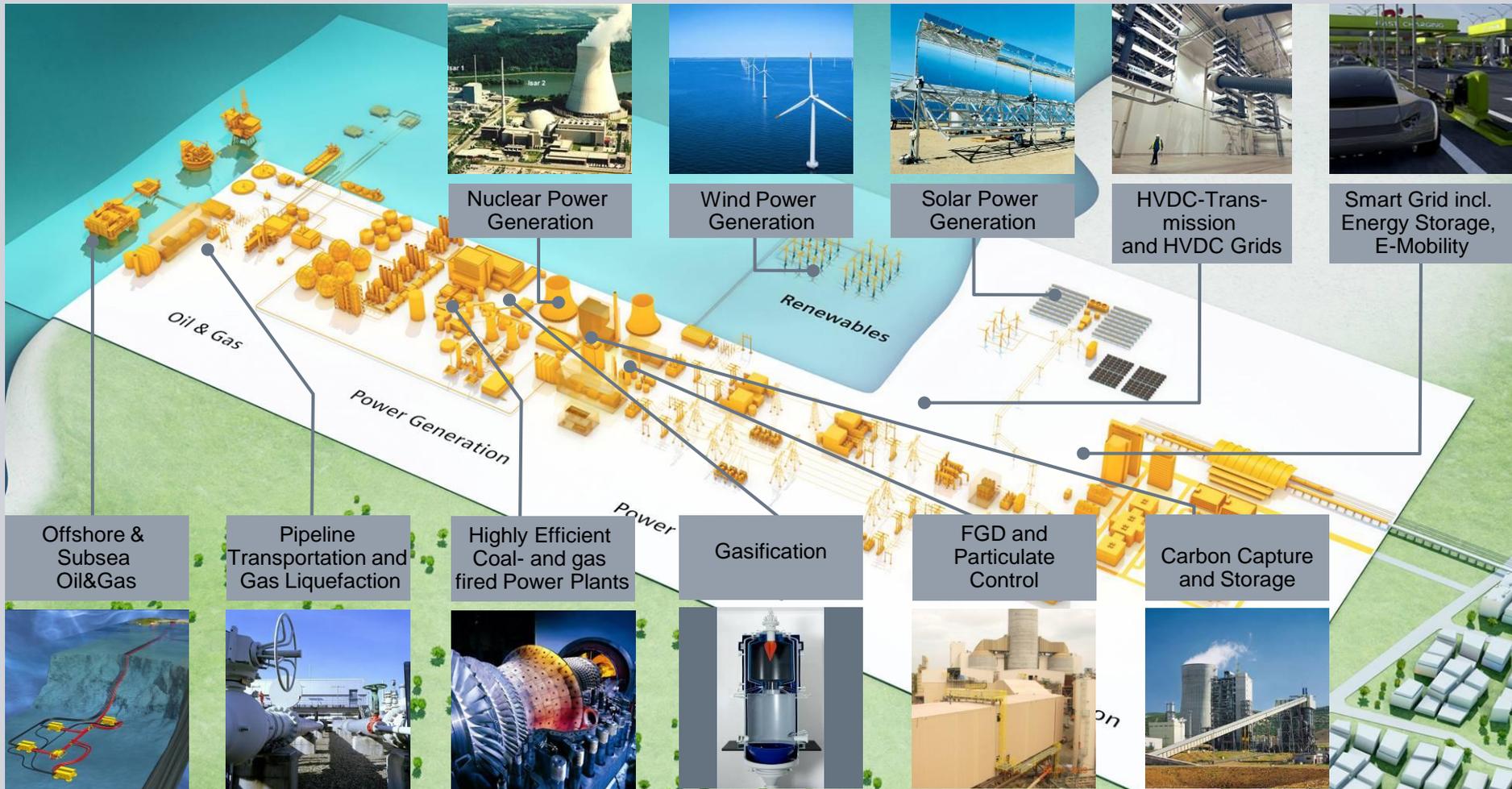


# **Slipstream Development & Testing of Post-Combustion CO<sub>2</sub> Capture and Separation Technology for Existing Coal-Fired Plants**

2.5 MWe Slipstream at TECO's Big Bend Station utilizing Siemens Amino Acid Salt (AAS) Solvent

NETL CO<sub>2</sub> Capture Technology Meeting  
DOE/NETL PM: Dave Lang

# Sampling of Siemens Product Markets



## Project Overview – Project Participants

**Tampa Electric – Host Site Provider,  
Big Bend Plant**

**DOE NETL – Project Sponsor /  
Awarding Agency**

**Siemens – Technology, Equipment,  
and Installation provider. Co-  
Sponsor**



# Project Overview – Overall Project Performance Dates



Activity		
Kick-off	 October 1, 2010	
Phase 1 – Process Design	October 1, 2010      July 31, 2011 	
Phase 2 – Procurement & Erection	Aug 1, 2011      Aug 31, 2012 	
Phase 3 – Operation & Testing	Sept 1, 2012      Jul 1, 2013 	
Issue Final Report (draft)	Jul 31, 2013 	

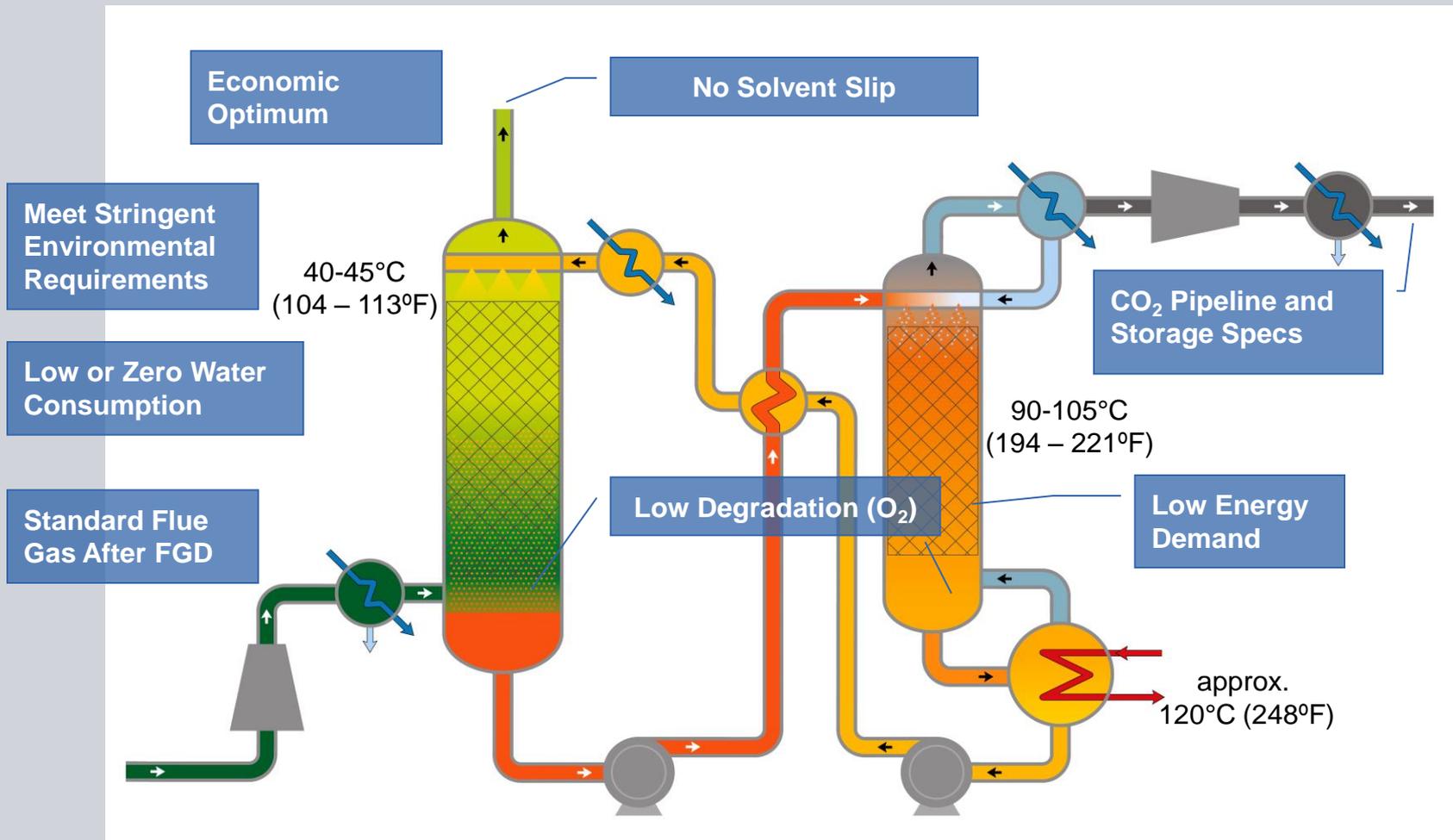
## Project Overview - Funding

	Budget Period 1 Process Design Oct 2010 – Jul 2011		Budget Period 2 Procurement & Erection Aug 2011 – Aug 2012		Budget Period 3 Operation & Testing Sep 2012 – Oct 2013	
	DOE share	Siemens share	DOE share	Siemens share	DOE share	Siemens share
Split (80/20) over 13 qtrs	\$1,411 K	\$353 K	\$10,580 K	\$2,645 K	\$3,008 K	\$752 K
DOE Project Total						<b>\$15,000 K</b>
Siemens Project Total						<b>\$3,750 K</b>

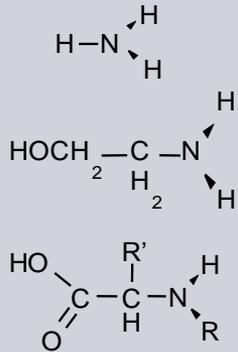
## Project Objectives

- Demonstrate the ability of POSTCAP technology to achieve 90% CO<sub>2</sub> removal and approach a 35% increase of cost of electricity produced.
  - **AAS technology can reach 90% CO<sub>2</sub> removal**
  - **Challenge of approaching 35% increase in COE**
- Demonstrate the scalability and feasibility of progressing the POSTCAP technology to full-scale commercial application (550 MW) on post-combustion CO<sub>2</sub> capture for coal fired power plants and to full-scale commercial application for industrial sources of CO<sub>2</sub> emissions.
  - **Proving scalability**
  - **Proving feasibility**

## Technology Fundamentals



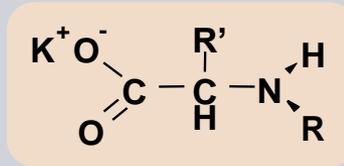
# Technology Fundamentals – Amino Acid Salt is the basis of our solvent



Ammonia

MEA

Amino acid



Amino acid salt

No vapor pressure

Chemically stable

Naturally present

Salts have no vapor pressure

- No thermodynamic solvent emissions
- Not flammable
- Not explosive
- Odorless
- No inhalation risk



Negative ion is less sensitive to O<sub>2</sub>

- Low degradation

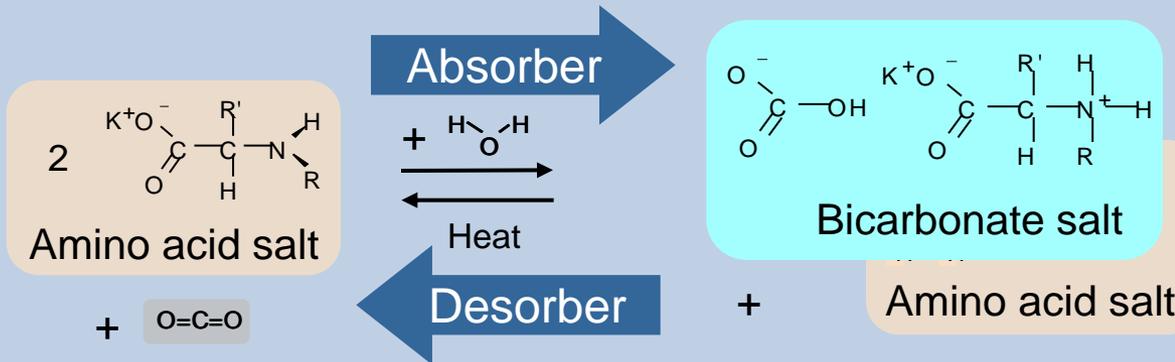
Amino acids are naturally present

- Biodegradable
- Nontoxic
- Environmentally friendly

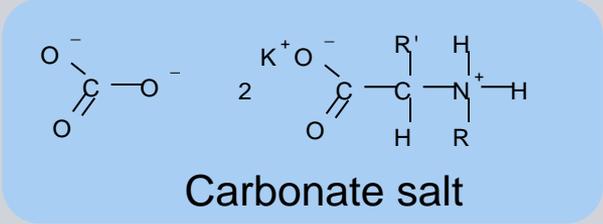
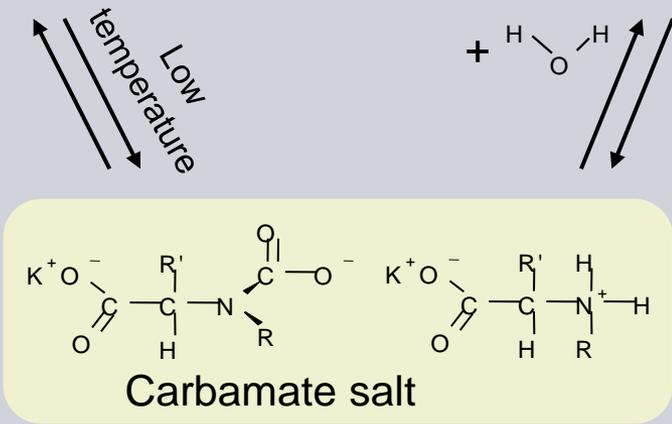


# Technology Fundamentals

Preferred reaction mode



Precipitation is an option for next-generation (2<sup>nd</sup>+) solvent



Intermediate reaction products fulfill the same HSE standard as amino acid salts

# Technology Background - Solvent Stability and Current Performance

Components	Amino Acid Salt w/o H <sub>2</sub> O wash
VOC	not detectable
Formaldehyde	not detectable
Methylamine	not detectable
∑Nitrosamines	not detectable
Ammonia	<1 ppm

- the solvent is highly stable and does not lead to measurable loss of active substance due to degradation
- by-products in the liquid phase are salts with no vapor pressure
- No production of any mentionable amounts of emissions
- small amounts of heat stable salts (HSS) and nitrosamines will be removed with reclaimers

The amino-acid salt is stable against thermal stress and oxygen environments

# Background - Siemens lab plant for CO<sub>2</sub> capture tests at Frankfurt Hoechst Industrial Park

**SIEMENS**

Desorption column

Synthetic gas flue gas mixtures

Reboiler made of glass so that boiling retardation effects can be recognized

Absorption column with operating pressure up to 10 bar

Reclaimer Units

Fully automated DCS system  
NDIR CO<sub>2</sub> analytic

# Background – E.ON Energie’s Staudinger 100 kW Pilot



Upscaling via Slip-Stream Demopants



# Advantages – Solvent Comparison of Amines and Amino Acid Salt Formulations at 90% Capture Rate



		Amines	Siemens POSTCAP
<b>Environmental Considerations</b>	<b>Capital Cost</b>	High Vapor Pressure requires additional equipment	Zero Vapor Pressure requires no additional equipment
	<b>Operations</b>	Inhalation Risk requires more stringent handling procedures	No Inhalation Risk; no complicated handling procedures
	<b>Public Acceptance</b>	Spill Considerations	Environmentally Friendly Odorless
<b>Chemical Efficiency (Reagent Degradation)</b>		Sensitive to Oxygen	75% less than MEA
<b>Siemens Auxiliary System Experience</b>		Limited Compression, Flue Gas Clean-up, Steam Extraction Experience	Demonstrated Experience in Flue Gas Clean-up, CO <sub>2</sub> Compression and Steam Extraction

# Challenges - applying AAS solvent technology to existing PC and industrial plants

- **Developing solvent suppliers on a large, commercial scale**
- **Minimize energy consumption**
- **Available footprint for large-scale carbon capture retrofits**
- **Combined cycle challenges to be overcome:**
  - ✓ **Low CO<sub>2</sub> concentration in flue gas**
  - ✓ **High oxygen content in flue gas**
  - ✓ **Operation with frequent load changes**
  - ✓ **Fewer integration options for low temperature heat from the capture plant**

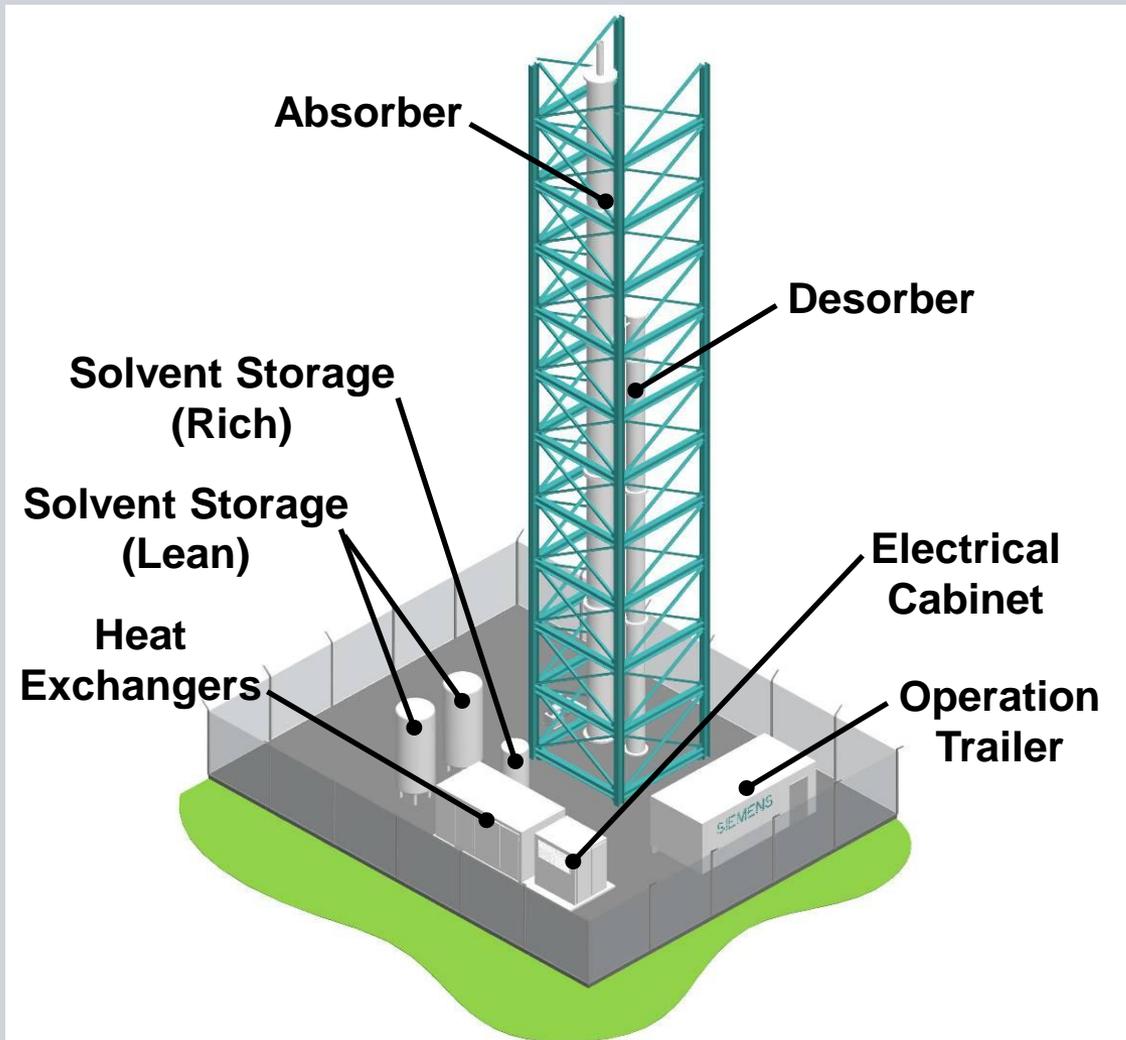
## Project Methodology

### Slipstream Project Work

- Preliminary Engineering
- Detailed Engineering & Design
- Development of Equipment/Procurement Packages
- Retrofit installation into existing Big Bend scrubber outlet
- Commissioning, Operation and Testing of plant
- Data Analysis, Report out
- Decommissioning/Dismantling



## Project Methodology – basic plant layout



# Project Methodology

## Schedule

Task 1.0 Preliminary Design Engineering	10/1/2010	2/28/2011
Task 2.0 Generation of Heat & Material Balance	10/1/2010	11/30/2011
Task 3.0 Generation of PFD's	10/1/2010	11/30/2011
Task 4.0 Plant Interface Engineering	10/1/2010	6/30/2011
Task 5.0 Preliminary Design	10/1/2010	2/28/2011
Task 6.0 Detail Design/Engineering	3/1/2011	7/31/2011
Task 7.0 Site Civil Work	8/1/2011	8/31/2011
Task 8.0 Plant Equipment & Material Procurement	8/1/2011	8/30/2012
Task 9.0 Complete Erection of Structural Steel	9/1/2011	2/15/2012
Task 10.0 Absorber/Desorber Installation Complete	9/1/2011	5/9/2012
Task 11.0 Mechanical Installation Complete	9/1/2011	5/9/2012
Task 12.0 Piping Component Installation	12/1/2011	8/30/2012
Task 13.0 Complete Electrical Installation	2/1/2012	7/13/2012
Task 14.0 Complete I&C Installation	2/1/2012	8/30/2012
Task 15.0 Test Plan Development	6/1/2012	8/31/2012
Task 16.0 Phase 3 - Commissioning, Testing, and Reporting	9/1/2012	7/31/2013
Task 17.0 Perform System Hydro Test	9/1/2012	10/1/2012
Task 18.0 Perform Plant Startup	10/31/2012	12/3/2012
Task 19.0 Steady State Plant Operation	12/3/2012	7/1/2013
Task 20.0 Perform Testing	12/3/2012	7/1/2013
Task 21.0 Data Analysis	7/2/2013	7/31/2013
Task 22.0 Decommission	8/1/2013	10/31/2013
Task 23.0 Disassemble (If Required)	8/1/2013	10/31/2013

## Future Development / Commercialization

### Siemens Post-Combustion Capture Process



- Scale up to larger demonstration units
- Integrated PostCAP Process Design Package (PDP) to Engineering, Construction and Commissioning.
- Project execution within Siemens Energy Sector
- Entirely Done within Siemens
- Collaboration with external engineering and construction contractors as needed

### Siemens Scope

applicable for retrofits and for new power plants

### Polishing of FGD Unit



### Power Plant Integration



### CO<sub>2</sub> Compression



### Balance of Plant Activities



To be provided by third party on behalf of investor (e.g. civil, Infrastructure, not process related)