

# A Study of H<sub>2</sub>S and PH<sub>3</sub> Effects on Alternative Anodes for Solid Oxide Fuel Cells

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### Background

#### Part 1: SMM Anode for PH, Tolerance

• Recent studies have shown that nickel-based anodes degrade rapidly in the presence of ppm levels of phosphine (PH<sub>3</sub>). Phosphine can cause loss in the cell performance primarily by:

- Ni catalyst fouling due to formation of secondary phases

- Changes in cell micro-structure (Ni migration to anode surface etc.)

• The objective of this work is to identify an oxide anode that shows tolerance to  $PH_3$ .

• Sr<sub>2</sub>MgMoO<sub>6- $\delta$ </sub> (SMM)\* powder was synthesized and fuel cell tests were conducted in syngas, H<sub>2</sub>, and H<sub>2</sub> containing 10 ppm PH<sub>3</sub> on electrolyte-supported cells.

#### Part 2: Ni/GDC Anode for H, S Tolerance

• H<sub>2</sub>S has also been shown to degrade the standard Ni/YSZ anode. The Ni/GDC anode however can withstand ppm levels of H<sub>2</sub>S without irreversible harm to the cell.

• The emphasis of this work was on the development and testing of a Ni/GDC anode with a GDC barrier layer at the active interface for evaluation of H<sub>2</sub>S tolerance.

\* Y.H. Huang, R.I. Dass, J.C. Denyszyn, J.B. Goodenough, J. Electrochem. Soc. 153 (2006) A1266

# **Cell Fabrication**

### Powder Synthesis for SMM Fuel Cells

• The SMM powder was made via a solid-state synthesis method.

- SrCO<sub>3</sub>, MgO, MoO<sub>3</sub> was used as raw materials.
- Calcination was completed at 1200°C for 4 hours.
- BET surface area = 4.711 m<sup>2</sup>/g.



### Architectures for SMM and Ni/GDC Fuel Cells

#### SMM Cell

SMM/GDC – 40 µm thickness

Barrier Layer – GDC – 5 μm

Electrolyte – YSZ (8 mol % Y) – 100 μm

Active Cathode - LSM/GDC – 10 μm

Cathode Current Collector- LSM – 40 μm

Ni/GDC Cell Active Anode - 50/50 wt % NiO/GDC – 10 μm Current Collection – 70/30 wt % NiO/GDC – 40 μm Barrier Layer – GDC – 5 μm Electrolyte – YSZ (8 mol %Y) – 100 μm Active Cathode - LSM/GDC – 10 μm Cathode Current Collector- LSM – 4ο μm











# Experimental Results for the SMM Anode





• Cell showed stability in wet H, for ~20 hrs. Upon adding 10 ppm PH, cell remained stable for ~40 hrs (1 mV drop). However, after 40 hrs in PH, increases in both series and polarization resistances occurred to the cell resulting in a loss in cell performance.



• PH, reduces cell power density by almost 46% after 100 hours exposure.



 SMM exhibits much better tolerance to PH, than the standard Ni/YSZ anode.

• The ultimate goal is to be able to run this cell on coal derived syngas. Initial results indicate a stable cell in syngas for 20 hrs upon switching the fuel stream from wet H, to syngas. The cell however exhibits relatively low performance in syngas compared to wet H<sub>2</sub>.

• The analysis detected a slight presence of phosphorus at the interface. Unlike the Ni/YSZ anode, changes to the anode microstructure are minimal and degradation of the cell is initially attributed to densification of the contact paste as well as possible cell de-lamination upon the introduction of  $10 \text{ ppm PH}_3$ .

• XPS indicates a lack of P2s peak at the active interface.



• SEM images of (a) poisoned Ni/GDC the anode interface, (b) clean reduced Ni/GDC anode interface, (c) Ni particle in the anode interface and (d) GDC particle in the anode interface.

• Verify the behavior of the cell in response to 10 ppm PH<sub>3</sub> and run this cell in fuel containing both H<sub>2</sub>S and PH, contaminants.

• Apply this cell to full size (10 x 10 cm) planar fuel cells for investigation of degradation rates using various flow configurations.



# Experimental Results for the Ni/GDC Anode



• The Ni/GDC cell operated in wet H<sub>2</sub> with increasing levels of H<sub>2</sub>S. In this fuel, the cell remained stable to 500 ppm H<sub>2</sub>S, during a 20 hr testing interval. In 1000 ppm H<sub>2</sub>S, the cell potential dropped almost 15 mV in 20 hrs.

• The ohmic resistance of the cell slowly increased during each level of H<sub>2</sub>S, whereas the polarization resistance increased most during the initial adsorption process and then remained stable thereafter.



• The Ni/GDC anode operating in syngas with and without 100 ppm H<sub>2</sub>S. Cell exhibited stability under these conditions and also did not degrade from cycling of the fuel contaminant.

ime vs V- Clean syngas OCV = 0.971 V Time vs V- Adding 100 ppm H2\$ OCV = 0.974 V Time vs V- Adding 200 ppm H2\$ OCV = 0.977 V Rate = 3.19 mV I 0.892 Ωcm • 0.640 Ωcm<sup>-2</sup> - + Time vs Plorization Resista 100 110 90 80 Time (hou

• The cell did not however maintain stability in 200 ppm H<sub>2</sub>S in syngas. The degradation rate of 3.19 mVhr<sup>-1</sup> suggests that 100 ppm was the limit for this cell in syngas.



• Depth profile of the XPS spectra on the H<sub>2</sub>S poisoned cell Ni surface. Oxidized S peak at 169-170 eV is only significant on the top Ni surface. Unoxidized S peak is detectable at 8 nm depth of Ni surface.

### **SMM Anode**

• Perform thermodynamic calculations to determine what (if any) reactions are anticipated between P and the anode constituents.

## Future Work

#### Ni/GDC Anode

• Determine degradation rates as a function of hydrogen and oxygen partial pressures to determine what fuel composition and contaminant levels are most suitable for operation.

• Identify the role of the barrier layer in tolerance of H<sub>2</sub>S.

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