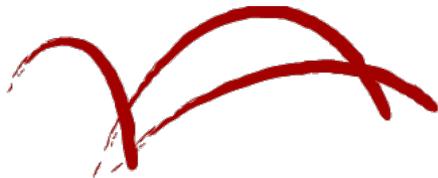


# Characterization of Oxy-combustion Impacts in Existing Coal-fired Boilers (DE-NT0005288)

Bradley Adams, Andrew Fry



*For Energy and  
Environmental  
Solutions*

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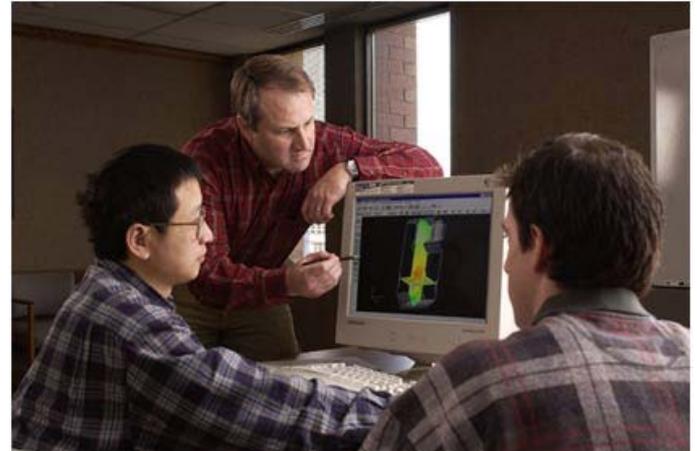
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**2011 NETL CO<sub>2</sub> Capture  
Technology Meeting  
August 22-26, 2011**

# REI Profile

- **Energy And Environmental Consulting Firm**
  - **Combustion System Design and Analysis**
    - **Combustion Performance, Emissions, Operational Impacts**
  - **Advanced CFD Simulations**
  - **Customized Process Software**
  - **R&D / Proof-of-Concept Testing**
  - **Specialized Test Equipment**
- **Use Advanced Technology to Solve Industrial Challenges**



# Oxy-Combustion Program Overview

- **Objective:** Characterize and predict performance and operational impacts of *oxy-combustion retrofit* designs on *existing coal-fired boilers*
- **3-year program (10/1/08 – 9/30/11)**
  - Recent no-cost extension to 3/31/2012
- **Funding:**
  - DOE Cost            \$2,276,327
  - FFRDC                \$100,000
  - Cost-Share          \$617,882
  - Total Program      \$2,994,209



# Project Team

<b>Team Member</b>	<b>Project Role</b>
<b>REI</b>	<i>program management, testing oversight, mechanism development, simulations</i>
<b>University of Utah</b>	<i>laboratory and pilot-scale testing, mechanism development</i>
<b>Siemens Energy</b>	<i>burner technology, firing system design</i>
<b>Praxair</b>	<i>oxygen and CO<sub>2</sub> supply</i>
<b>Brigham Young Univ.</b>	<i>soot measurements</i>
<b>Corrosion Management</b>	<i>corrosion tests, mechanism development</i>
<b>Sandia National Labs</b>	<i>bench-scale testing, mechanism development</i>
<b>Vattenfall AB</b>	<i>mechanism development, validation data</i>
<b>PacifiCorp, Praxair, Southern Company, Vattenfall, DTE</b>	<i>Advisory Panel provides industrial perspective on R&amp;D needs, retrofit requirements and constraints, suggested assessment studies</i>



# Project Approach

- Utilize multi-scale testing and correlations to develop:
  - **Fundamental data** that describe flame characteristics, corrosion rates, and ash properties during oxy-coal firing
  - **Validated mechanisms** that describe oxy-combustion processes
  - **Firing system principles** that guide oxy-burner design and flue-gas recycle properties
- Incorporate validated mechanisms into CFD model to **evaluate full-scale oxy-combustion retrofit designs**
  - Predict flame characteristics and surface impacts for different full-scale oxy-firing designs and FGR properties



# Years 1 and 2 Focus

- **Mechanism identification**
- **Testing**
  - Oxy-firing burner principles
  - Ignition & flame attachment
  - Char oxidation
  - NO<sub>x</sub>, SO<sub>x</sub>, Hg
  - Soot
  - Fine particulates
  - Heat flux profiles
  - Ash chemistry
  - Waterwall and superheat corrosion
- **Mechanism refinement and implementation into CFD**
  - Slagging sub-model



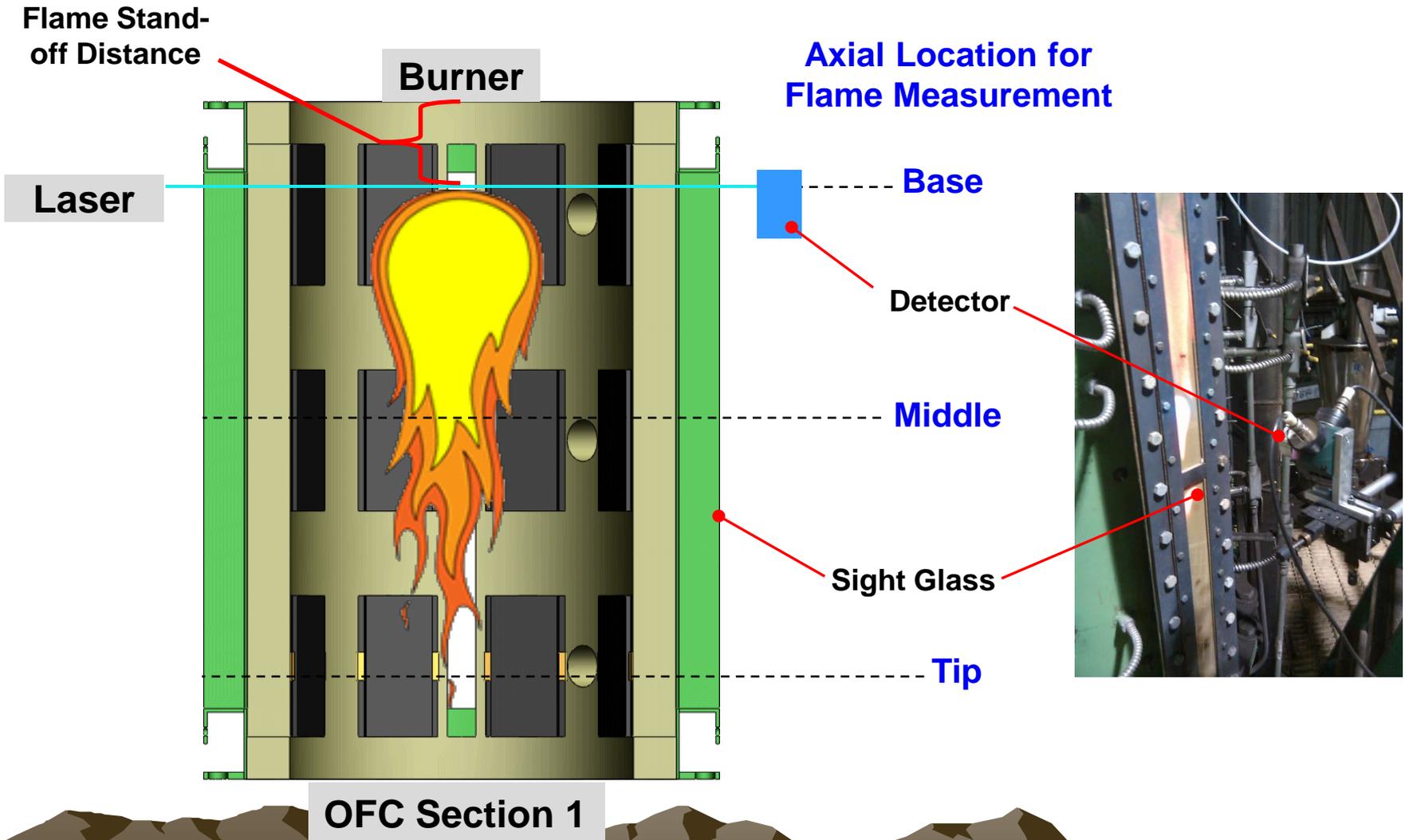
# Year 3 Focus

- **Complete Testing**
  - Soot
  - Fine particulates
  - Char oxidation
- **Complete mechanism refinement / validation and implement into CFD**
  - Char oxidation (done)
  - Gas radiation (done)
  - Soot (in-process)
  - Corrosion (in-process)
- **Full-scale oxy-retrofit assessment**
  - Candidate boiler firing-system design
  - CFD modeling

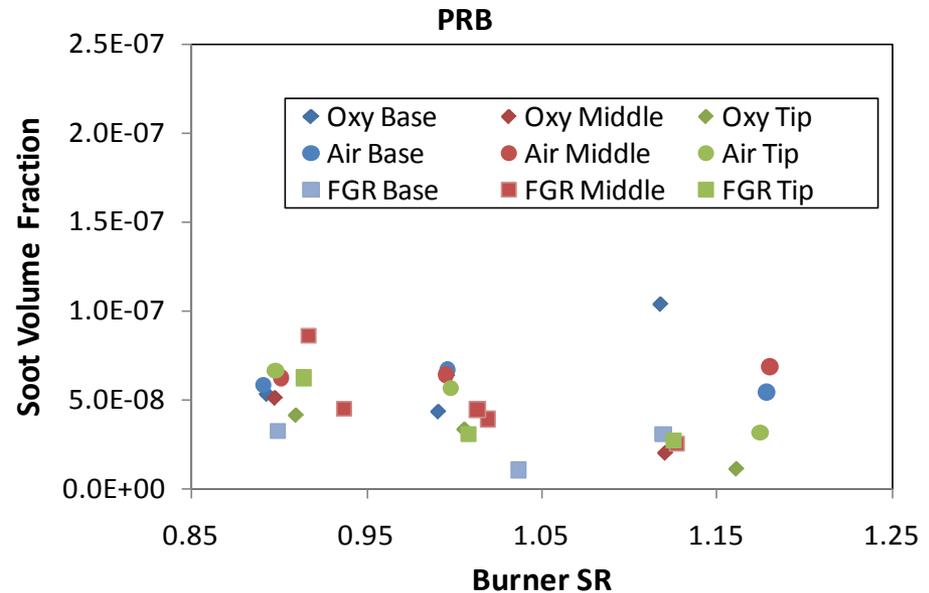
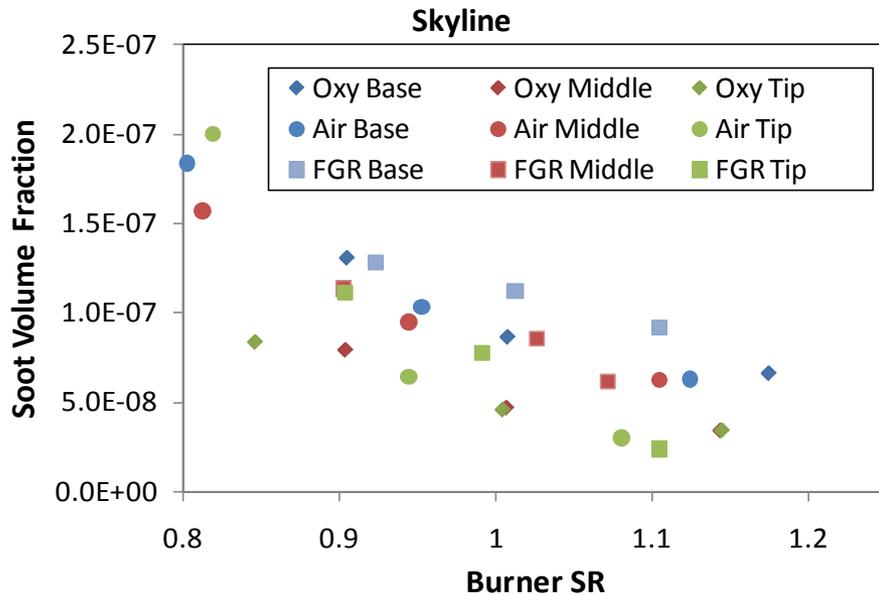


# Line-of-sight Soot Measurements (OFC)

## *Experimental Setup*



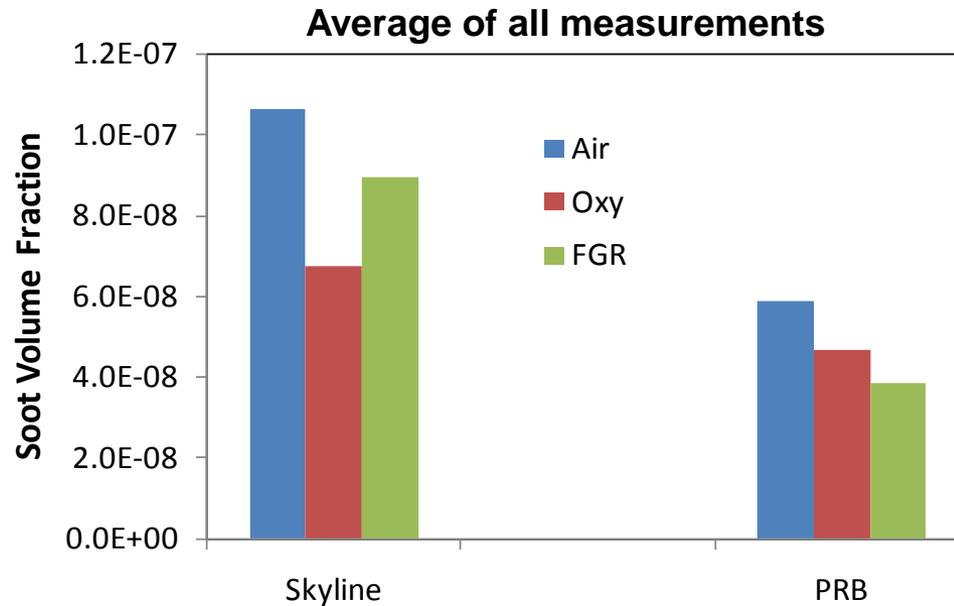
# Line-of-sight Soot Measurement Data



- Soot volume fraction dependent on SR, increases with decreasing SR; PRB SR dependence less pronounced
- For Skyline coal, SVF generally highest at flame base and lowest at flame tip; PRB had less differentiation through flame
- SVF higher for Skyline coal than PRB coal



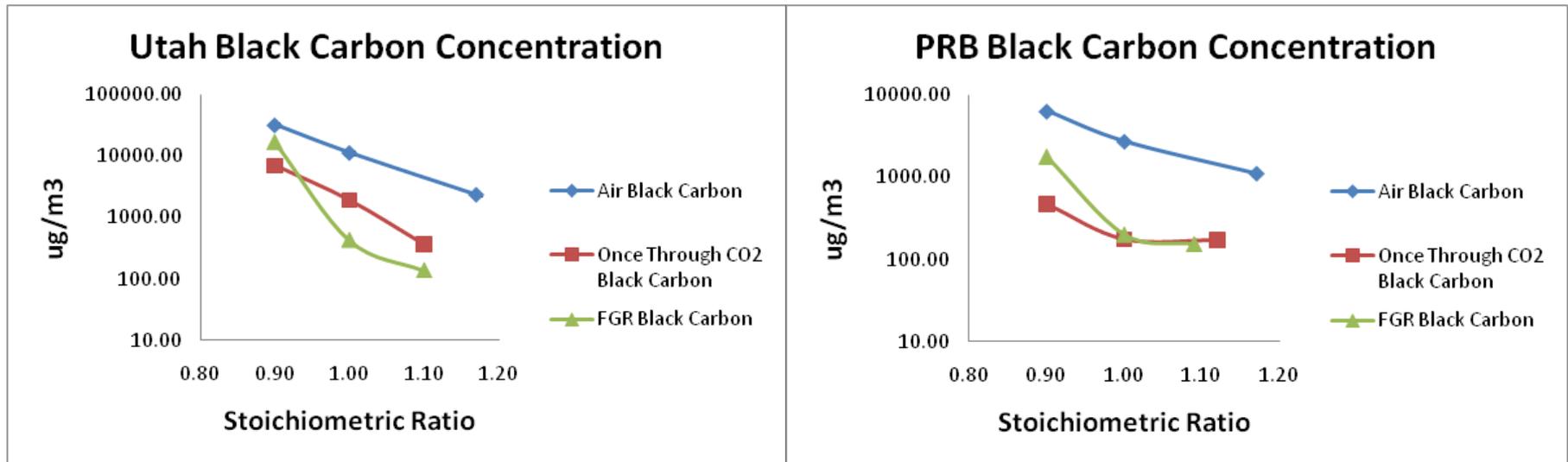
# Line-of-sight Soot Measurement Data



- **SVF higher for Skyline coal than PRB coal**
- **SVF lower for oxy-combustion than air-combustion**
- **Soot generation/destruction tied to flame aerodynamics and gas stream mixing**



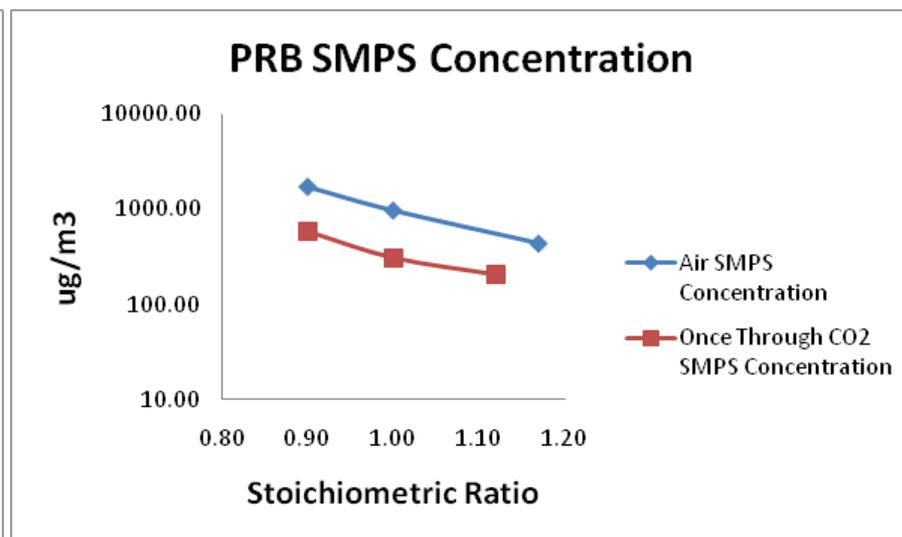
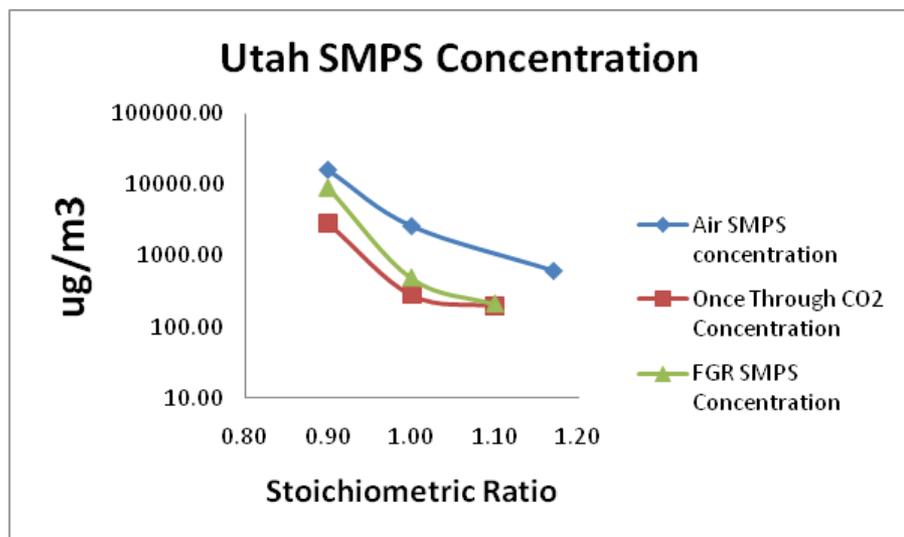
# OFC Black Carbon Results (PA analyzer)



- **Black carbon emissions increase with decreasing SR**
- **Utah coal produced higher black carbon emissions than PRB**
- **Oxy-firing reduces black carbon emissions from flames when compared to air-firing for all coals tested (Utah, PRB, Illinois)**
- **The presence of >30% water vapor in RFG can potentially reduce black carbon emissions due to steam impact on combustion**



# OFC Size Distribution Results (SMPS)



- Ultrafine particle concentrations increase with decreasing SR
- Black carbon or soot particles are significant contributors to ultrafine particle concentrations
- When recycling untreated flue gas, it is possible to increase the concentration of ultrafine particles in the furnace

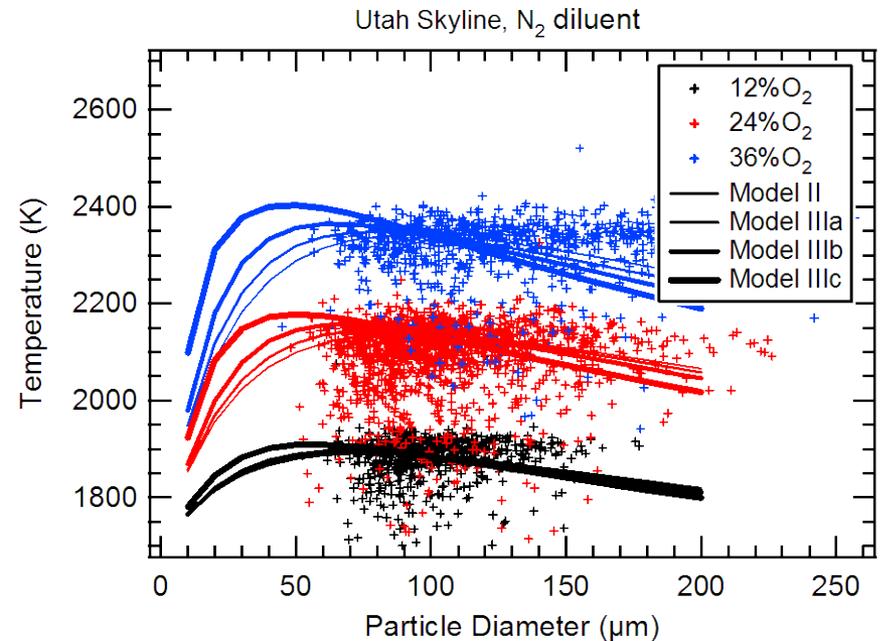
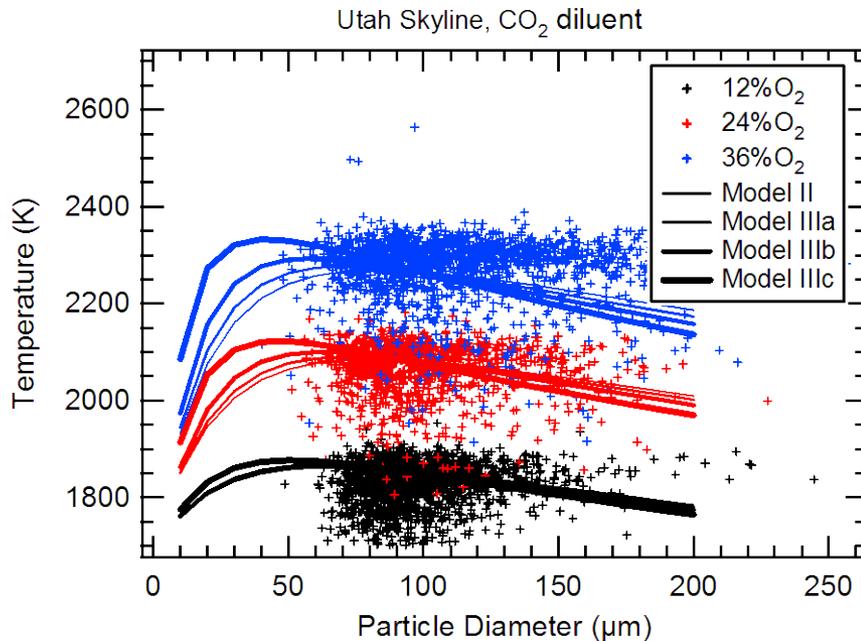


# Char Oxidation Mechanism

- **Original mechanism has oxidation-only single film model, different behavior with oxy-combustion (higher O<sub>2</sub>, CO<sub>2</sub>, H<sub>2</sub>O)**
  - BL diffusion & reactions, gasification reactions
- **Experimental investigation**
  - Optical measurements on individual particles burning in controlled lab-scale environments (O<sub>2</sub>, H<sub>2</sub>O concentrations; N<sub>2</sub> or CO<sub>2</sub> diluent)
  - Measured particle temperature-size data as basis for model comparison and estimation of fitting parameters for use in CFD code
- **Extended Single Film model**
  - Include (heterogeneous) steam and CO<sub>2</sub> gasification reactions in commonly employed oxidation-only single film model
  - Fit rate parameters to match observed temperatures of 100 μm particles burning in N<sub>2</sub> (with 12% and 36% O<sub>2</sub>) and CO<sub>2</sub> (36% O<sub>2</sub>)
  - Predict char oxidation characteristics for both air and oxy-fired environments at different O<sub>2</sub> conc. and 10-200 μm particles



# Extended Single-film Model Comparisons



- **Char temperatures increase with increasing O<sub>2</sub> concentration, nearly independent of size**
- **Predictions capture temperature behavior of trusted size range (roughly 100  $\mu\text{m}$ )**
- **Good agreement for both air & oxy environments**

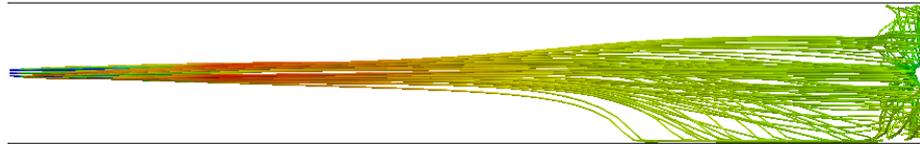


# Char Oxidation Mechanism Summary

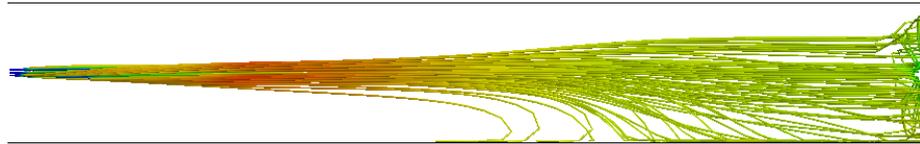
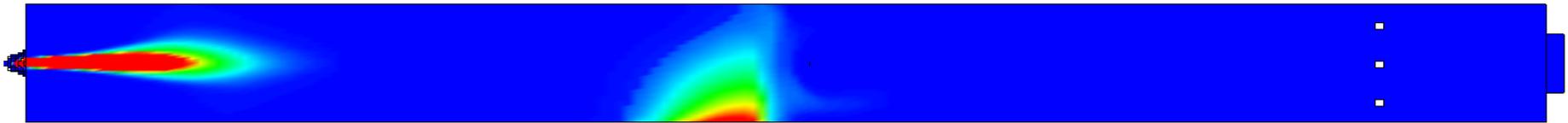
- **Extended Single Film model:**
  - **Reliable CFD predictions seem feasible for both conventional and oxy-combustion environments if steam and CO<sub>2</sub> gasification reactions are included in Single-Film model**
  - **Char consumption rates appear to be similar for both CO<sub>2</sub> and N<sub>2</sub> environments at equal O<sub>2</sub> concentrations, but are sensitive to gasification rates at high particle temperatures (due to high O<sub>2</sub> concentrations)**
  - **Gasification reactions matter at high temperatures (high O<sub>2</sub>), not only where CO<sub>2</sub> concentrations are high**
- **Implement in CFD code and test impacts on model of L1500 pilot-scale furnace**



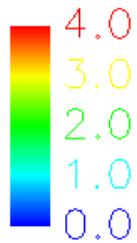
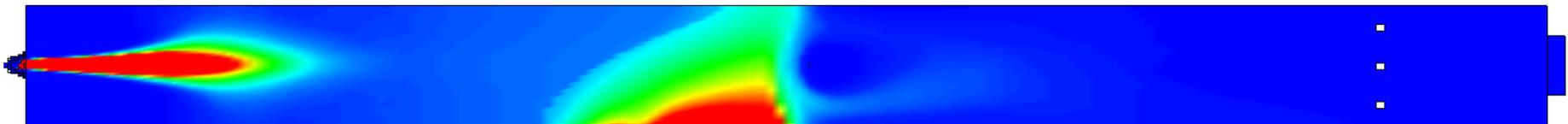
# L1500 Particle Trajectories and CO Profiles



Skyline Air



Skyline Oxy



CO Conc.  
(vol%, wet)

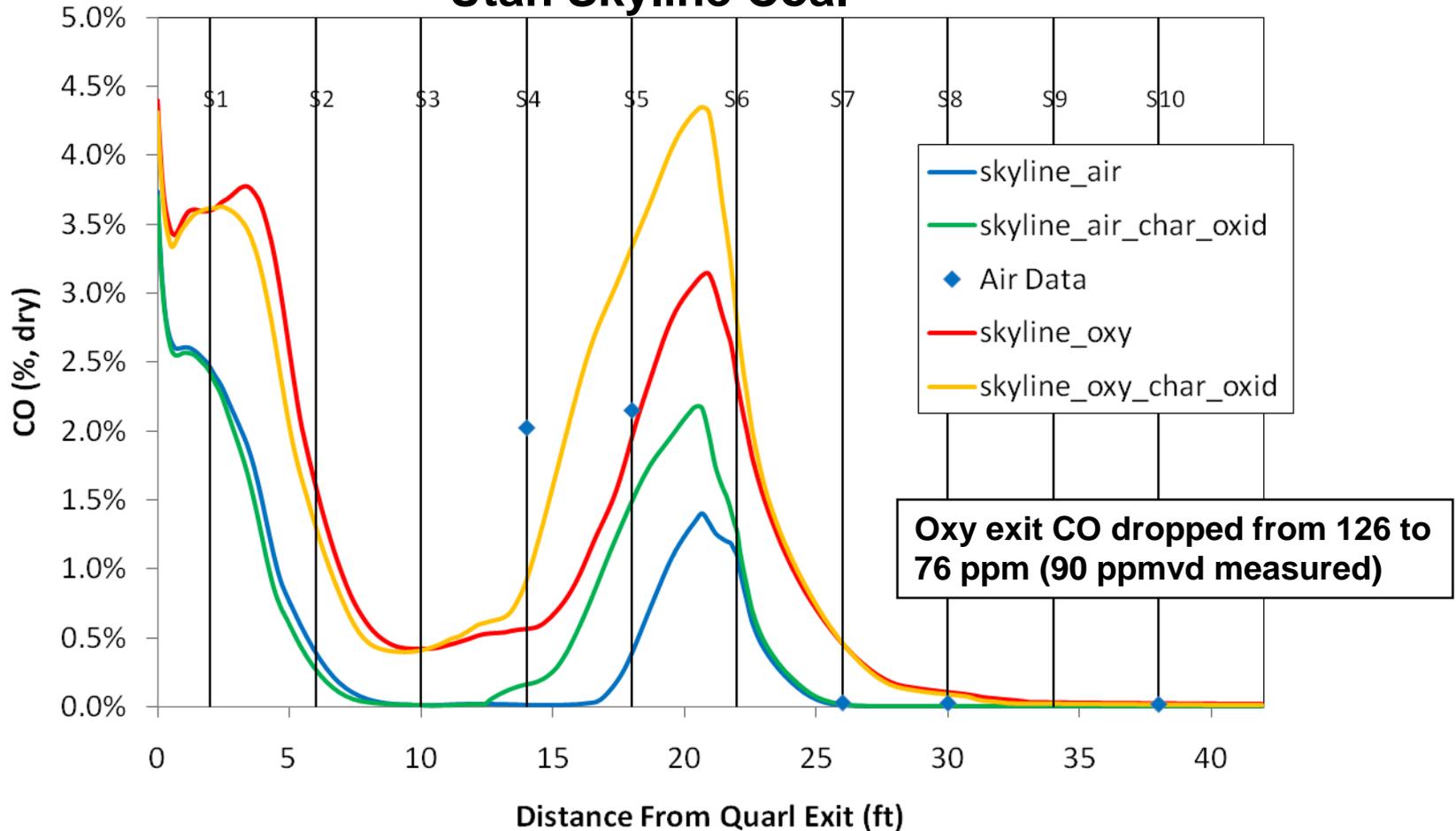
OFA

BSR = 0.9  
Exit  $O_2 \sim 3.1\%$   
Air  $O_2 = 21\%$   
Oxy  $O_2 = 27\%$

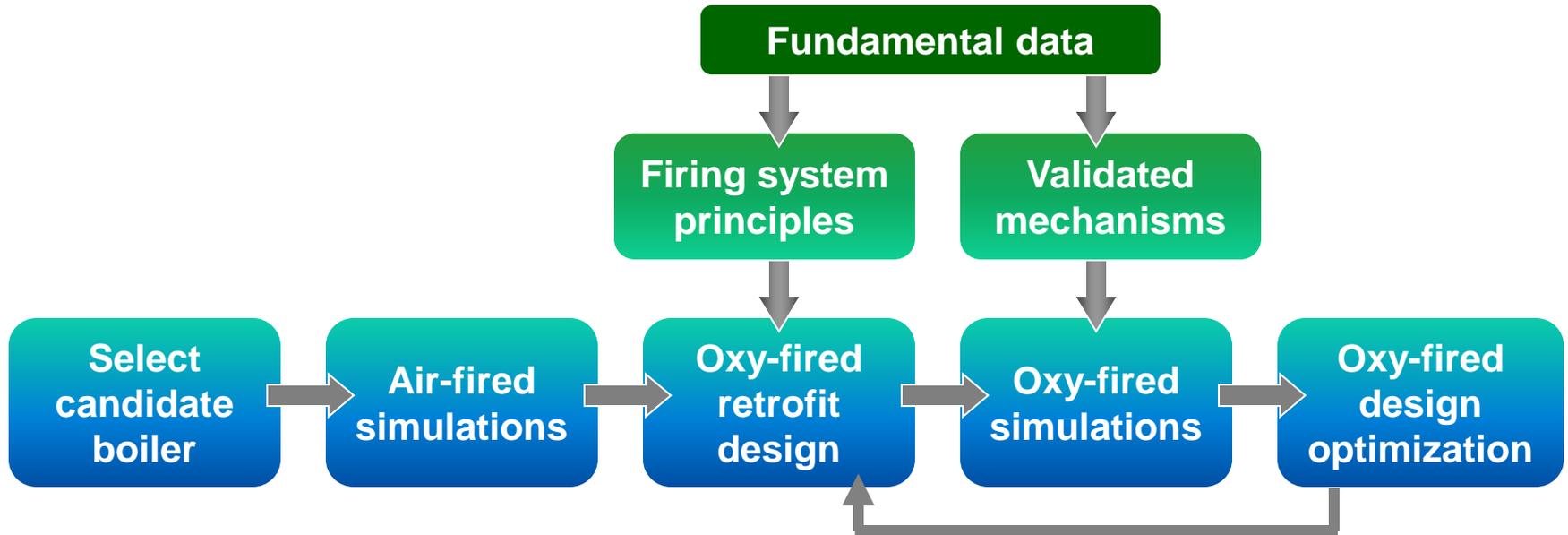


# Average CO Concentration Comparison (with extended char oxidation model)

## Utah Skyline Coal



# Full-scale Boiler Assessment Approach



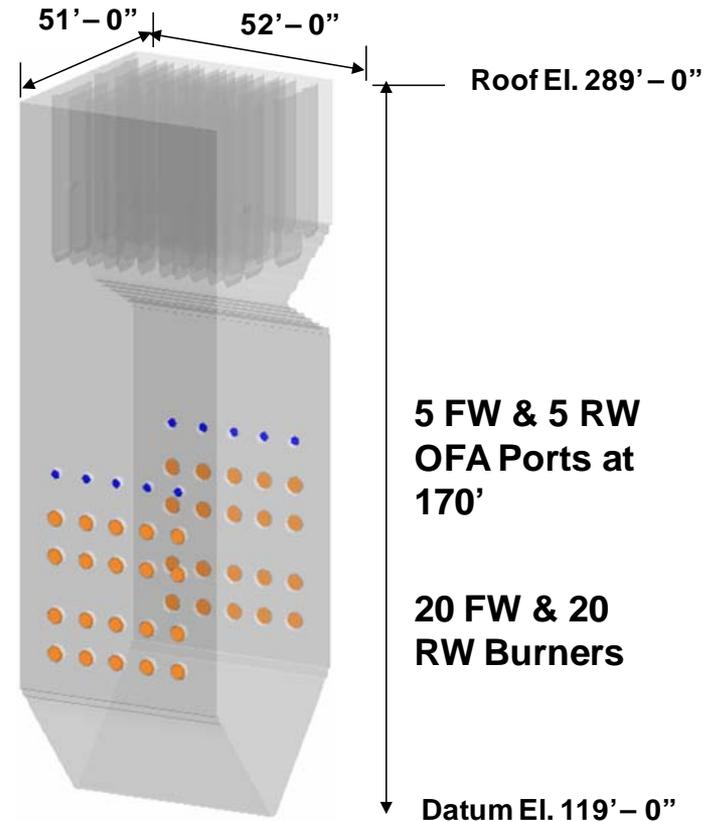
## Design and optimization criteria:

- Match air-fired heat duties
- Maximize combustion efficiency
- Minimize surface impacts (corrosion, slagging, fouling)
- Minimize trace pollutant emissions



# PacifiCorp Hunter Unit 3

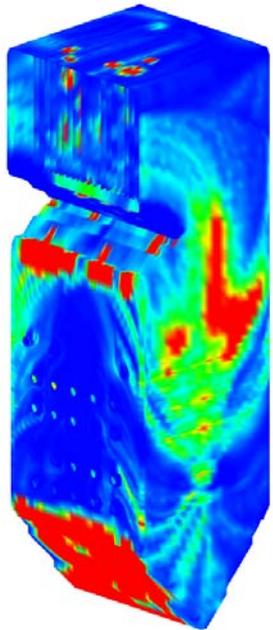
- 460 MW<sub>e</sub> opposed wall-fired
- 40 Staged low-NO<sub>x</sub> burners with 10 overfire air ports
- Fires Utah bituminous coal
- Steam cycle well-characterized during LNB/OFA retrofit
- Modeling includes radiant furnace and back pass
  - CFD model for local detail (combustion, deposition, heat transfer, pollutants)
  - Process model for steam circuit impacts



# Hunter 3 Air-fired Results

**Baseline**

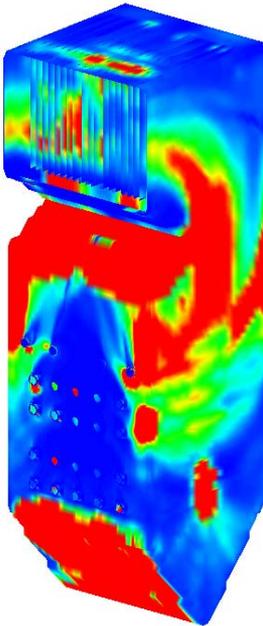
12.7% of Coal  
Mineral Matter  
Is Deposited



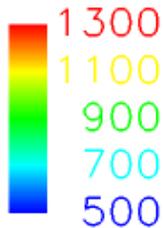
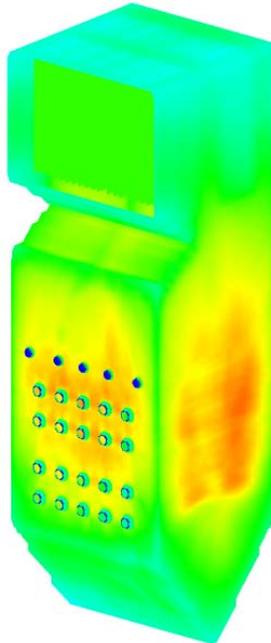
**Deposition Flux  
(lb/ft<sup>2</sup>-s)**

**Slagging**

27.0% of Coal  
Mineral Matter  
Is Deposited

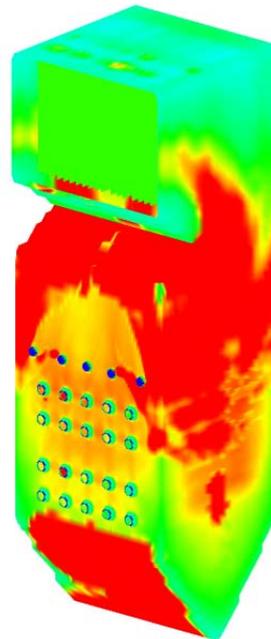


**Baseline**



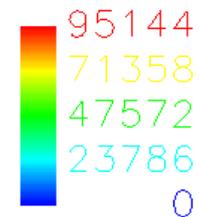
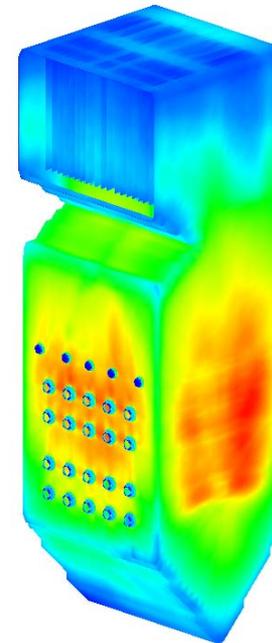
**Wall Temp ( F )**

**Slagging**



**Baseline**

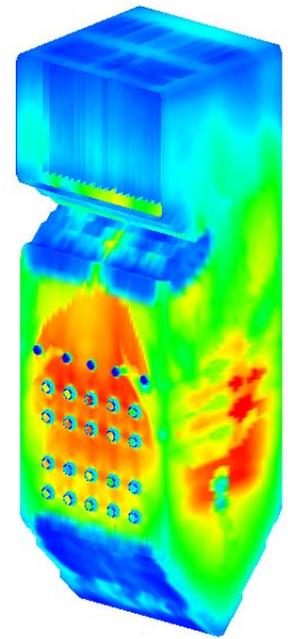
$T_{ex} = 1862 \text{ F}$   
UBC = 7.0%



**Heat Flux  
(Btu/hr-ft<sup>2</sup>)**

**Slagging**

$T_{ex} = 1938 \text{ F}$   
UBC = 4.6%



# Overview of Firing System Design

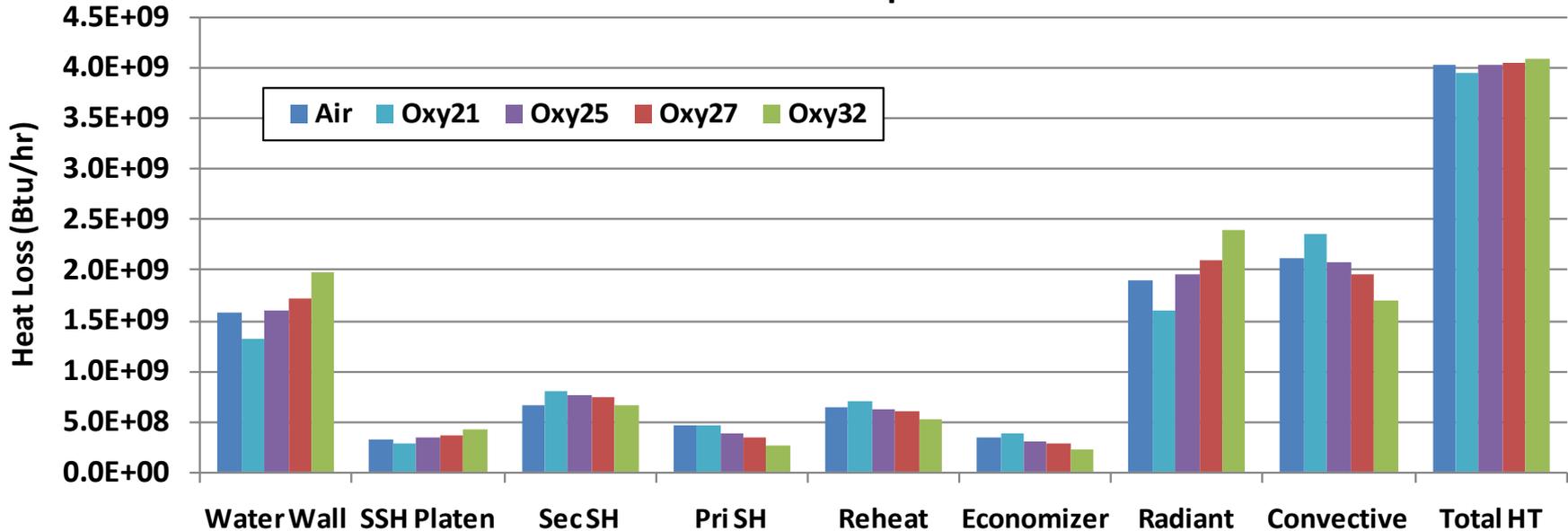
- **SteamGen Expert (process model) used to estimate heat transfer during air-firing and oxy-firing at various oxygen concentrations and FGR flow rates**
  - **Air-fired boiler measurements used to guide setup of radiant and superheat heat exchanger modules**
- **Calculations performed to determine whether burners should be designed for air or oxy-fired conditions**
  - **Calculations based on Siemens' new burner design to determine register velocities under air- and oxy-fired conditions**





# Heat Exchanger Comparison (SGE)

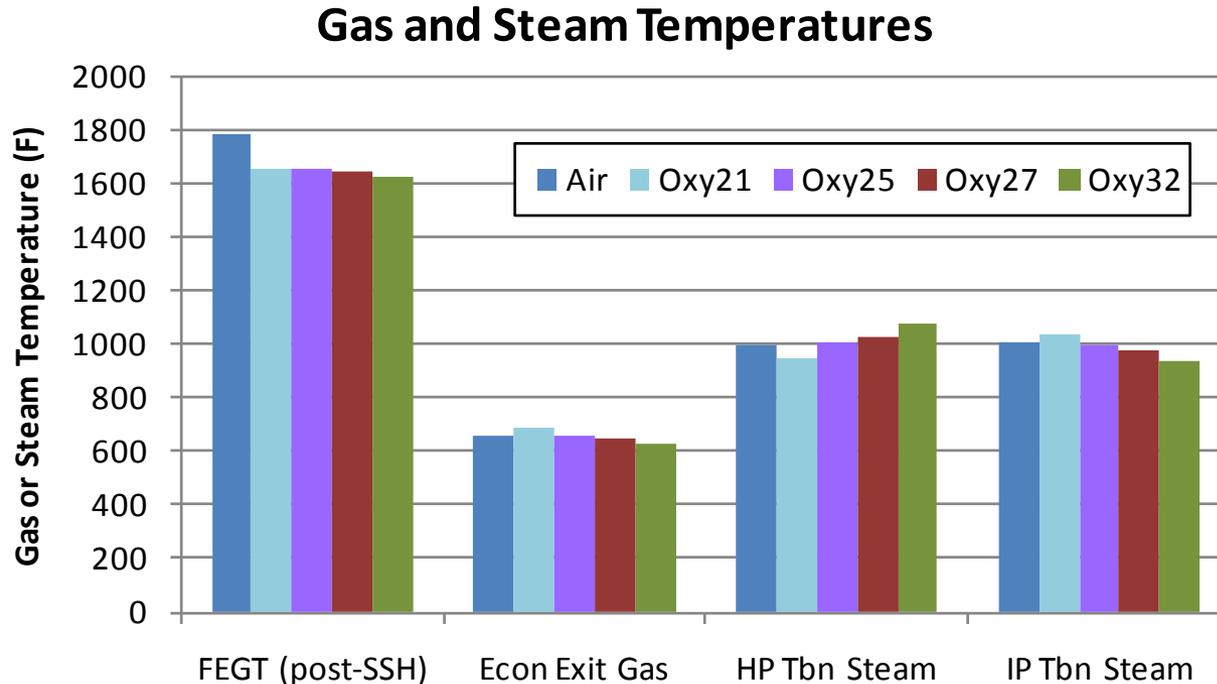
Heat Transfer Comparison



- Waterwall HT increases with increasing O<sub>2</sub> due to hotter flames
- Convective HT decreases with increasing O<sub>2</sub> due to decreased gas flow
- Oxy25 appears to best match air-fired heat transfer (see also next slide)



# Gas and Steam Temperature Comparison (SGE)

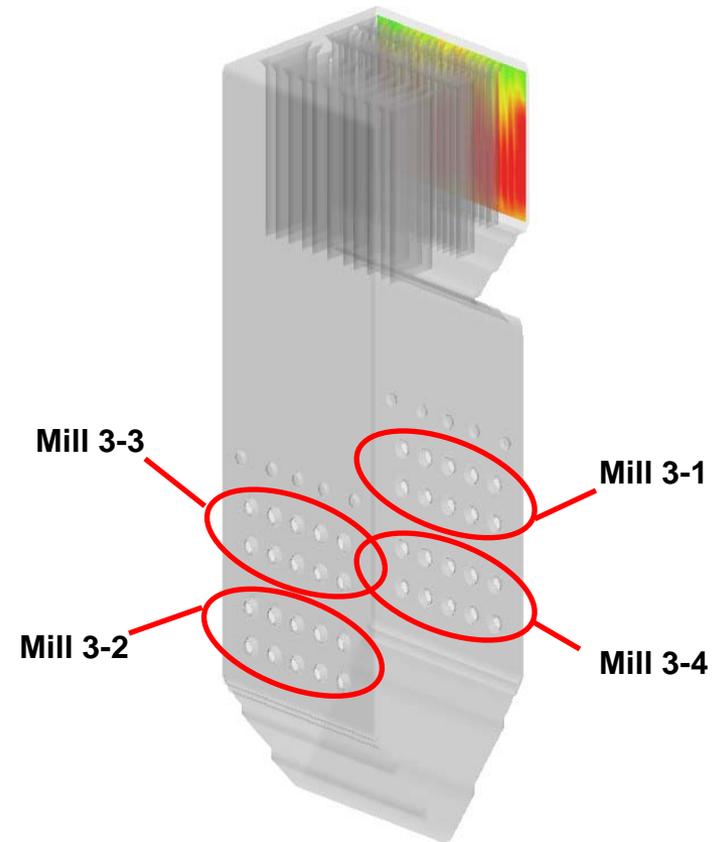


- **Oxy FEGTs lower than air, similar (furnace gas temperature changes balanced by heat absorption changes)**
- **HP turbine steam temp trend opposite SSH absorption trend, but consistent with waterwall and platen absorption trends, which dominate**
- **IP turbine steam temp trend matches RH absorption trend**



# Determination of Burner Retrofit Approach

- When designing burners for air-fired conditions, oxy-firing velocities are much lower
  - Determine what increase in velocity is caused by removing one mill from service and operating with 30 burners on oxy-firing at the same firing rate
- The oxy-firing velocities were too high with one mill out of service
  - Significant modifications to the firing conditions (BSR and Pri Gas/Fuel) necessary to match design velocities
- Therefore the burner should be designed for oxy-firing
  - Concessions may be necessary on emission performance or firing rate during air-firing



4 mills total, 10 burners on each mill



# Firing System Design Summary

- **SteamGen Expert was used to model heat transfer during oxy-firing at various oxygen concentrations**
  - 25% O<sub>2</sub> and 27% O<sub>2</sub> were found to best match air-fired heat transfer rates, therefore 26% O<sub>2</sub> was chosen as the design criteria for oxy-firing
- **Burner should be designed for oxy-fired conditions and the operation may be modified when air-firing**
  - FGR assumed clean (~90% SO<sub>2</sub> removal)
  - 21% O<sub>2</sub> wet in primary for air and oxy-firing
- **Calculated burner register velocities for Siemens' new burner used for oxy and air-fired modeling inputs**



# Program Status Summary

- **Bench-, Lab-, Pilot-Scale Testing Completed**
- **Remaining Key Tasks**
  - Complete validation and refinement of remaining mechanisms; implement in CFD code
  - Complete conceptual full-scale retrofit firing system design
  - Assess oxy-combustion retrofit impacts on existing boilers
    - PacifiCorp Hunter 3; DTE River Rouge 3
  - Document results in final report to DOE
- **Future Objectives**
  - Model ~15-30 MW<sub>th</sub> pilot-scale oxy-fired unit for validation
  - Support oxy-combustion demonstration on full-scale unit



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Department of Energy under Award Number DE-NT0005288;  
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