# Joint Computational/Experimental Study of Flashback in Hydrogen-rich Gas Turbines

Venkat Raman (PI) Noel Clemens (co-I)

The University of Texas at Austin

# Challenges in Simulating Gas Turbines

#### Lack of appropriate physical models

Unsteady dynamics, wall-flame interactions, multiple combustion regimes

#### Less than ideal validation data

- Diagnostic fidelity reduces with flow complexity
  - High-pressure confined environment

#### Geometric complexity

- Vanes, swozzles, etc.
- Unstructured grid systems are indispensible

#### Uncertainty

Boundary conditions, chemistry, operating conditions

# Operating Hypotheses

- Combined LES and RANS capabilities
  - → LES is not the solution to all problems
  - RANS has lot of unrealized potential
- Experiments in the absence of modeling guidance is not useful for advancing predictive capability
  - Models should capture sensitivity to parameters in a real gas turbine
  - Experiments should be designed to reproduce this sensitivity
    - Non-trivial exercise
    - Current simulation approaches cannot provide this guidance

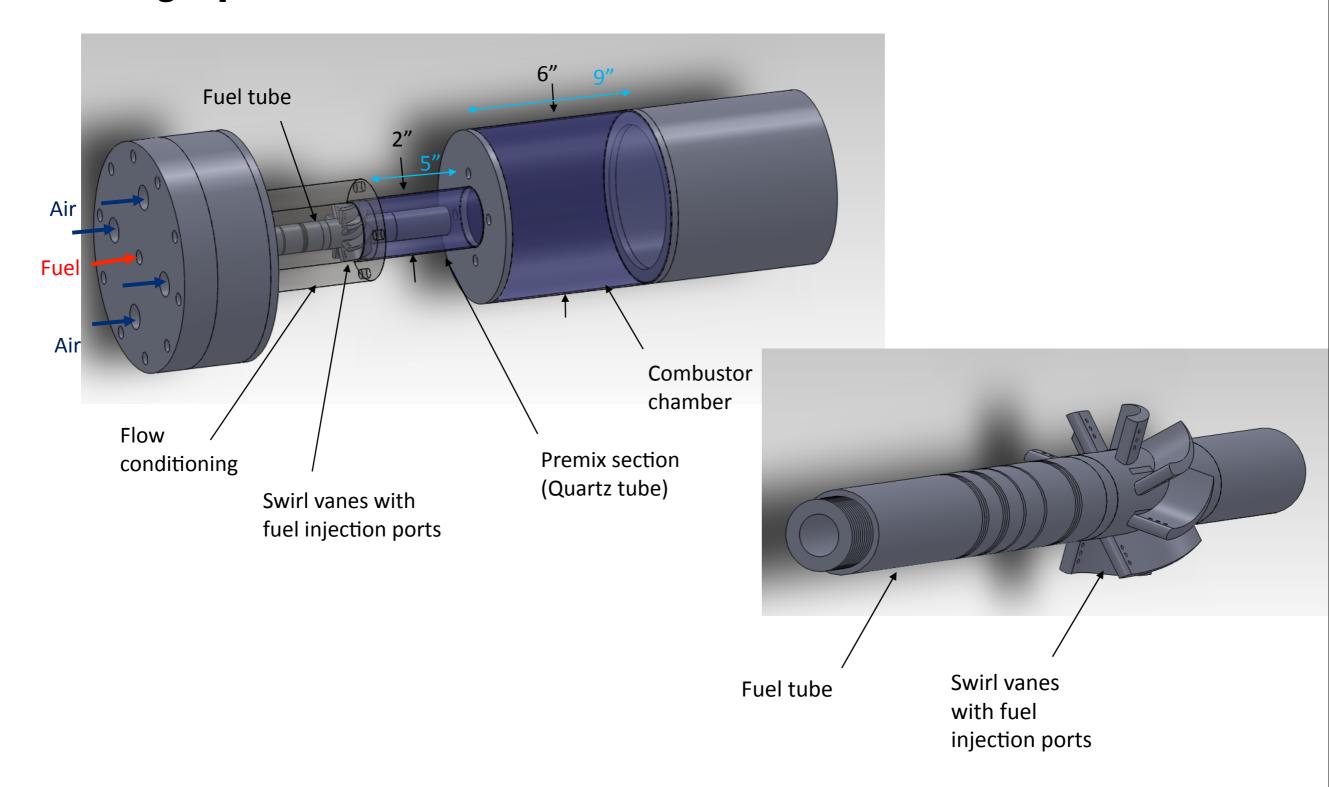
# **Objectives**

- Integrate high and low fidelity computational models (LES, RANS) with experiments
  - To capture unsteady dynamics in gas turbine combustors
  - Provide predictive insight in the design process

- Target-based model development
  - UT high-pressure combustor as the overarching simulation

# Target System

#### • UT high-pressure swirl combustor



# Key Issues

#### Fuel injection, mixing, and combustion

- Crossflow jet configuration
- Flame stabilization and mixing issues

#### Flashback dynamics

- Flame propagation in turbulent core flow
- Flame-wall interaction and boundary layer modulation

# Key Computational Issues

#### LES-based modeling

- Combustion models in complex geometries
- Flame-wall interaction modeling
- Jet-in-crossflow anomalous behavior

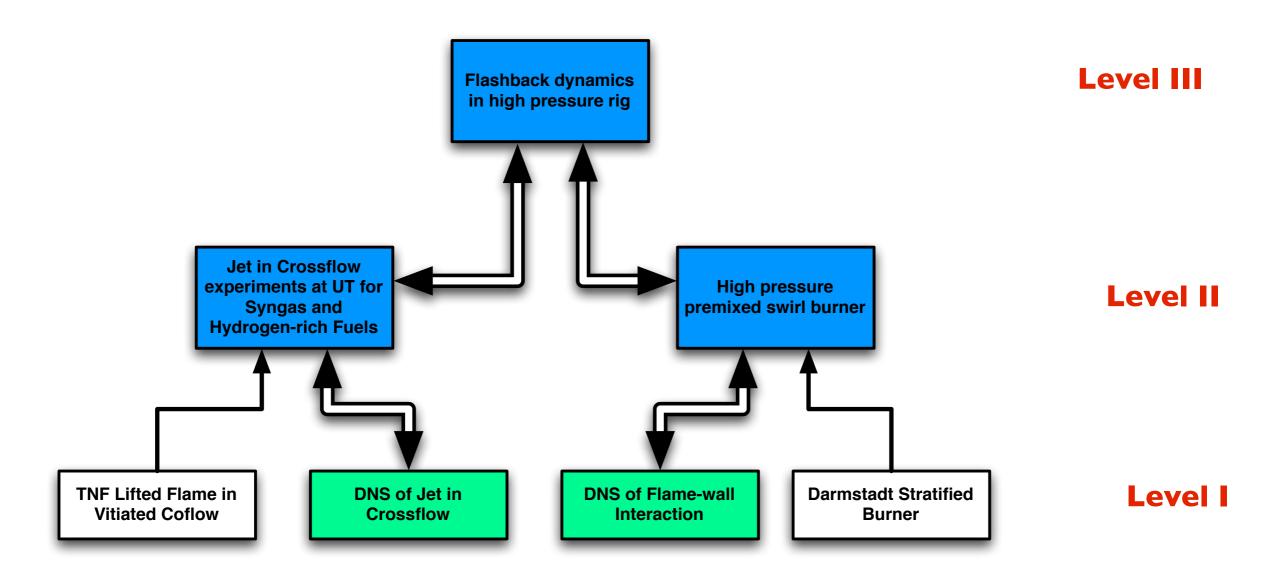
#### Predictive uncertainty in RANS

Highly parameter dependent turbulence models

#### Technology transfer

→ A common platform to share advances with industry

# Hierarchical Validation Pyramid



- Level 1 Fundamental data from legacy expts. and direct numerical simulations (DNS)
- Level 2 UT re-configurable experiments designed for validation
- Level 3 UT target system experiments

## Research Plan

#### UT high-pressure swirl combustor experiments

Validation driven experiments

#### LES model development

- Eulerian probability density function (PDF) approach for complex geometries
- Transported-equation based dissipation rate model

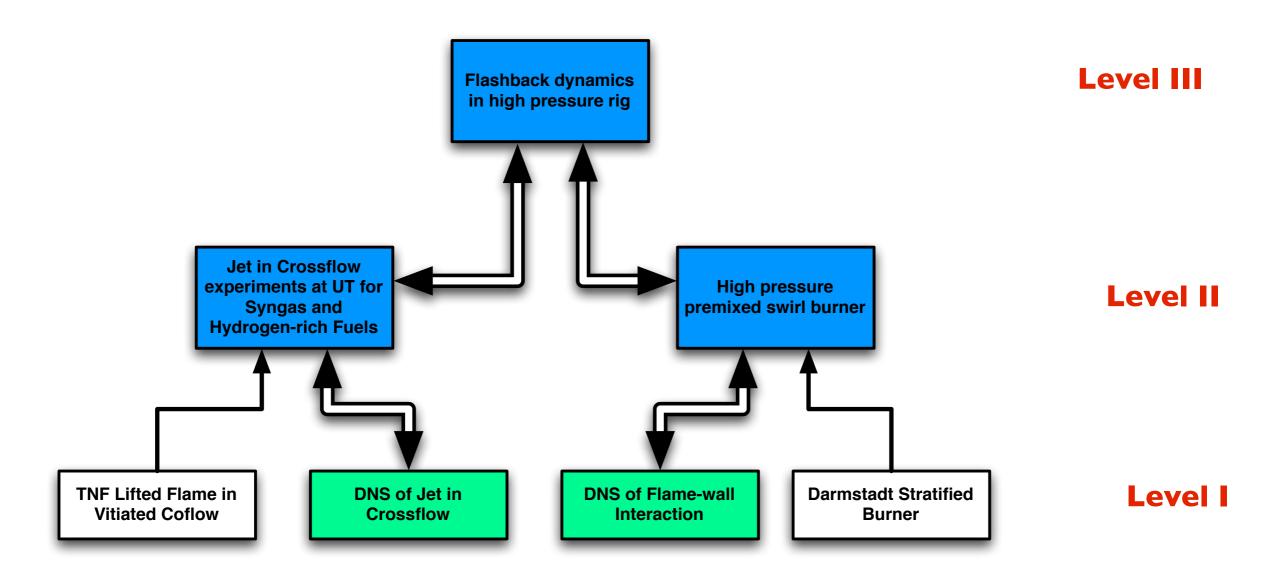
#### RANS accuracy improvement

- Calibration as a mathematical approach
- Propagating uncertainties in chemistry and boundary conditions

#### Open source model transfer

OpenFOAM based model implementation

# Hierarchical Validation Pyramid



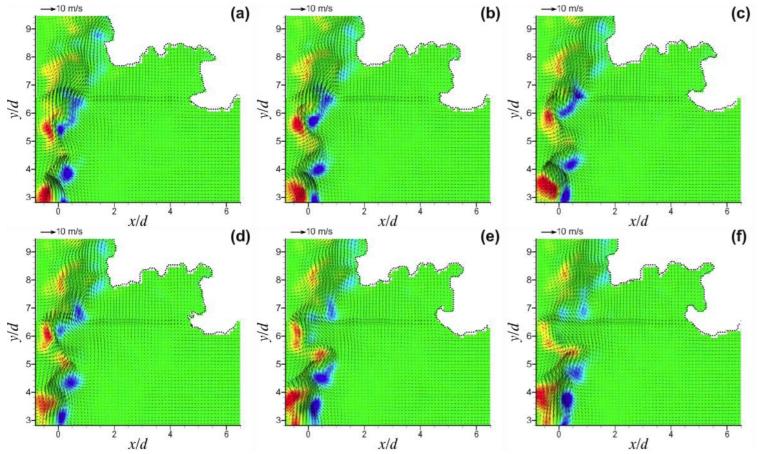
- Level 1 Fundamental data from legacy expts. and direct numerical simulations (DNS)
- Level 2 UT re-configurable experiments designed for validation
- Level 3 UT target system experiments

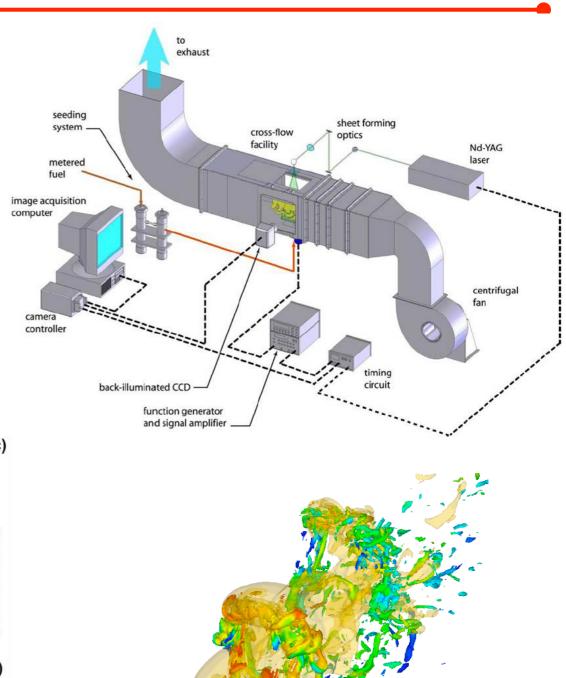
### Pitched Jets in Crossflow

# Variations in jet angle, fuel composition



Figure 12: Jet flames in crossflow with different levels of premixing. The fuel is 70% CH4 + 30% H2. (a) non-premixed, (b) jet fluid diluted by 25% (volume basis) with air, and (c) jet fluid diluted by 50% with air.



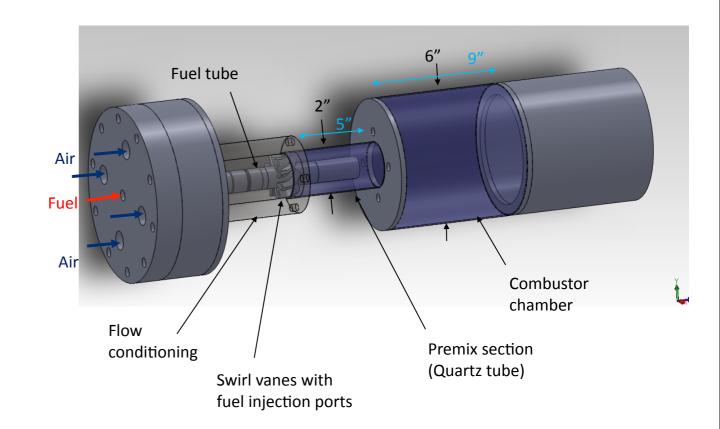


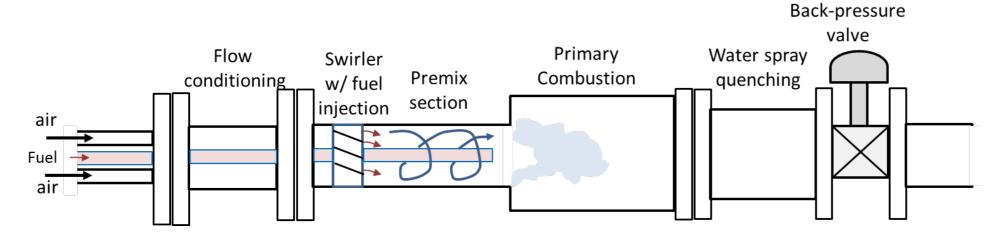
**LES of JICF** 

**Simultaneous PLIF +PIV** 

# Flashback Dynamics

- Fuel injection through swirl vanes
- Flashback induced through back-pressure valve
- Optical access for simultaneous velocity/scalar measurements





# Modeling Approach

- Probability density function (PDF) approach
  - Solve a high-dimensional transport equation for joint-PDF of gas phase scalars
- In LES calculations, the filtered moments of the composition vector are required

$$\widetilde{\boldsymbol{\phi}} = \int \mathcal{G}(\boldsymbol{\zeta}) P_{\xi}(\boldsymbol{\zeta}; \mathbf{x}, t) d\boldsymbol{\zeta}$$

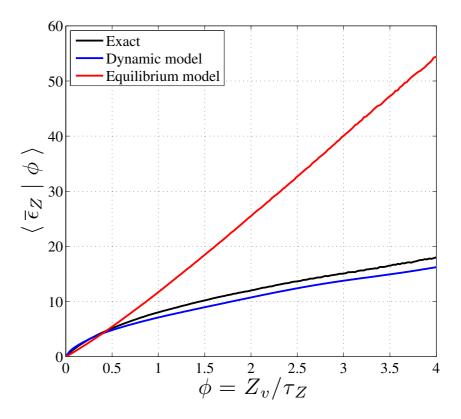
PDF transport equation

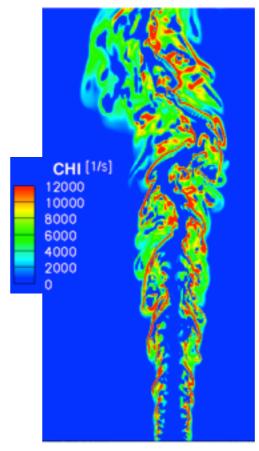
$$\frac{\partial P}{\partial t} + \frac{\partial}{\partial x_j} \left[ \widetilde{Pu_j | \zeta} \right] = -\frac{\partial}{\partial \zeta_\alpha} \left[ \widetilde{P\mathcal{M}_\alpha | \zeta} \right] - \frac{\partial}{\partial \zeta_\alpha} \left[ PS_\alpha \right]$$
 Conditional Diffusion

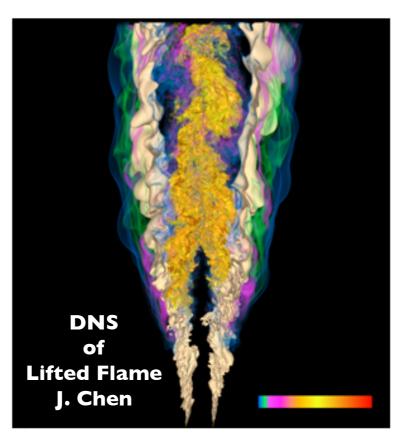
Condition diffusion requires a model for scalar dissipation rate

# Nonequilibrium Dissipation Rate Model

- Currently used dissipation rate models rely on equilibrium assumption
  - Highly restrictive
  - Invalid even in homogeneous isotropic turbulence
- Transport-equation based dissipation model
  - Incorporates spatial transport of scalar energy
  - Allows scalar and turbulence scales to be decoupled

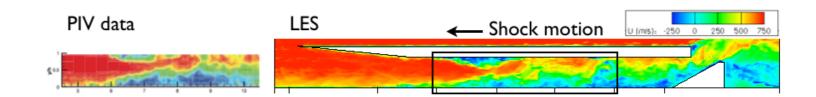


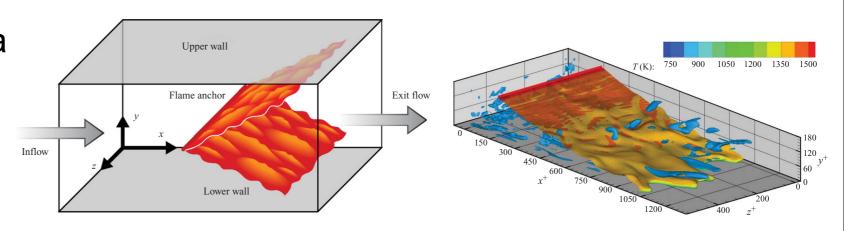




#### Flame-Wall Interaction

- Propagation of flames in a boundary layer
  - Modulates the turbulent boundary layer
  - Alters turbulent energy transport and dissipation
- Similar to unstart propagation in scramjets
  - Propagation of density/ pressure fronts through a separated boundary layer
- DNS-based analysis of turbulent flux models

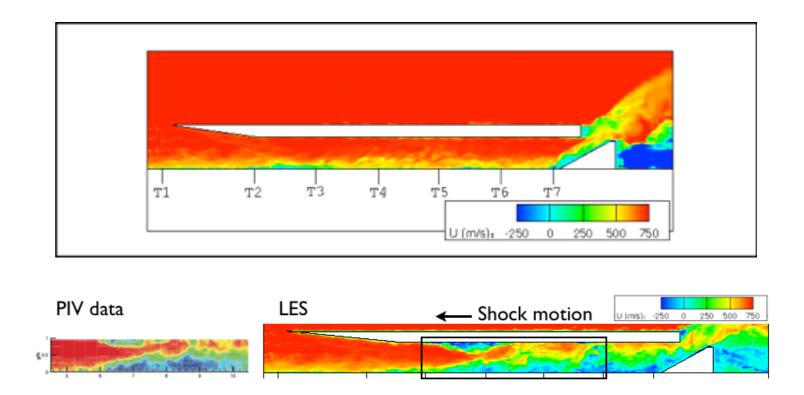


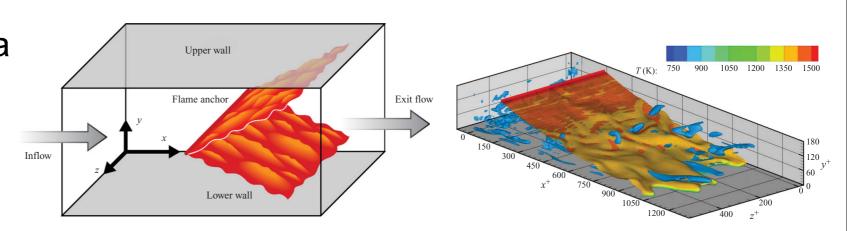


DNS of J. Chen (Sandia)

### Flame-Wall Interaction

- Propagation of flames in a boundary layer
  - Modulates the turbulent boundary layer
  - Alters turbulent energy transport and dissipation
- Similar to unstart propagation in scramjets
  - Propagation of density/ pressure fronts through a separated boundary layer
- DNS-based analysis of turbulent flux models





**DNS of J. Chen (Sandia)** 

# Modeling PDF Transport Equation

#### PDF transport equation

$$\frac{\partial P}{\partial t} + \frac{\partial}{\partial x_j} \left[ P\widetilde{u_j | \boldsymbol{\zeta}} \right] = -\frac{\partial}{\partial \zeta_\alpha} \left[ P\widetilde{\mathcal{M}_\alpha | \boldsymbol{\zeta}} \right] - \frac{\partial}{\partial \zeta_\alpha} \left[ PS_\alpha \right]$$
Conditional Diffusion

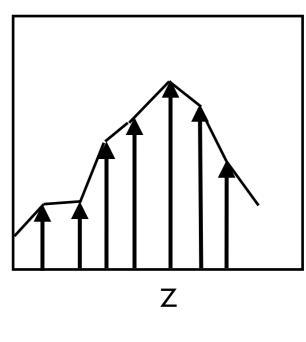
**Chemical Source** 

- PDF equation is high-dimensional
  - → If N species present in chemistry, N+5 dimensions
- Lagrangian Monte-Carlo approach typically used
  - Stochastic in nature
  - Numerical stability is highly flow dependent
  - Difficult to maintain numerical accuracy in complex geometries
  - Highly expensive for realistic flow configurations

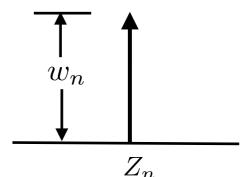
# Direct-Quadrature Method of Moments (DQMOM)

- DQMOM uses dirac-delta functions to discretize the PDF
- Each delta-function characterized by a weight and abscissa
  - Transport equations for these two variables can be formulated
- Similar in structure to scalar transport equations

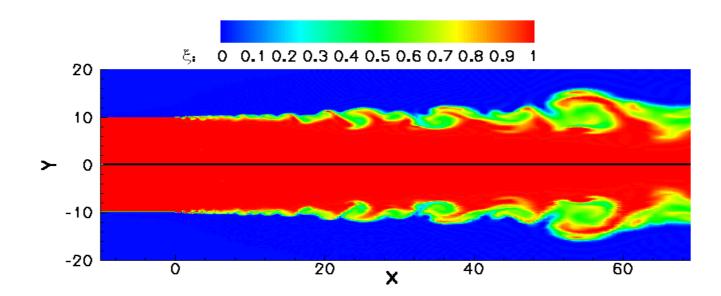
$$\frac{\partial w_n}{\partial t} + \overline{U_i} \frac{\partial w_n}{\partial x_i} = \frac{\partial}{\partial x_i} \left( \Gamma \frac{\partial w_n}{\partial x_i} \right) + a_n$$



P(Z)



# Test case: 2-D shear layer



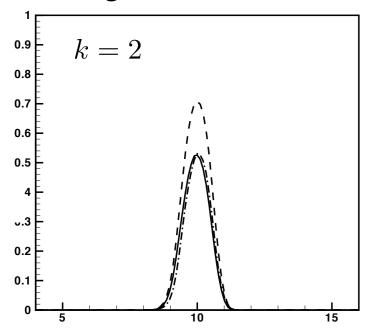
- Flow conditions similar to the experiment of Mungal and Dimotakis (1984)
- Two streams at velocity of 8.8 m/s and 22 m/s
- Single step chemistry formulated using progress-variable and mixture fraction

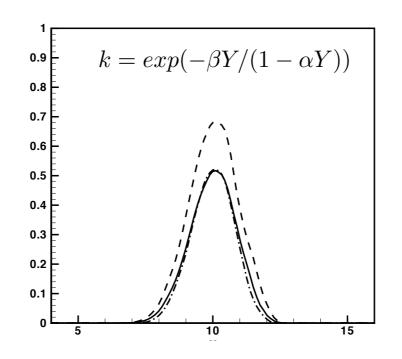
$$S(Y,Z) = k \left(\frac{Z}{Z_{st}} - Y\right) \left(\frac{1 - Z}{1 - Z_{st}} - Y\right)$$

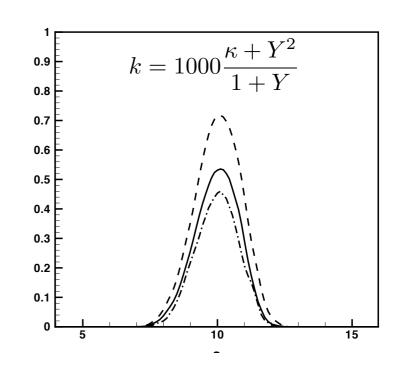
- Test cases performed
  - → LES simulation of first moment of Y,Z and second moment of Z
  - Lagrangian simulations with IEM mixing model
  - → DQMOM simulation with IEM mixing model and 2-peak formulation
  - Different functional form for rate constants

#### Test results

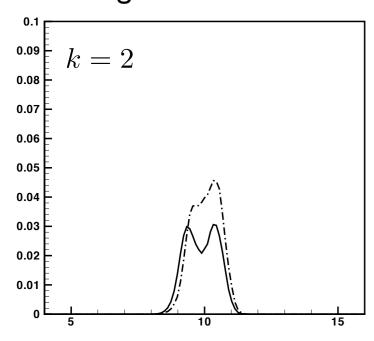
#### Progress variable mean

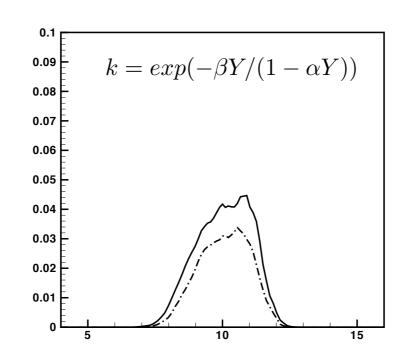


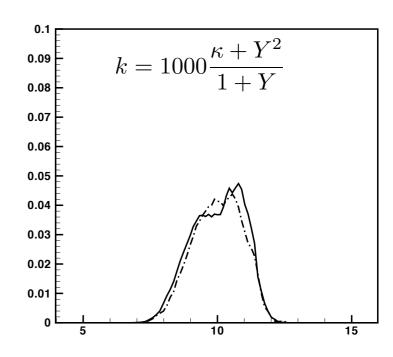




#### Progress variable variance





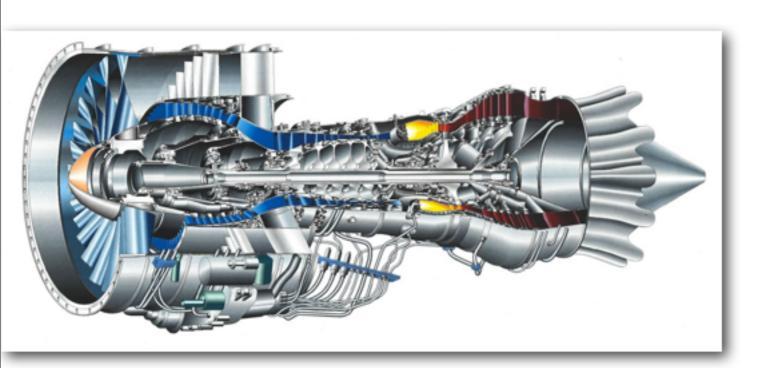


Solid - DQMOM: Dash-dotted - Lagrangian: Dashed - No subgrid model

# Decision Making, Risks, and CFD

- CFD is a vital tool for understanding practical engineering devices
- CFD models are also highly unreliable
  - Modeling is as much an art as science
- Can we rely on CFD results to make critical decisions?



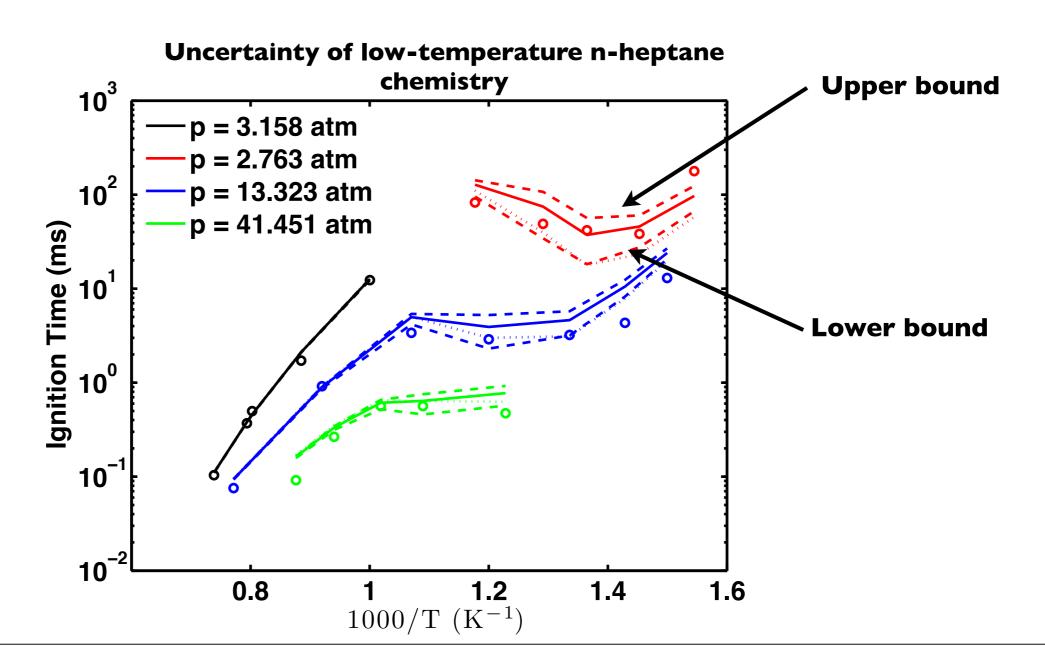






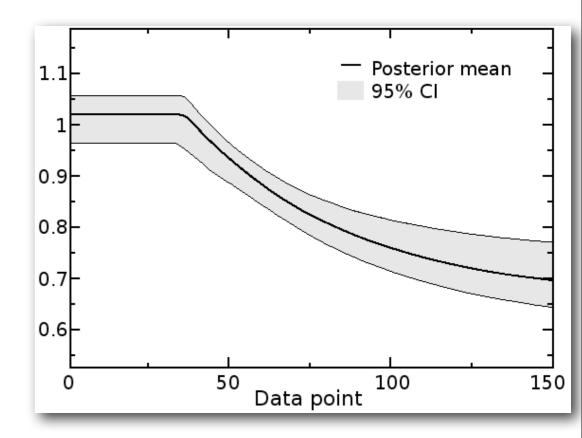
# DOE Predictive Science Academic Alliance Program

- PECOS Center at UT Austin focuses on estimating uncertainties
- Quantifying uncertainties
  - Use experiments and models to determine simulation error bars



# Uncertainty Quantification (UQ)

- Since models will always incur errors, the best strategy is to quantify the errors
  - In a simple sense, compute error bars for the solution
  - More broadly, CFD results are no longer deterministic "plots" but probabilistic distributions
- The quantifiable error in the computations is termed uncertainty
  - Expressed in terms of confidence in results, which are also computed



#### RANS Models for Scalar Flux

#### RANS scalar transport equation

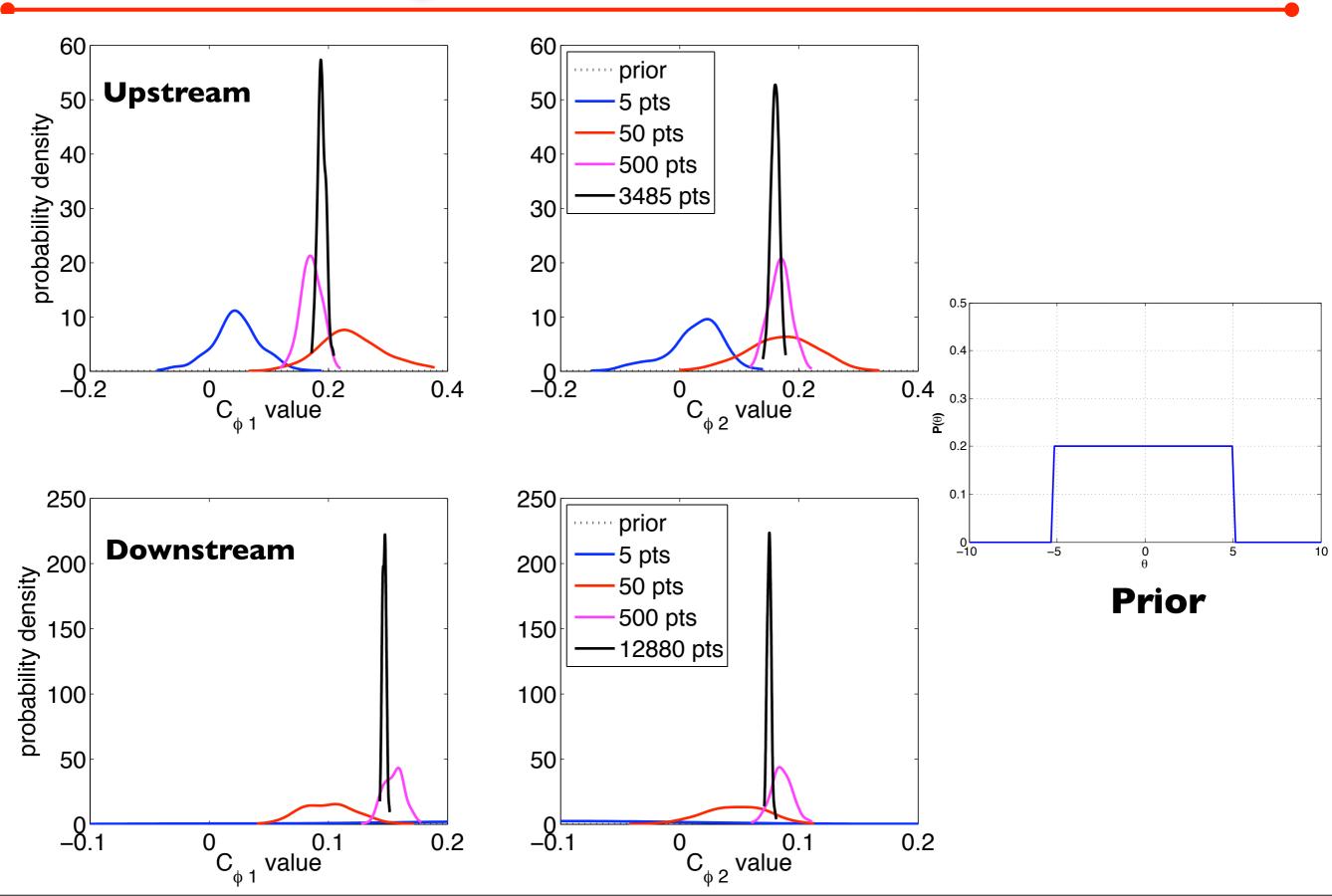
$$\frac{\partial \overline{\rho} \widetilde{\phi}}{\partial t} + \frac{\partial \overline{\rho} \widetilde{u}_{j} \widetilde{\phi}}{\partial x_{j}} - \frac{\partial}{\partial x_{j}} \left( \overline{\rho} D \frac{\partial \widetilde{\phi}}{\partial x_{j}} \right) = -\frac{\partial \overline{\rho} u_{j}' \phi'}{\partial x_{j}} + \underbrace{\widetilde{S}(\phi)}_{\text{Chemical source term}}_{\text{Scalar flux}}$$

- Closures for the scalar flux needed
- Several models considered
  - E.g., Combination generalized gradient diffusion model

$$\widetilde{u_i'\phi'} = -\tau_T \left( C_{\phi 1} \widetilde{u_i'u_j'} + C_{\phi 2} \frac{\widetilde{u_i'u_k'} \, \widetilde{u_k'u_j'}}{k} \right) \frac{\partial \widetilde{\phi}}{\partial x_j}$$

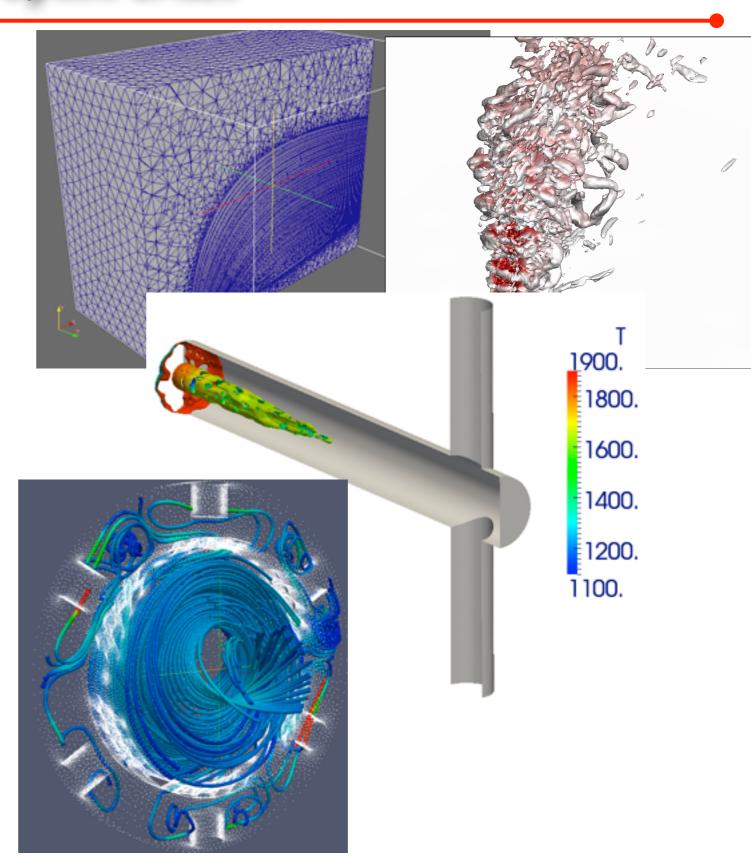
ightharpoonup Model coefficients ( $C_{\phi 1}, C_{\phi 2}$ ) need to be determined

# Probabilistic Description of RANS Model Constants



# Technology Transfer Using OpenFOAM

- Open source software
- Large-scale code modification
  - Numerics changed to accommodate LES computations
  - New flow solvers for turbulent combustion problems
  - Arbitrary chemistry inclusion with chemkincompatible interface



# UT Gas Turbine Program

#### LES/RANS combined modeling approach

- LES for unsteady dynamics
- Calibration-based RANS for parametric studies

#### Well-characterized experimental setup

- Simultaneous PIV/PLIF measurements under high pressure conditions
- Pitched jets in crossflow with varying fuel compositions

#### Open source technology transfer

OpenFOAM based transfer of models