

Solid Oxide Fuel Cell Research at Argonne National Laboratory

**R. Kumar, R. Ahluwalia, T. Cruse, J. Ralph, X. Wang, and
M. Krumpelt**

**2nd Solid State Energy Conversion Alliance Workshop
Arlington, VA
March 29-30, 2001**

Task areas

- Low-temperature cathode materials
- Sulfur-tolerant anode materials
- Metallic interconnect (bipolar) plates
- Cell, stack, and systems modeling

Low-Temperature Cathode Development Overview

- LSM is a poor cathode material at $<900^{\circ}\text{C}$, even as LSM/YSZ composite
- Need to develop a mixed conducting material to achieve better power densities at $\leq 800^{\circ}\text{C}$
- Options:
 - replace Mn in LSM by Co, Fe, or Ni
 - move to differently structured materials
- $\text{La}(\text{Sr})\text{FeO}_3$ (LSF) has proven to be the most compatible and best performing cathode with YSZ

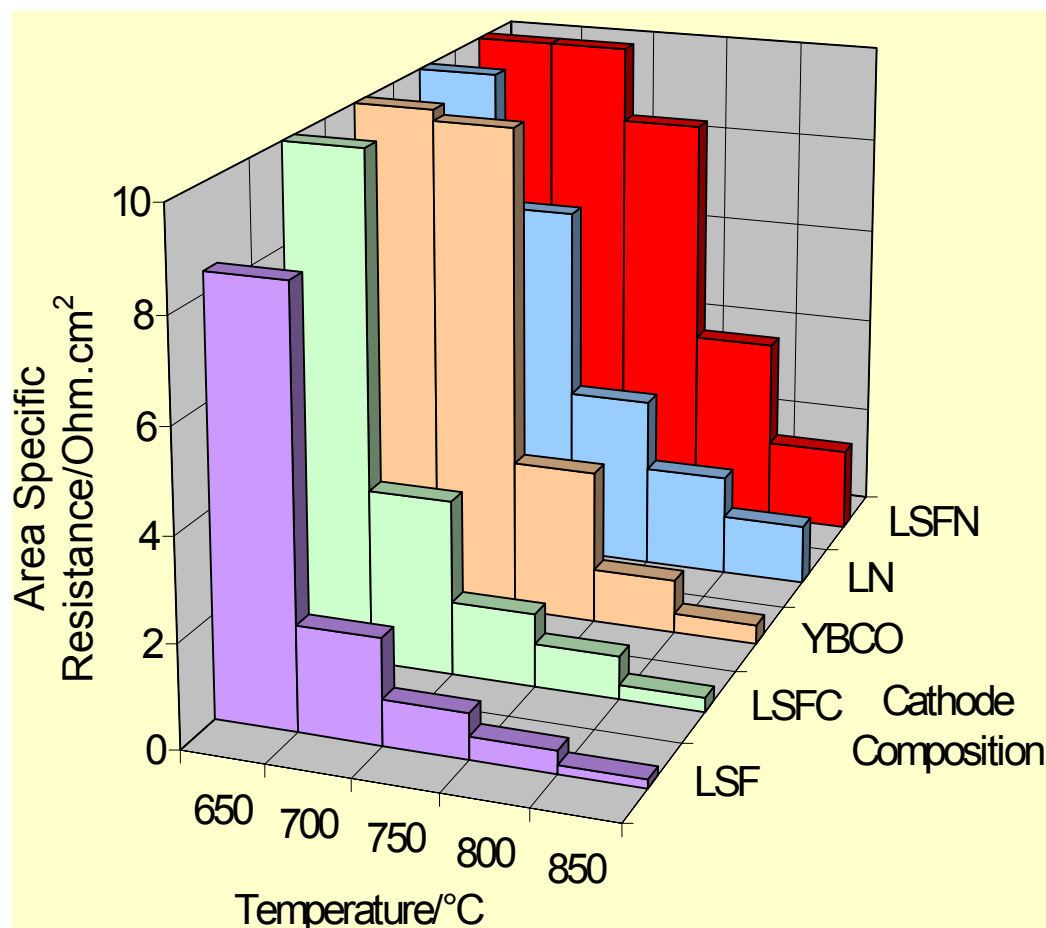
Low-Temperature Cathode Development

Perovskite-based cathodes

Composition	Electronic Conductivity (Scm^{-1}) at 800°C	Ionic Conductivity (Scm^{-1}) at 900°C
$\text{La}_{1-x}\text{Sr}_x\text{CoO}_3$	1000-2000	8×10^{-1}
$\text{La}_{1-x}\text{Sr}_x\text{FeO}_3$	400-500	1×10^{-2}
$\text{La}_{1-x}\text{Sr}_x\text{NiO}_3$	500	-
$\text{La}_{1-x}\text{Sr}_x\text{MnO}_3$	100-200	10^{-7}
$\text{La}_{1-x}\text{Sr}_x\text{CrO}_3$	<100	< 10^{-7}

Low-Temperature Cathode Development

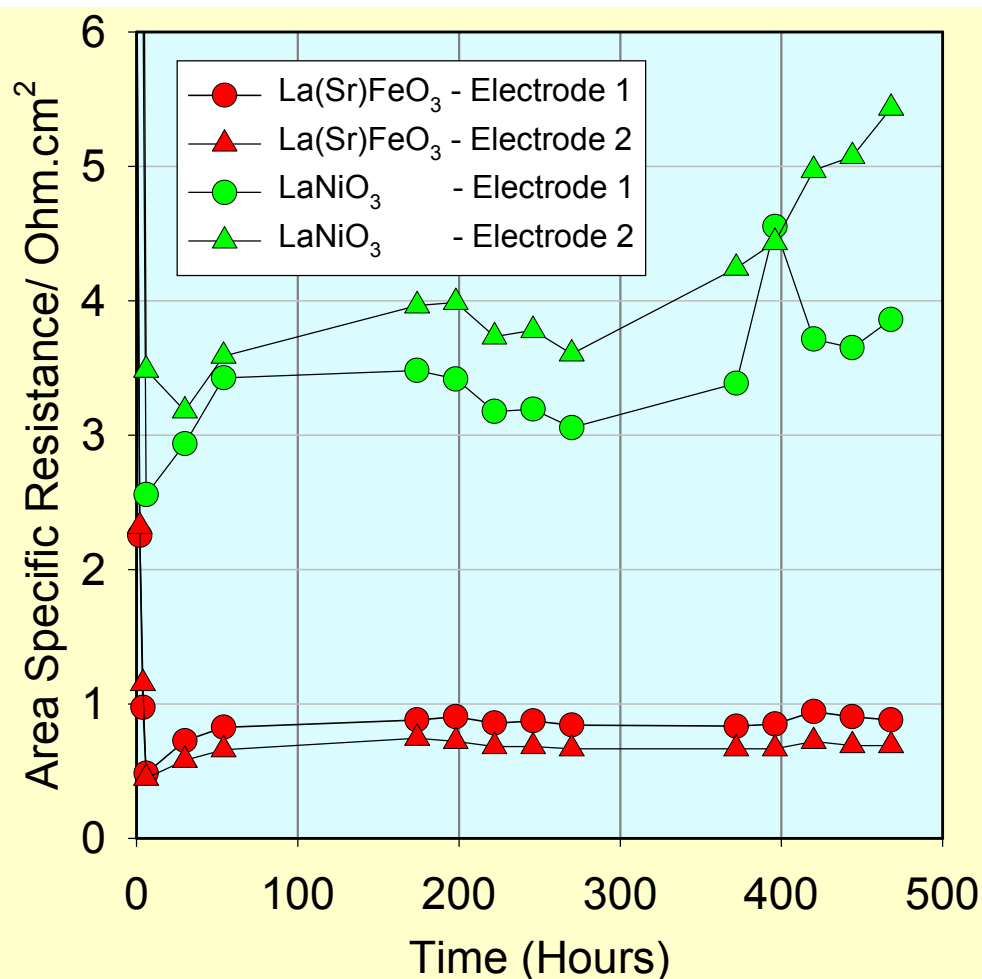
Area-specific resistances on YSZ



- Ferrite-based perovskites display best performance at all temperatures (initial target ASR is $<1 \text{ } \Omega \text{ cm}^2$)
- Layered structures show good performance at $\geq 850^\circ\text{C}$ but high activation energies preclude use at $\leq 800^\circ\text{C}$
- Nickelate-based perovskite has potential if the structure can be stabilized when doped

Low-Temperature Cathode Development

Long-term ASR on YSZ at 800°C

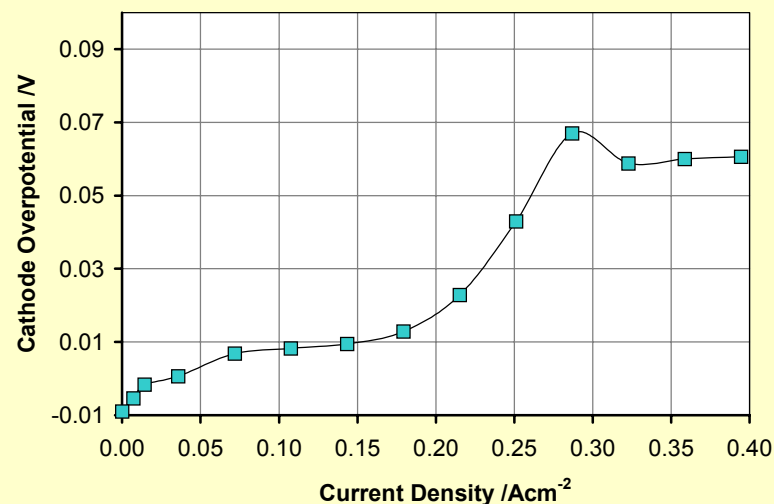
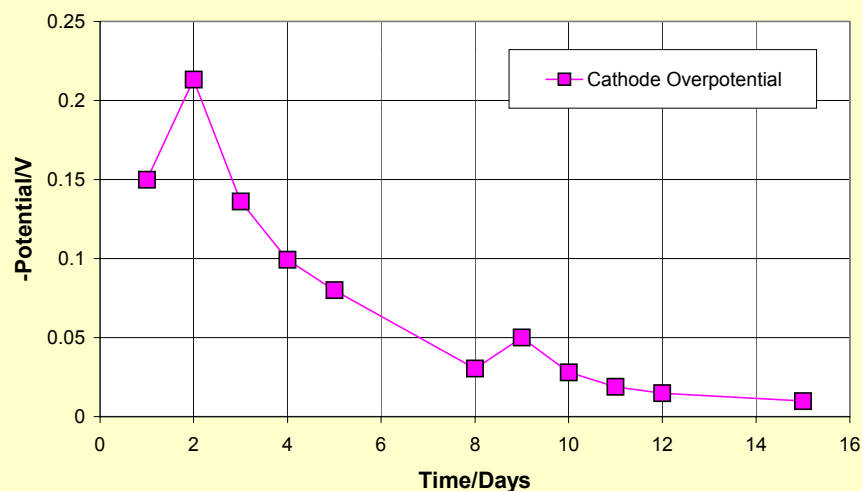


- LSF displays the most stable performance with an ASR of $<1 \Omega \text{ cm}^2$
- LN has too high an ASR at 800°C

Low-Temperature Cathode Development

Polarization curves for La(Sr)FeO₃ on YSZ

- Current conditioned for ~ 330 h at 250 mA cm^{-2} at 800°C
- Overpotentials decreased with time over the 16 days
- Values for LSF at 800°C are similar to LSM at 1000°C



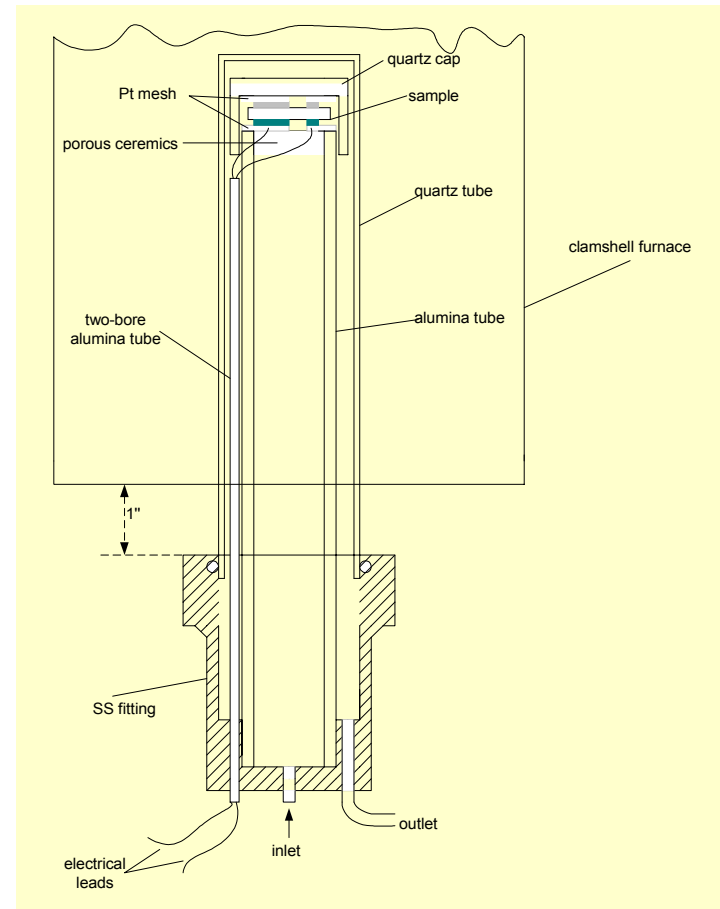
Sulfur-Tolerant Anode Materials

Approach

- Modify conventional anode material with an additive that has suitable redox chemistry
 - additive captures H_2S in preference to Ni; the H_2S is subsequently oxidized to SO_2
- Replace the Ni in Ni-YSZ with other metal or alloy active for electrooxidation of H_2 but resistant to poisoning by H_2S
- Investigate new classes of materials based on carbides and/or sulfides

Sulfur-Tolerant Anode Materials Status

- Several candidate anode materials have been coated on commercial YSZ disks for half-cell tests
- Testing will get underway within the next few weeks with fuel gases containing 0-100 ppm H_2S



Test Apparatus Schematic

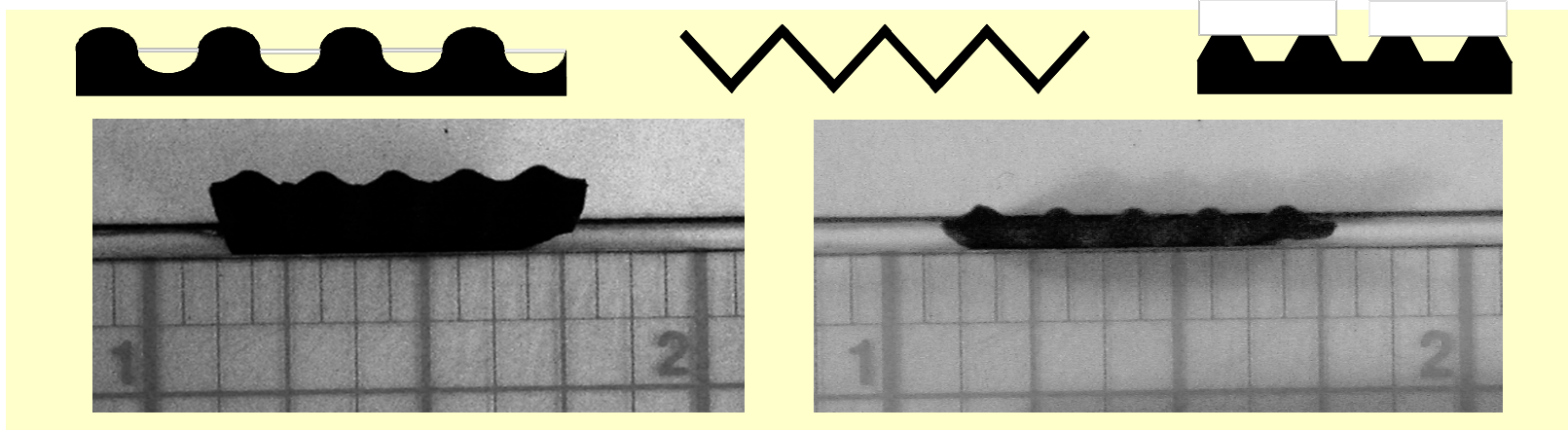
Metallic Interconnect Development

Materials requirements

- Electronically conductive
- Chemically stable under under both anodic and cathodic conditions
- Coefficient of thermal expansion similar to the other fuel cell materials
- Formable (for internally manifolded stack designs)

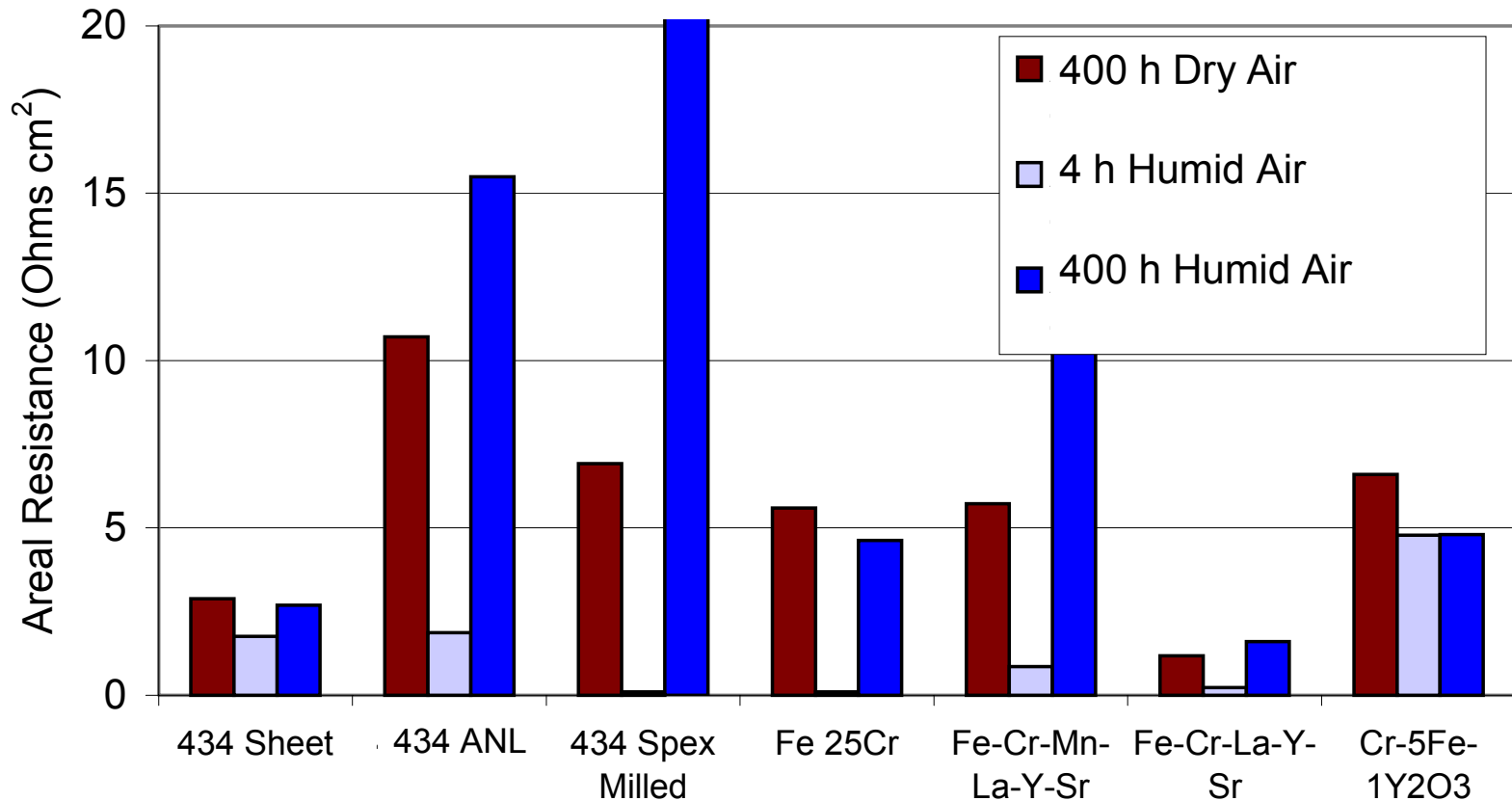
Metallic Interconnect Development Approach

- Alloys similar to ferritic stainless steels
 - reduce Cr, other elements that can degrade fuel cell performance
 - additives to improve properties and protective scale
- Coated materials to impart chemical stability
- Powder production by mechanical alloying techniques
- Processing technique can yield almost any desired shape
 - flat, corrugated, textured, functionally graded



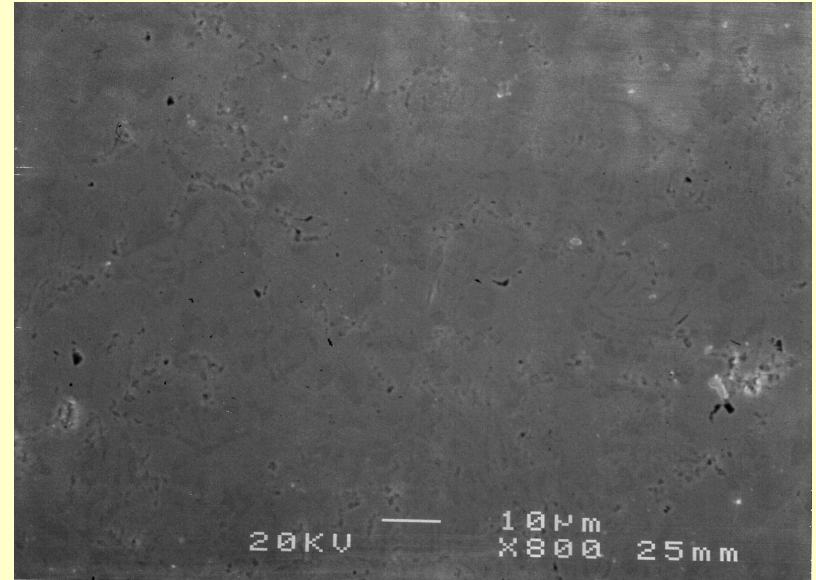
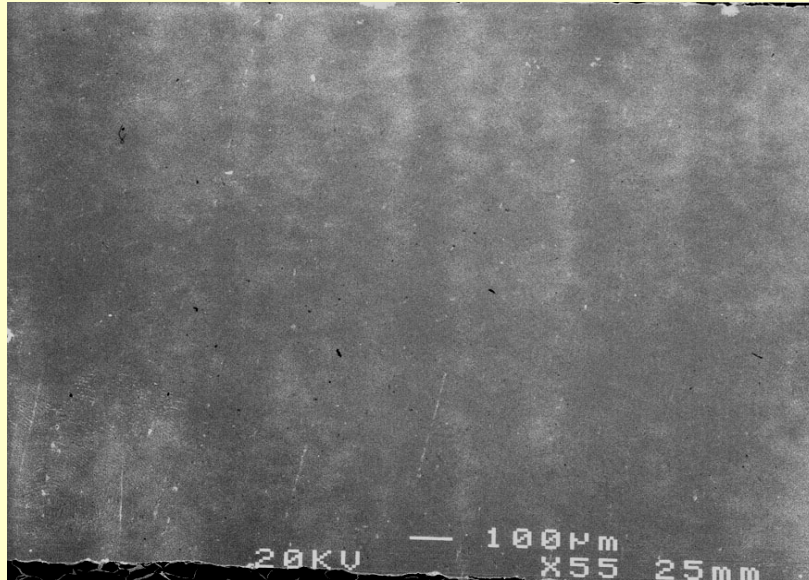
Metallic Interconnect Development

Electrical resistance of the oxide scale



Metallic Interconnect Development

Multi-layer plates show excellent bonding

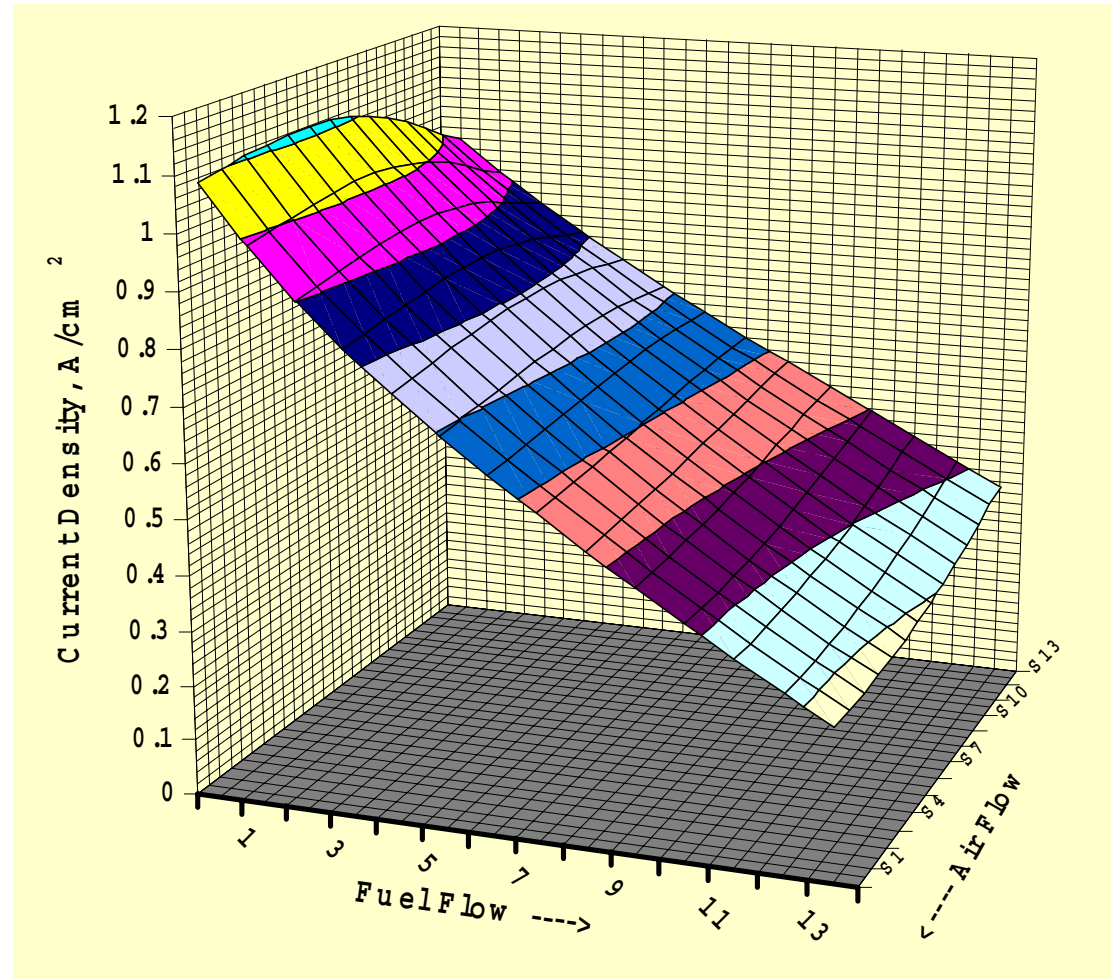


10 layers of ferritic stainless steel alloy
Each layer $\sim 140\text{ }\mu\text{m}$ thick
(Fe-Cr-La-Y-Sr)

Cell, Stack, and Systems Modeling

Current density distribution, 0.7 V, 85% u_f

- Single cell model:
sample results
- Current density can vary by a factor of 5



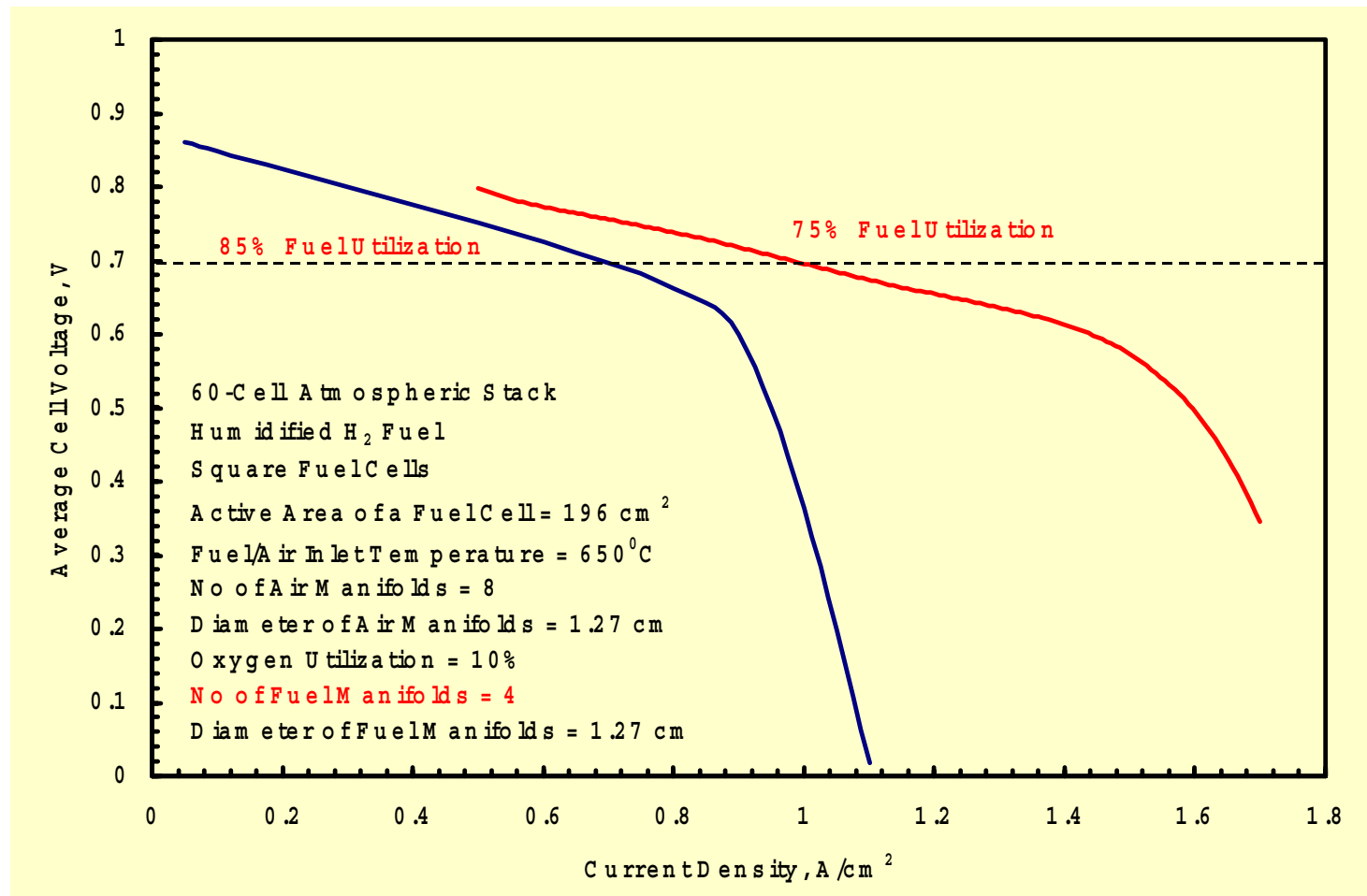
Cell, Stack, and Systems Modeling

Cell performance change with reformat

	H u m i d i f i e d H ₂ R e f o r m a t e	
A c t i v e C e l l A r e a	1 9 6 c m ²	1 9 6 c m ²
F u e l C o m p o s i t i o n	9 5 . 2 % H ₂	5 9 . 2 % H ₂
	4 . 8 % H ₂ O	1 9 . 3 % H ₂ O
		4 . 2 % C H ₄
		1 0 . 3 % C O
		7 . 1 % C O ₂
I n l e t T e m p e r a t u r e	6 5 0 ⁰ C	6 5 0 ⁰ C
M a x C e l l T e m p e r a t u r e	8 0 4 ⁰ C	8 0 0 ⁰ C
F u e l U t i l i z a t i o n	8 5 . 3 0 %	8 5 . 3 0 %
O x y g e n U t i l i z a t i o n	7 . 3 0 %	9 . 4 0 %
C a l l V o l t a g e	0 . 7 V	0 . 7 V
A v g N e m s t P o t e n t i a l	0 . 8 6 V	0 . 8 4 V
A v g C u r r e n t D e n s i t y	0 . 6 5 A / c m ²	0 . 5 1 8 A / c m ²
G r o s s P o w e r	8 9 . 4 W	7 1 W
N e t P o w e r	8 7 . 1 W	7 0 . 1 W

Cell, Stack, and Systems Modeling

Stack performance vs. fuel utilization



Summary

Current and future work

- Micro-engineer the cathode-electrolyte interface to further improve cathode performance
- Evaluate anode materials with 0-100 ppm H_2S in fuel gas
- Characterize oxide scale on metallic bipolar plates for growth rates and electrical conductivity
- Test developed materials in full cell and short stack configurations, as appropriate

