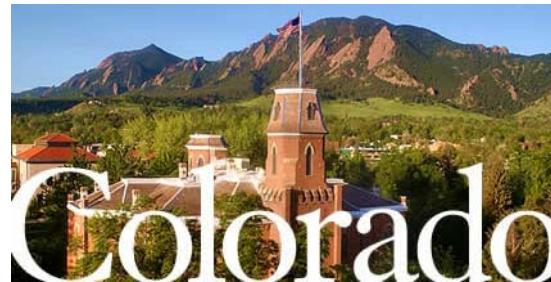


# *MFIX-DEM Enhancement for Industrially-Relevant Flows*



## 2017 Crosscutting Research Project Review

Pittsburgh, PA  
March 20-23, 2017

*Project Leads:* ***Dr. Ray Cocco (PSRI, co-PI)***  
***Dr. Ray Grout (NREL, co-PI)***  
***Prof. Thomas Hauser (Univ. CO, co-PI)***  
***Prof. Christine Hrenya (Univ. CO, PI)***

# Project Team

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**University of Colorado  
Chemical & Biological Engineering**

*DEM modeling of granular and gas-solid flows, MFIX*



**Prof. Christine Hrenya Dr. William Fullmer Dr. Peiyuan Liu**

**University of Colorado  
Research Computing**

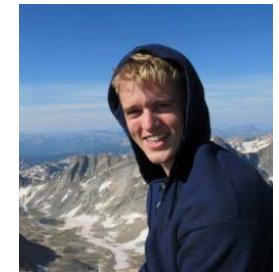
*High-performance computing, CFD*



**Prof. Thomas Hauser**



**Dr. Dane Skow**



**Tim Brown**



**Dr. Ray Cocco**



**Dr. Ray Grout Dr. Hari Sitaraman**



**Deepthi  
Vaidhynathan**



**Rasa Kales**



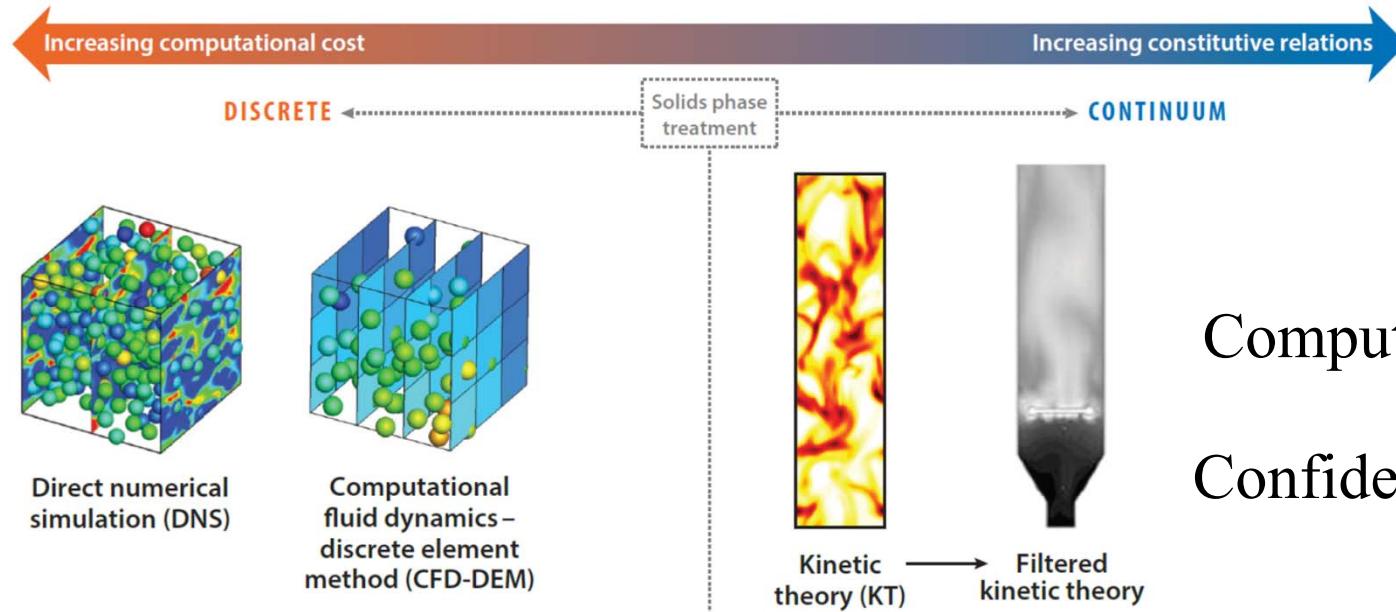
**Dr. Allan Issangya**

**PSRI**

*Industrial Application and Experiments of Particle Flows*

**Aaron Holt**

# Motivation



Fullmer & Hrenya  
(Annu. Rev. Fluid Mech. 2017)

Barriers:  
Computational Overhead  
vs  
Confidence in Predictions

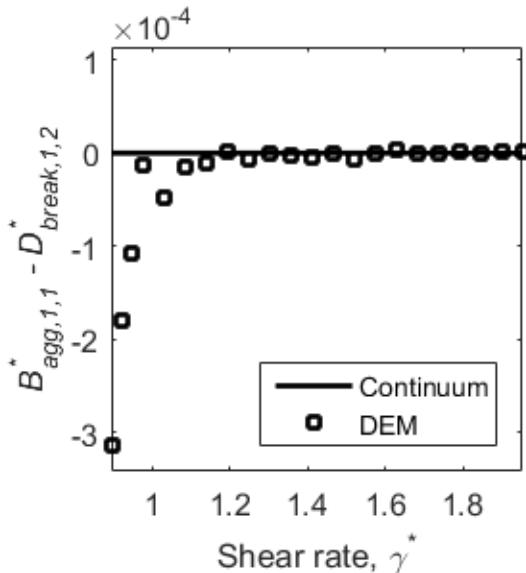
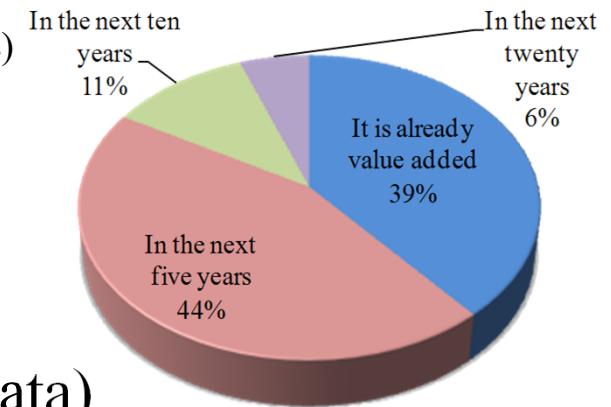
Motivation:  
DEM application  
toward industrially-  
relevant systems

## Potential significance of the results of the work

### Expected value added through DEM:

PSRI Industrial Survey  
 (Cocco et al., *Chem. Eng. Prog.*, in press)

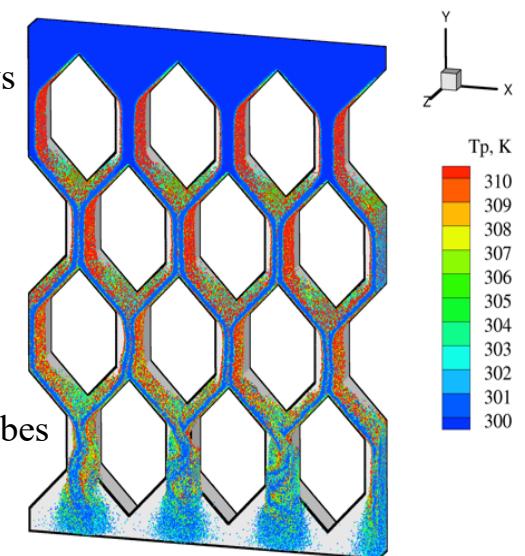
- Expanded industrial use of DEM
- Indirect: Improved physics in continuum and hybrid modeling (DEM as benchmark data)
- Direct: Aid in design/optimization of industrial components



### Agglomeration balance of doublets:

Continuum Theory for Rapid, Cohesive-Particle Flows  
 (Kellogg, Liu, LaMarche & Hrenya, submitted)

**Fully-developed characteristics:**  
 Heat transferred to particles falling over heated tubes  
 (Morris et al., *Solar Energy*, 2016)



# Phase I Statement of Project Objectives (SOPO)

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## Task 1 - Project Management and Planning

### Task 2 - Profiling MFIX DEM

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Task 5c: Compare enhancements on multiple Xeon/Xeon Phi architectures

### Task 6 - Industrially Relevant Problem

Task 6a: Survey of PSRI member companies

Task 6b: Experiments of Interacting Nozzles

### Task 7 - Uncertainty Quantification

Task 7a: Test Problem

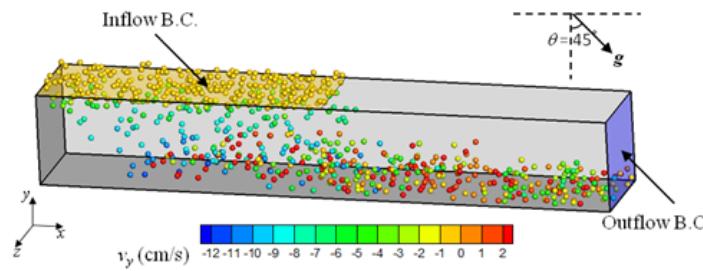
Task 7b: Challenge Problem

Task 7c: Industrially Relevant Problem

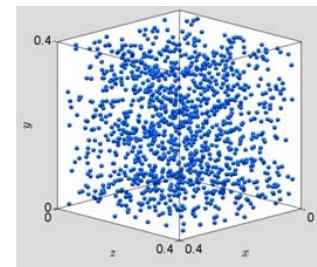
## Milestone 2: Benchmark Cases

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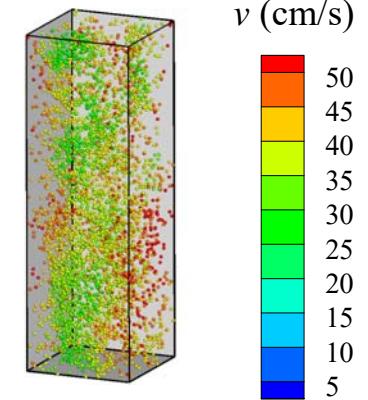
*Dilute, nearly instantaneous collisions*



Ramp flow

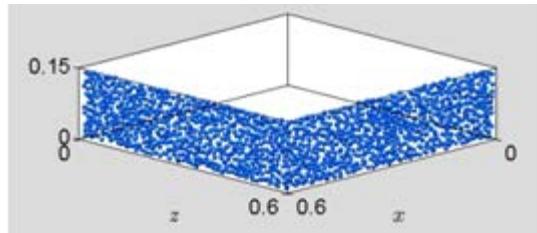


Homogeneous cooling

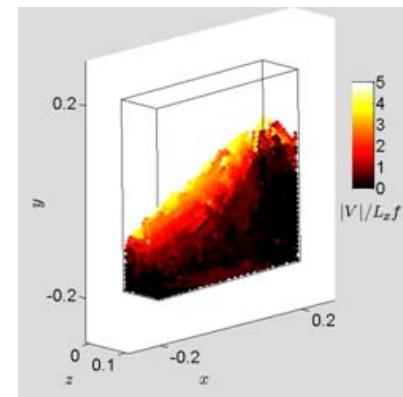


Riser flow

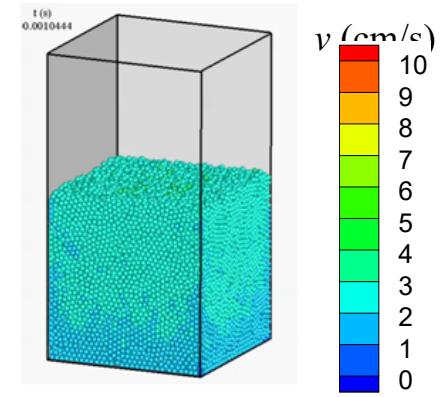
*Dense, enduring contacts*



Settling



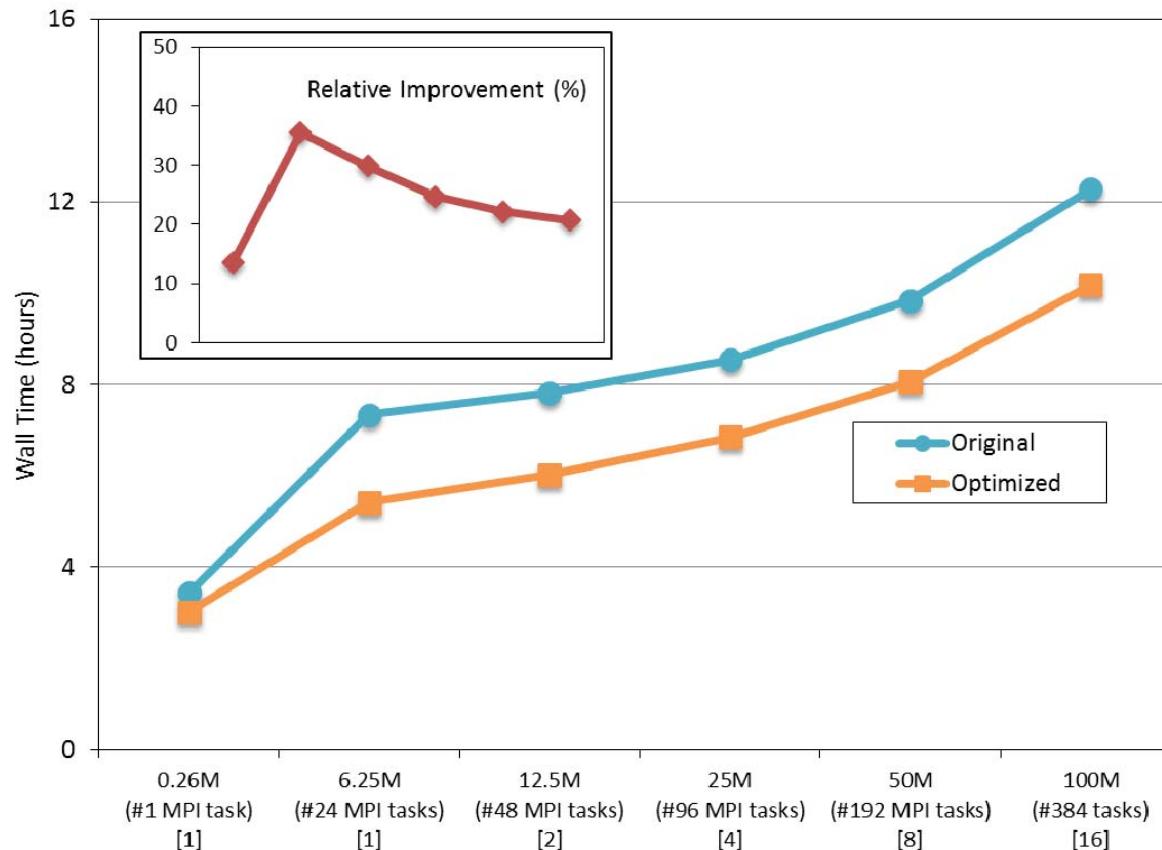
Square tumbler



Fluidized bed

## 100M Particle Settling – Weak Scaling

- Locality-based Particle Sorting – improves neighbor search
- State-based Particle sorting – improves vectorization
- Masking – improves vectorization



Milestone 5 report (submitted to DOE)

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Task 6b: Experiments of Interacting Nozzles

### **Task 7 - Uncertainty Quantification**

Task 7a: Test Problem

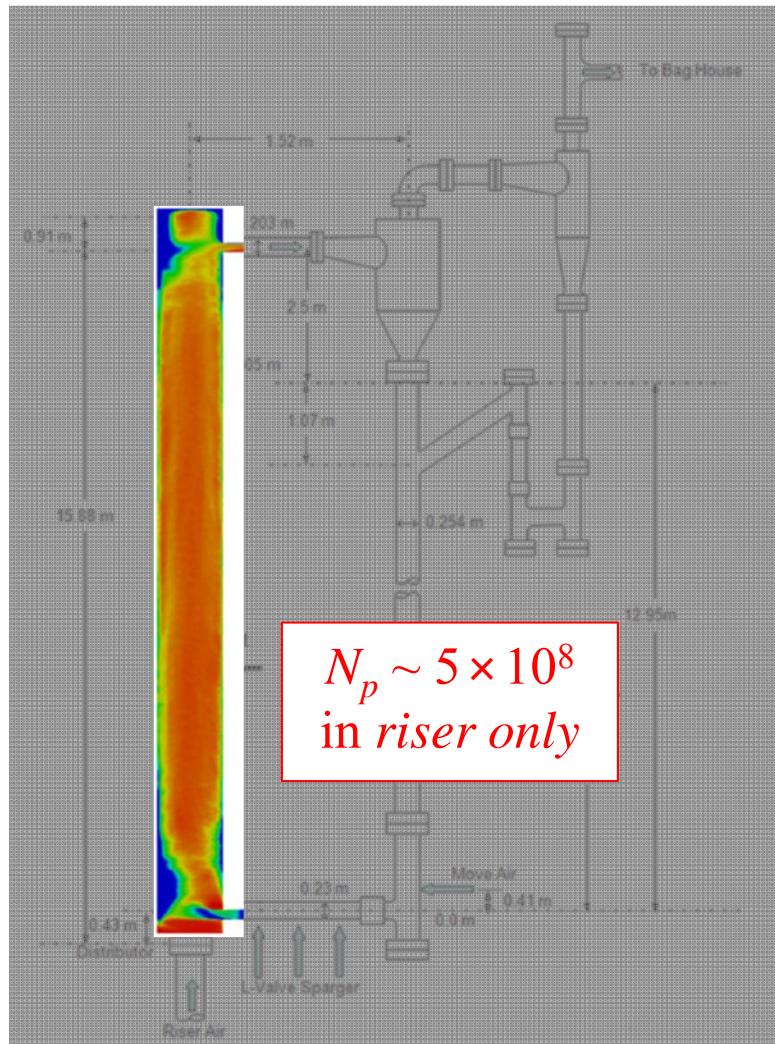
Task 7b: Challenge Problem

Task 7c: Industrially Relevant Problem

## Need for CFD-DEM Validation Data

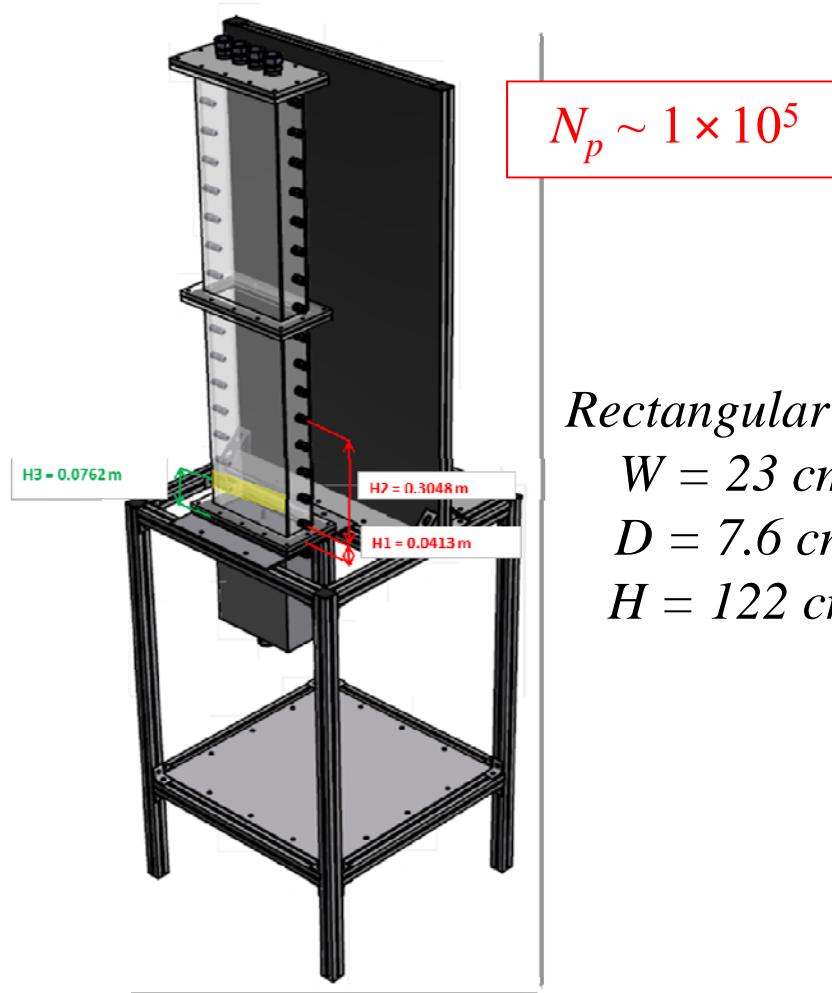
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*NETL/PSRI Challenge Problem III*



(Li et al., *Chem. Eng. Sci.*, 2012)

*NETL Small-Scale Challenge Problem I*



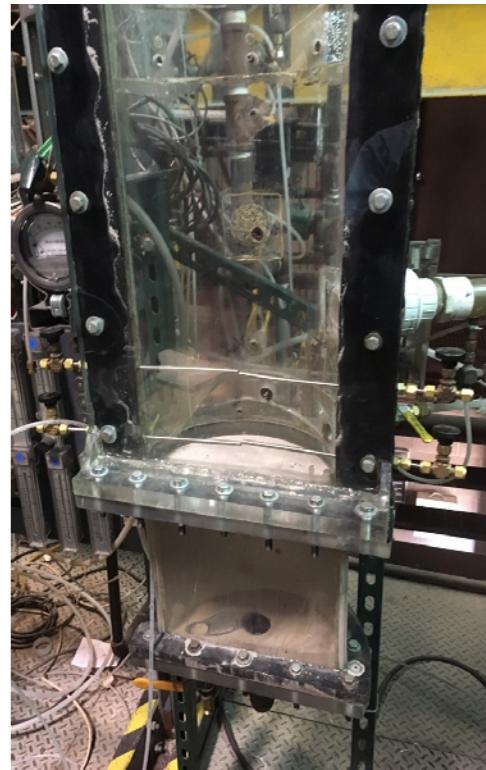
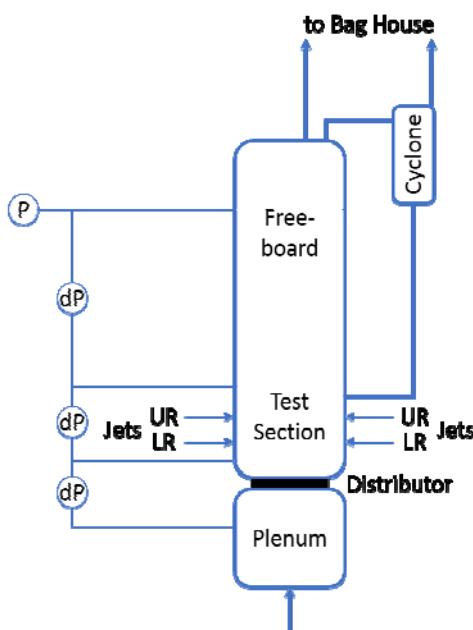
*Rectangular FB*  
 $W = 23\text{ cm}$   
 $D = 7.6\text{ cm}$   
 $H = 122\text{ cm}$

(Gopalan et al., *Powder Tech.*, 2016)

## Horiz. Jet Experiments: Unit and Materials

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### Semi-circular Fluidized Bed with Side Jets



### Materials



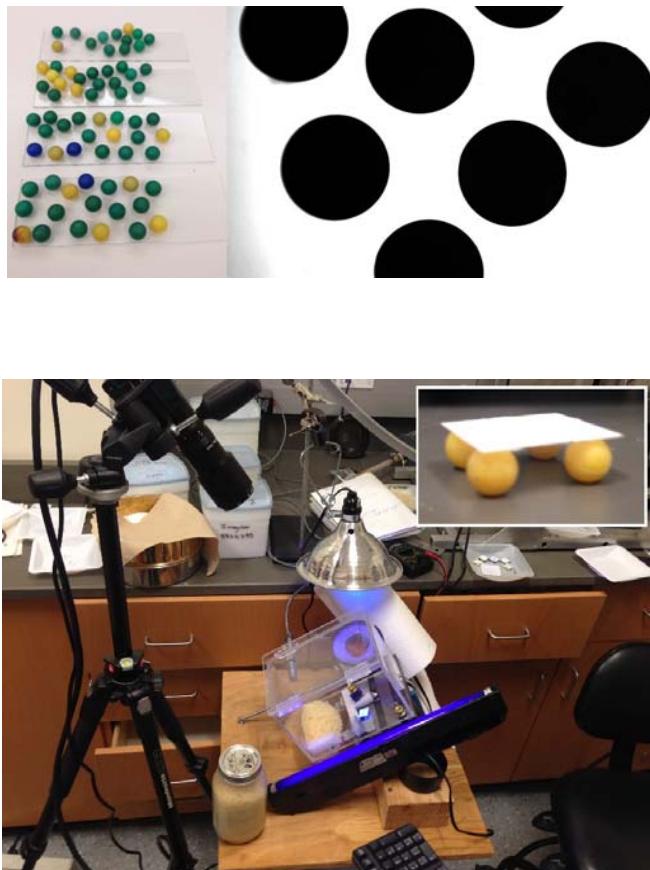
- **6.0 mm plastic:**  $N_p \sim 6 \times 10^4$
- **3.0 mm ceramic:**  $N_p \sim 4 \times 10^5$
- **1.6 mm mix:**  $N_p \sim 3 \times 10^6$
- **1.5 mm glass:**  $N_p \sim 4 \times 10^6$
- **1.0 mm ceramic:**  $N_p \sim 1 \times 10^7$
- **0.8 mm glass:**  $N_p \sim 3 \times 10^7$

### Characteristics:

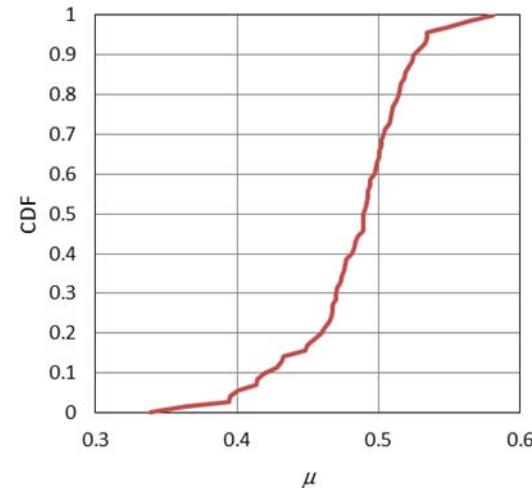
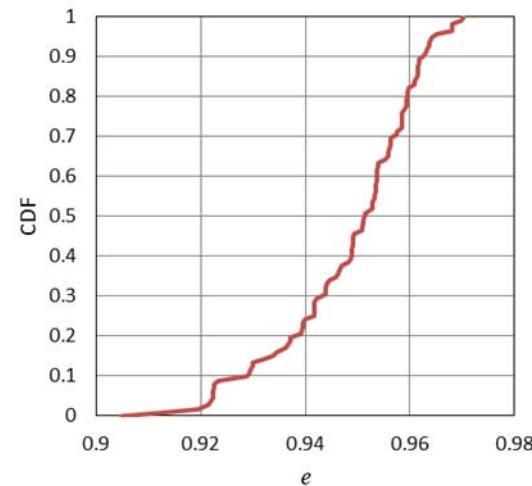
- $W = 11.25$  in
- $h_{bed} \sim W$
- $d_j \sim 4$  mm
- $U \sim U_{mf}$   
~ 30-150 cm/s
- $U_j \sim 200$  m/s

## Horiz. Jet Experiments: Particle Characterization

### *Methods*

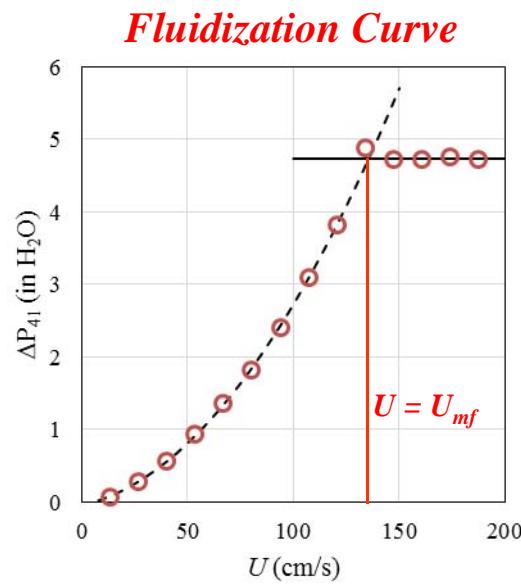


### *Results*

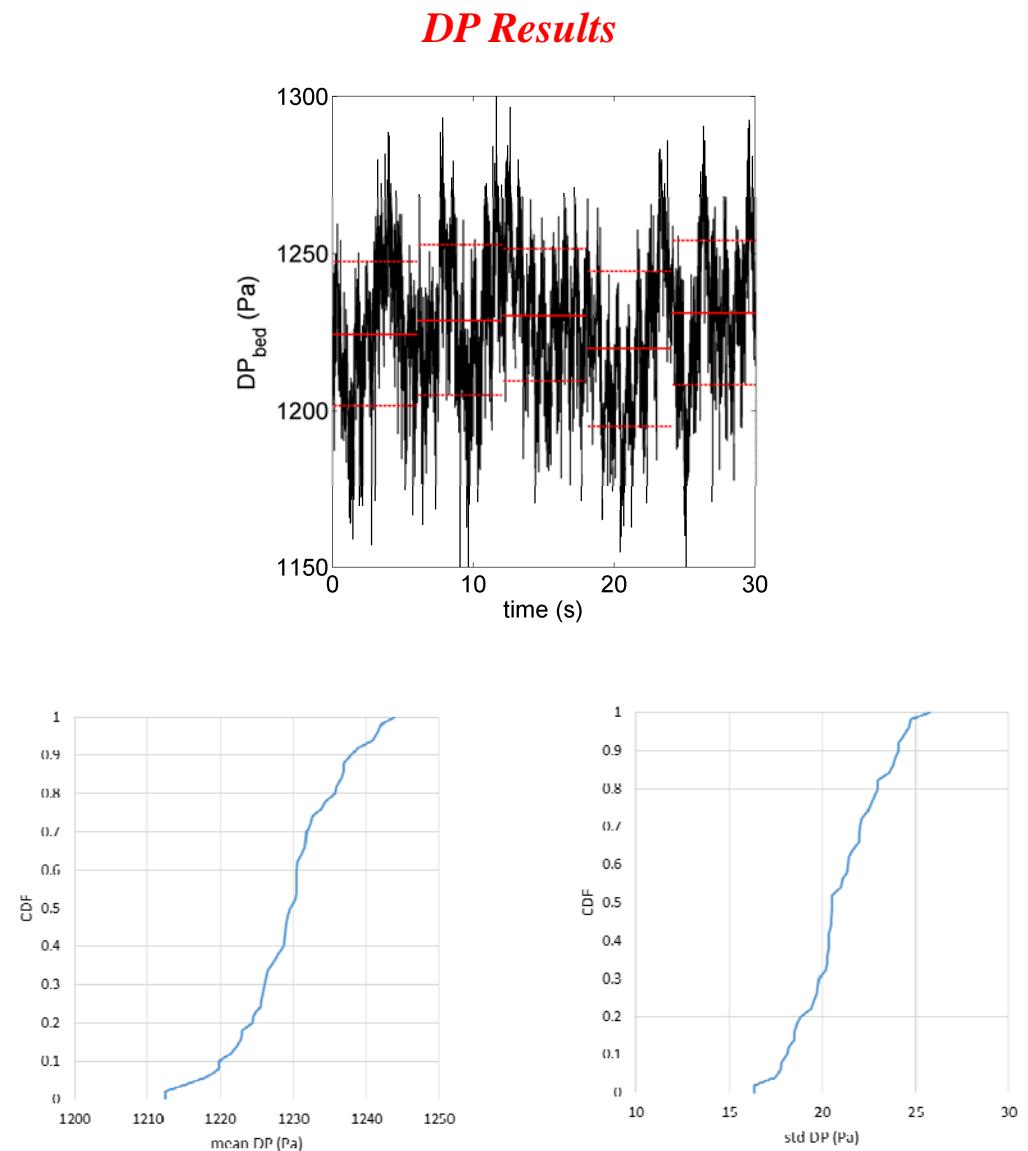


## Horiz. Jet Experiments: Pressure Drop

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$U_{mf} = 135$  cm/s  
Bed operated at:  
 $U \sim 90\% \text{ & } 110\%$  of  $U_{mf}$



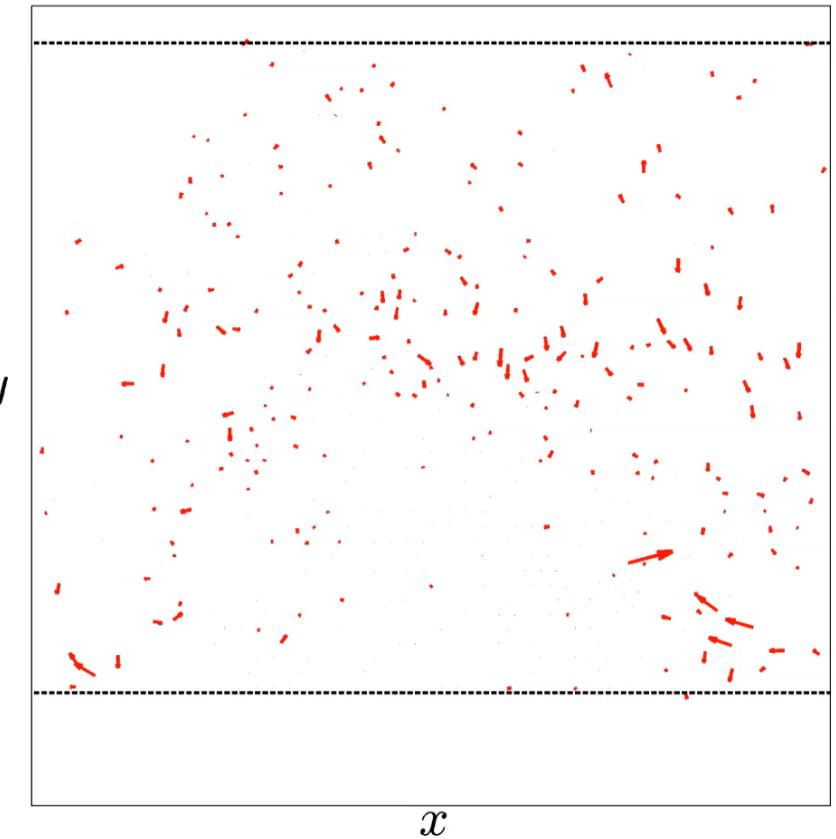
## Horiz. Jet Experiments: HSV and PT

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*Raw HSV Data*

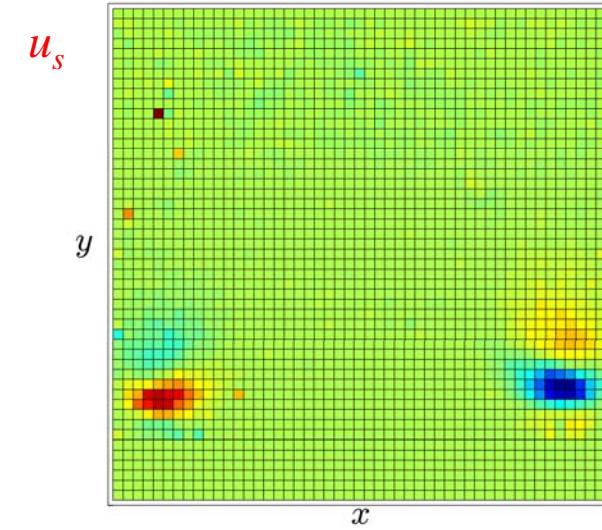


*Particle Tracking (PT) Analysis*



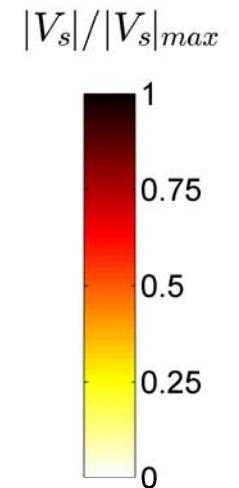
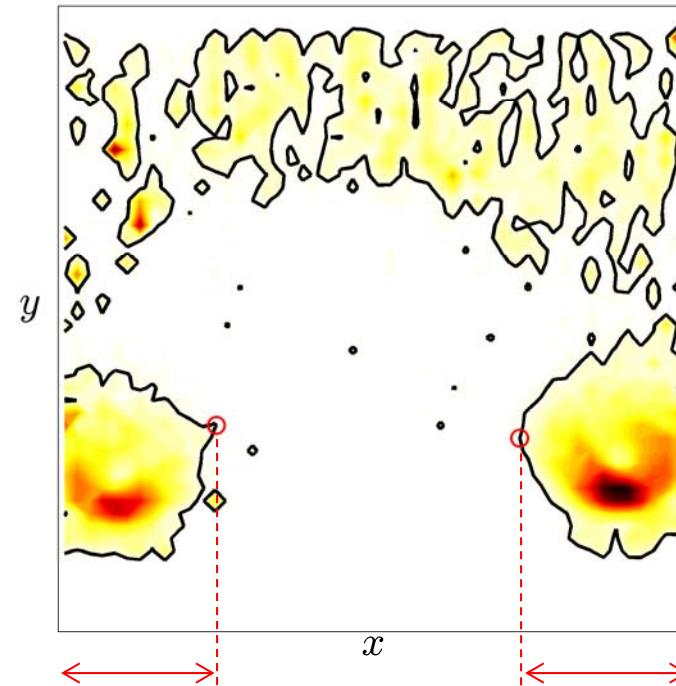
## Horiz. Jet Experiments: PT Post-processing

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*Jet Penetration Results*

5% Isoline



*Milestone 6b report (submitted to DOE)*

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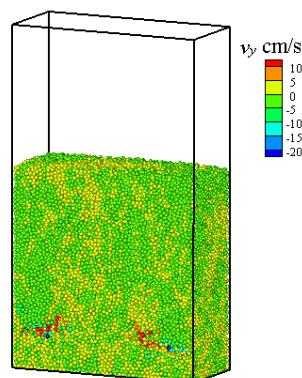
Task 7c: Industrially Relevant Problem

## CFD-DEM+UQ: Base Case

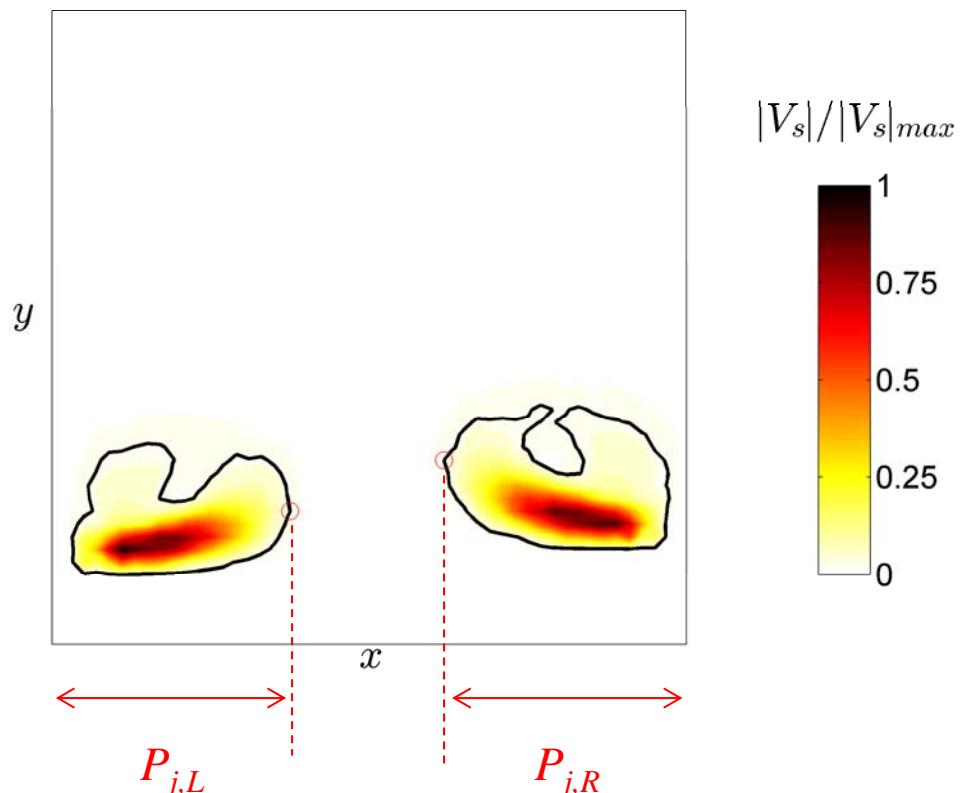
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### *CFD-DEM Model Description*

- Rectangular geometry
- Point sources for jets
- Incompressible
- No shear- or particle-induced turbulence models
- Uniform inflow
- No-slip wall BC for gas
- $\Delta x \sim 2 d_p$



*Jet Penetration Depth:*  
same analysis as exp data



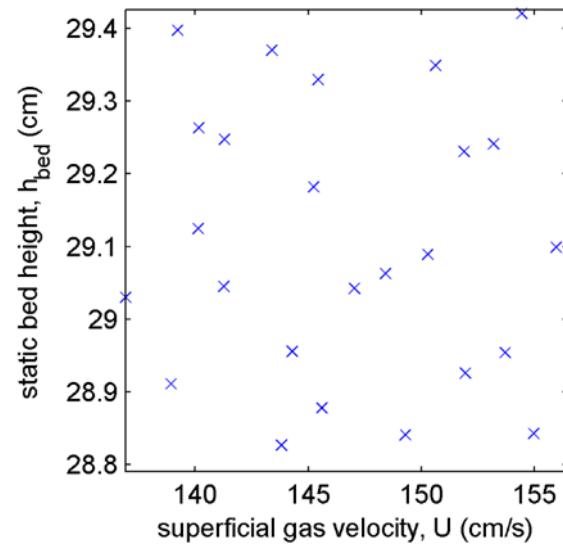
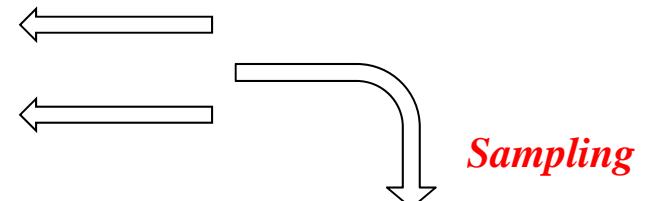
## CFD-DEM+UQ: PIRT

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### *Parameter Identification and Ranking Table*

Parameter	Input Uncertainties				SRQ Ranking		
	lower bound	base case	upper bound	type	$P_{i,L}$	$P_{i,R}$	$\Delta P$
Bed							
$U$ (cm/s)	136.9	146.7	156.5	e	100.0	100.0	100.0
$U_{i,L}$ (m/s)	189.2	200.9	212.5	e	2.2	1.1	1.2
$U_{i,R}$ (m/s)	182.8	194.4	205.9	e	0.5	4.9	1.0
$h_{bed}$ (cm)	28.8	29.1	29.4	e	0.3	1.1	29.9
$A$ (cm <sup>2</sup> )	333.1	340.4	347.8	e	-	-	-
Left Jets							
$A_{i,L}$ (cm <sup>2</sup> )	0.1168	0.1171	0.1174	e	-	-	-
$y_{i,L}$ (cm)	5.067	5.146	5.225	e	0.0	0.0	0.0
$z_{i,L}$ (cm)	1.588	1.667	1.746	e	0.0	0.0	0.0
$d_{i,L}$ (cm)	-0.3175	0.000	0.3175	e	-	-	-
Right Jets							
$A_{i,R}$ (cm <sup>2</sup> )	0.1168	0.1171	0.1174	e	-	-	-
$y_{i,R}$ (cm)	5.377	5.456	5.535	e	0.0	0.0	0.0
$z_{i,R}$ (cm)	1.667	1.746	1.826	e	1.5	18.2	2.1
$d_{i,R}$ (cm)	-0.3175	0.000	0.3175	e	-	-	-
Particle-phase Properties							
$d_p$ ( $\mu\text{m}$ )	5761	5924	6006	a	1.8	4.9	6.8
$\phi$ (-)	0.931	0.943	0.948	a	0.0	0.0	0.0
$\rho_p$ (g/cm <sup>3</sup> )	1.042	1.0435	1.045	e	0.2	0.3	1.2
$e_{pp}$ (-)	0.819	0.948	0.990	a	3.3	9.4	0.6
$\mu_{pp}$ (-)	0.338	0.482	0.581	a	2.8	6.3	2.2
$e_{pw}$ (-)	0.905	0.948	0.970	a	0.0	1.0	0.1
$\mu_{pw}$ (-)	0.338	0.482	0.581	a	0.4	0.6	2.7
Gas-phase Properties							
$\rho_g$ (g/cm <sup>3</sup> $\times 10^3$ )	1.1104	1.1697	1.2290	e	7.3	10.6	3.3
$\mu_g$ (g/cm-s $\times 10^5$ )	1.7	1.8	1.9	e	2.3	2.9	0.5

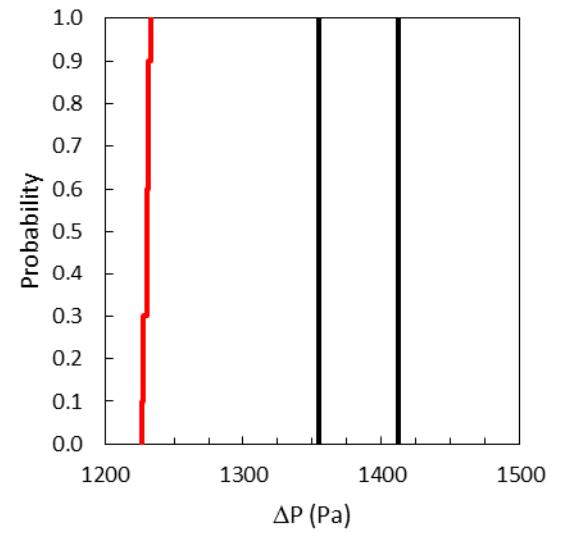
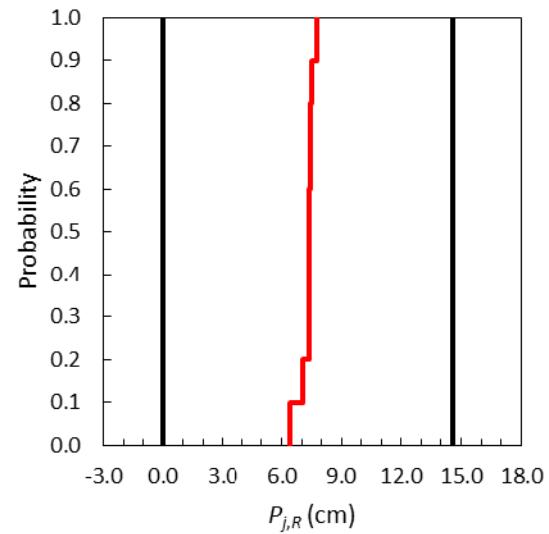
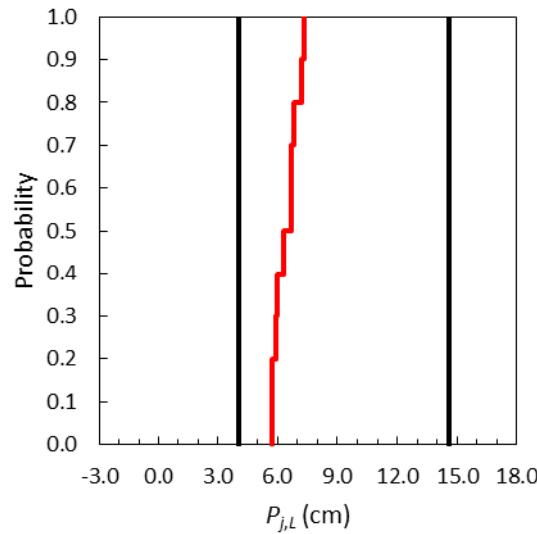
- 1.  $> 10^{1.5}$  Important
- 2.  $10^{1.5} - 10^{1.0}$  Mildly Important
- 3.  $10^{1.0} - 10^{0.5}$  Marginal
- 4.  $10^{0.5} - 10^{0.0}$  Mildly Insignificant
- 5.  $< 10^{0.0}$  Insignificant



## CFD-DEM+UQ: Results

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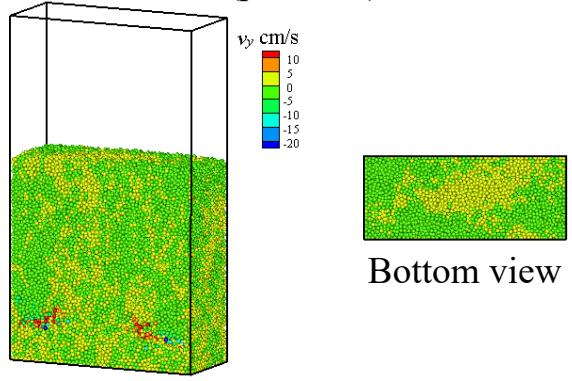
Empirical CFDs of the *experimental results (red line)*  
with the *CFD-DEM propagated UQ in the SRQs (black lines)*



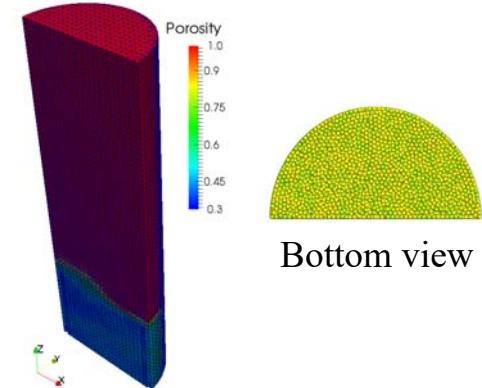
## Phase-II CFD-DEM+UQ: Very Preliminary Results

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Rectangular geometry w/ point-source jets  
(previous)

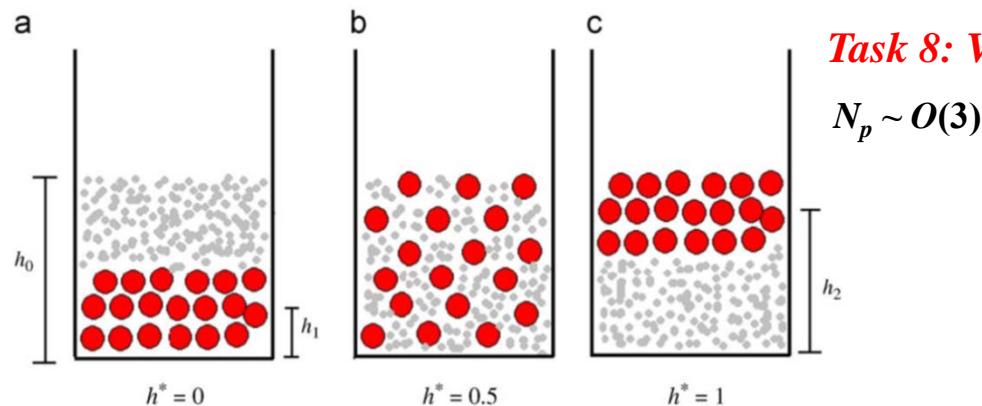


Semi-elliptical geometry w/ cut-cells & point-source jets  
(in progress)



## Phase-II Outlook

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*Task 8: Very, Very Small Scale Problem*

3' diameter  
22' height



*Task 9: Countercurrent Air Flow Stripper Unit*



thank you  
for your  
attention