

Project Kickoff Meeting Transformational SOFC Technology (DE-FE0027584)

Presented To: National Energy Technology Laboratory (NETL)

November 16, 2016 Webconference

Public Version

Ultra-Clean, Efficient, Reliable Power



Attending Organizations:National Energy Technology Laboratory (NETL/DOE),
FuelCell Energy, Inc. (FCE), Northwestern University (NU)

12:15 pm - 12:30 pm	Introductions and brief procurement discussions	NETL
12:30 pm – 12:40 pm	Project Overview	H. Ghezel-Ayagh
12:40 pm – 1:05 pm	Cell Technology and Manufacturing	Scott Barnett / Eric Tang
1:05 pm - 1:25 pm	Stack Design and Fabrication	Scott Corey / Keith Davis
1:25 pm - 1:30 pm	Q&A and Follow up Discussion	All

* Times are in EDT (Eastern Daylight Saving Time)



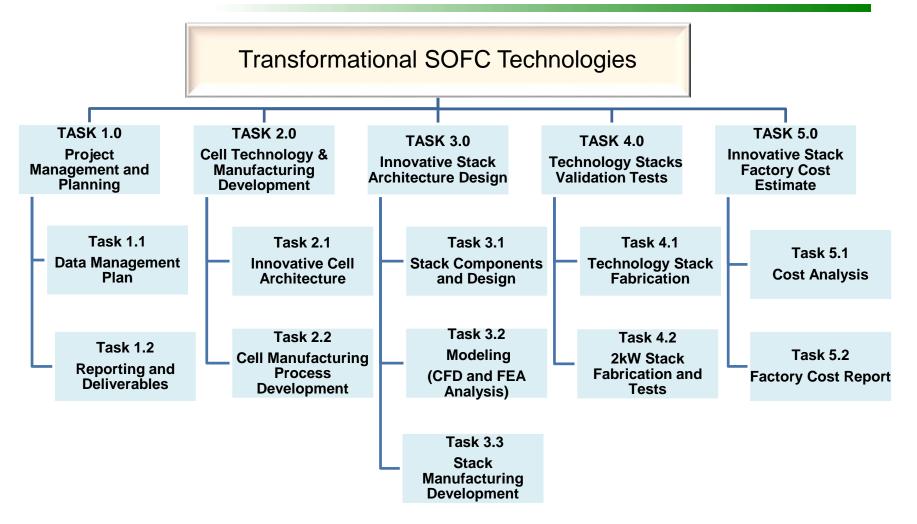
Project Overview



The overall project goal is to advance the SOFC technology at the cell and stack levels by focusing on the following objectives:

- Enhancements in reliability, robustness and endurance
- Reduction in overall system cost
- Reduction in operating and maintenance cost
- The approach in meeting the objectives are targeted on:
 - Increased redox stability of the existing cell technology
 - Developing a new novel single-stage sintered cell technology
 - Develop an integrated stack architecture incorporating balance-of-plant functionality and enabling reduction in materials usage
 - Simplify plant maintenance and repair





The work breakdown structure is designed to ensure success in achieving the program objectives with minimal risk.



FuelCell Energy Danbury	FuelCell Energy Calgary	Northwestern University			
Project Coordination	TSCIII Optimization for Redox Tolerance	Single-Stage Sintered Cell			
Integrated Stack Design	Cell Manufacturing Process Modification	Bi-layered Electrolyte			
BOP Components Design and Integration	Stack Repeat Components Design				
Validation Tests	Technology Cell & Stack Tests				
Factory Cost Estimate					



Projects Schedule

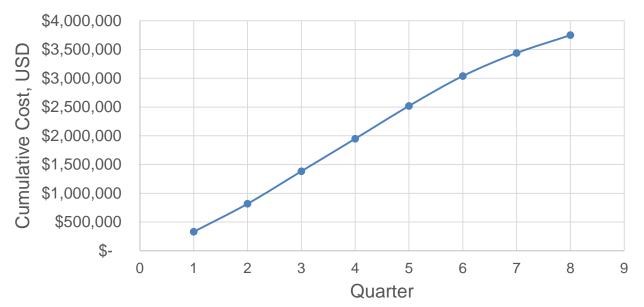
Two-Year Project Schedule

0	Task Name	Start	Finish 1	16 2017 2019
		Mon 10/3/16	Wed 10/31/18	16 2017 2018 Q3 Q4 Q1 Q2 Q3 Q4 Q1 Q2 Q3 Q4
2	1.0 Project Management and Planning	Mon 10/3/16 Mon 10/3/16	Fri 9/28/18	
3	Project Management and Planning	Mon 10/3/16	Mon 10/31/16	
, 1	1.1 Data Management Plan (DMP)			
	Update Data Management Plan	Mon 10/3/16	Mon 10/31/16	₩ 10/31
	Updated Data Management Plan	Mon 10/31/16 Mon 10/3/16	Mon 10/31/16 Wed 10/31/18	÷ 10/31
	1.2 Reports and Deliverables			*
-	Update Project Management Plan (PMP)	Mon 10/3/16		10/31
	Updated Project Management Plan		Mon 10/31/16	-
	Quarterly Reports	Tue 1/31/17		
3	Kickoff Meeting	Fri 11/11/16	Fri 11/11/16	→ 11/11
)	2.0 Cell Technology & Manufacturing Development	Mon 10/3/16	Fri 8/17/18	Y
)	2.1 Innovative Cell Architecture	Mon 10/3/16	Wed 6/20/18	· · · · · · · · · · · · · · · · · · ·
	2.1.1 Single Stage Sintered Cell Development	Mon 10/3/16	Wed 6/20/18	¥¥
	Anode support / AFL development	Mon 10/3/16	Thu 3/16/17	
	Bi-layer Electrolyte development	Mon 10/3/16	Thu 3/16/17	
	CFL Development	Mon 10/3/16	Thu 3/16/17	
	Infiltration of Anode & Cathode Electocatalysts	Fri 2/3/17	Thu 7/20/17	→
	Atomic Layer Deposition process development	Fri 3/17/17	Thu 8/31/17	dimension in the second se
	Demonstrate Feasibility of Single Stage Cell Sintering Process	Thu 7/20/17	Thu 7/20/17	7/20
	Decision Point: Select the Cell Sintering Temperature	Thu 7/20/17	Thu 7/20/17	▼7/20
	Process Standardization and Optimization	Fri 7/21/17	Wed 6/20/18	
	2.1.2 TSC III Microstructure Optimization	Mon 10/3/16	Wed 4/25/18	
	Develop strengthened anode support and AFL	Mon 10/3/16	Fri 11/25/16	10000
	AFL Catalyst Grading	Mon 10/31/16	Thu 2/16/17	→
	Redox barrier layer development	Fri 1/6/17	Thu 4/27/17	()
	Fabrication and Testing of Redox Tolerant TSC III Cells	Fri 4/28/17	Thu 6/22/17	(* **)
1	Pre-Oxidation processing development	Fri 5/26/17	Thu 7/20/17	
	Complete Feasibility Evaluation of Redox-Tolerant TSC III Cell Technology	Thu 7/20/17	Thu 7/20/17	7/20
1	Single Cell Fabrication, Testing, and Optimization	Fri 7/21/17	Wed 4/25/18	*
	Demonstrate Redox Tolerant TSC III Cell Technology over 10 cycles	Wed 4/25/18		a [*] 4/25
1	2.2 Cell Manufacturing Process Development	Mon 12/26/16	Fri 8/17/18	
1	Develop cell design geometry	Mon 12/26/16	Thu 9/14/17	
	Develop scalable manufacturing processes for Single Stage Sintered + Redox Tolerant TSC III Cells	Fri 9/15/17	Wed 4/25/18	
	Go/No-Go Decision Point: Incorporate Redox Tolerant TSC III Cells OR Single Stage Sintered Cell Technology into Deliverable Stack Test	Wed 4/25/18	Wed 4/25/18	4/25
	Single Cell Production Trials	Thu 4/26/18	Wed 8/15/18	
	Single Cell Performance Testing	Fri 2/3/17	Fri 8/17/18	
	Demonstrate feasibility of cell technology for scalable, high-yield manufacturing process	Wed 8/15/18	Wed 8/15/18	8/15
	3.0 Innovative Stack Architecture Design	Mon 10/3/16	Wed 6/20/18	↓
	3.1 Stack Components and Design	Mon 10/3/16	Wed 4/18/18	
	Thin Interconnect Development	Mon 10/3/16	Thu 2/2/17	
	Fuel Reformer Development	Mon 10/3/16	Thu 9/14/17	
1	Catalytic Oxidizer Development	Mon 10/3/16	Thu 9/14/17	
	Integrated Fuel Recycle Development	Mon 11/28/16	Thu 10/12/17	
1	Decision Point: Implement Integrated Fuel Recycle in Deliverable Stack	Thu 10/12/17		₹ 10/12
1	Manifold Design	Fri 2/17/17	Thu 11/23/17	
1	Horizontal Stack Design	Fri 2/17/17	Thu 11/23/17	••••••••
1	Decision Point: Horizontal or Vertical Stack Orientation		Thu 11/23/17	♦ 11/23
1	Stack Enclosure/Containment Development	Fri 9/22/17	Wed 4/18/18	• • • • • • • • • • • • • • • • • • •
1	Complete Integrated Stack Design	Wed 4/18/18		4/18
	3.2 Modeling (CFD & FEA)	Fri 2/24/17	Wed 4/18/18	
1	CFD Modeling	Fri 2/24/17	Wed 4/18/18	4
ł	Finite Element Analysis	Fri 4/7/17	Wed 4/18/18	
1	3.3 Stack Manufacturing Process Development	Fri 2/17/17	Wed 6/20/18	
+	4.0 Technology Stacks Validation Tests	Fri 3/10/17	Fri 9/28/18	
	4.1 Technology Stacks Fabrication and Testing	Fri 3/10/17	Wed 2/21/18	
	4.1 Technology Stacks Fabrication and Testing 4.2 Stack Fabrication and Testing	Thu 4/19/18	Fri 9/28/18	
	4.2 Stack Fabrication and Testing Deliverable Stack Fabrication	Thu 4/19/18	Wed 5/30/18	
	Performance & Endurance Testing of Deliverable Stack	Thu 5/31/18	Fri 9/28/18	
	Performance & Endurance Testing of Deliverable Stack Complete >1000 hrs. Tests of the Deliverable Stack with <1% per 1000 hrs. Degradation	Fri 9/28/18	Fri 9/28/18	9/28
+		Thu 3/1/18	Fri 9/28/18	
	5.0 Advanced Stack Factory Cost Estimate		Wed 8/22/18	
	5.1 Cost Analysis	Thu 3/1/18		
1	Preliminary Technology Screeening Cost Analysis	Thu 3/1/18	Wed 4/25/18	
	Final Stack Cost Analysis	Thu 6/28/18	Wed 8/22/18	
2.1	5.2 Factory Cost Report	Thu 8/9/18	Fri 9/28/18	
5	Complete Validation of SOFC Stack Cost Reduction	Fri 9/28/18	Fri 9/28/18	₹9/28



	Project 10/01/16-	Total		
	Government Share	Cost Share		
Total	\$3,000,000	\$750,000	\$3,750,000	
Percentage	80.0%	20.0%		

Spending Plan







Risk Categories:

- Technology
- Resources
- Management

		IMPACT				
		LOW	MODERATE	HIGH		
T7	LOW	Low	Moderate Modera			
PROBABILITY	MOD	Moderate	Moderate	High		
PR	HIGH	Moderate	High	High		

Degree of Risk Calculation Chart



ld.	Task /Subtask No.	Milestone Description	Planned Completion	Actual Completion	Verification Method
1	1.1	Updated Data Management Plan (DMP)	10/31/16	10/31/16	DMP File
2	1.2	Updated Project Management Plan (PMP)	10/31/16	10/31/16	PMP File
3	1.2	Project Kickoff Meeting	11/11/16	11/16/16	Presentation File
4	2.1.1	Demonstrate Feasibility of Single Stage Cell Sintering Process	7/20/17		Quarterly Report
5	2.1.2	Complete Feasibility Evaluation of Redox-Tolerant TSC III Cell Technology	7/20/17		Quarterly Report
6	2.1.2	Demonstrate Redox Tolerant TSC III Cell Technology over 10 Testing cycles	4/25/18		Quarterly Report
7	2.2	Demonstrate Feasibility of Cell Technology for Scalable, High-Yield Manufacturing Process	8/14/18		Quarterly Report
8	3.1	Complete Integrated Stack Design	4/18/18		Quarterly Report
9	4.2	Complete >1000 hrs. Tests of the Deliverable Stack with <1% per 1000 hrs. Degradation	9/28/18		Quarterly Report
10	5.2	Complete Validation of SOFC Stack Cost Reduction	9/28/18		Factory Cost Report



Decision Point	Date	Success Criteria
Select Cell Sintering Temperature	7/20/17	The lowest single stage cell sintering temperature (<1350 °C) will be selected which provides adequate electrolyte densification and also prevents interdiffusion amongst layers. The decision will be based on the results of cell testing.
Implement Integrated Fuel Recycle in Deliverable Stack	10/12/17	CFD modeling, and/or bench-testing, shows the feasibility of integrated anode recycle concepts to provide sufficient levels of steam to achieve a steam-to-carbon ratio >1.6 at the anode inlet.
Implement Horizontal or Vertical Stack Orientation in Deliverable Stack Test	11/23/17	Based on the results of CFD and FEA modeling, horizontal stack architecture will be selected if it shows promise to enable larger stacks without introducing significantly-greater technical risks.



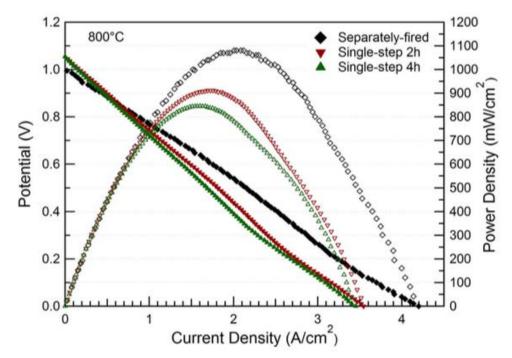
Work Scope Task 2



- Objective
 - To develop cell materials that are tolerant to reduction and oxidation cycling (Redox cycling) which can be expected in real-world system operation
- Approach
 - Building on VPS' strong anode-supported cell development experience since 1997
 - Leveraging cell and stack advancements from previous SECA projects
 - Implementing multi-prong approaches in developing innovative redox tolerant anode-supported cell through reducing anode strain upon Ni re-oxidation
- Work Plan
 - Promising results from several approaches will be incorporated in a redox tolerant TSCIII cell technology
 - The final cell design will undergo a testing regime with 10 thermal cycles and 10 Redox cycles in single-cell (10 cm x 10 cm) test platform
 - Single-cell tests will be deemed successful by targeting equivalent or lower performance loss on redox cycling than that is found with thermal cycling.



- Single-step firing: process simplification
- Reduced temperature firing
 - Essential to minimize cathode sintering, electrolyte interactions
 - Single-step (1250 °C) fired cells (Ni-YSZ / YSZ / LSM-YSZ) show similar performance as conventional cells



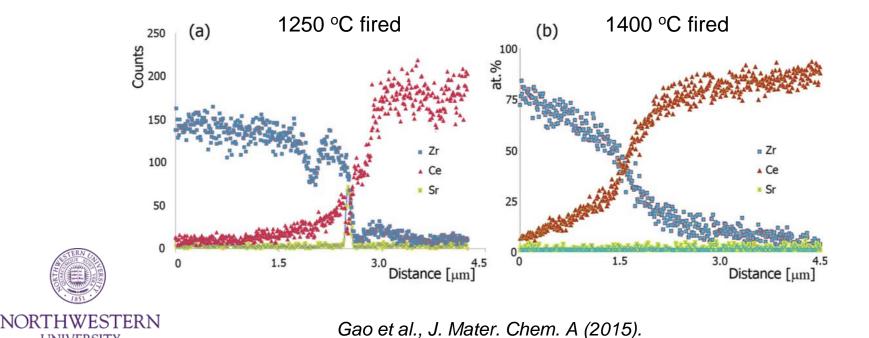


Wang et al. J Electrochemical Society 163, F196-F201 (2015)



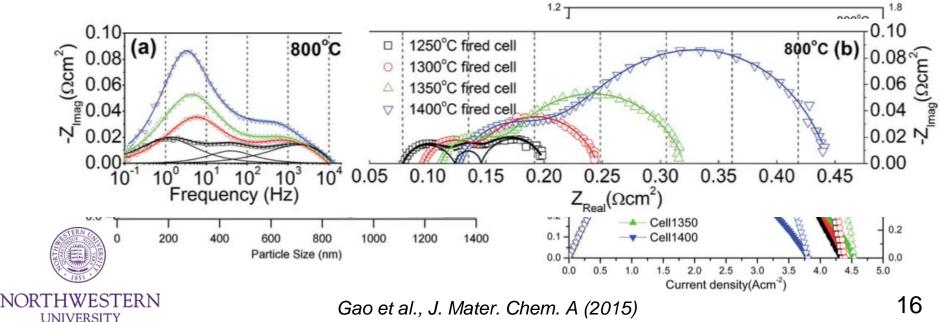
UNIVERSITY

- Single-step firing: process simplification
- Reduced temperature firing
 - Essential to minimize cathode sintering, electrolyte interactions
 - Essential to minimize YSZ/GDC interdiffusion
 - Reduced interdiffusion eliminates large ohmic resistance



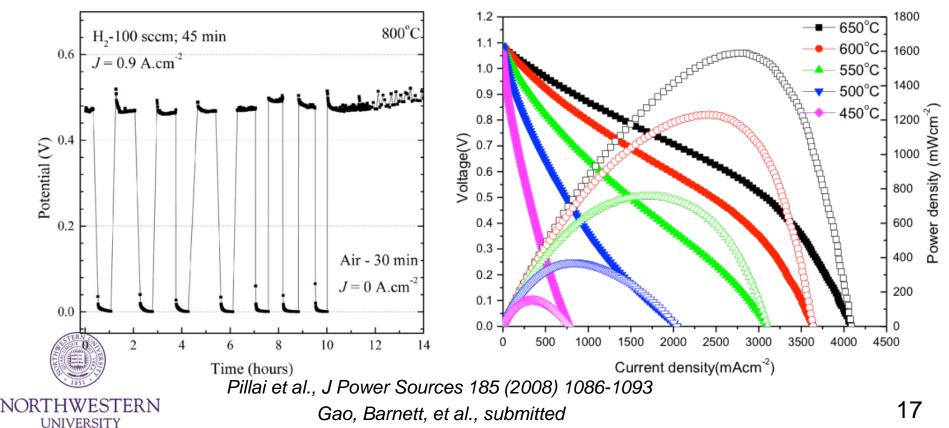
FuelCell Energy Single-Step Reduced-Temperature Firing

- Single-step firing: process simplification
- Reduced temperature firing
 - Essential to minimize cathode sintering, electrolyte interactions
 - Essential to minimize YSZ/GDC interdiffusion
 - Finer-scale anode microstructure improved performance
 - Data from Ni-YSZ / YSZ / GDC / LSCF cells



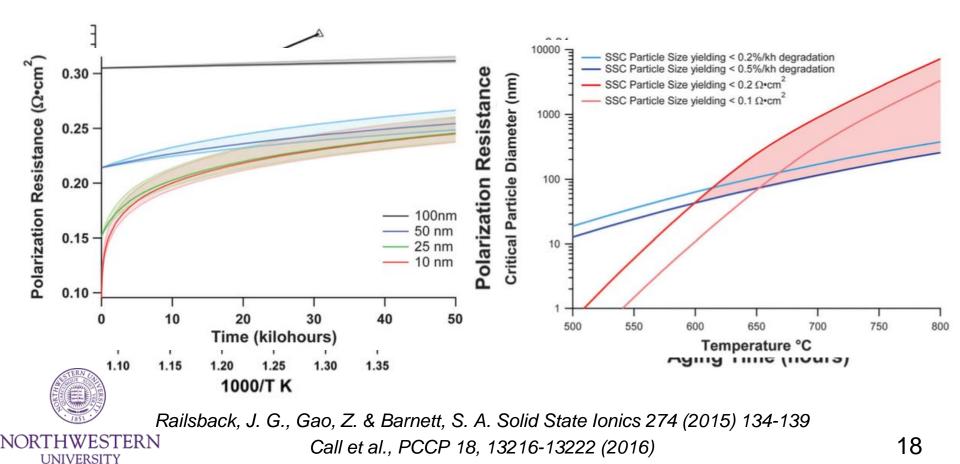


- Redox cycle stability: (left) stable operation after several redox cycles of a cell with (Sr,La)TiO₃ support, Ni-YSZ AFL, YSZ electrolyte, and LSM-YSZ cathode
- Good low-temperature performance of cell after infiltration of nano-scale Ni particles into anode



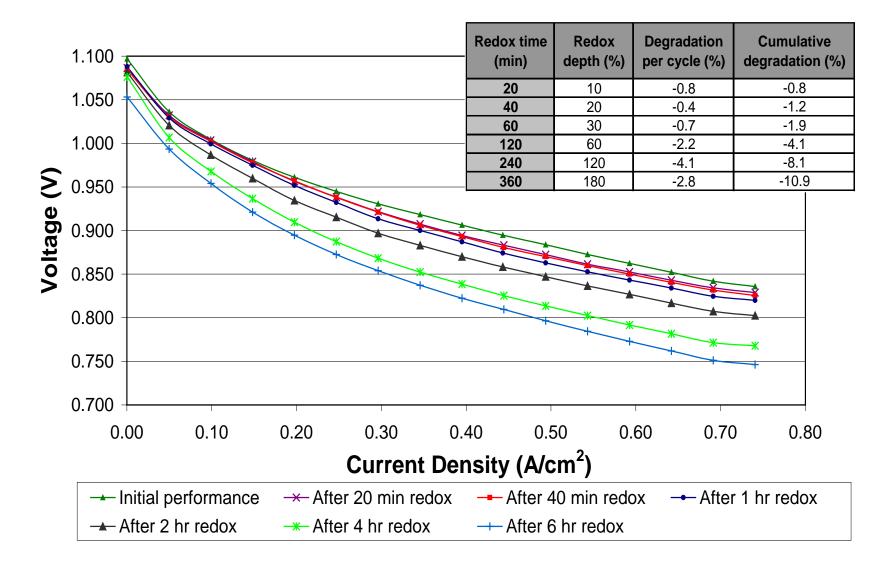


- Selection of best infiltrate/scaffold combinations
- Performance and long-term stability validation
 - Accelerated testing and modeling





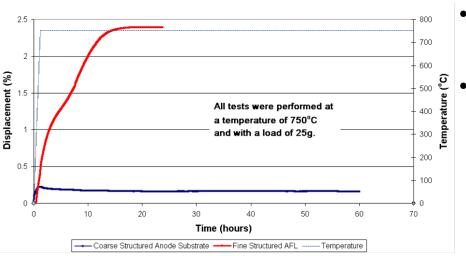
Baseline Cell Redox Tolerance

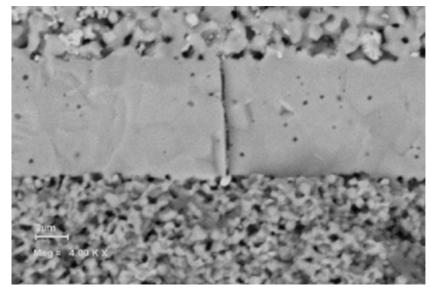


The Mechanism of Redox Failure



- Nickel in the anode expands 69% by volume upon oxidation to nickel (II) oxide
- Sarantaridis *et al* showed numerically that mechanical failures occur by different mechanisms and result in different allowable anode expansions before failure for different SOFC cell architectures
- Anode-supported cells fail by tensile cracking of the electrolyte and may tolerate very limited anode expansion using 7-8 um electrolyte
- Redox tests of baseline cells showed electrolyte cracking in SEM posttest analysis





- Ni-YSZ anode support and anode functional layer has porosity of 15-25% as prepared and 35-45% reduced
 - Thermomechanical analysis of pressed bars with AFL microstructure showed that upon re-oxidation:
 - Anode substrate does not change measurably in bulk dimensions due to the nickel content, porosity and microstructure
 - Anode functional layer (AFL) expanded by more than 2%

D. Sarantaridis and A. Atkinson; Proceedings of the 7th European SOFC Forum; Bossel, U., Ed.; EFCF:Lucerne, Swizerland, 2006; p. P0728. 20



- Objective
 - Major cell material improvements, breakthroughs and cost reduction achievements from Task 2.1 will be validated and incorporated into the improved production cells through extensive cell manufacturing process development
- Approach
 - Explore cell fabrication boundary for cell size and thickness for various stack design approaches.
 - Computational thermo-mechanical modeling will be further developed and expanded for the analysis of various cell designs to improve compliance and reliability during manufacturing and normal operating conditions.
 - Cell geometry, including aspect ratio, will be cost-benefit-analyzed and defined.
 - Various cell component design parameters will be evaluated to identify the optimum cell configuration for system operation.
- Work Plan
 - A new baseline cell technology will be established based on inputs from Task 2.1
 - After meeting cell performance and endurance criteria, a sufficient number of cells will be produced for assembly for the technology stacks and the 2-5-kW validation stack



Work Scope Tasks 3, 4, and 5



Goals

- Develop a transformational <u>hot-swappable stack</u> that enables low-cost, densely packaged SOFC systems.
- Demonstrate performance of stack with <u>integrated system elements</u> at 2-to-5 kW power level for ≥1000 hours of operation.
- Develop factory and integration cost estimates that undercut DOE's cost goals for SOFC plants.

General approach

- Investigate incorporating system level elements (heat exchangers, oxidizer, anode gas recycle) into the Innovative stack assembly.
- Focus component designs amenable to <u>high volume</u>, <u>low cost</u> <u>fabrication</u>.
- Reduce installation and maintenance costs significantly
- Aim for reducing \$/kWdc, not just increasing W/cm²
 - >2x reduction in \$/kWdc is a plausible target



Lessons from Prior DOE Projects



60 kW,

(relative scale)

Each integration of BOP into the Modular Power Block (MPB) resulted in a number of benefits

- Improved cell thermal performance
- Reduced chrome poisoning
- Increased power density and decreased parasitic losses
- Reduction in plant footprint, material costs, and capital costs

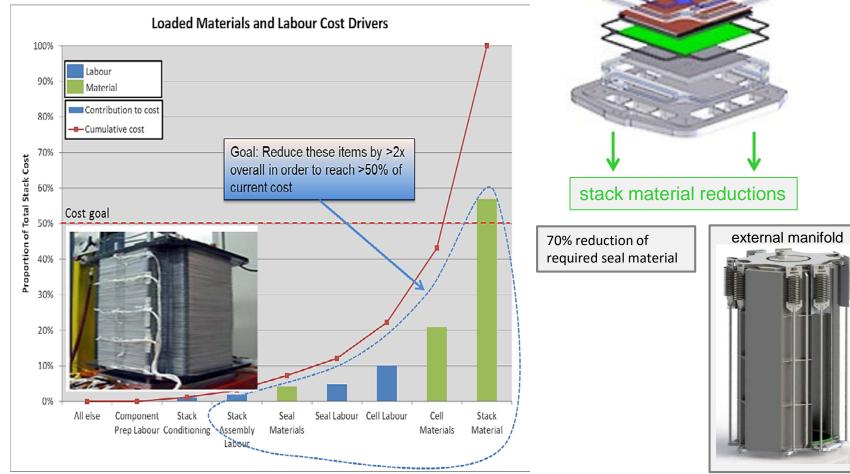
MODULE			WIDTH	DEPTH	HEIGHT	Volume	Vol %	Pwr Dens %
(kW)	STATUS	Level of Integration	(in)	(in)	(in)	(ft³)	vs. 60kW	kW/ft³
30	Built	No Integration. Single Stack or Tower	64.0	64.0	96.4	228	58%	.132
60	Built	Quad Base, Fuel Radiator HX, Elec. Series Towers	90.5	86.0	87.6	394	100%	.152
50	In Test	60 Plus: Cat. Ox/HX & Reformer	59.5	76.5	69.7	184	47%	.272
100	In Mfg	50 Plus: Anode Recup., Desiccant Regen HX, Ceramic Start-up Heaters	61.5	69.9	91.5	228	58%	.438
100 (RPU)	Proposed	Stack-Level Integration of all Hot System Processes	36	25	36	19	<5%	5.25

SOFC system power density, kW/ft³ > 5

Building Upon DE-FE0026093



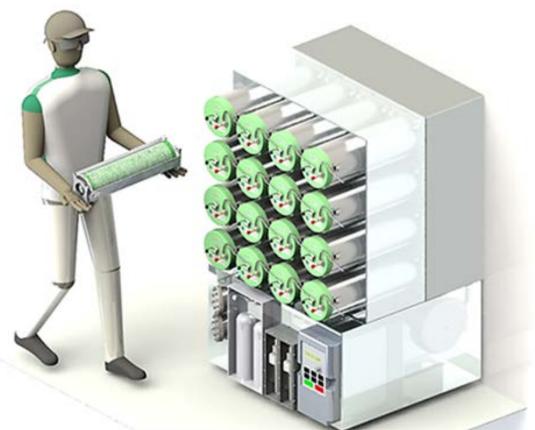
 Design activities will build upon cost reduction development activities from DE-FE0026093





Task 3.0 -Transformational SOFC

- Serviceable by a single technician, minimal tooling
- No heavy equipment required during maintenance
- Hot-swappability minimizes number of shutdowns during plant lifecycle
- Reduction in equivalent forced outage rates (EFOR)
- Lower \$/kW, Higher kW/ft³





Objective

• Validate the advanced cell architectures and stack design features developed under Tasks 2.0 and 3.0.

Test Plan

- Fabricate and test (@ NOC) a 2-5 kW stack (RPU)
- Test duration for ≥ 1000 hours to demonstrate the performance and stability improvements of the integrated stack system
- Lead-up activities include testing of reduced cell-count (250 W to 500 W) to prove-out the cell / stack design features and manufacturing processes developed
 - Validate CFD models to iteratively arrive at the optimum stack design
- Test stand modifications will be made, as necessary, to accommodate the new stack architecture interfaces



- A factory cost model will be developed for RPU
 - Will include capital costs, depreciation and maintenance costs
 - Will include labour estimates and allowance for labour efficiency and yield
 - Will include representative overhead costs
- Quotes will be secured for components at target volumes
 - Start at 250 kW/yr volumes to avoid costs that are only feasible at higher volumes
 - Extend cost exercise up to 250 MW/year to show potential and identify roadblocks to large volumes
- Estimates of installation and maintenance costs will also be developed