

Steam Turbine Materials and Corrosion



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Office of Fossil Energy



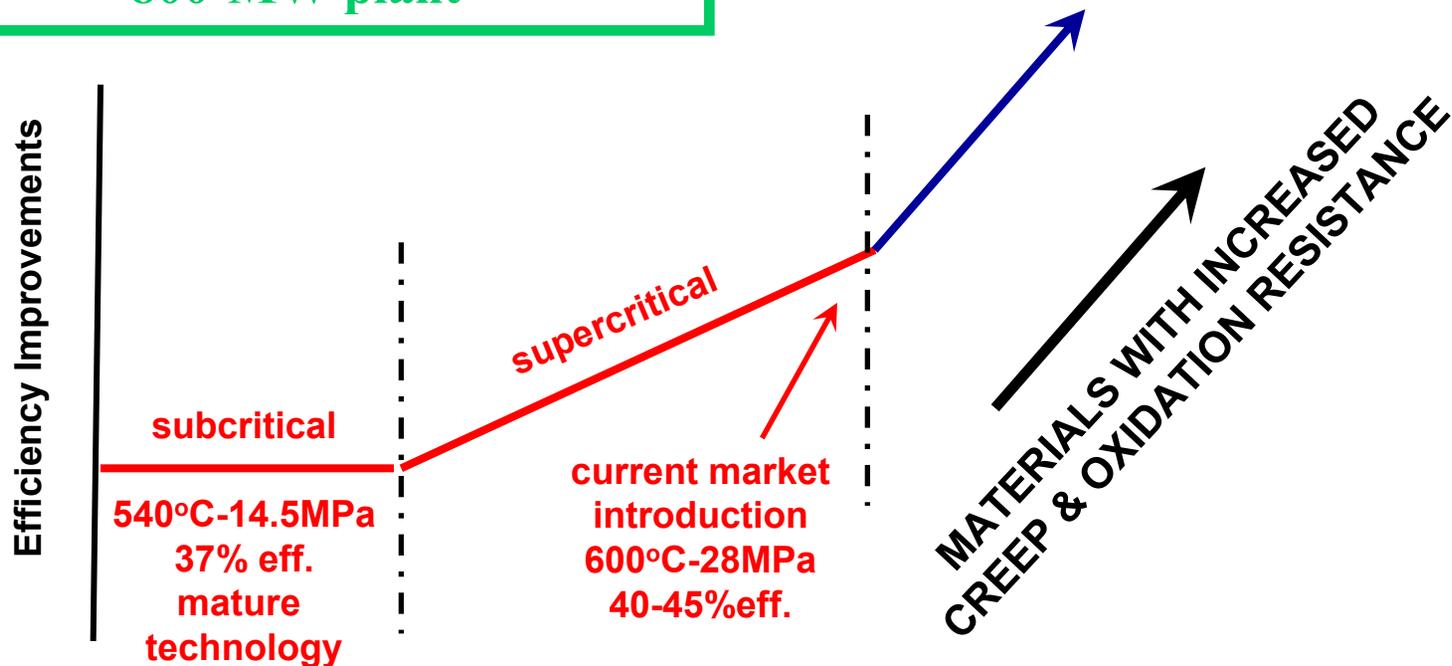
Outline

- **Introduction**
 - Overview
 - Goals
 - Background
 - **Accomplishments**
 - Alloy Behavior
 - Reactive Evaporation of Chromia
 - **Future plans**
 - **Summary**
-

Increasing Efficiency

Each 1% increase in efficiency eliminates ~1,000,000 tons of CO₂ emissions over the lifetime of an 800-MW plant

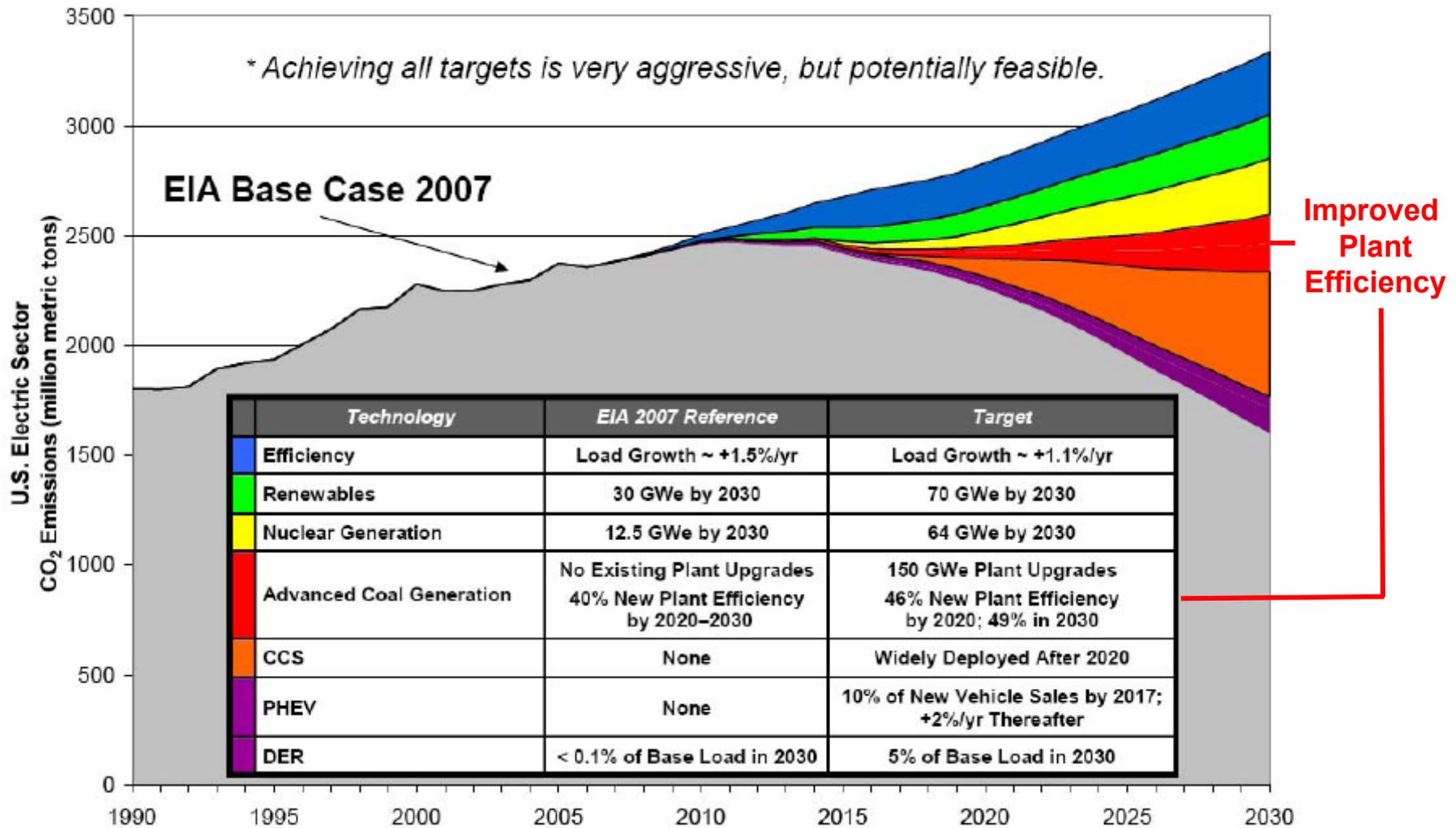
US-DOE Advanced Power System Goal
60% efficiency from coal generation
Steam condition: 760°C – 35 MPa



Plants operating above 22MPa at 538 to 565°C are “supercritical”, and above 565°C are “ultra-supercritical (USC)”.

Adapted from: Viswanathan, et al , 2005 and Swanekamp, 2002

Senate Hearing “The Future of Coal: Options for a Carbon-Constrained World” March 2007, Deutch & Moniz, MIT



Project Goals and Objectives

- **Understand materials degradation in USC steam environments**
 - **Identify or develop viable materials for use in USC steam turbines**
 - **Characterize the steam oxidation resistance of candidate commercial alloys (primarily nickel-base superalloys)**
 - Compliment and not duplicate USC consortium research
 - **Develop steam oxidation models for use in USC steam turbine environments**
 - Chromia evaporation
 - **Project success defined as**
 - Steamside corrosion data sufficient for industry to use in USC turbines (for example in their turbine blade life models)
 - Identify and mitigate unexpected failure mechanisms
-

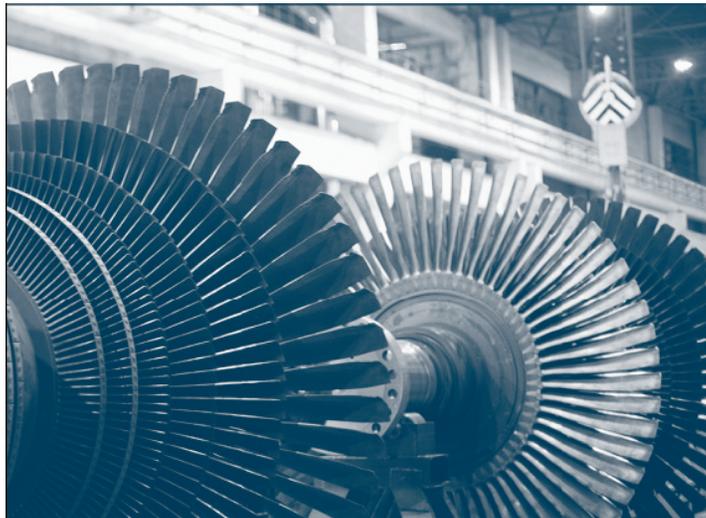
Critical Materials Properties for USC Turbines

- **Rotating Blades**

- High temperature strength
- Creep resistance
- Steam oxidation resistance
- Thermal expansion close to that of the rotors
- Ability to be peened

- **HP and IP Rotors**

- Creep strength
- Low cycle fatigue strength
- Fracture toughness
- Steam oxidation resistance
- Weldability



Cost vs Temperature

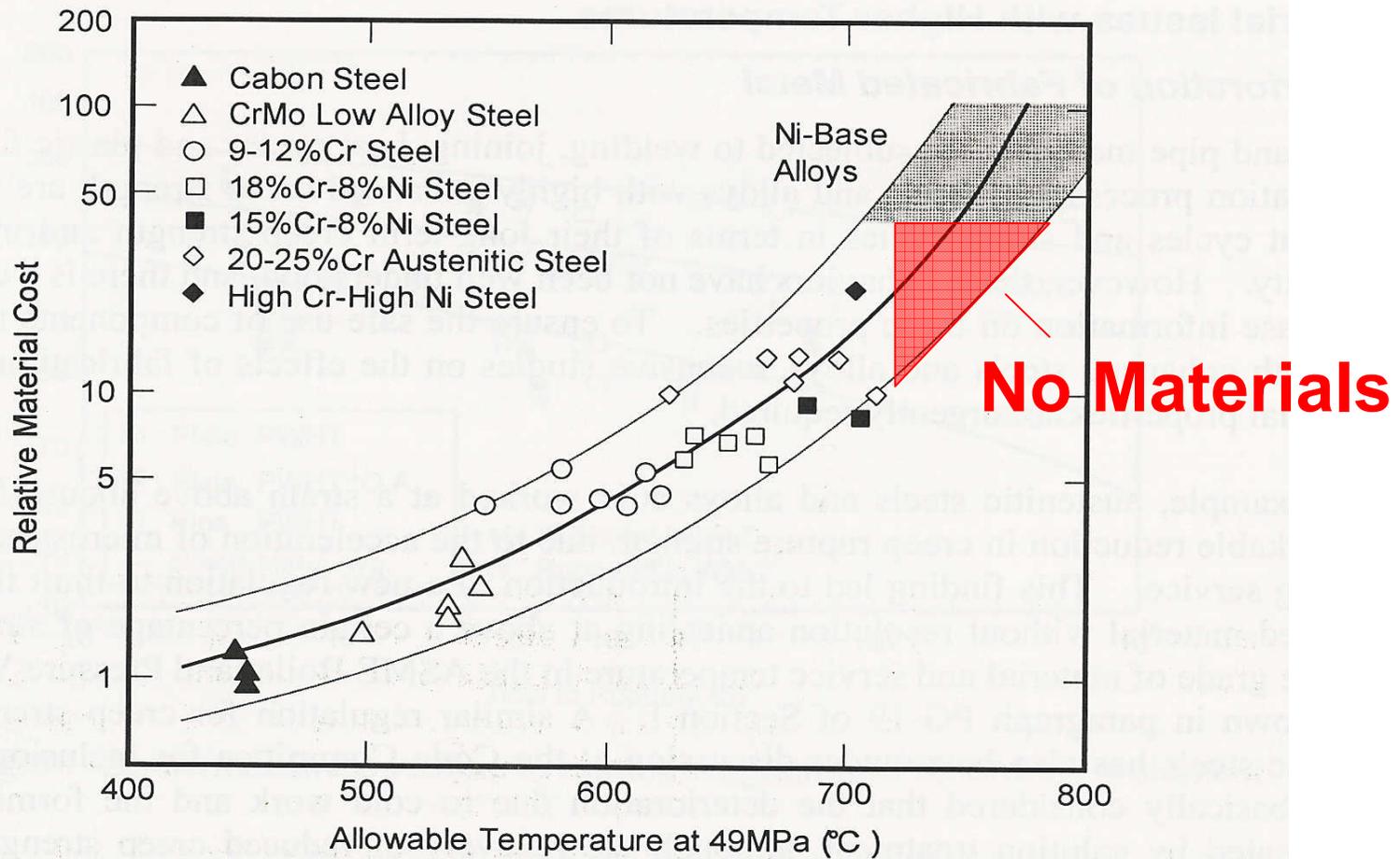


Fig. 7 Relation between allowable metal temperature at the allowable stress of 49MPa and the relative material cost

Commercial Alloys of Interest



Alloy	Class	USC Boiler	EPRI Turbine Candidate	Scholven Unit F Turbine	UK-US	USC Turbine
T92	Fe Ferritic	X			RR	
SAVE12 9.5Cr	Fe Ferritic	X			X	
SAVE12 10.5Cr	Fe Ferritic	X			X	
TP347HFG	Fe Austenitic	X			RR	
HR6W	High Ni & Cr	X				
Haynes 230	Ni Superalloy	X			X	
Haynes 282	Ni Superalloy					X
Inconel 617	Ni Superalloy	X		X	X	
Inconel 625	Ni Superalloy			X	X	
Inconel 718	Ni Superalloy		X		X	
Inconel 740	Ni Superalloy	X			RR	
Nimonic 90	Ni Superalloy		X		X	
Nimonic 105	Ni Superalloy					X
Udimet 720Li	Ni Superalloy					X

Environment and Conditions

Condition	Current Advanced Supercritical	Target Ultra Supercritical	Current Tests	Future Tests
Temperature	560-620°C	760°C	650-800°C	650-800°C
Pressure	280-310 bar	350-385 bar	1 bar	Up to 350 bar
Atmosphere	Steam	Steam	Moist Air	Steam
Gas Velocity	Boiler 10-25 m/s Turbine 300 m/s	Boiler 10-25 m/s Turbine 300 m/s	$\sim 2-8 \times 10^{-3}$ m/s	Up to 40 m/s

Best practices in corrosion testing involves

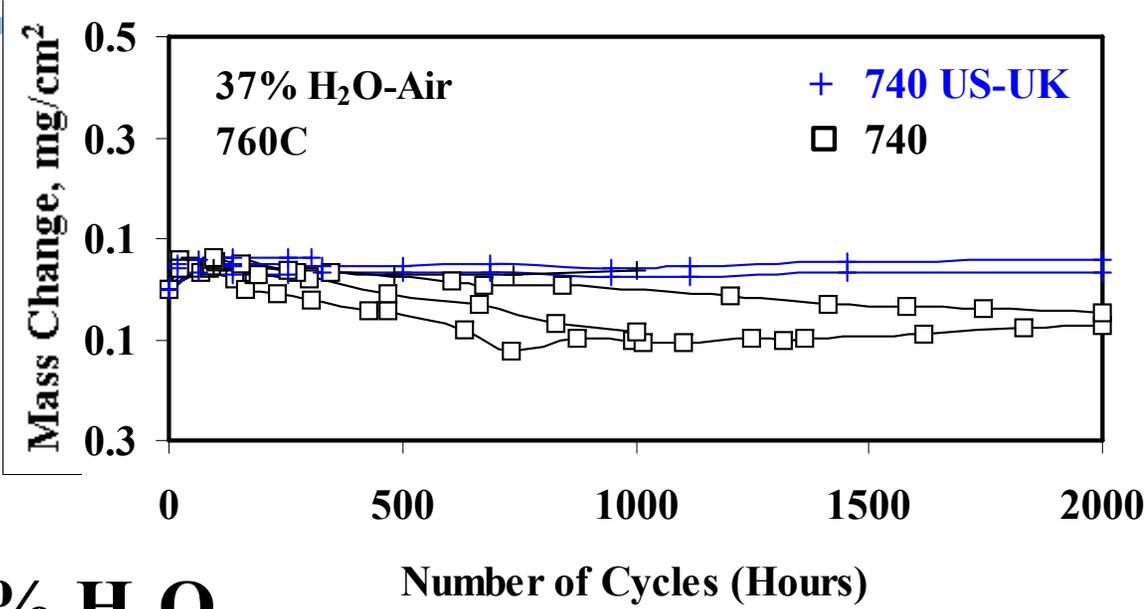
- **Duplication of the environment**
- **Use conditions that give the same corrosion mechanisms**

Commercial Alloy Behavior Result Comparison

760°C after 2000 cycles or hours

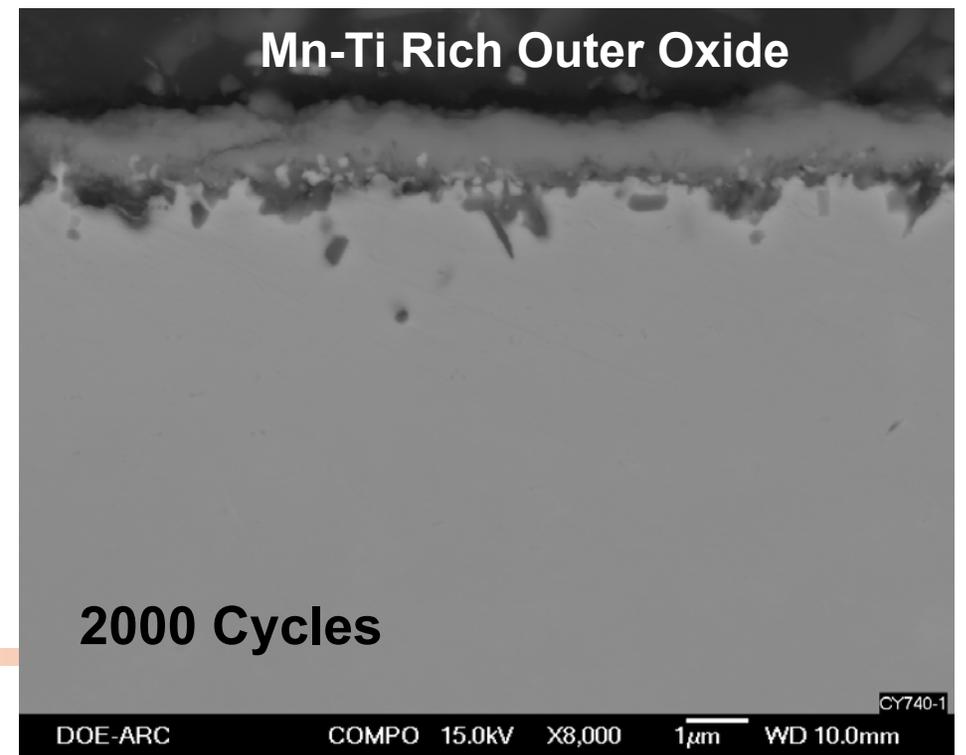
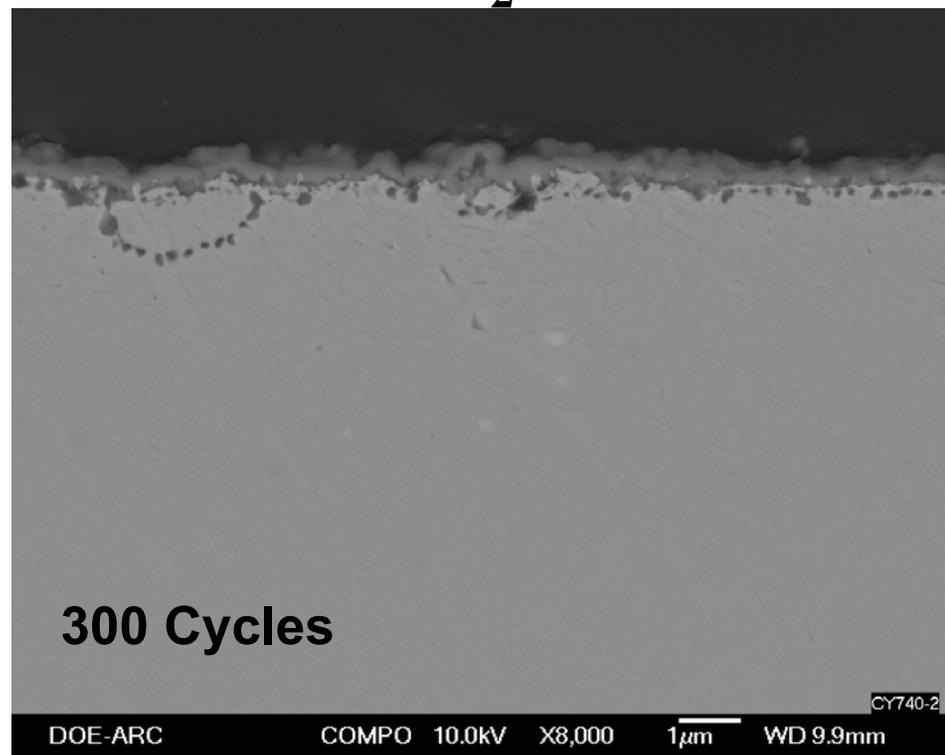
Alloy	Cyclic with Air+40%H ₂ O			Furnace with Air+3%H ₂ O		
	Max Internal Oxidation, μm	Max Scale Thickness, μm	Mass Change, mg/cm^2	Max Internal Oxidation, μm	Max Scale Thickness, μm	Mass Change, mg/cm^2
Haynes 230	12.7	3.1	-0.217	5.1	3.6	0.097
Inconel 617	11.8	4.4	0.008	3.8	2.7	0.118
Inconel 718	6.7	2.9	-0.031	4.0	3.1	0.183
Inconel 740	10.2	2.7	-0.059	5.1	1.8	0.180
Nimonic 90	18.2	6.7	0.363	8.7	3.1	0.818

Inconel 740

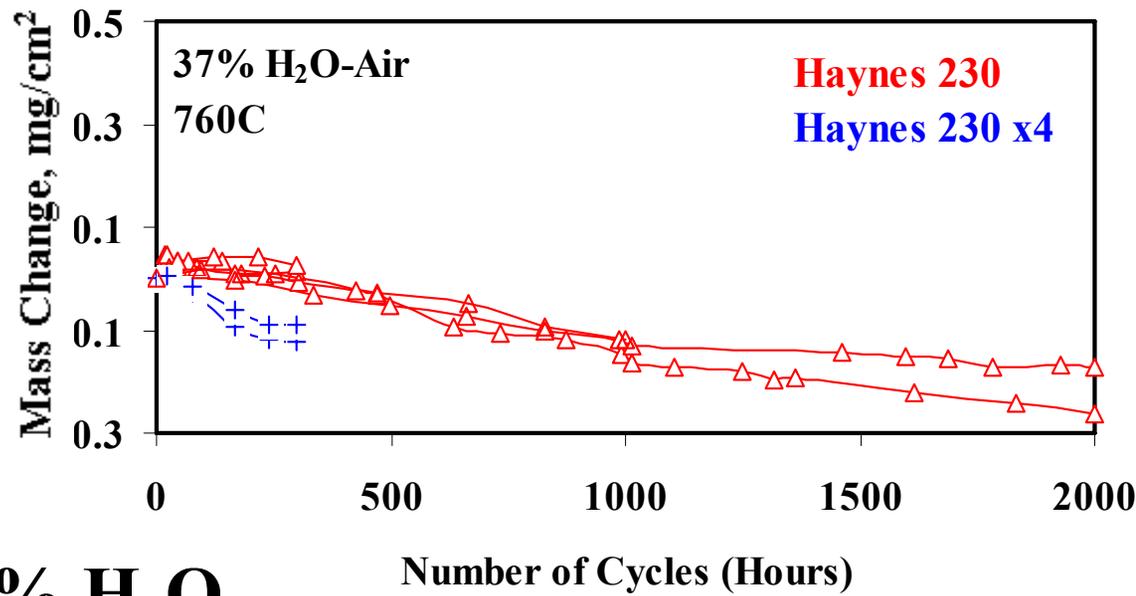


760°C

Air + 37% H₂O

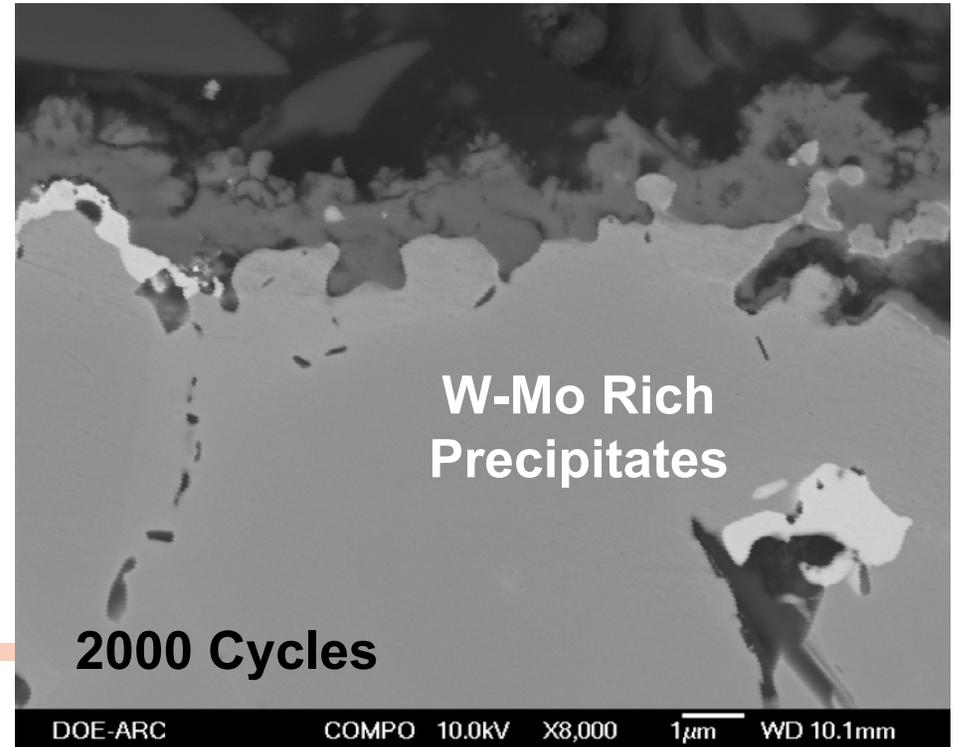
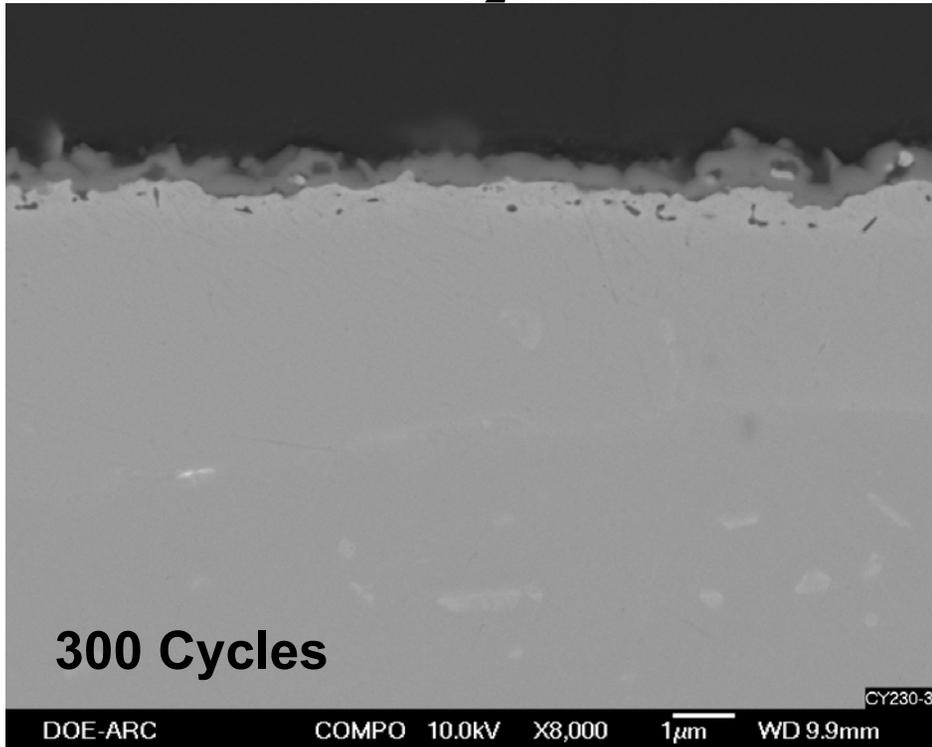


Haynes 230



760°C

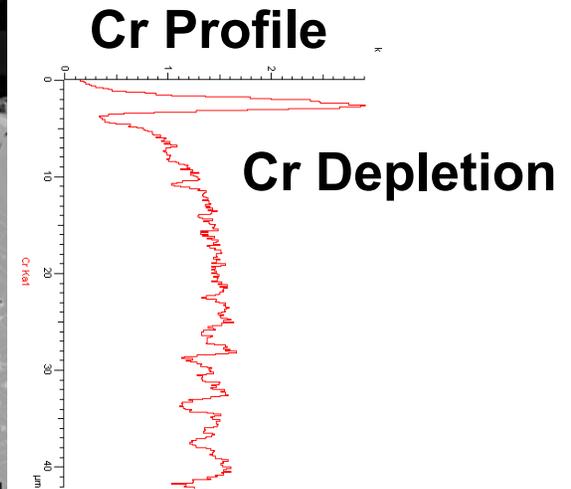
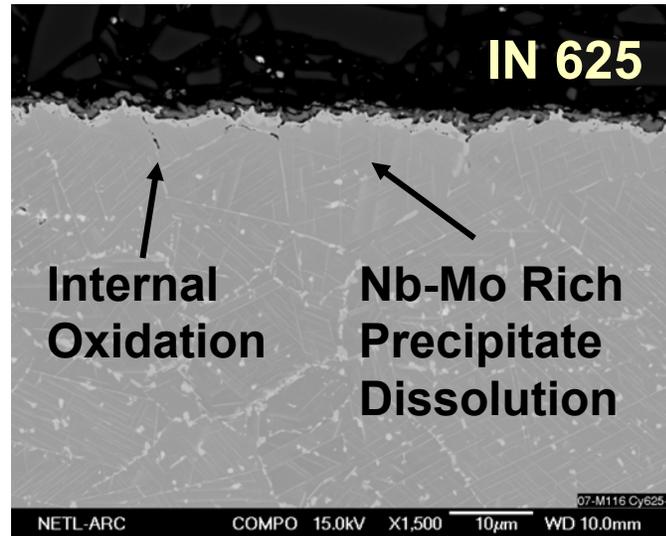
Air + 37% H₂O



Result Comparison

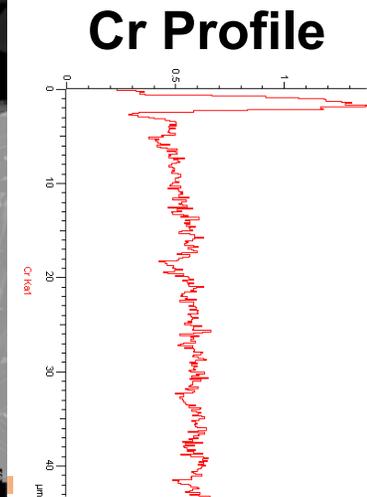
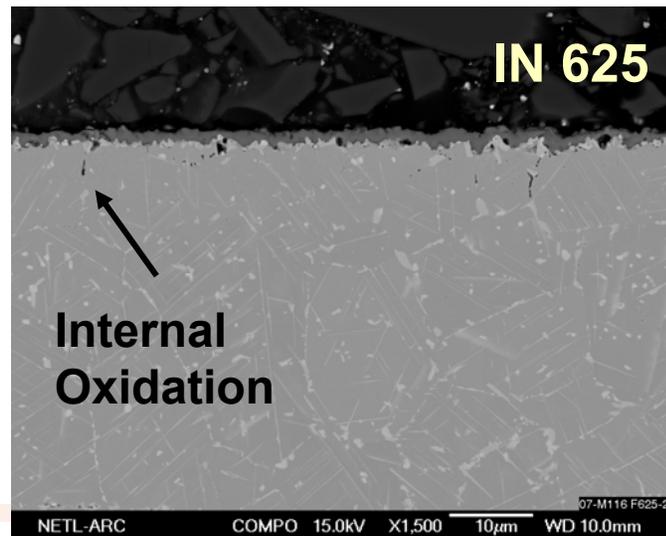
Cyclic Oxidation
2000 Cycles
760°C
Air + 37% H₂O
Low Gas Flow
Boldly Exposed

Cr Evaporation



Furnace Exposure
2000 Hours
800°C
Air + 3% H₂O
Low Gas Flow
Sheltered Exposure

Suppressed Cr Evaporation



Evaporation of Chromia

- Very small effect in dry oxidation until $> 900^{\circ}\text{C}$



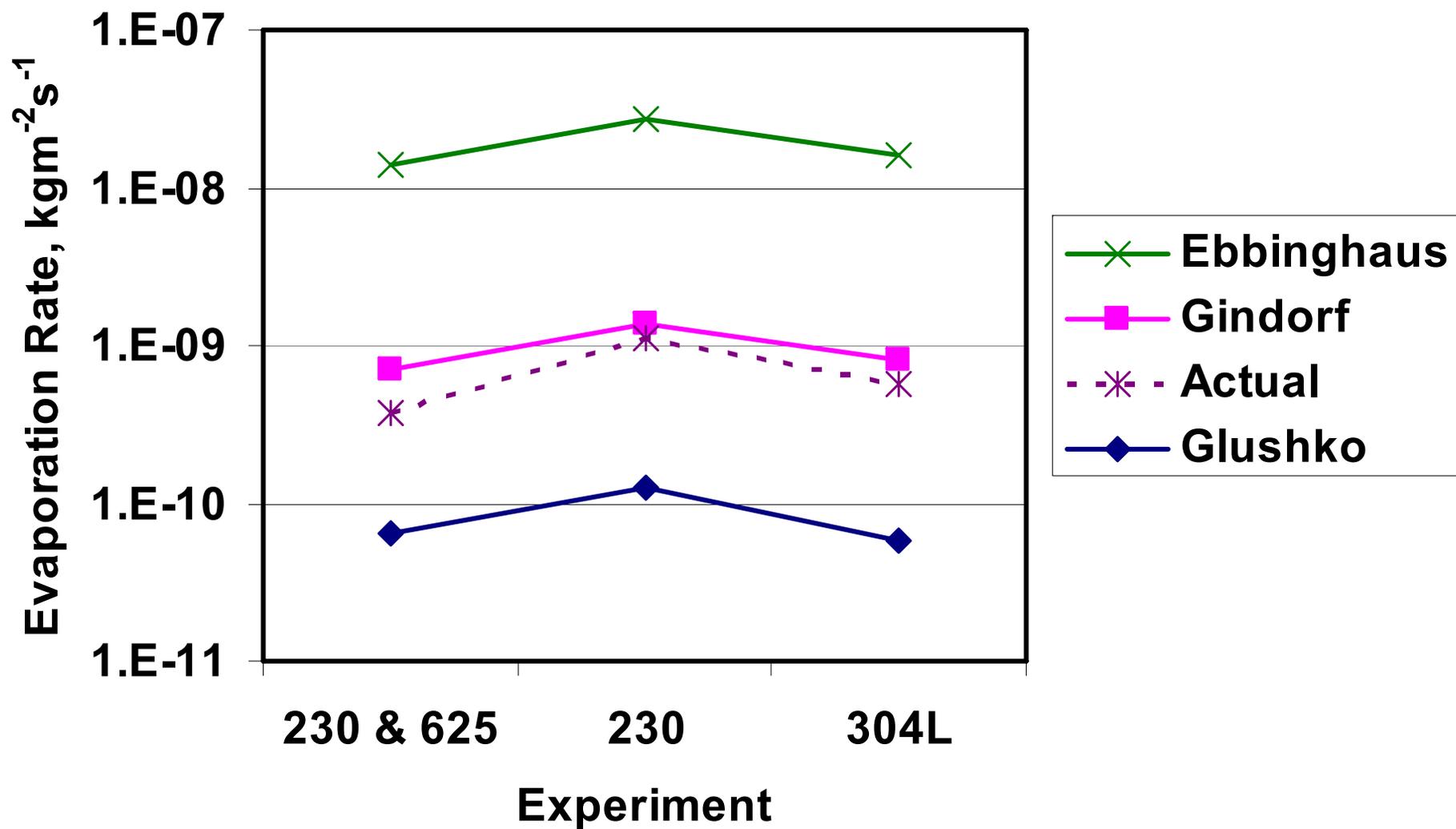
- Water allows another reaction important at lower temperatures



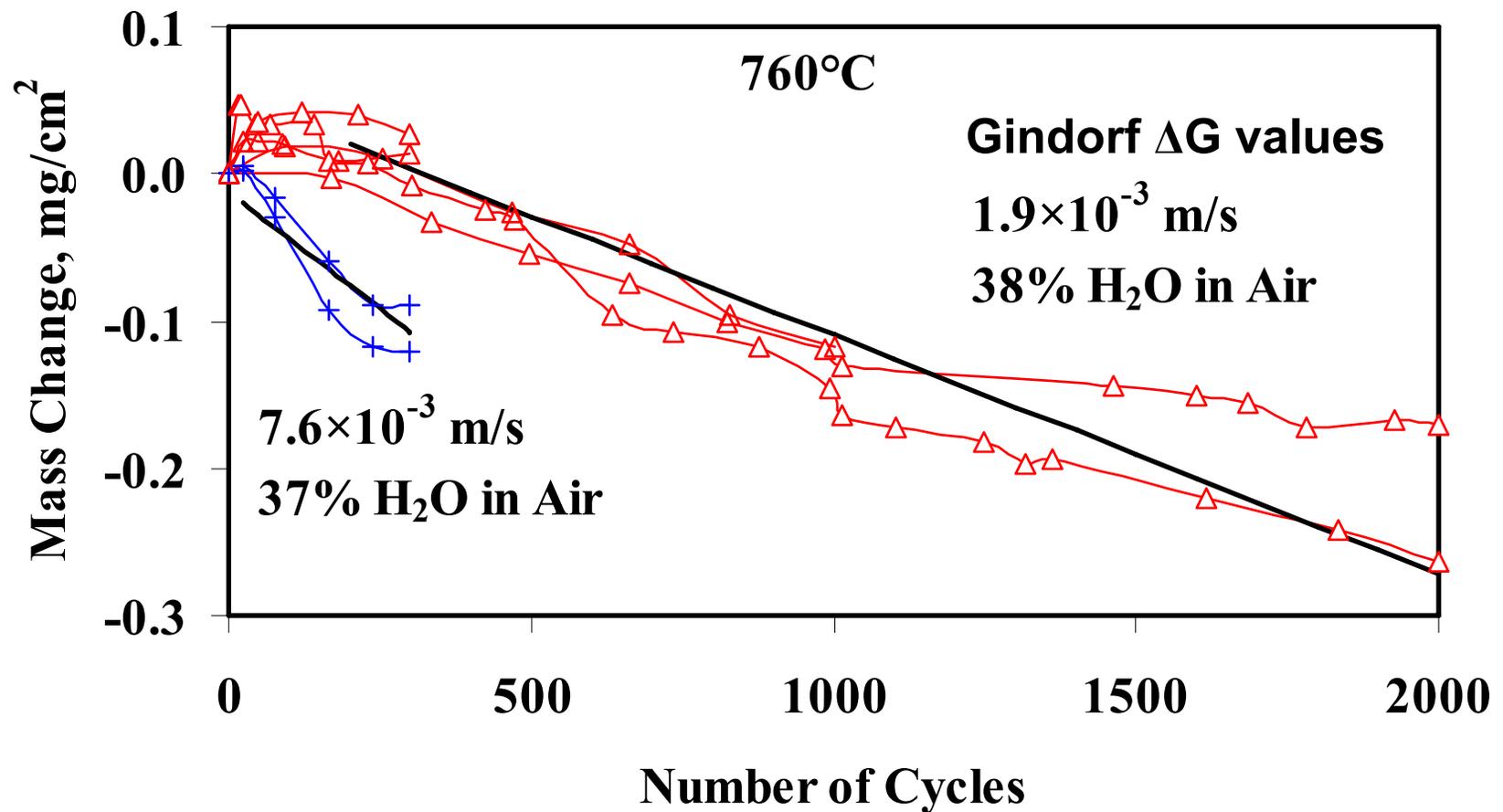
Evaporation

$$k_e \left(\frac{\text{kg}}{\text{m}^2 \text{s}} \right) = \overbrace{Sh_{Ave} \frac{D_{AB} M_{CrO_2(OH)_2}}{LRT}}^{\text{Kinetics}} \left(\underbrace{P_{CrO_2(OH)_2}}_{\text{Thermodynamics}} - \overbrace{P_{CrO_2(OH)_2}^\circ}^{\text{Saturation}} \right)$$

Thermodynamics of $\text{CrO}_2(\text{OH})_2(\text{g})$



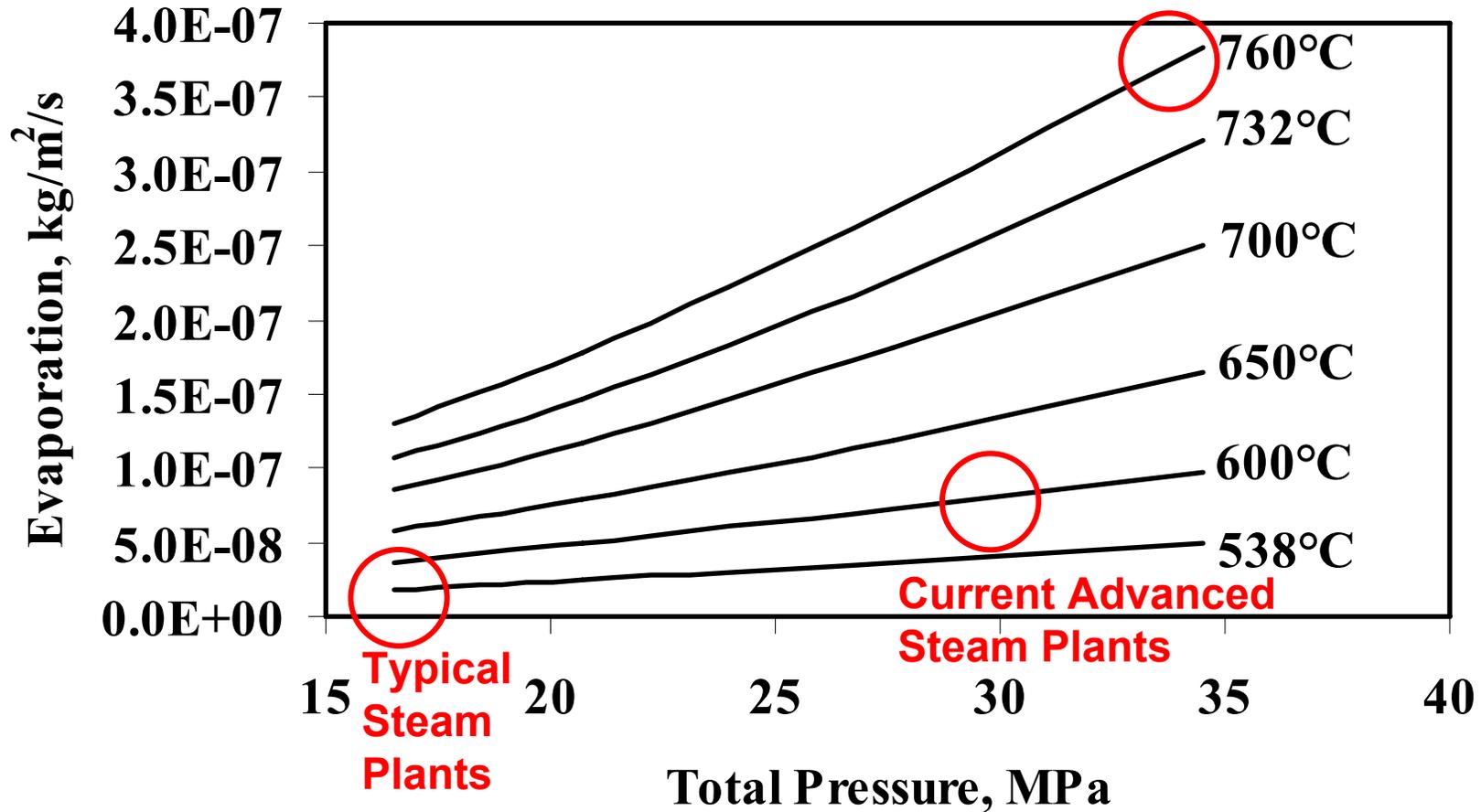
Evaporation Model – Some Verification Haynes 230



Advanced Steam Turbine Environments

Velocity of 300 m/s

DOE Goal for
60% Efficiency



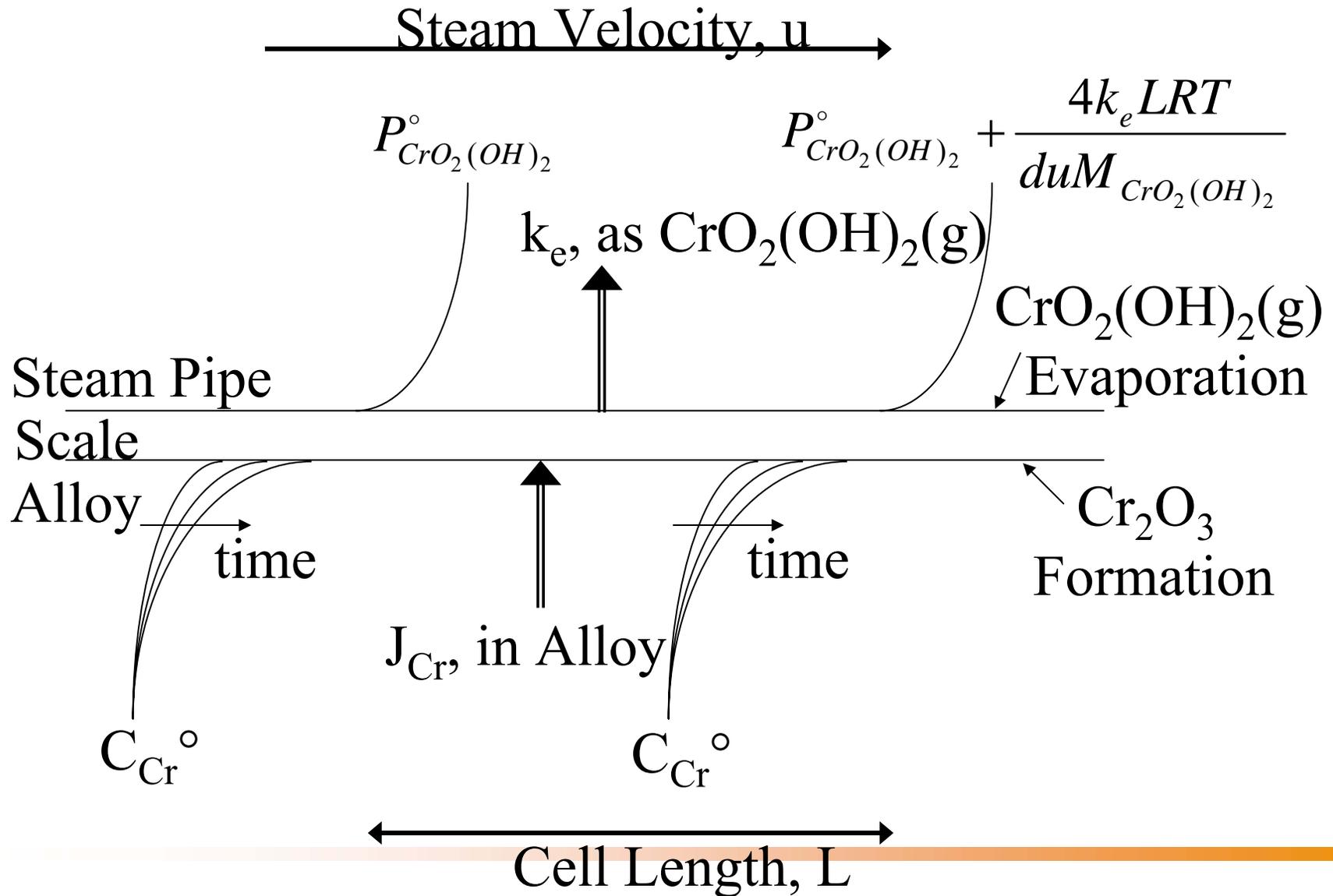
Additional Model Development

- Aim is to answer the question:

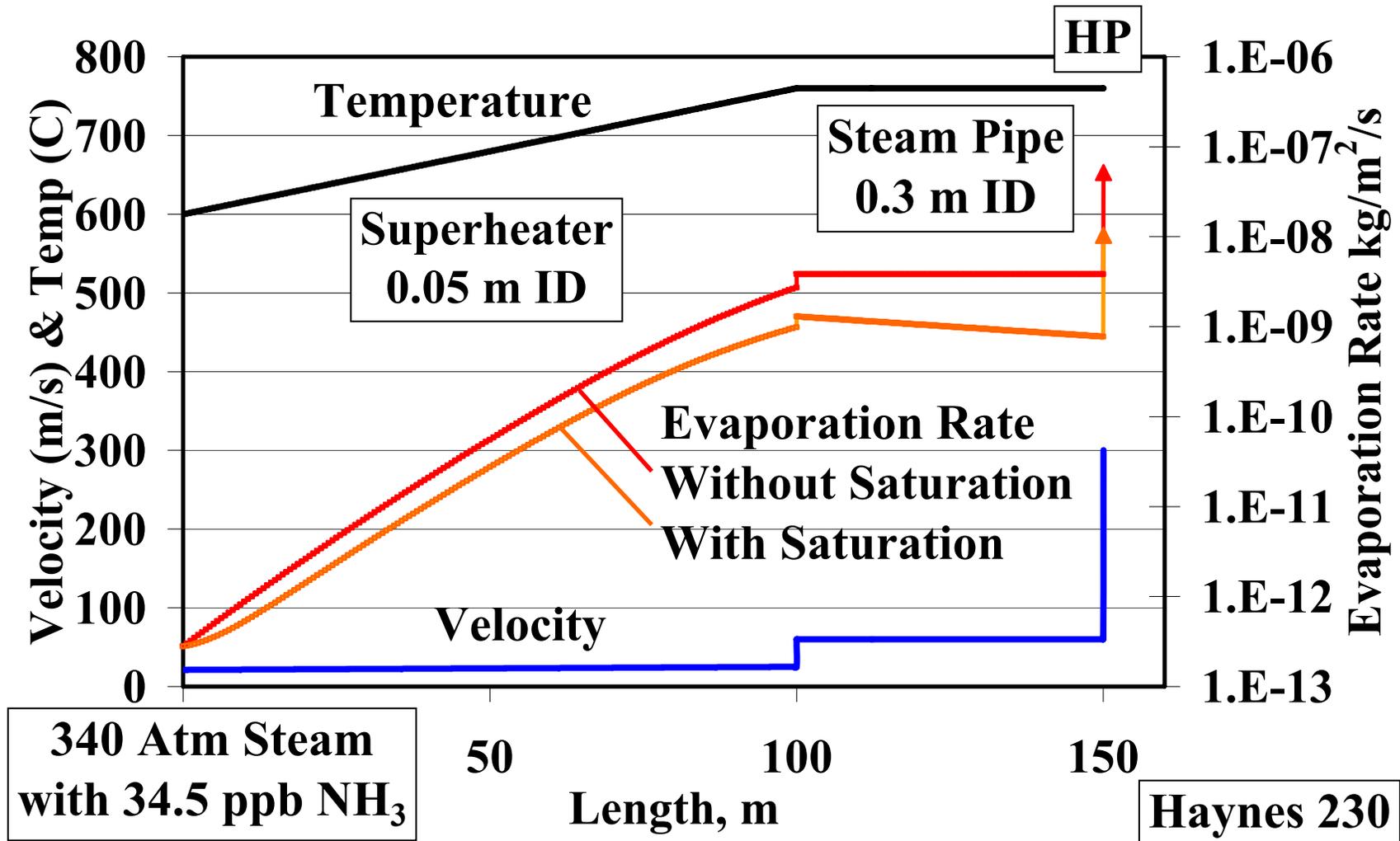
Should evaporation of chromia be a concern in USC boilers and turbines?

- Saturation of steam with $\text{CrO}_2(\text{OH})_2(\text{g})$
 - Translation of evaporation rates to breakaway oxidation times
 - Inclusion of Opila thermodynamic measurements
-

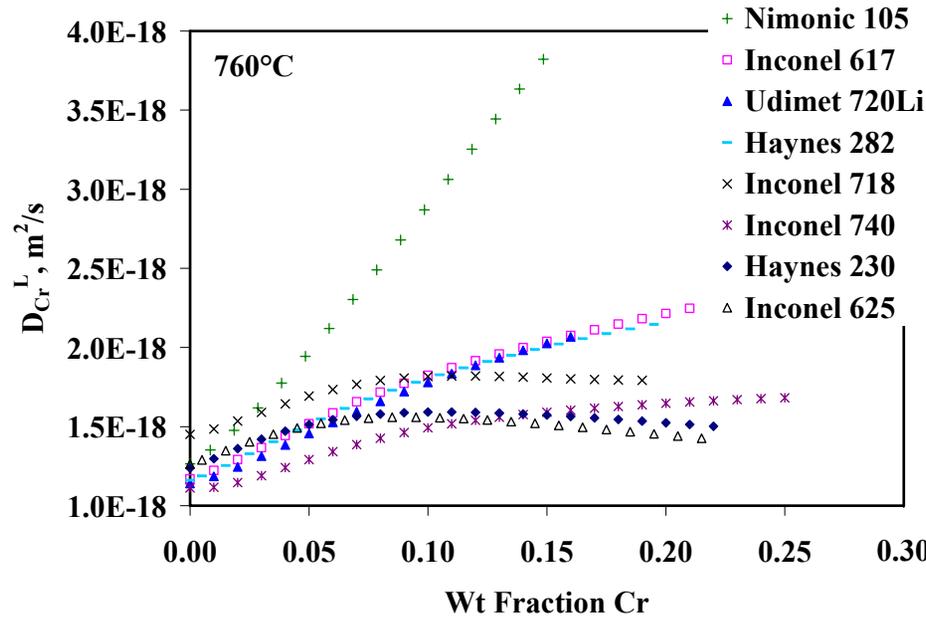
Saturation from Upstream Evaporation



Saturation from Upstream Evaporation



Translation of Evaporation Loss to Breakaway Oxidation

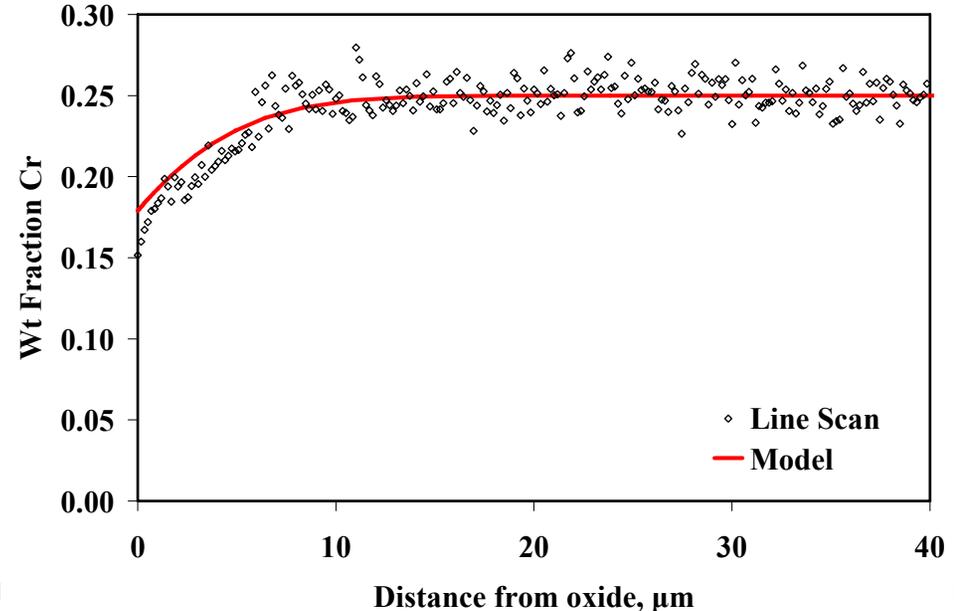


$$D_{Cr} \cong D_{Cr}^L + \frac{2\delta}{\lambda} D_{Cr}^{gb}$$

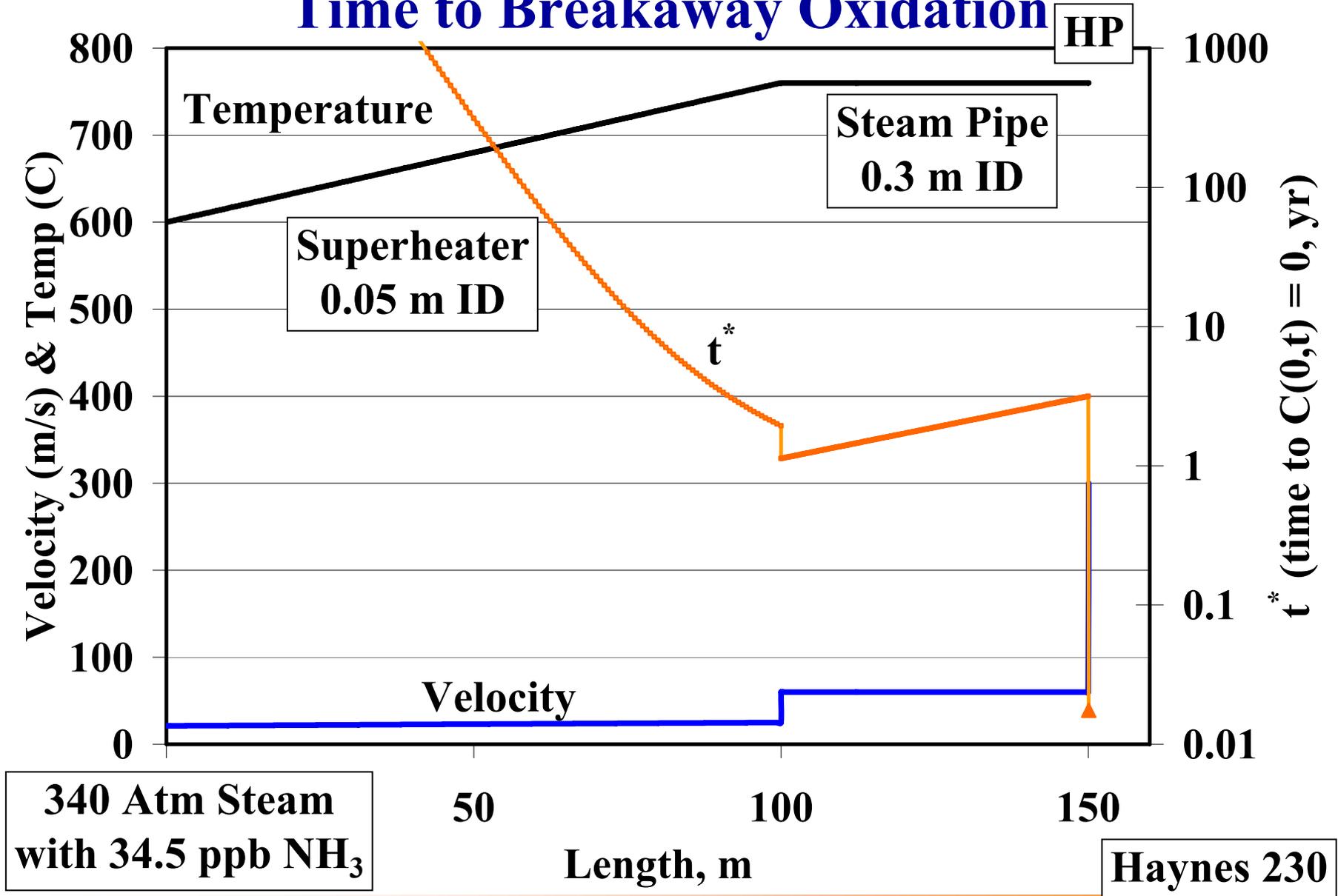
D_{Cr}^L from Dictra for the FCC phase
 D_{Cr}^{gb} from ratio for IN800 (Paul, 1994)

Transient diffusion of Cr given a constant evaporative loss
 t^* is the time at which Cr becomes zero at the surface

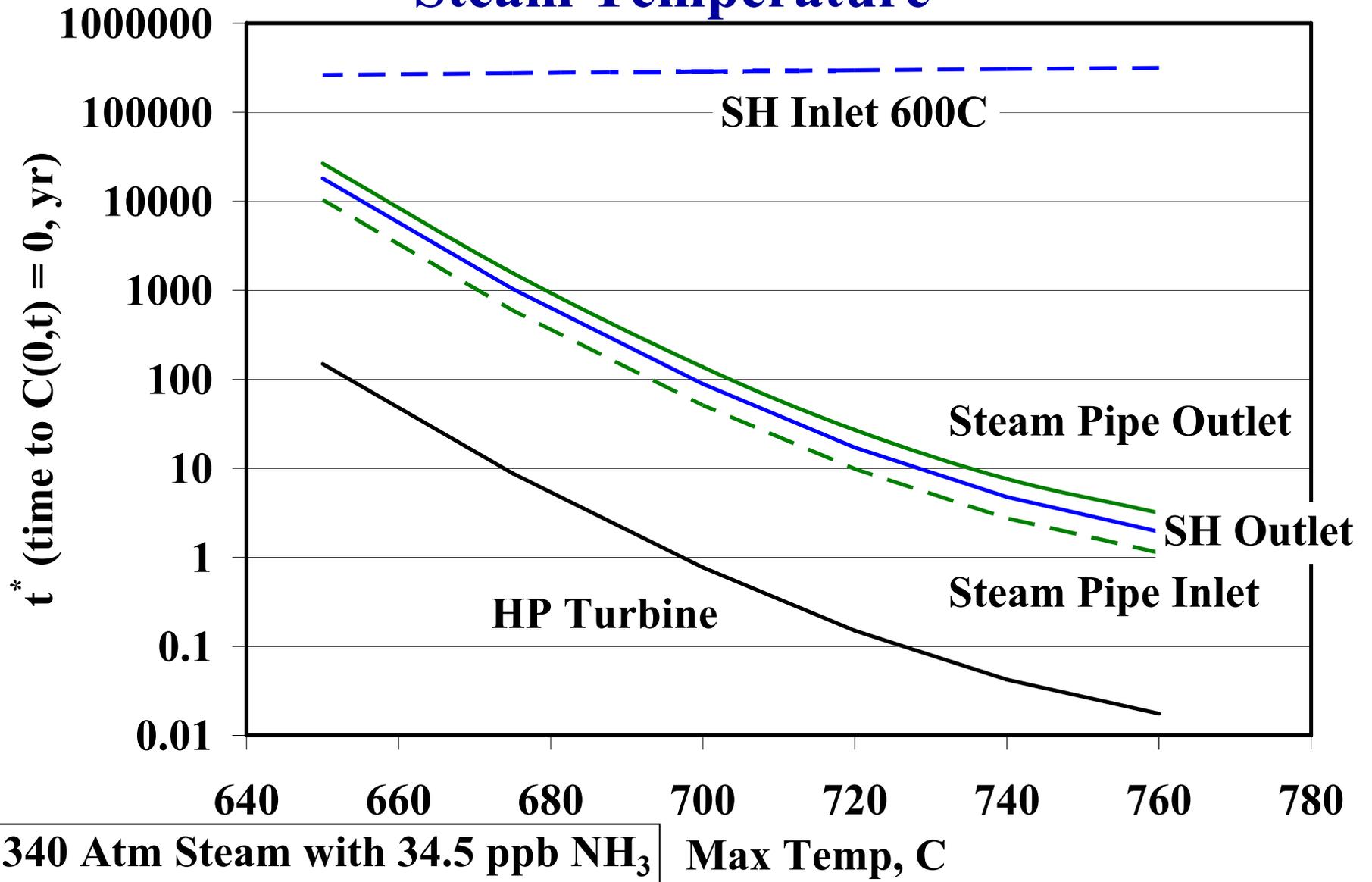
$$t^* = \frac{\pi D_{Cr}}{4} \left(\frac{M_{CrO_2(OH)_2} C_{Cr}^o}{k_e} \right)^2$$



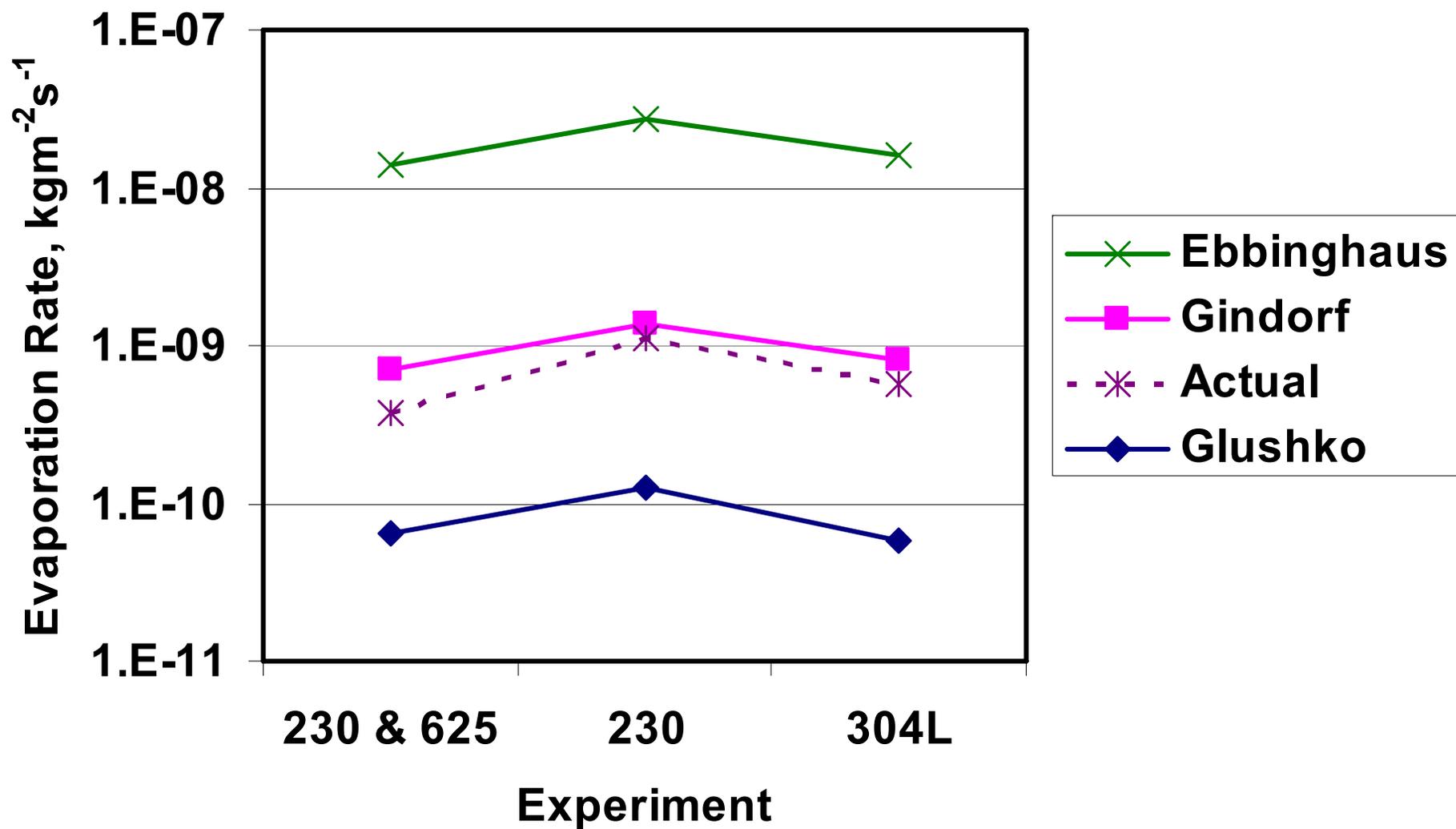
Time to Breakaway Oxidation



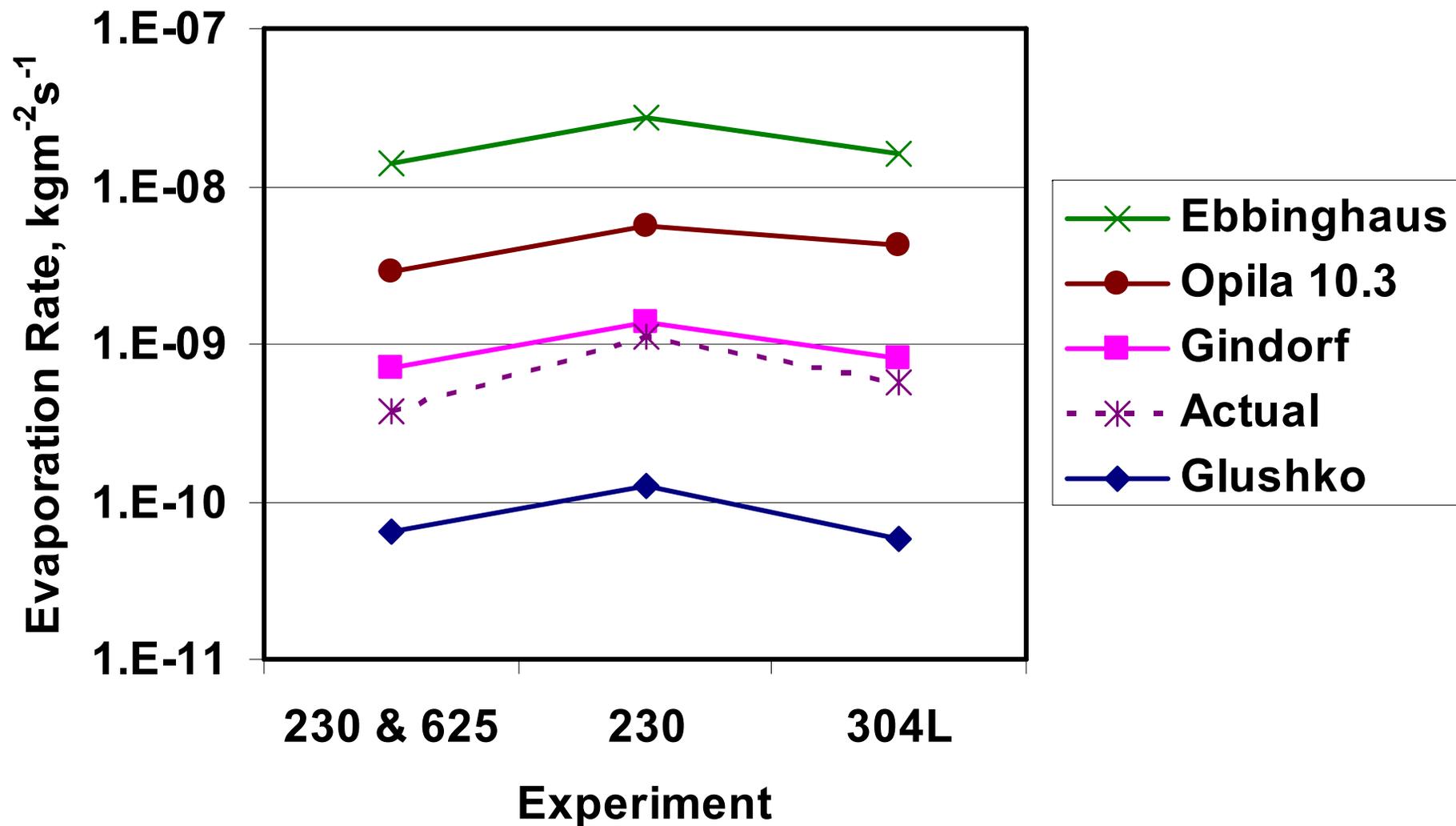
Steam Temperature



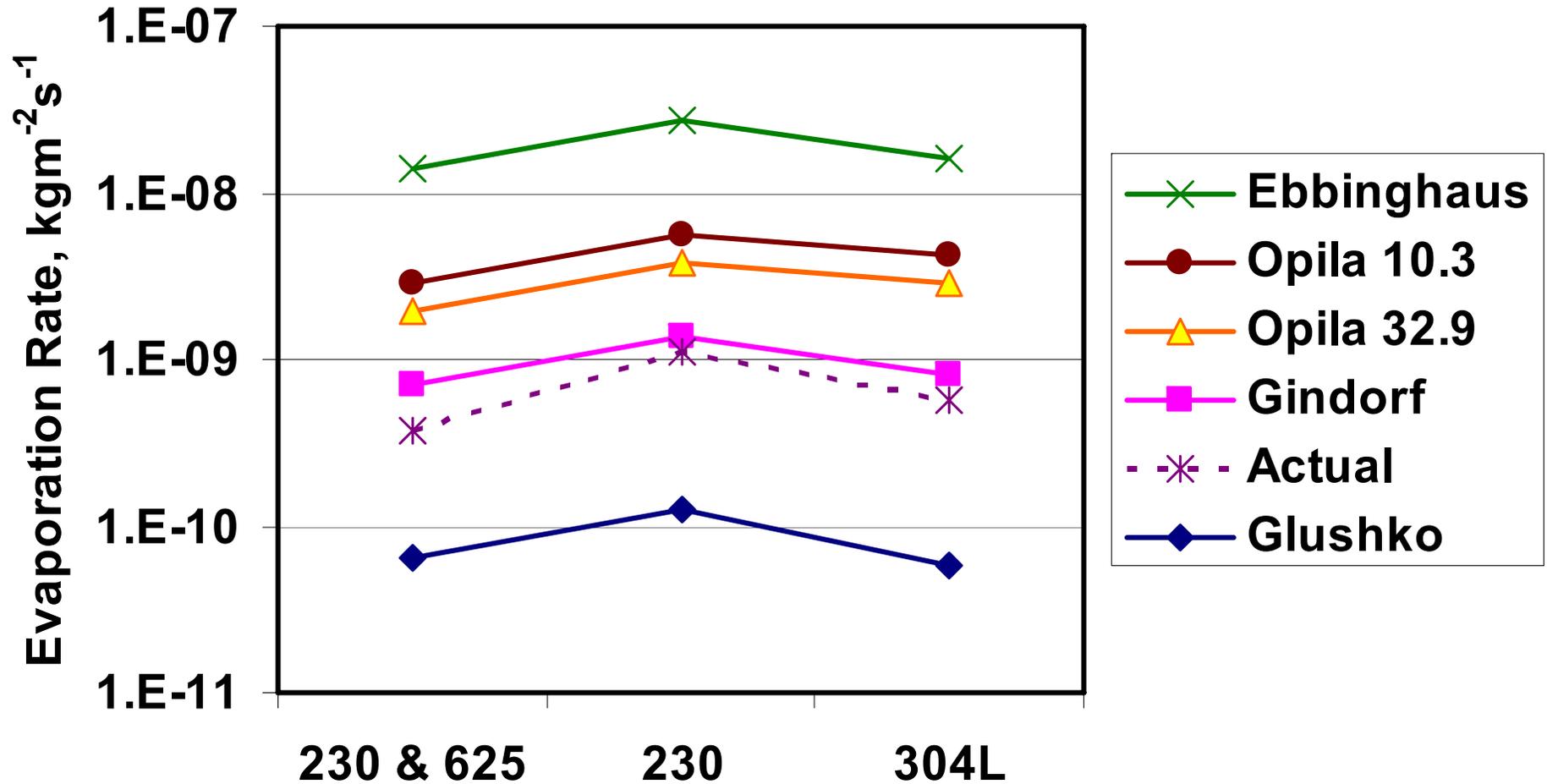
Thermodynamics of $\text{CrO}_2(\text{OH})_2(\text{g})$



Thermodynamics of $\text{CrO}_2(\text{OH})_2(\text{g})$



Thermodynamics of $\text{CrO}_2(\text{OH})_2(\text{g})$

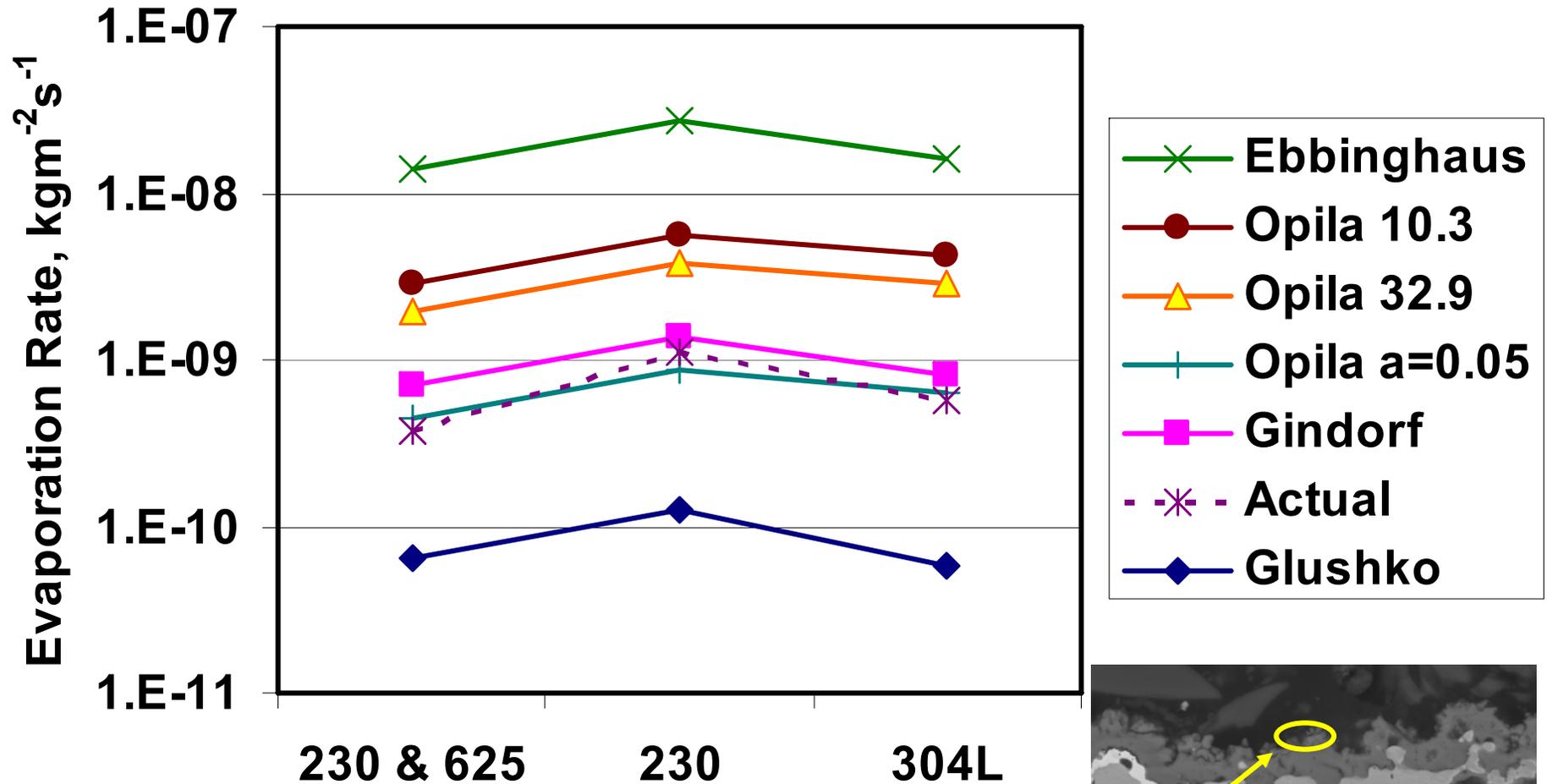


$$D_{AB} = \frac{(3.203 \times 10^{-4}) T^{1.75}}{P_T (v_A^{1/3} + v_B^{1/3})^2} \sqrt{\frac{1}{M_A} + \frac{1}{M_B}}$$

Experiment, 10.3 cm³/mol for $\text{CrO}_2(\text{OH})_2$ based on Cr-O bond in CrO

Opila model of $\text{CrO}_2(\text{OH})_2 \Rightarrow$ 32.9 cm³/mol based on Cr-H bond

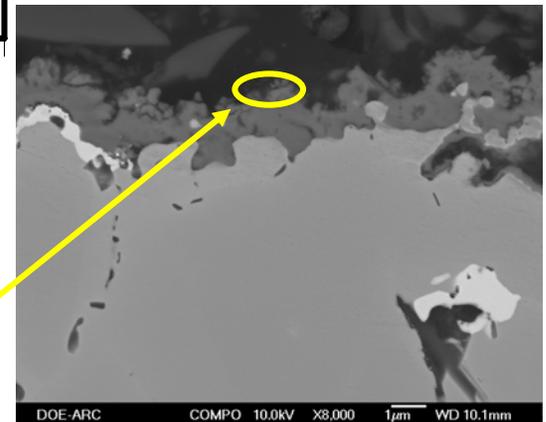
Thermodynamics of $\text{CrO}_2(\text{OH})_2(\text{g})$



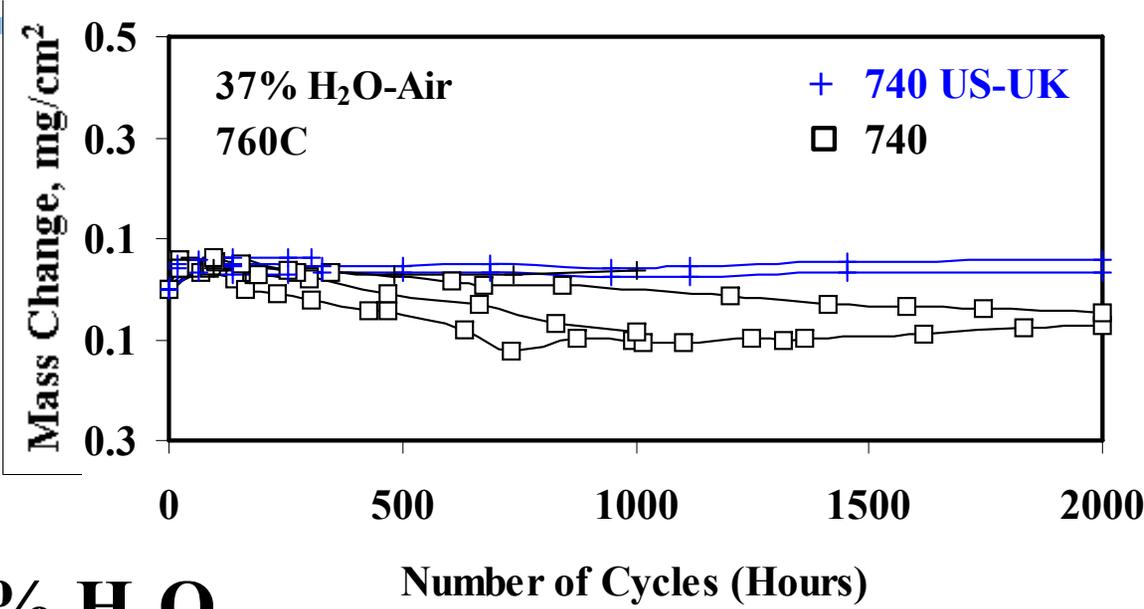
In comparison, MnCr_2O_4 has an activity of Cr_2O_3 of about 0.0006 (Holcomb & Alman 2006)

Experiment

Decreased Chromia Activity at the Scale-gas interface

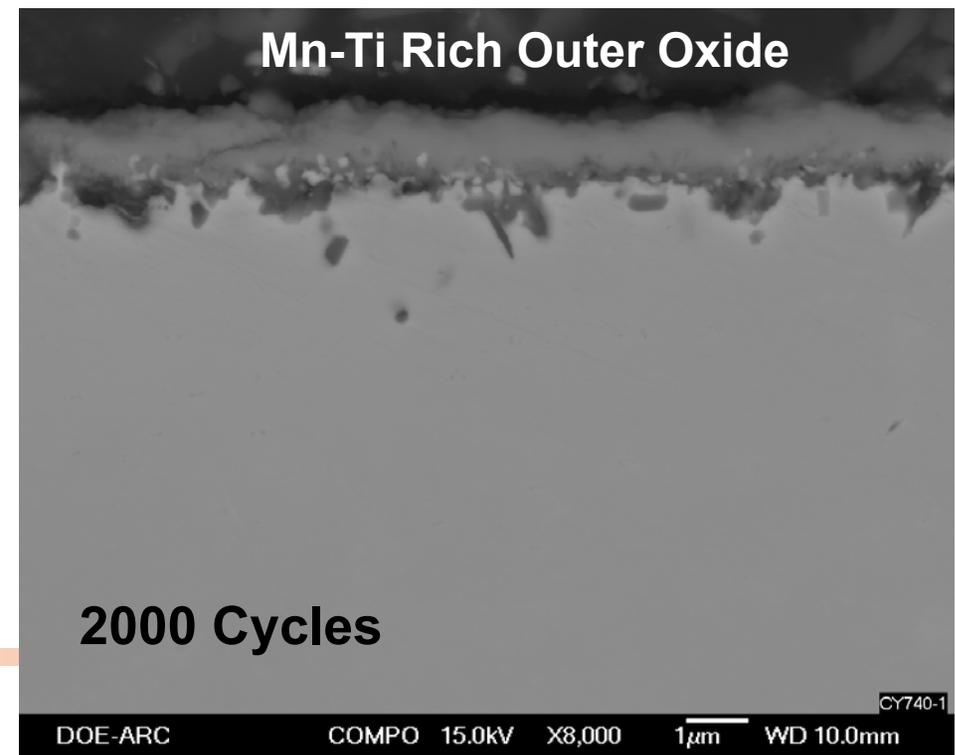
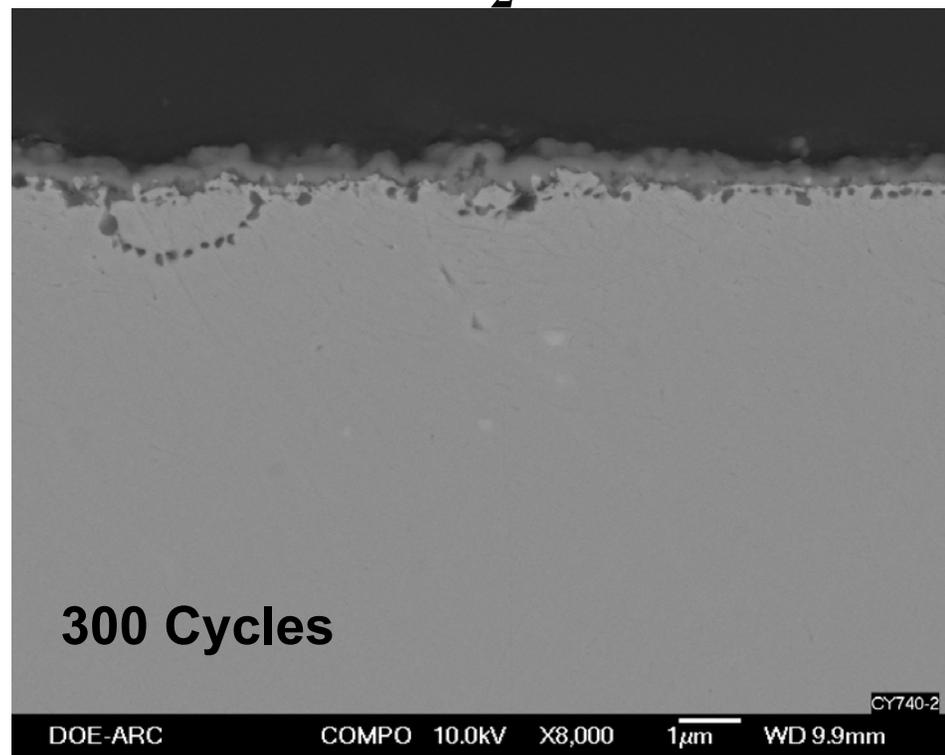


Inconel 740

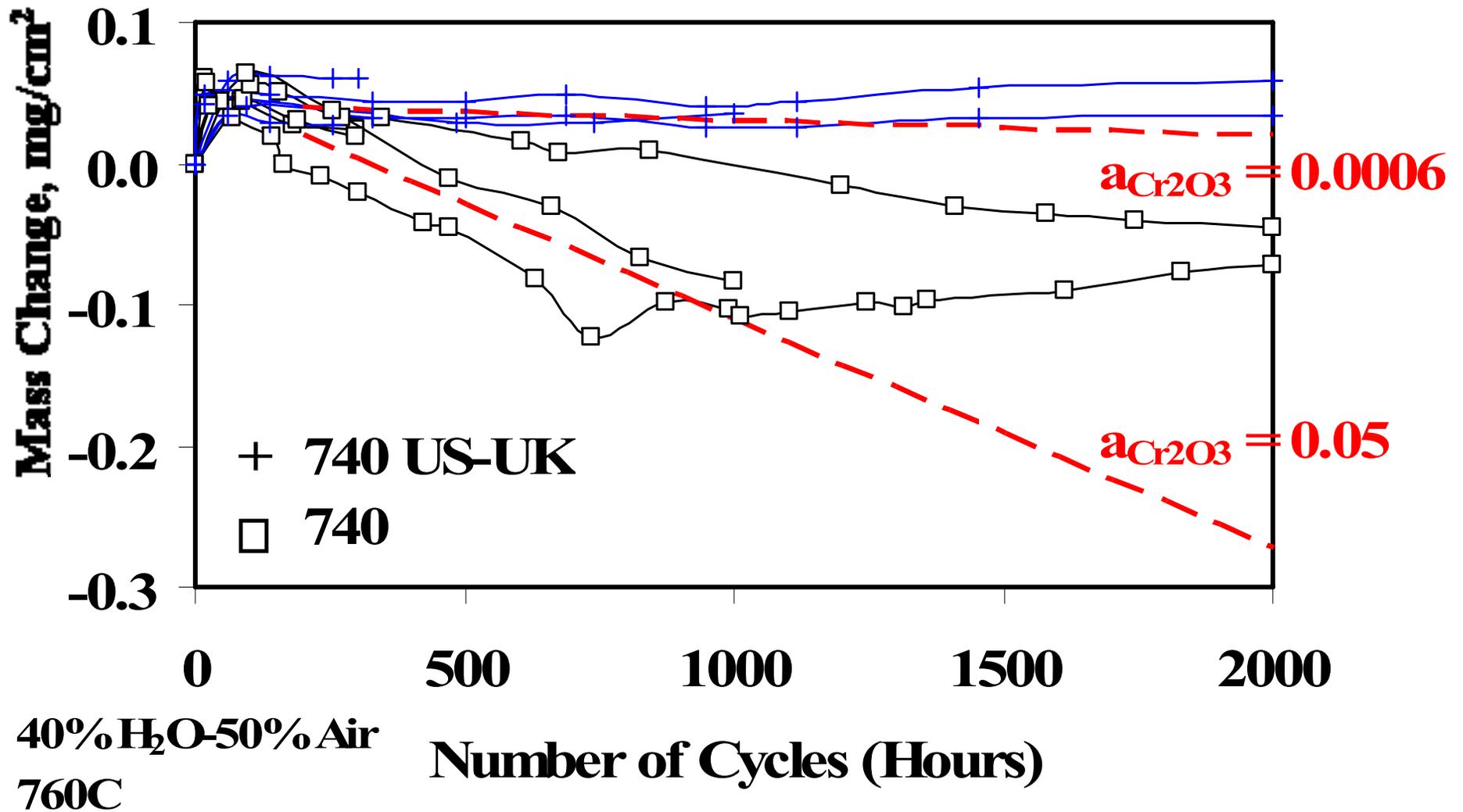


760°C

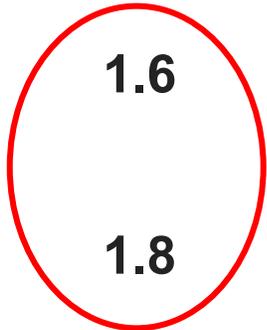
Air + 37% H₂O



Inconel 740



Alloy	Mn	Ti	Apparent Cr₂O₃ Activity
230	0.5	--	0.05
617	0.1	0.3	0.05
740	0.3	1.6	Initially 0.05 Then ~0.0006
740 US/UK	0.3	1.8	~0.0006

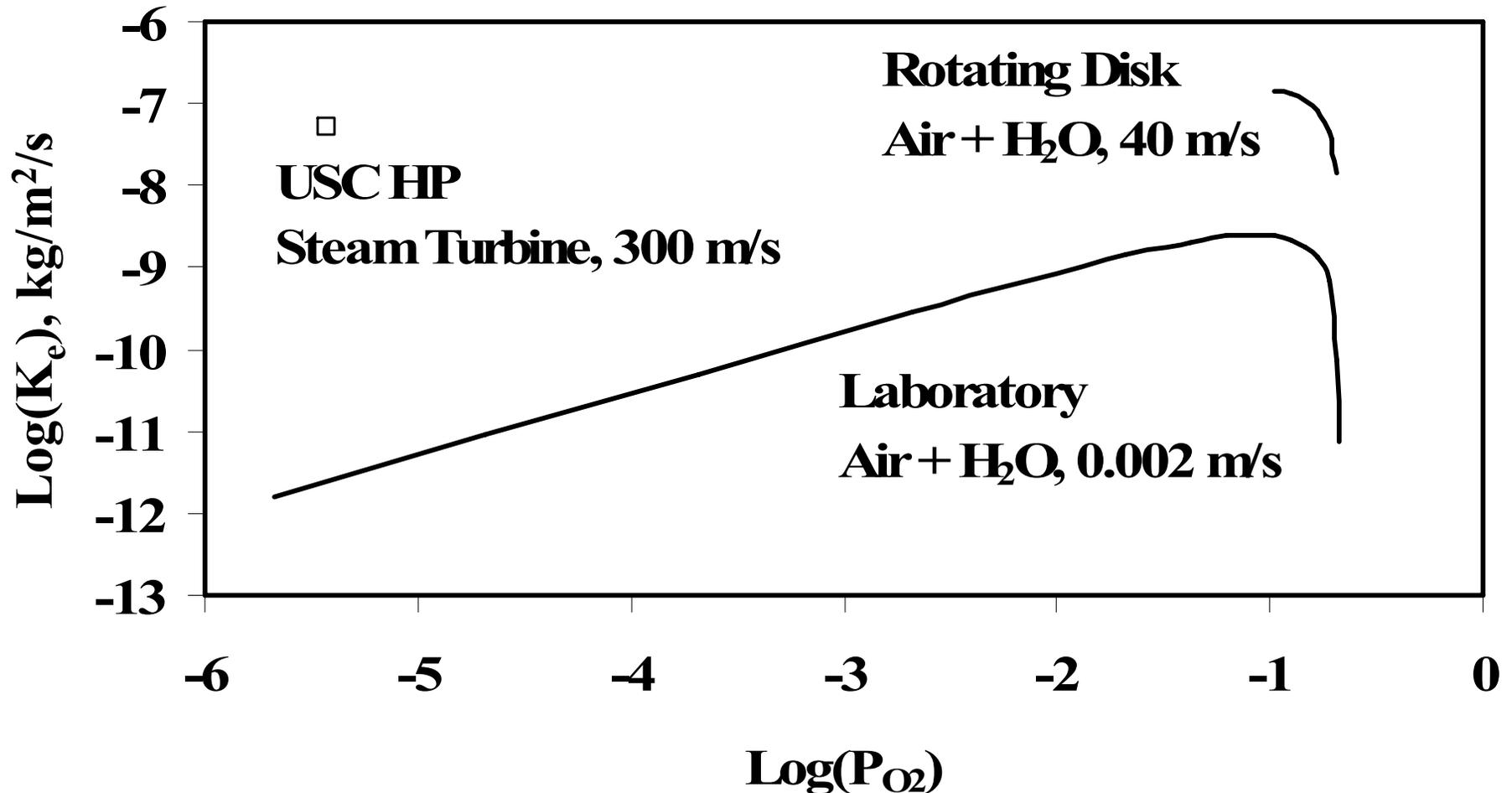


Future Work

- **Additional Model Verification**
 - Exposures in up to 40 m/s moist air
 - ESCA analysis of oxide scale surface for composition and oxidation state
 - **Examine Oxidation Behavior of Cast Alloys Compared with Wrought Alloys**
 - Haynes 230, 263, 282
 - Inconel 617, 625, 740
 - Nimonic 105
 - Scaling and internal oxidation in steam, both at atmospheric pressure and at up to 5000 psi
 - Evaporation in moist air
 - **Compare results with that from the Niles steam loops (Babcock & Wilcox)**
-

Advanced Steam Turbines vs Laboratory Exposures

760°C



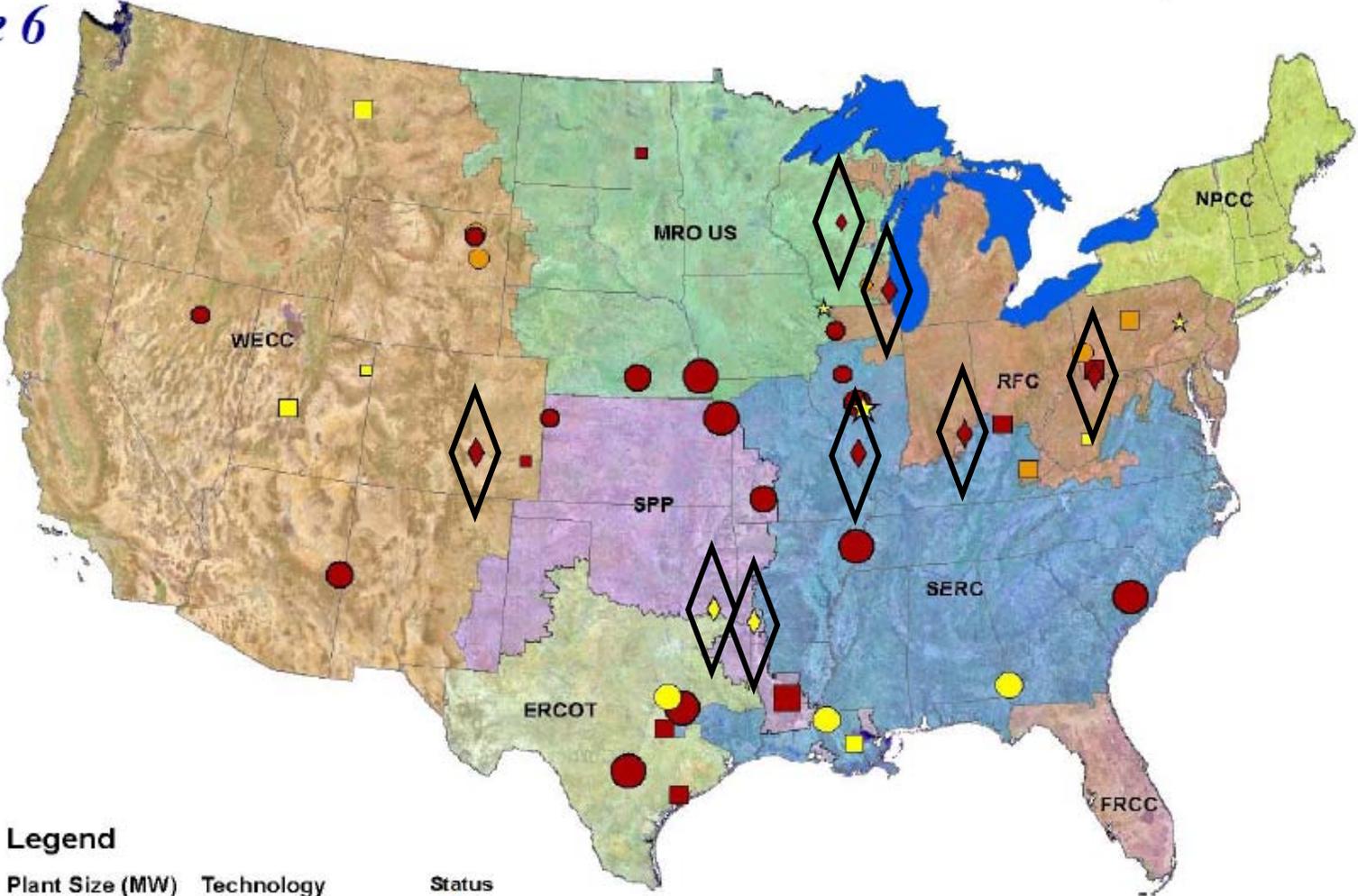
Evaporation at a maximum
at 57% H₂O

Summary

- **Nickel-base superalloys for USC applications experience 3 main oxidation behaviors**
 - Scale formation
 - Internal Oxidation
 - Deeper penetration and section loss than scaling
 - Reactive Evaporation
 - Model development—Kinetics, Thermodynamics, Saturation, Alloy Cr Depletion
 - Not important below 650°C
 - Expected to dominate above 700°C
 - ***Should evaporation of chromia be a concern in USC boilers and turbines? Yes***
-

Geographical Map by NERC Regions: Coal-Fired Plants (Permitted, Near Construction, and Under Construction)

Figure 6



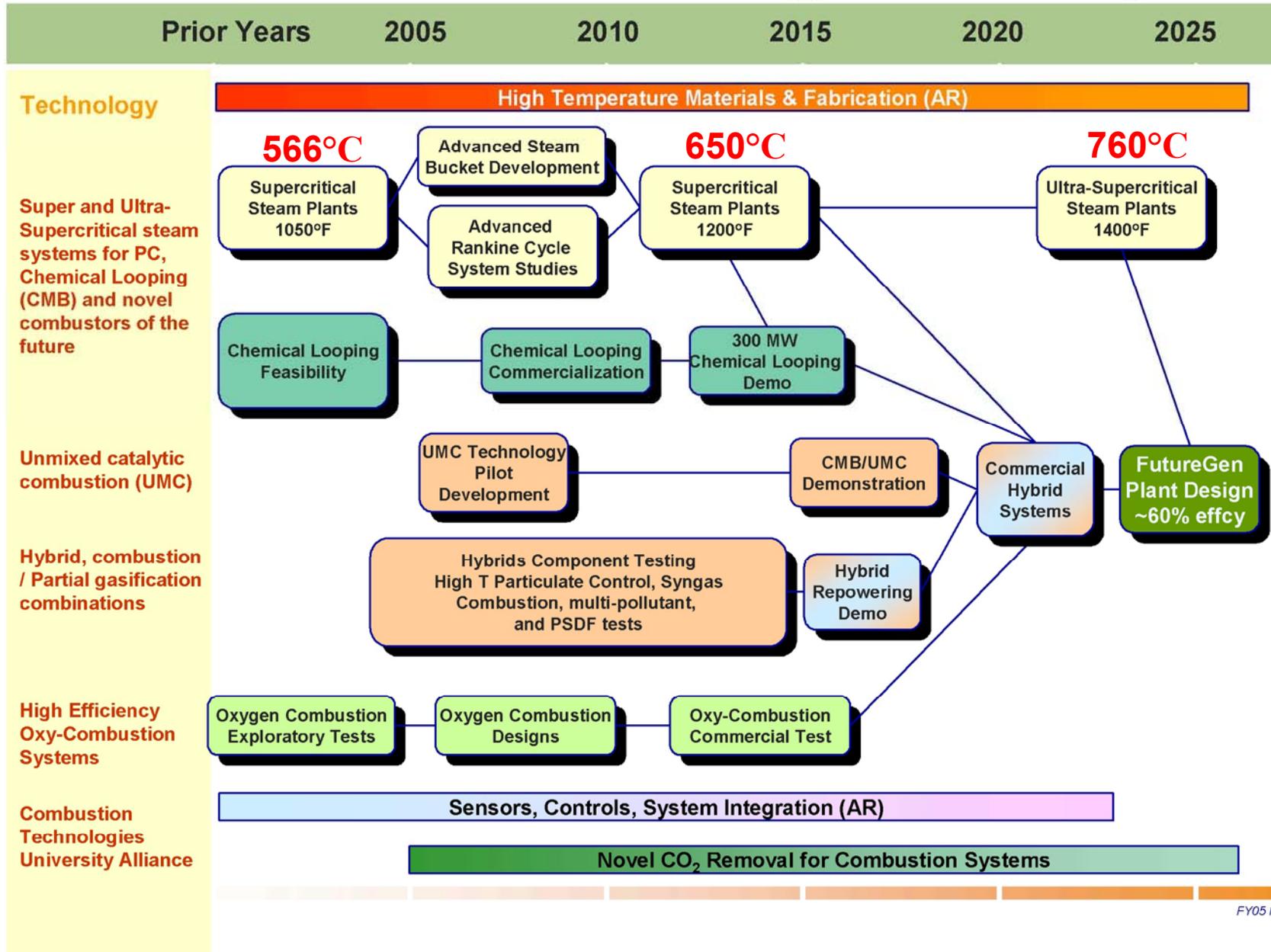
Legend

Plant Size (MW)	Technology	Status
◦ 7 - 219	□ CFB	○ Near Construction
○ 220 - 599	☆ IGCC	○ Permitted
○ 600 - 1634	◇ Supercritical	○ Under Construction
	○ PC Subcritical	



Source: Global Energy Decisions – Velocity Suite (12/31/2007)

Combustion Technologies Roadmap



Evaporation Model - Kinetics

- Controlled by fluid properties and evaporation reaction.
- Evaporation is limited by mass transport of the volatile specie in the boundary layer.

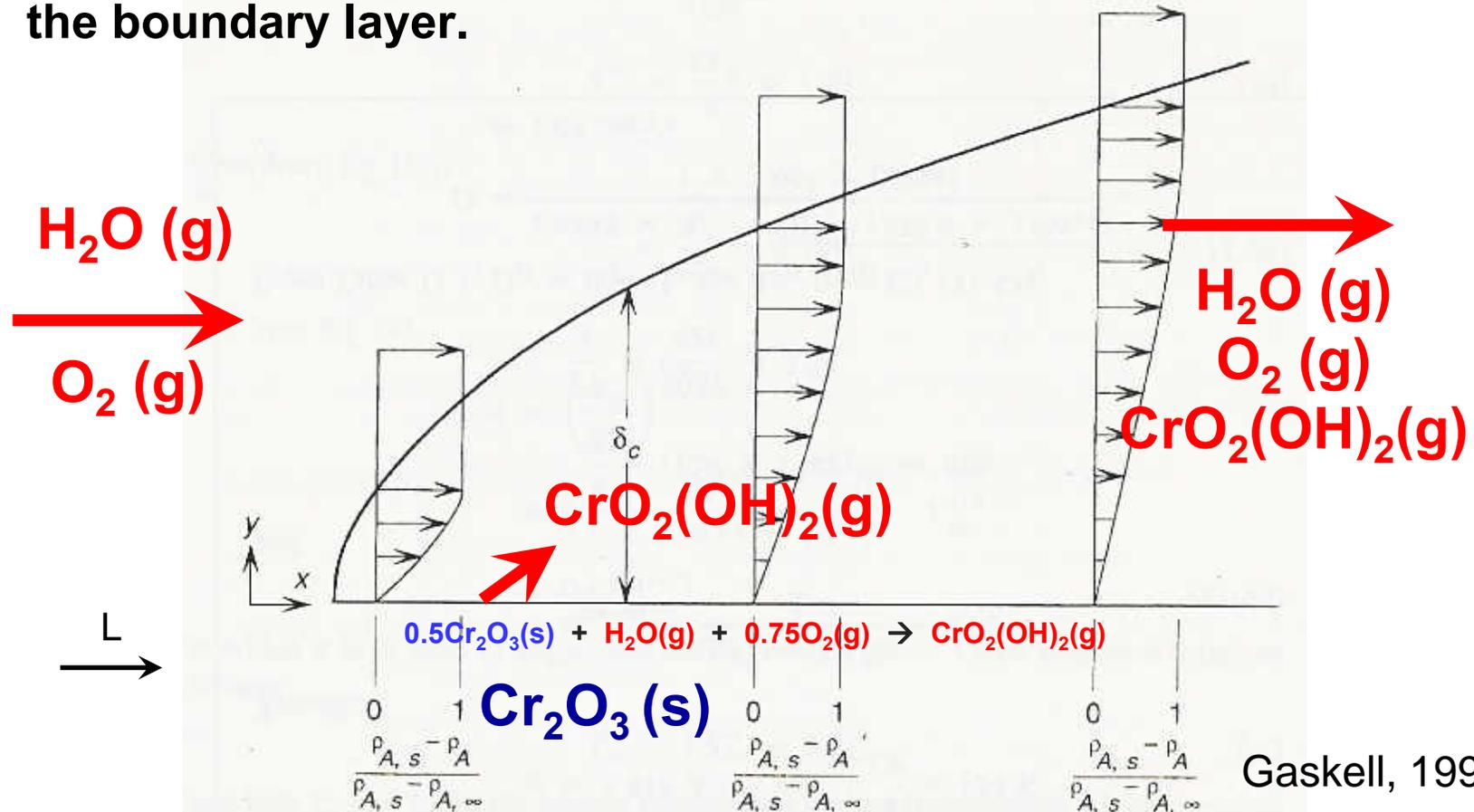


FIGURE 11.17. Normalized concentration profiles of A in the concentration boundary layer on the surface of solid A over which fluid B is flowing, when A is slightly soluble in B.

Nickel-base Superalloy Compositions

Alloy	Fe	Cr	Ni	Co	Mo	C	Si	Ti	Al	B ppm	Mn	Other
Haynes 230	1.5	22	Bal	2.5	2	0.1	0.4		0.3	75	0.5	0.02 La 14 W
Haynes 282	0.75	19.5	Bal	10	8.5	0.06	0.075	2.1	1.5	50		0.15 Cu
Inconel 617	1.5	22	Bal	12.5	9	0.1	0.5	0.3	1.15	30	0.5	0.25 Cu
Inconel 625	2.5	21.5	Bal	0.5	9	0.05	0.25	0.2	0.2		0.25	3.65 Nb
Inconel 718	Bal	19	52	0.5	3.05	0.04	0.175	0.9	0.5	30	0.175	5.125 Nb 0.15 Cu
Inconel 740	0.7	25	Bal	20	0.5	0.03	0.5	1.8	0.9		0.3	2 Nb
Nimonic 105	0.5	14.85	Bal	20	5	0.085	0.5	1.2	4.7	65	0.5	0.075 Zr 0.1 Cu
Udimet 720Li		16	Bal	14.75	3	0.015		5	2.5	150		1.25 W 0.0375 Zr

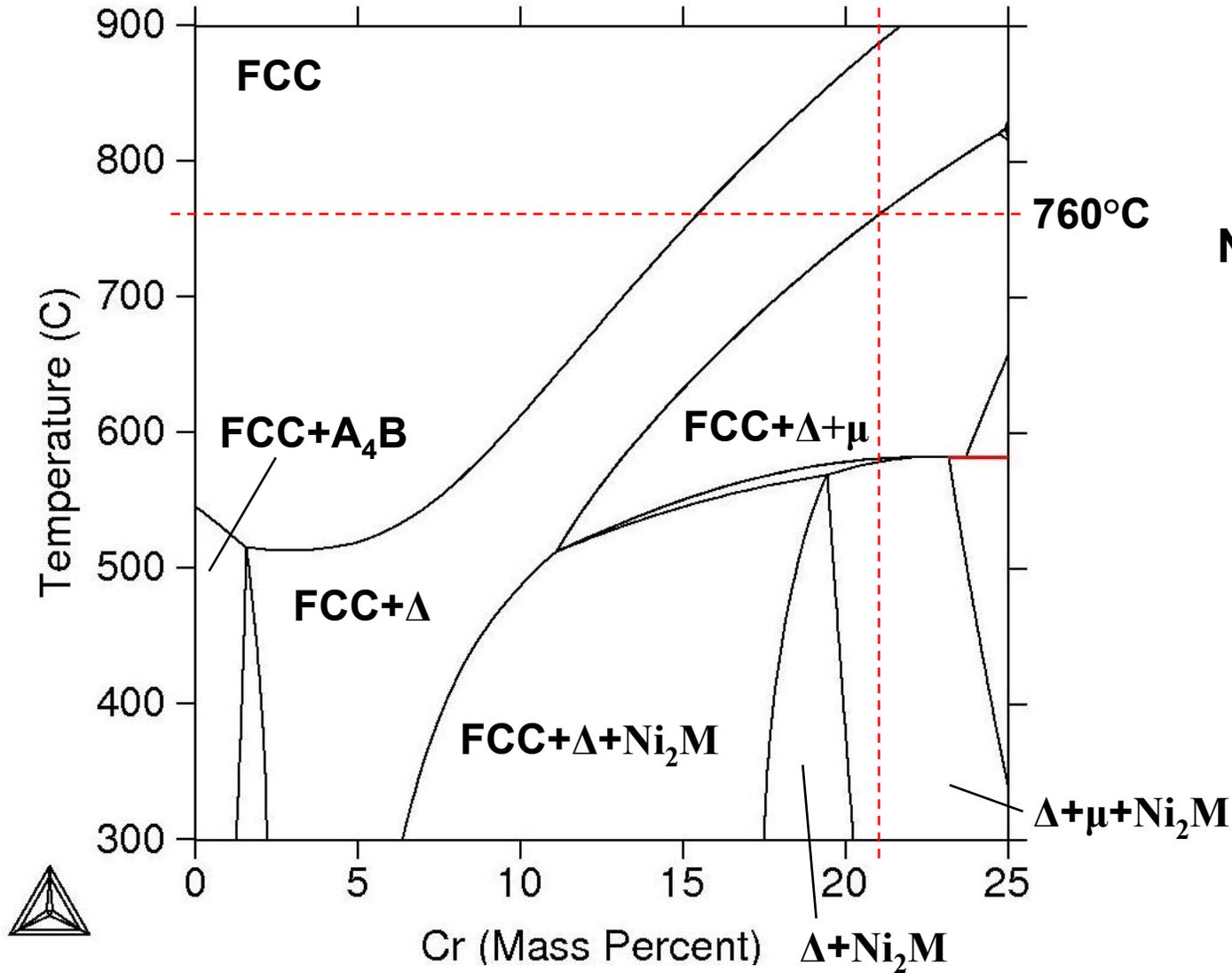
Other Alloy Compositions

Alloy	Analysis	Fe	Cr	Ni	Co	Mo	Nb	Mn	Si	Ti	Al	Other
SAVE12-9.5Cr	XRF	83.0	9.5	0.4	2.6	0.04	0.05	0.5	0.4	0.02		2.9 W 0.3 V
SAVE12-10.5Cr	XRF	82.9	10.3	0.2	3.0		0.06	0.5	0.8	0.01		2.9 W 0.3 V
HR6W	XRF	24.2	23.6	43.4	0.4	0.2	0.2	1.0	0.3	0.2	0.04	6.1 W 0.1 Cu
T92	Nom		9	<0.4		0.5		0.5	<0.5		<0.04	1.75 W 0.2 V 0.07 Cb
TP347HFG	Nom	Bal	18	11			*	2.0	1.0			Nb+Ta≥10xC

DATABASE:NI

21.5
wt%Cr

Inconel 625

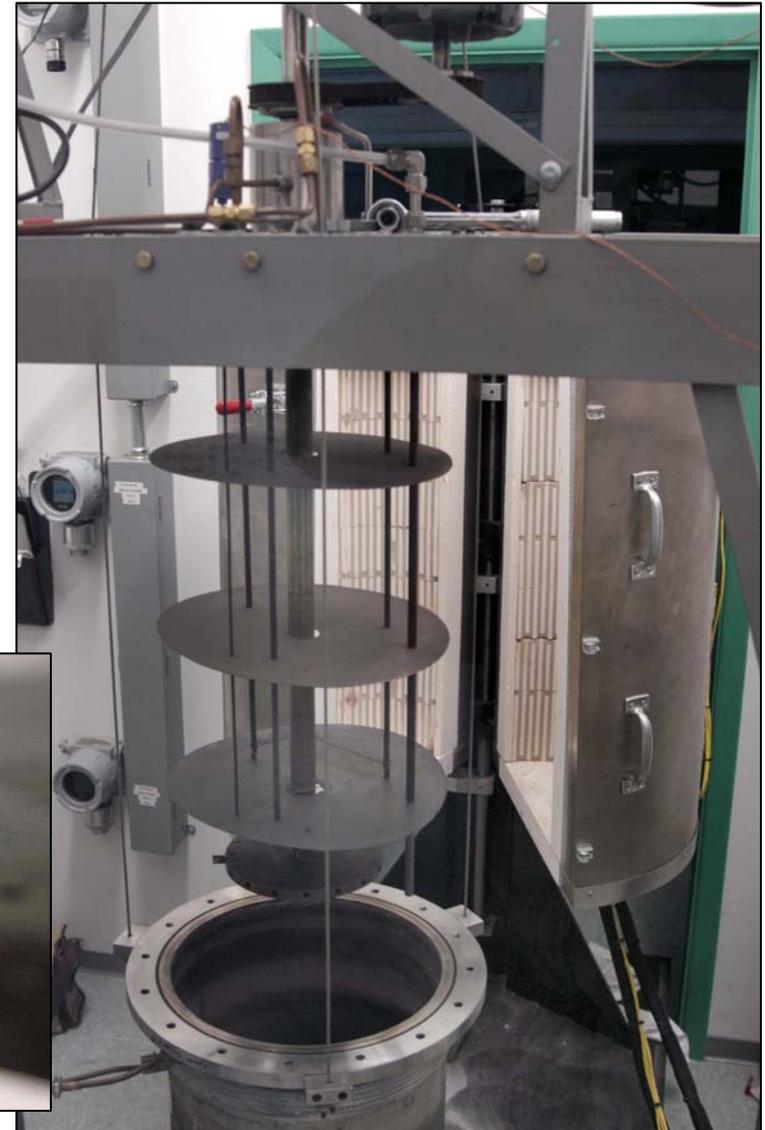


$A_4B \approx Ni_4Mo$
 $\Delta \approx Ni_3(Nb-Mo)$
 $Ni_2M \approx Ni_2(Cr-Mo)$
 $\mu \approx NiMoCr$

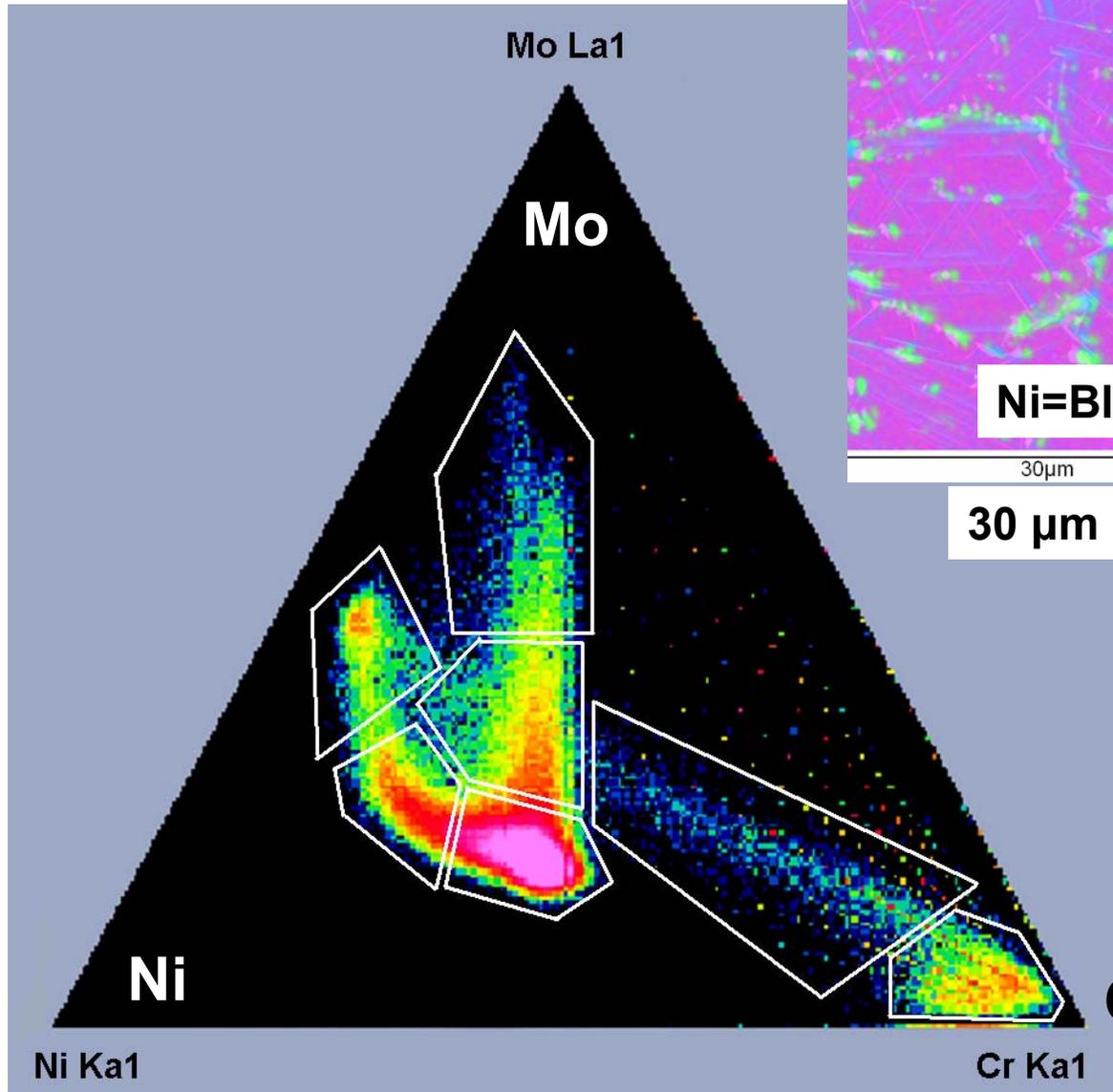
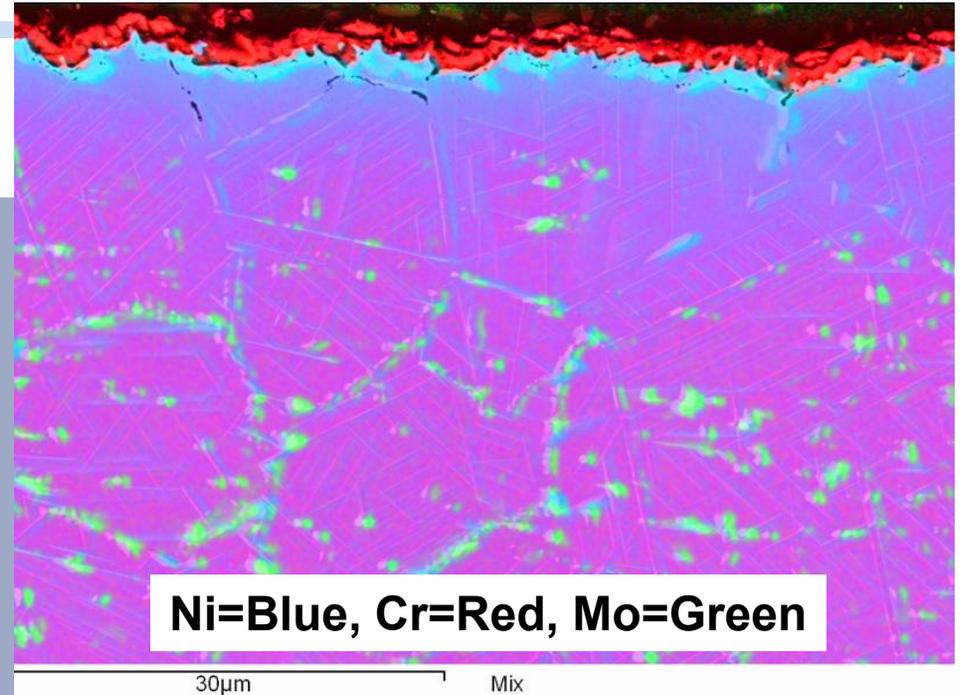
Isopleth with Mo = 9 wt% and Nb = 3.65 wt%

High Velocity Exposures in Moist Air

- Rotating disk up to 40 m/s
- Moist environments
- Cr evaporation model
 - Turbulent: $v^{0.8}$
 - Laminar: $v^{0.5}$



Inconel 625



Inconel 625
Ni-21.5Cr-9Mo-3.65Nb

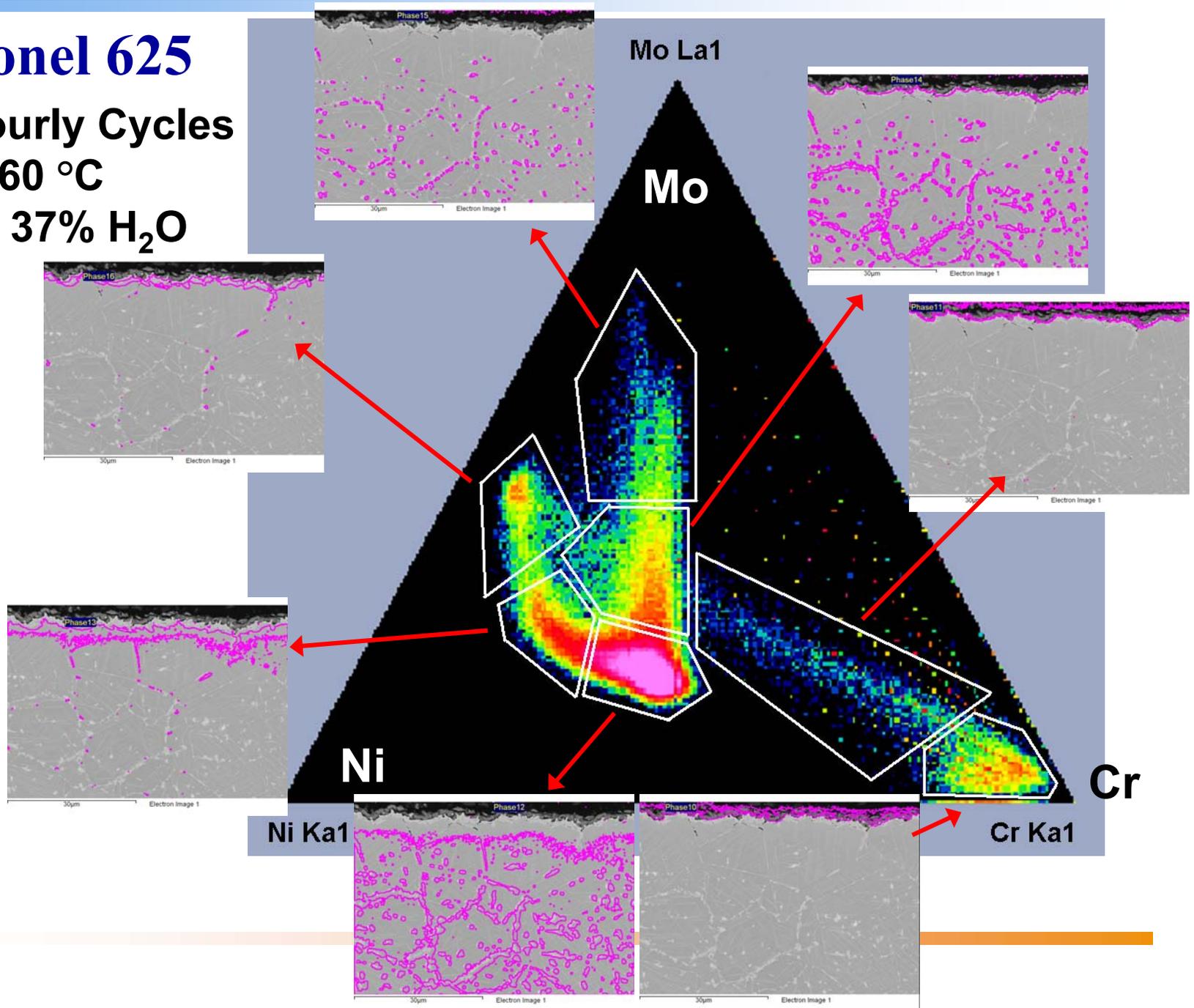
2000 Hourly Cycles
760 °C
Air + 37% H₂O

Inconel 625

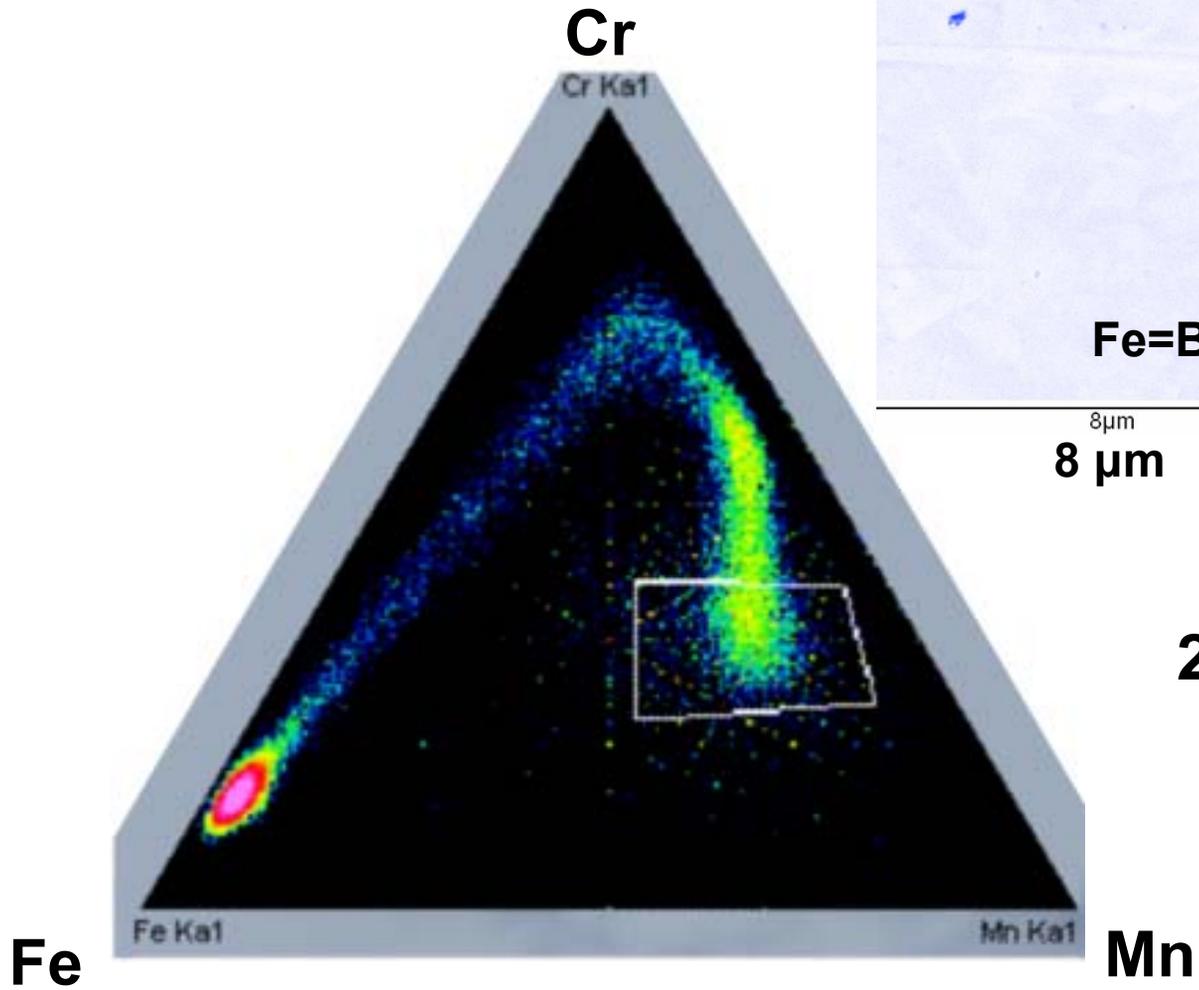
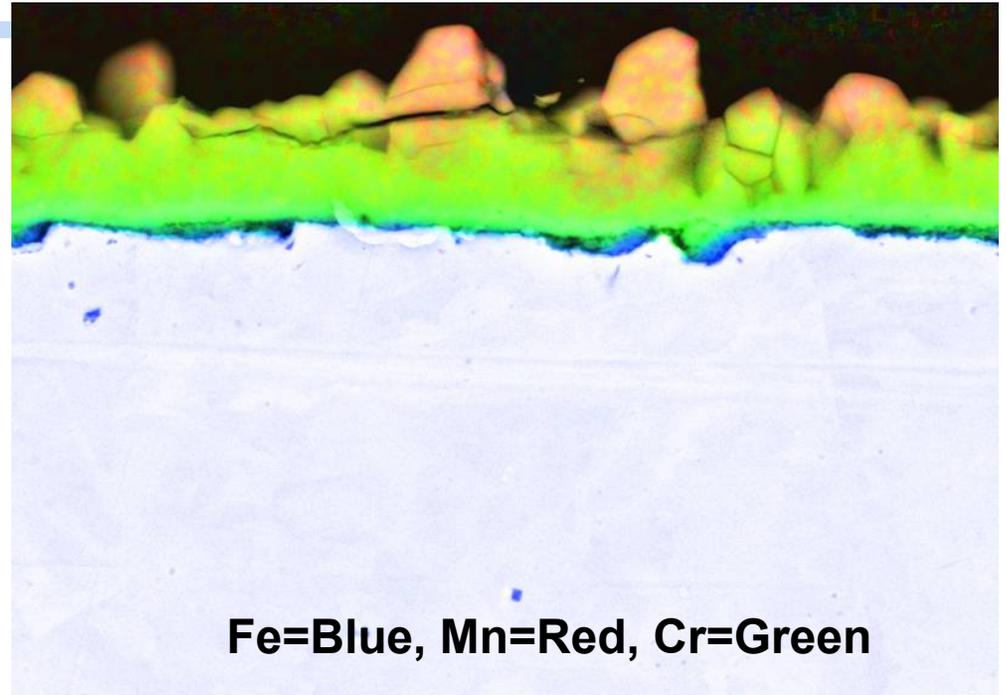
2000 Hourly Cycles

760 °C

Air + 37% H₂O



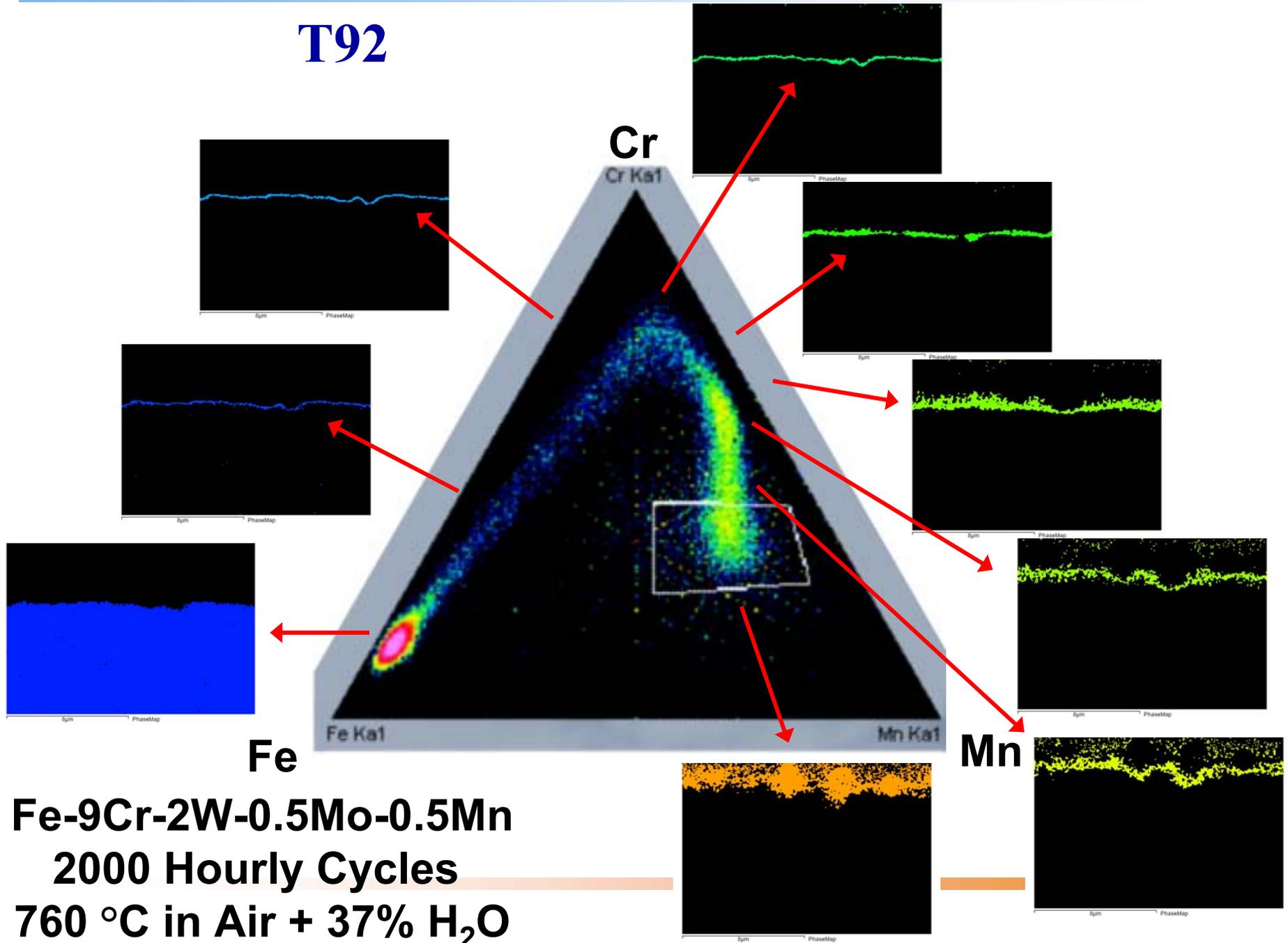
T92



8 μ m
8 μ m

2000 Hourly Cycles
760 °C
Air + 37% H₂O

T92



Fe-9Cr-2W-0.5Mo-0.5Mn
2000 Hourly Cycles
760 °C in Air + 37% H₂O

Evaporation Model – Some Verification

Table 5 – Comparison of experimental and predicted evaporation rates (all on a Cr₂O₃ basis).

Alloy and Conditions	Experimental Slope (kg m ⁻² s ⁻¹)	Evaporation based on Glusko ¹⁶ CrO ₂ (OH) ₂ (g) data (kg m ⁻² s ⁻¹)	Evaporation based on Gindorf ²⁰ CrO ₂ (OH) ₂ (g) data (kg m ⁻² s ⁻¹)	Evaporation based on Ebbinghaus ¹⁷ CrO ₂ (OH) ₂ (g) data (kg m ⁻² s ⁻¹)
Haynes 230 UNS NO6230 760°C 38% H ₂ O in air 1.9×10 ⁻³ m/s	-3.46×10 ⁻¹⁰ (21)	-6.50×10 ⁻¹¹	-7.00×10 ⁻¹⁰	-1.38×10 ⁻⁰⁸
Haynes 230 UNS NO6230 760°C 37% H ₂ O in air 7.6×10 ⁻³ m/s	-1.11×10 ⁻⁹ (21)	-1.27×10 ⁻¹⁰	-1.37×10 ⁻⁹	-2.69×10 ⁻⁰⁸
304L UNS S30403 600°C 10% H ₂ O in O ₂ 2.5×10 ⁻² m/s	-5.68×10 ⁻¹⁰ (7)	-3.79×10 ⁻¹¹	-5.23×10 ⁻¹⁰	-1.03×10 ⁻⁰⁸

Asteman et al., 2000

Advanced Steam Turbines – Mitigation Techniques

- **Reduce Cr activity → spinels**
 - Manganese-Chromium Spinel Formation
 - $0.5\text{MnCr}_2\text{O}_4 + \text{H}_2\text{O} + 0.75\text{O}_2 = \text{CrO}_2(\text{OH})_2 + 0.5 \text{MnO}$
 - Lowers Evaporation by a factor of:
 - 55 at 700°C
 - 35 at 800°C
 - **Reduce Cr activity → coatings**
 - **Thermal barrier coatings to reduce metal temperature and give a much thicker diffusion boundary layer**
 - **Steam chemistry—Reduce dissolved oxygen (DO)**
 - Limited by water dissociation and other steam cycle corrosion
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