Use Of High Temperature Electrochemical Cells For Co-Generation Of Chemicals And Electricity

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Approach

- Direct-Methane Solid Oxide Fuel Cells (SOFCs) for:
 Electricity generation and
 - Production of syngas (H₂+CO) or other chemicals Motivation
- Increase value of SOFC stacks via sale of both electricity and chemical products
 - Improve prospects for commercialization
- Achieve highly efficient utilization of natural gas
- Reduce cost of syngas produced from natural gas
- Cost of hydrogen (from syngas) too high compared with DoE targets (\$2.50/kg, equivalent to 1 gallon gasoline)
- Reduce cost of liquid fuels derived from syngas (methanol, synthetic diesel)

Other Advantages

- No dilution of syngas by nitrogen, as in air partial oxidation
 Avoids explosive methane-air mixtures as in partial oxidation reformers
- More appropriate H₂/CO ratio (≈2) for Fischer-Tropsch synthesis than steam reforming

Electrochemical Partial Oxidation (EPOx)

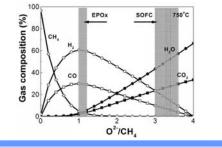
· Desired reaction is partial oxidation:

 $CH_{A} + O^{2-} = CO + H + 2e^{-}(-22KJ@750^{\circ})$

- Adjust CH_4 flow rate such that $O^{2-}/CH_4 \sim 1$
- 3-4 times that in a direct-methane SOFC, where the aim is to produce electricity by completely oxidizing methane:

$$\frac{1}{4}CH_4 + O^{2-} = \frac{1}{4}CO_2 + \frac{1}{2}H_2O + 2e^{-}(-200KJ@750)^{0}$$

Predicted equilibrium products versus O²⁻/CH₄



Problems with EPOx

Issues in prior EPOx work:

- •Anode coking during direct methane SOFC operation
- •SOFC power densities and syngas production rates were relatively low
- •Expensive non-standard SOFC anode materials, e.g. Pt, used to avoid coking
- Thermal self-sustainability of EPOx reactor
- Minimum requirement: $-\Delta \mathbf{H} = \mathbf{E}_{FC}$
- -AH=22kJ mol-1 CH4 at 750°C (reaction enthalpy change)
- EFC=nFV=135kJ / mol CH4 (V=0.7V, n=2 electrons/ CH4)

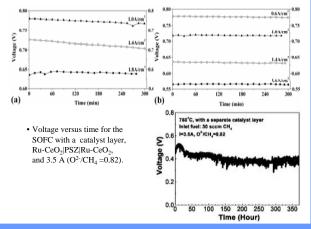
(electrical energy extracted)



· Extend from methane to natural gas

Solutions to Stable SOFC Operation

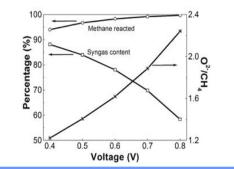
Stable, coke-free, high power density operation realized with barrier/catalyst layer
 Cell voltage versus time at constant current J for SOFCs operated in humidified methane at 8000C without (a) and with (b) barrier layer.

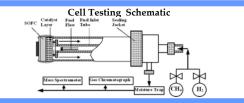


Tactics for Thermal Self-Sustainability

Thermo-neutral operation can be achieved by:

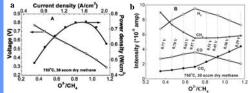
- Lower operating voltage, less electrical energy extracted per mole of methane
 But high enough to maintain high power output
- · Increase O2-/CH4 above 1, yielding more heat by increased complete oxidization



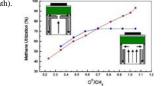


Experimental Results

Results for the SOFC NiO-YSZ|YSZ|YSZ-LSM, LSM, tested in 30 sccm dry methane in the anode and ambient air in the cathode at 750 °C. a, Voltage and power density versus current density or O²⁻/CH₄ ratio. b, The product gas peak intensity versus O²/CH₄ ratio.



Methane utilization versus O²/CH₄ ratio for SOFCs operated on 30 sccm dry methane at 750°C. Results are compared for identical SOFCs with the standard (•) and modified (•) gas-flow geometries indicated schematically in the insets (the arrows illustrate the fuel flow path).



Conclusions

- Methane-fueled SOFCs operated under appropriate conditions produce both syngas and electricity
- · Coking can be suppressed by using barrier layers
- SOFCs operated at T≈750 °C, V≈0.4V, and O²⁻/CH₄≈1.2:
- High electrical power output (~0.7 W cm⁻²)
- High syngas production rates (~20 sccm cm⁻²)
- Thermally self-sustaining conditions
- Can produce syngas/hydrogen at lower cost than other methods
 Due to the value of the electricity produced
- Sale of both electricity and syngas increases the value of the fuel cell
 Important because fuel cell cost is a key barrier to commercialization

Acknowledgments

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