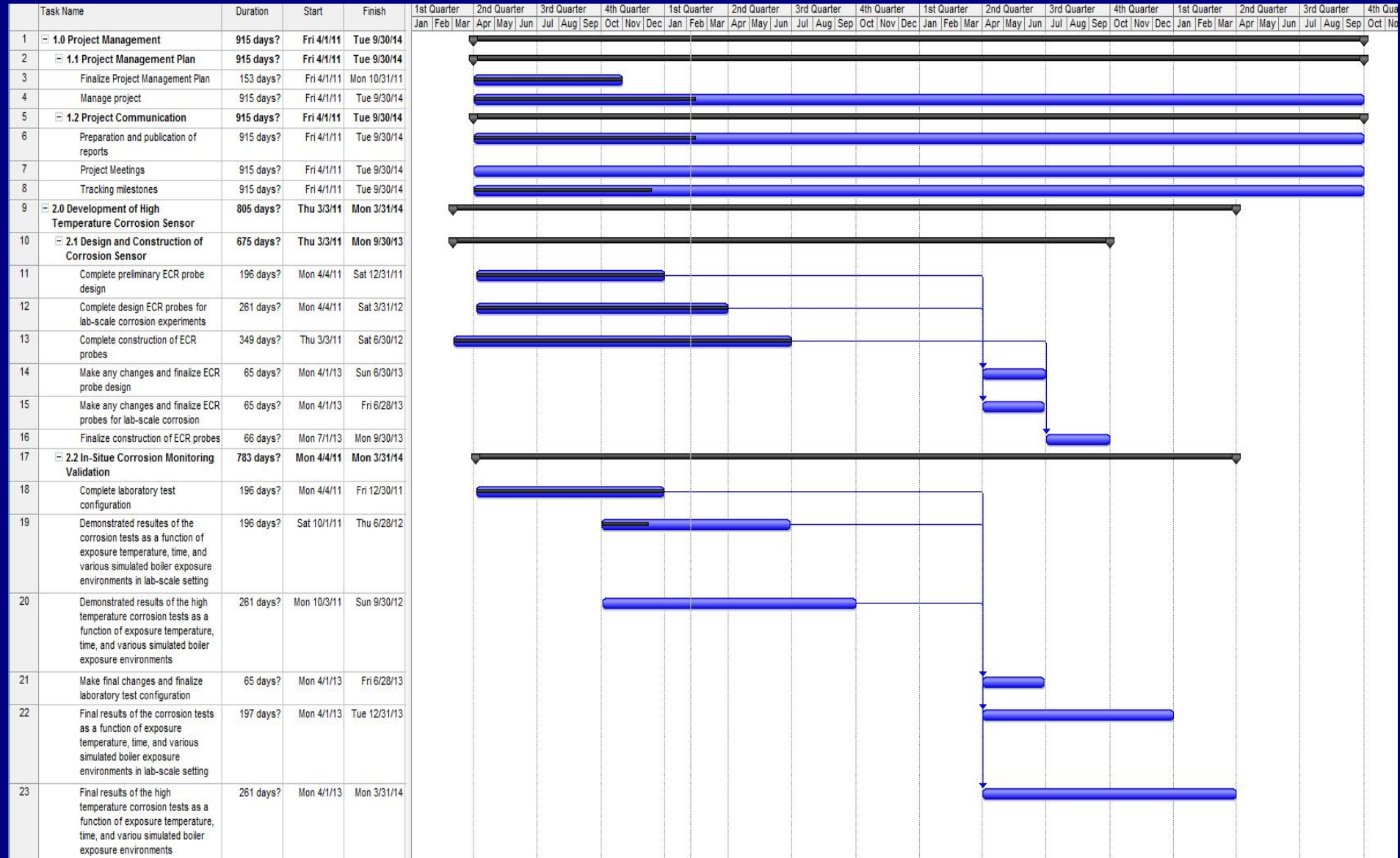
## Next Steps:

- Profile TEG power vs. temperature range
- Demonstrate wireless transmission capability with simulated signal
- Finalize specifications of signal converter for corrosion sensor input
- Complete lab scale demonstration

# Future Work

- Validate results with real-time USC boiler systems
- Extend test results to develop corrosion model for USC boiler systems
- Make alterations to sensor design to include power source and transmitter
- Test sensor reliability and sensitivity for in situ applications

# Milestone Status Report



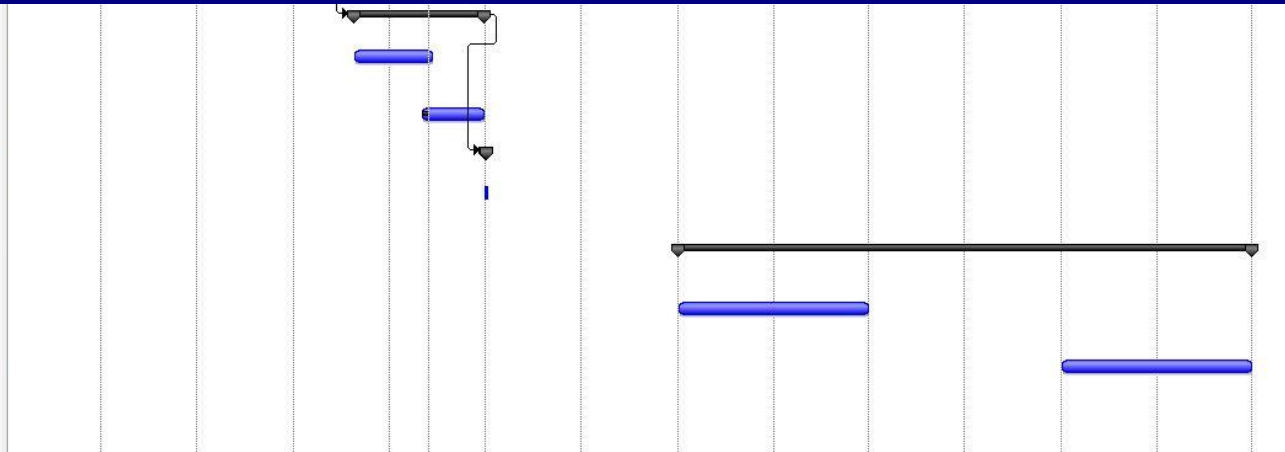
# Milestone Status Report

Task Name	Duration	Start	Finish	1st Quarter			2nd Quarter			3rd Quarter			4th Quarter			1st Quarter			2nd Quarter			3rd Quarter			4th Quarter			1st Quarter			2nd Quarter										
				Jan	Feb	Mar	Apr	May	Jun	Jul	Aug	Sep	Oct	Nov	Dec	Jan	Feb	Mar	Apr	May	Jun	Jul	Aug	Sep	Oct	Nov	Dec	Jan	Feb	Mar	Apr	May	Jun	Jul	Aug	Sep	Oct	Nov	Dec	Jan	Feb
24	2.3 Post Mortem Analysis	522 days?	Sun 4/1/12	Mon 3/31/14	[Gantt bar spanning from Sun 4/1/12 to Mon 3/31/14]																																				
25	Quantify results of corrosion tests and the rate of corrosion development in lab-scale tests	197 days?	Sun 4/1/12	Mon 12/31/12	[Gantt bar spanning from Sun 4/1/12 to Mon 12/31/12]																																				
26	Quantify results of high temperature corrosion tests and the rate of corrosion in lab-scale tests	261 days?	Sun 4/1/12	Sun 3/31/13	[Gantt bar spanning from Sun 4/1/12 to Sun 3/31/13]																																				
27	Final results of corrosion tests and the rate of corrosion development in lab-scale tests	66 days?	Tue 10/1/13	Tue 12/31/13	[Gantt bar spanning from Tue 10/1/13 to Tue 12/31/13]																																				
28	Final results of high temperature corrosion tests and the rate of corrosion in lab-scale tests	130 days?	Tue 10/1/13	Mon 3/31/14	[Gantt bar spanning from Tue 10/1/13 to Mon 3/31/14]																																				
29	3.0 Electrochemical Modeling and Predictive Model Development	522 days?	Sun 4/1/12	Mon 3/31/14	[Gantt bar spanning from Sun 4/1/12 to Mon 3/31/14]																																				
30	3.1 Develop Electrochemical Model to Characterize the General Corrosion of Boiler Tube	392 days?	Sun 4/1/12	Mon 9/30/13	[Gantt bar spanning from Sun 4/1/12 to Mon 9/30/13]																																				
31	Predictive model to characterize the performance and life expectation of materials under lab-scale simulated USC operating conditions	326 days?	Sun 4/1/12	Sun 6/30/13	[Gantt bar spanning from Sun 4/1/12 to Sun 6/30/13]																																				
32	Validate model with data obtained under industrial USC operating conditions	392 days?	Sun 4/1/12	Mon 9/30/13	[Gantt bar spanning from Sun 4/1/12 to Mon 9/30/13]																																				
33	3.2 Develop Predictive System for Localized Corrosion in the Boiler Tubes	522 days?	Sun 4/1/12	Mon 3/31/14	[Gantt bar spanning from Sun 4/1/12 to Mon 3/31/14]																																				
34	Develop method to detect localized corrosion via EN and EIS	458 days?	Sun 4/1/12	Tue 12/31/13	[Gantt bar spanning from Sun 4/1/12 to Tue 12/31/13]																																				
35	Confirm method to identify nature of corrosion products	522 days?	Sun 4/1/12	Mon 3/31/14	[Gantt bar spanning from Sun 4/1/12 to Mon 3/31/14]																																				
36	4.0 Development of Self-Powered Hardware Selection and Modeling of TEG Array	177 days?	Mon 8/1/11	Sun 4/1/12	[Gantt bar spanning from Mon 8/1/11 to Sun 4/1/12]																																				
37	4.1 Hardware selection and design of TEG array	86 days?	Mon 8/1/11	Fri 11/25/11	[Gantt bar spanning from Mon 8/1/11 to Fri 11/25/11]																																				
38	Identify and purchase commercial hardware for wireless transmission of sensor data	43 days?	Mon 8/1/11	Wed 9/28/11	[Gantt bar spanning from Mon 8/1/11 to Wed 9/28/11]																																				
39	Hardware ordered	1 day?	Thu 9/29/11	Thu 9/29/11	[Gantt bar spanning from Thu 9/29/11 to Thu 9/29/11]																																				
40	Hardware received	1 day?	Mon 8/29/11	Mon 8/29/11	[Gantt bar spanning from Mon 8/29/11 to Mon 8/29/11]																																				
41	Identify, purchase and evaluate TEG	66 days?	Mon 8/29/11	Fri 11/25/11	[Gantt bar spanning from Mon 8/29/11 to Fri 11/25/11]																																				
42	Hardware ordered	1 day?	Mon 8/29/11	Mon 8/29/11	[Gantt bar spanning from Mon 8/29/11 to Mon 8/29/11]																																				
43	Hardware received	1 day?	Wed 9/21/11	Wed 9/21/11	[Gantt bar spanning from Wed 9/21/11 to Wed 9/21/11]																																				
44	4.2 Demonstrate TEG and wireless communication system	90 days?	Mon 11/28/11	Fri 3/30/12	[Gantt bar spanning from Mon 11/28/11 to Fri 3/30/12]																																				
45	Demonstrate the wireless communication system functionality in lab-scale tests	55 days?	Mon 11/28/11	Fri 2/10/12	[Gantt bar spanning from Mon 11/28/11 to Fri 2/10/12]																																				
46	Demonstrate the TEG functionality via lab-scale tests	44 days?	Tue 1/31/12	Fri 3/30/12	[Gantt bar spanning from Tue 1/31/12 to Fri 3/30/12]																																				



# Milestone Status Report

44	4.2 Demonstrate TEG and wireless communication system	90 days?	Mon 11/28/11	Fri 3/30/12
45	Demonstrate the wireless communication system functionality in lab-scale tests	55 days?	Mon 11/28/11	Fri 2/10/12
46	Demonstrate the TEG functionality via lab-scale tests	44 days?	Tue 1/31/12	Fri 3/30/12
47	4.3 Demonstrate TEG and wireless communication system	1 day?	Sun 4/1/12	Sun 4/1/12
48	Demonstrate wireless/TEG functionality under USC operating conditions	1 day?	Sun 4/1/12	Sun 4/1/12
49	5.0 In-Situ Corrosion Monitoring Testing in Industrial USC Boiler Setting	391 days?	Mon 10/1/12	Mon 3/31/14
50	Determine reliability and precision of corrosion sensors operating in industrial USC boiler conditions	130 days?	Mon 10/1/12	Sun 3/31/13
51	Optimize sensor construction and corrosion model development	130 days?	Tue 10/1/13	Mon 3/31/14





*Thank You*