

*Reversible Ionic Liquids as  
Double-Action Solvents for  
Efficient CO<sub>2</sub> Capture*

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School of Chemistry and Biochemistry

Georgia Tech, Atlanta

# *Chemical Engineering and Chemistry 21-Year Collaboration at Georgia Tech*

- Jointly Directed Students and Postdoctorals
  - ✓ Chemical Engineers
  - ✓ Chemists
  - ✓ > 50 PhDs Completed
- >50 Joint Research Grants
- >250 Publications and Presentations
- **2004 Presidential Green Chemistry Challenge Award**



# *Project Goal: CO<sub>2</sub> from Coal-Fired Power Plants*

- Long-Term Goal
  - ✓ Capture 90% of CO<sub>2</sub> with less than 30% cost increase by 2020
- This Project
  - ✓ **Solvent with Optimum Balance of Properties**
    - Synthesize and Characterize
    - Use in Process Design
    - Determine Best by Energy, Economics
  - ✓ **Optimum Solvent**
    - Demonstrate on Lab Scale
    - Design Pilot Scale Process
    - Develop Scalable Process for Synthesis
- **Bottom Line:** Superior Process for Post-Combustion CO<sub>2</sub> Capture from Coal-Fired Power Plants

# *Funding – \$ in Thousands*

## *By Budget Period, DOE and Cost Share*

<b>Expenditure</b>	<b>BP1 DOE</b>	<b>BP1 Share</b>	<b>BP2 DOE</b>	<b>BP2 Share</b>	<b>BP3 DOE</b>	<b>BP3 Share</b>	<b>Total DOE</b>	<b>Total Share</b>
<b>Personnel</b>	372	79	417	85	434	85	1251	263
<b>Equipment</b>	92	71		118				150
<b>Supplies</b>	30		76		75		228	
<b>Services</b>	21		38		38		114	
<b>Travel</b>	9		9		9		27	
<b>TOTAL</b>	524	150	540	203	556	85	1620	413
<b>Share %</b>		28.6		37.5		15.2		27

# *Overall Project Performance Dates*

**First Year**

**Second Year**

**Third Year**

**Q1 Q2 Q3 Q4 Q1 Q2 Q3 Q4 Q1 Q2 Q3 Q4**

**PROJECT MANAGEMENT, PLANNING, AND REPORTING**

**1-COMPONENT SILYL AMINE-  
BASED ILS**

**1-COMPONENT SILYL GUANIIDINE-BASED ILS**

**THERMODYNAMICS AND RATES OF IL  
FORMATION**

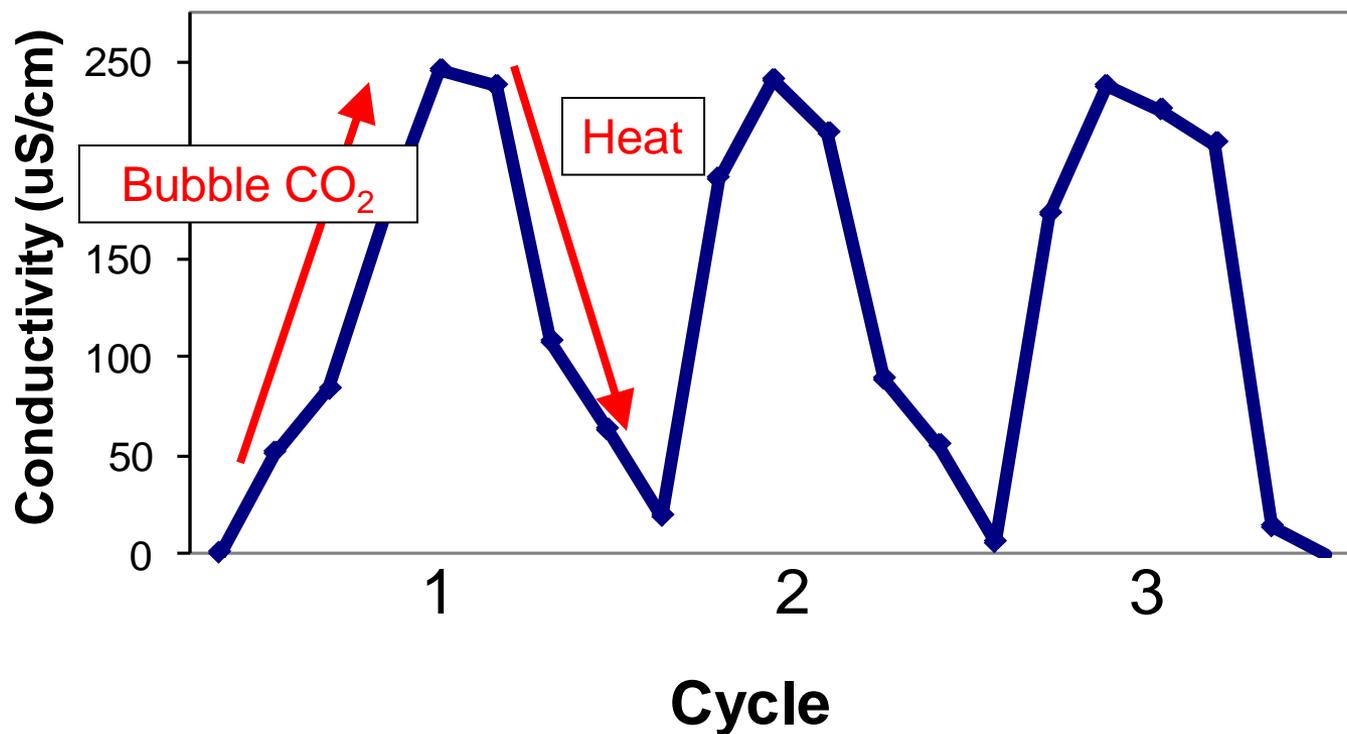
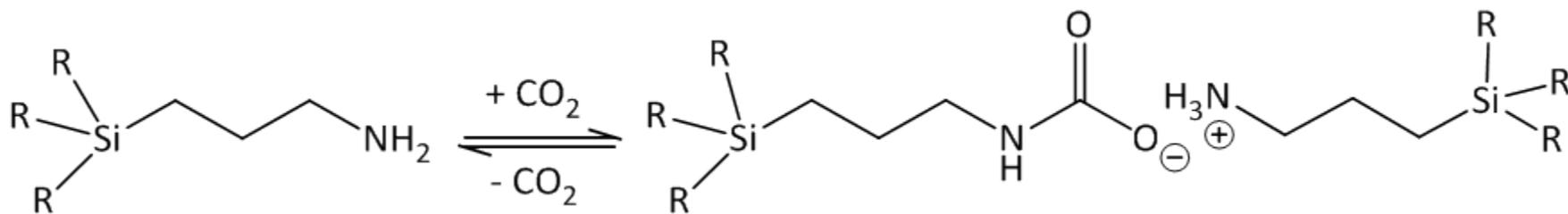
**OPTIMIZE CO<sub>2</sub> CAPTURE SOLVENT  
STRUCTURE**

**PROCESS DESIGN AND ECONOMIC  
ANALYSIS**

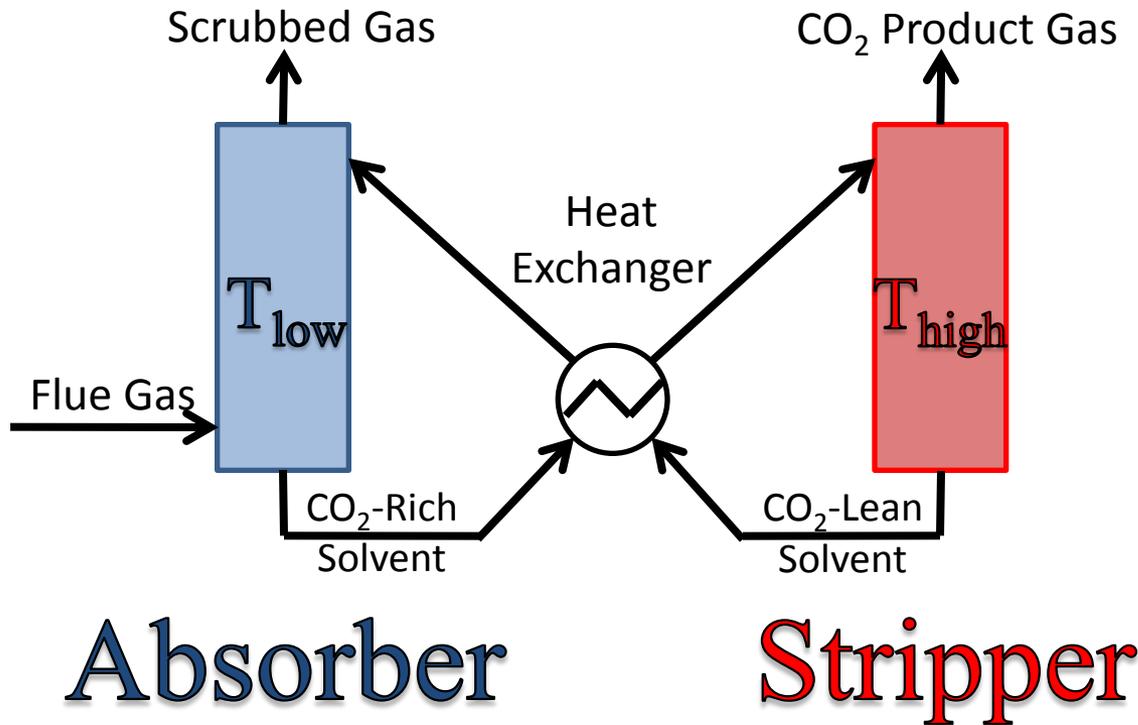
# *Project Participants*

- **Chemical Engineers** and **Chemists** Supported on this Grant
  - ✓ Faculty – **Charles Eckert**, **Charles Liotta**
  - ✓ Postdocs – **Elizabeth Biddinger**, **Manish Talreja**, **Manjusha Verma**
  - ✓ PhD Students – **Olga Dzenis**, **Ryan Hart**, **Gregory Marus**, **Amy Rohan**
  - ✓ Undergraduate – **Melissa Burlager**
- **Other Contributors**
  - ✓ Research Scientist – **Pamela Pollet**
  - ✓ PhD Student – **Kyle Flack**
  - ✓ Undergraduates – **Sean Faltermeier**, **Paul Nielson**

# Scientific Background: Sustainable Reversible Ionic Liquids (RevILs)



# Advantages of RevILs for CO<sub>2</sub> Capture



Heat Energy

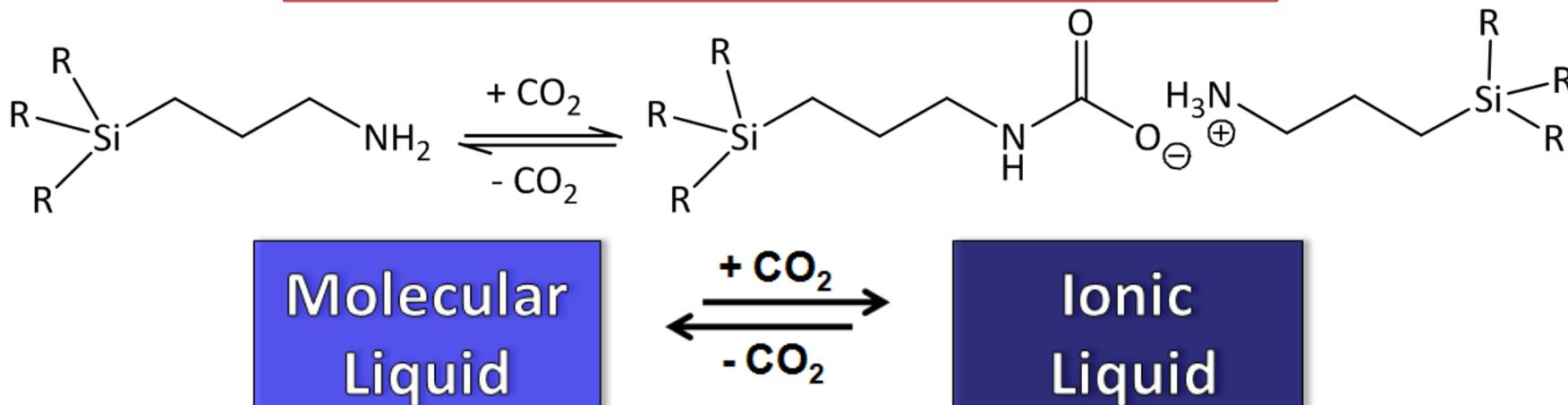
$$Q = mC_p\Delta T + \text{Regeneration}$$

## Cost Savings

1. Minimize solvent and energy needs
2. Optimize  $\Delta T$  and  $\Delta H_{rxn}$
3. Optimize both physisorption and chemisorption

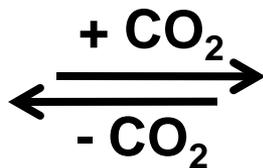
# Utilizing a Dual Capture Mechanism

## Highly Selective Chemical Absorption



## Added Capacity By Physical Absorption

Ionic  
Liquid



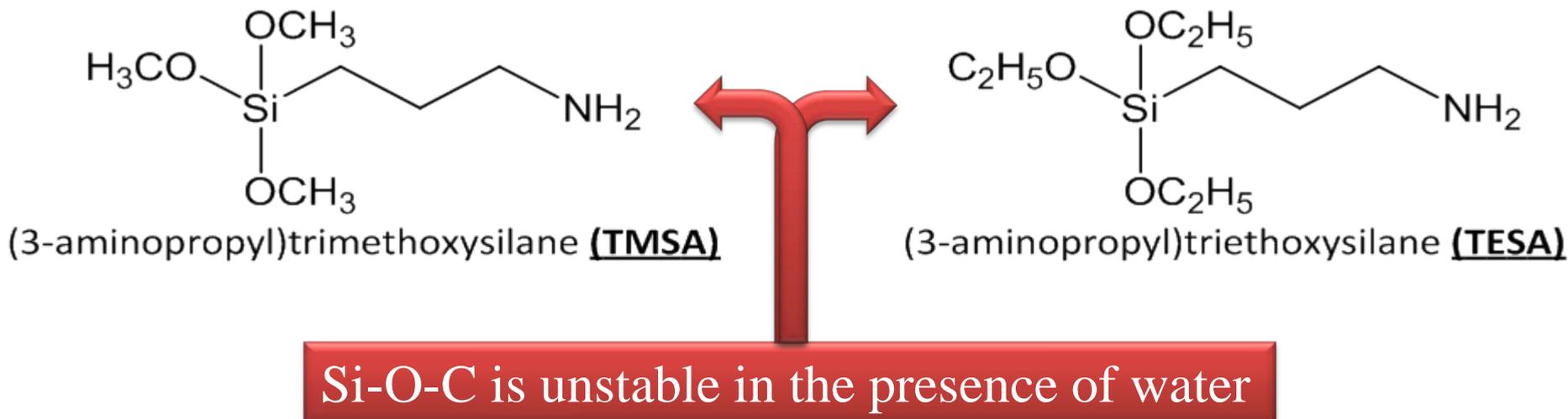
CO<sub>2</sub>  
Swollen  
Ionic Liquid

# *Technical and Economic Challenges*

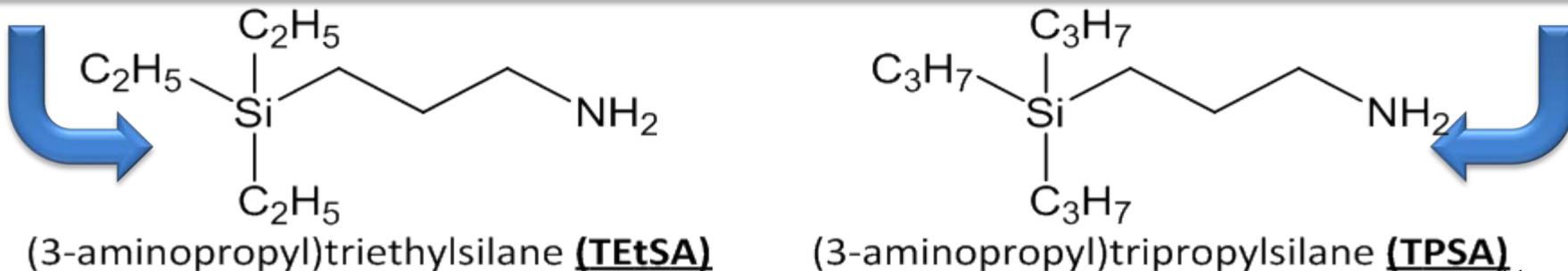
- Optimize Solvent Structure
  - ✓ Capacity – Maximize Both Capacities
  - ✓ Uptake/Release – Optimize  $\Delta T$  and  $\Delta H_{\text{rxn}}$
- Minimize Solvent Cost/Losses
  - ✓ Scaleup for Effective Manufacture
- Eliminate Transport Limitations
  - ✓ Both Mass and Heat

# Progress and Current Status

## First and Second Generation RevILs



Alkyl substituted compounds were synthesized to improve stability



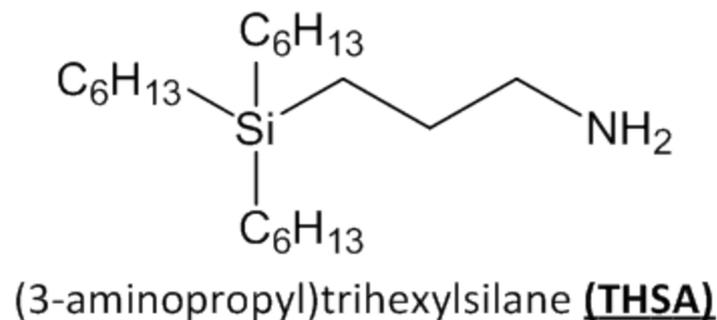
# Third Generation

## Silyl-Amine Reversible Ionic Liquids

- Much Easier Synthesis than Guanidines
- Superior Capacity to Guanidines
- Structure is Easily Modified

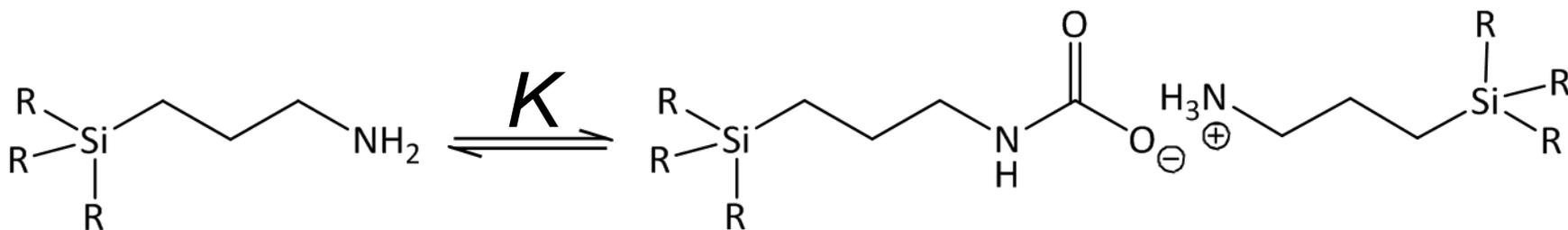
Ionic Liquid	Swelling	Physical Absorption Capacity (mol/kg amine)
TEtSA	16%	12.3
TPSA	31%	17.9

\* Capacities measured at 900 psi and 35 C.  
(Published in Fuel, 2009)





# Developing an Optimal Solvent Thru Structure Property/Relationships



Equilibrium Constant

$$K = \frac{a_{\text{IonicLiquid}}}{a_{\text{Precursor}} a_{\text{CO}_2}}$$

Solution  
Nonideality

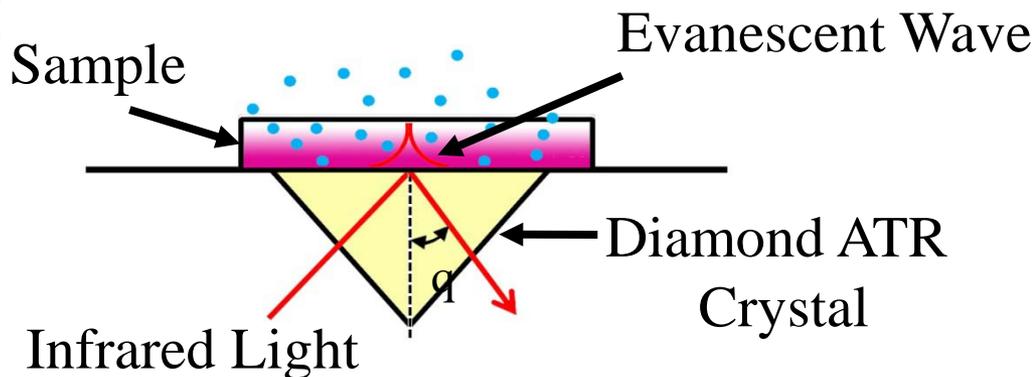
van 't Hoff Plot

Thermodynamic Properties

$$K = \exp\left[\frac{-\Delta G^{abs}}{RT}\right] \quad \frac{d(\Delta G^{abs} / RT)}{dT} = -\frac{\Delta H^{abs}}{RT^2}$$

# Novel Spectroscopic Technique for Measuring $CO_2$ Absorption

- How it works:



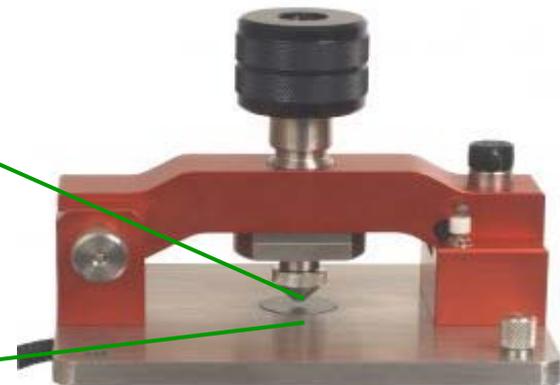
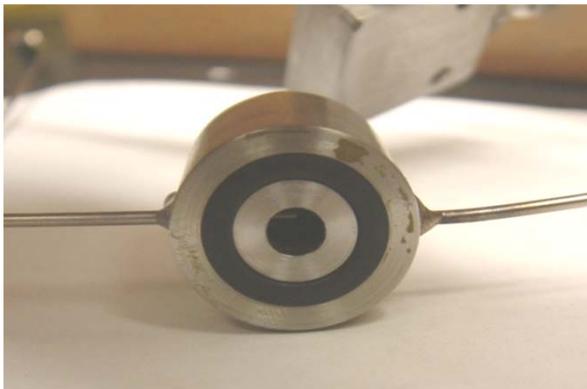
- Application of Beer-Lambert Law:

$$A = \varepsilon \cdot b \cdot c$$

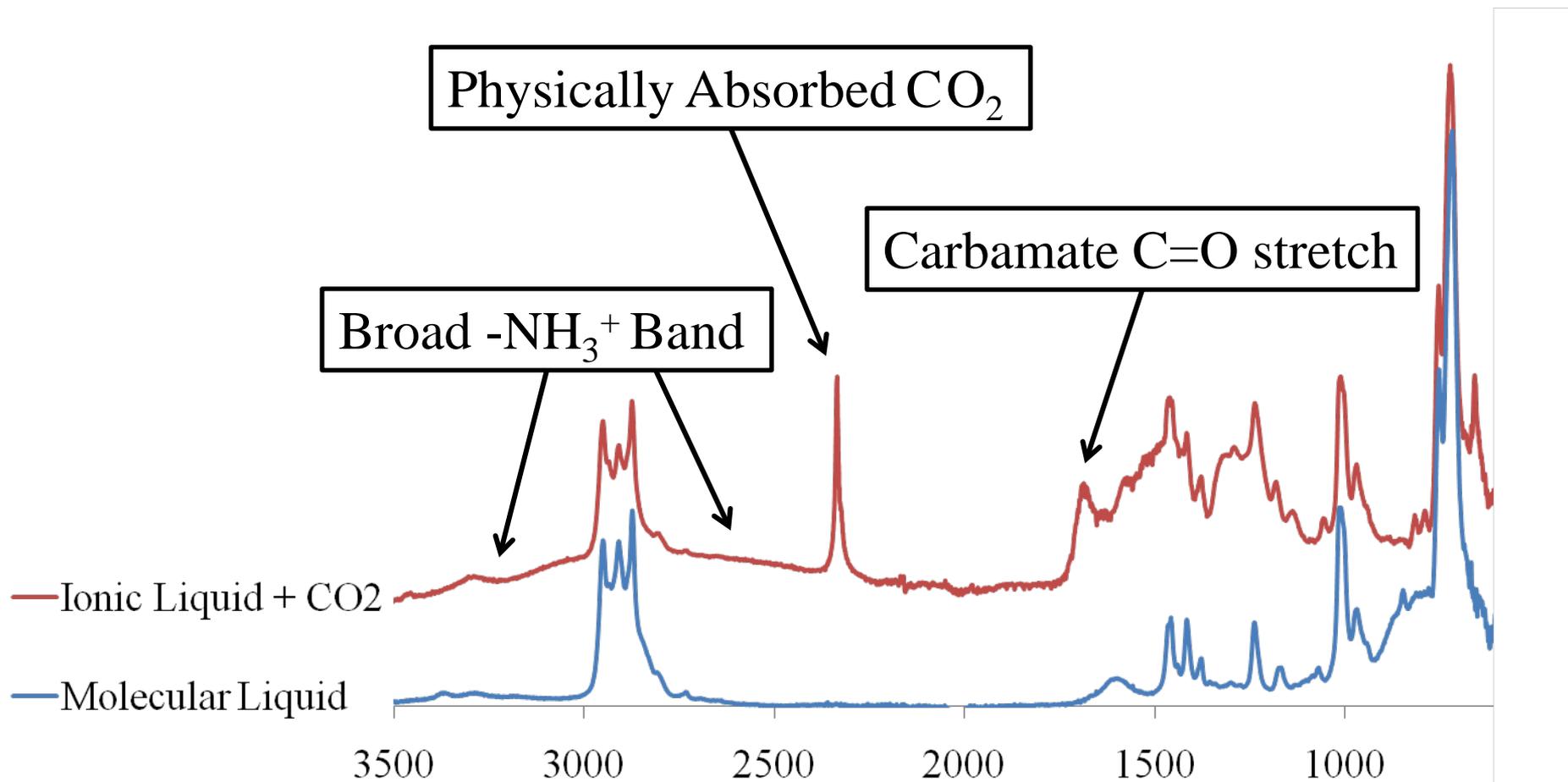
$A$  = absorbance [A.U.]  
 $\varepsilon$  = molar absorptivity [ $L \text{ mol}^{-1} \text{ cm}^{-1}$ ]  
 $b$  = path length [cm]  
 $c$  = concentration [ $\text{mol L}^{-1}$ ]

# *Custom Design Sample Cell for ATR*

- Design Collaboration with *Prof. Sergei Kazarian*
  - ✓ Ease of Assembly, Operation, and Maintenance
  - ✓ Low Volume, High Pressure
  - ✓ Custom Built to Our Specifications
  - ✓ Rapid and Accurate Measurements
  - ✓ Measures both Chemical and Physical Absorption



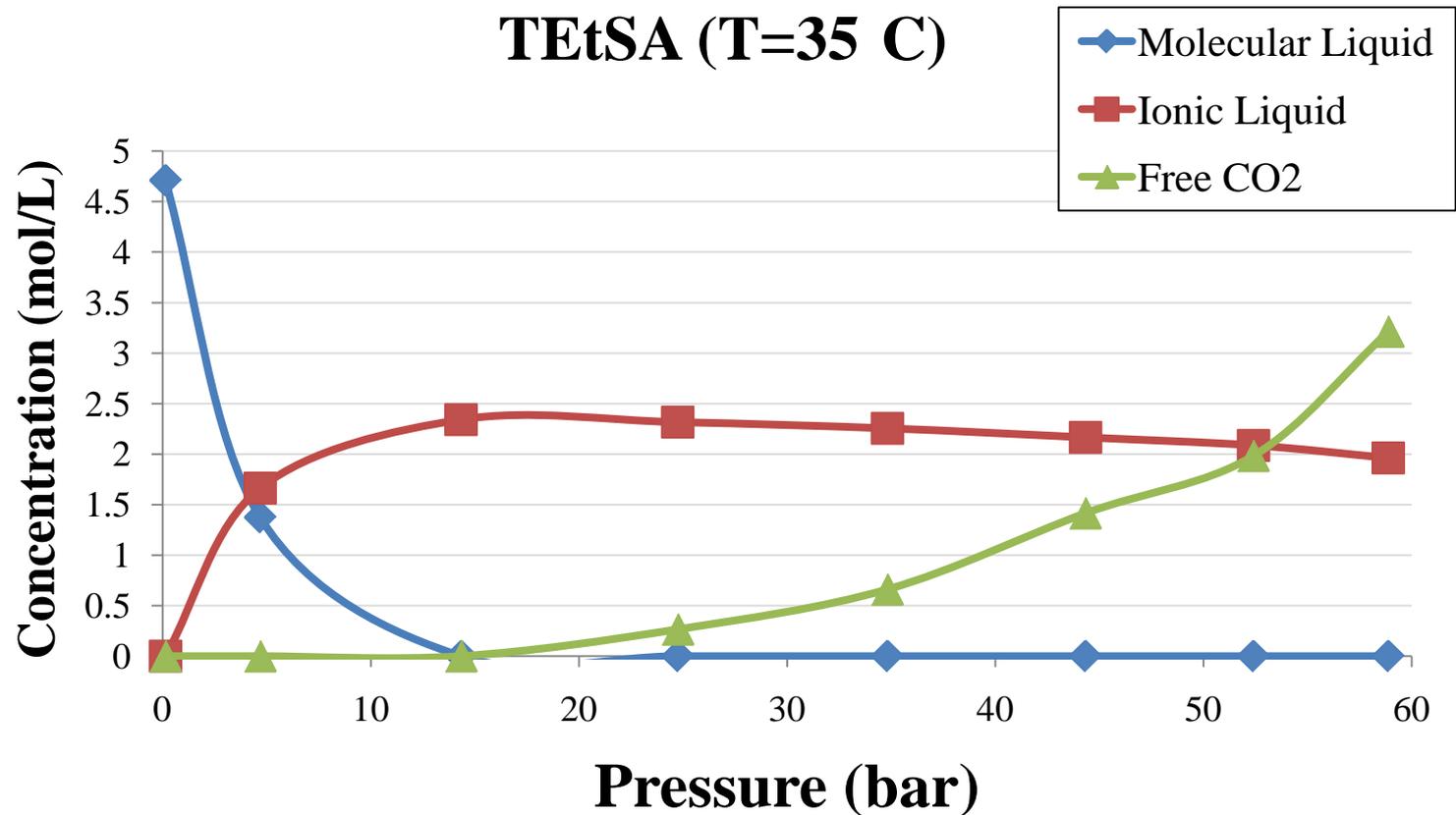
# *Infrared Spectra of TEtSA Ionic Liquid - Formation and Physical Absorption -*



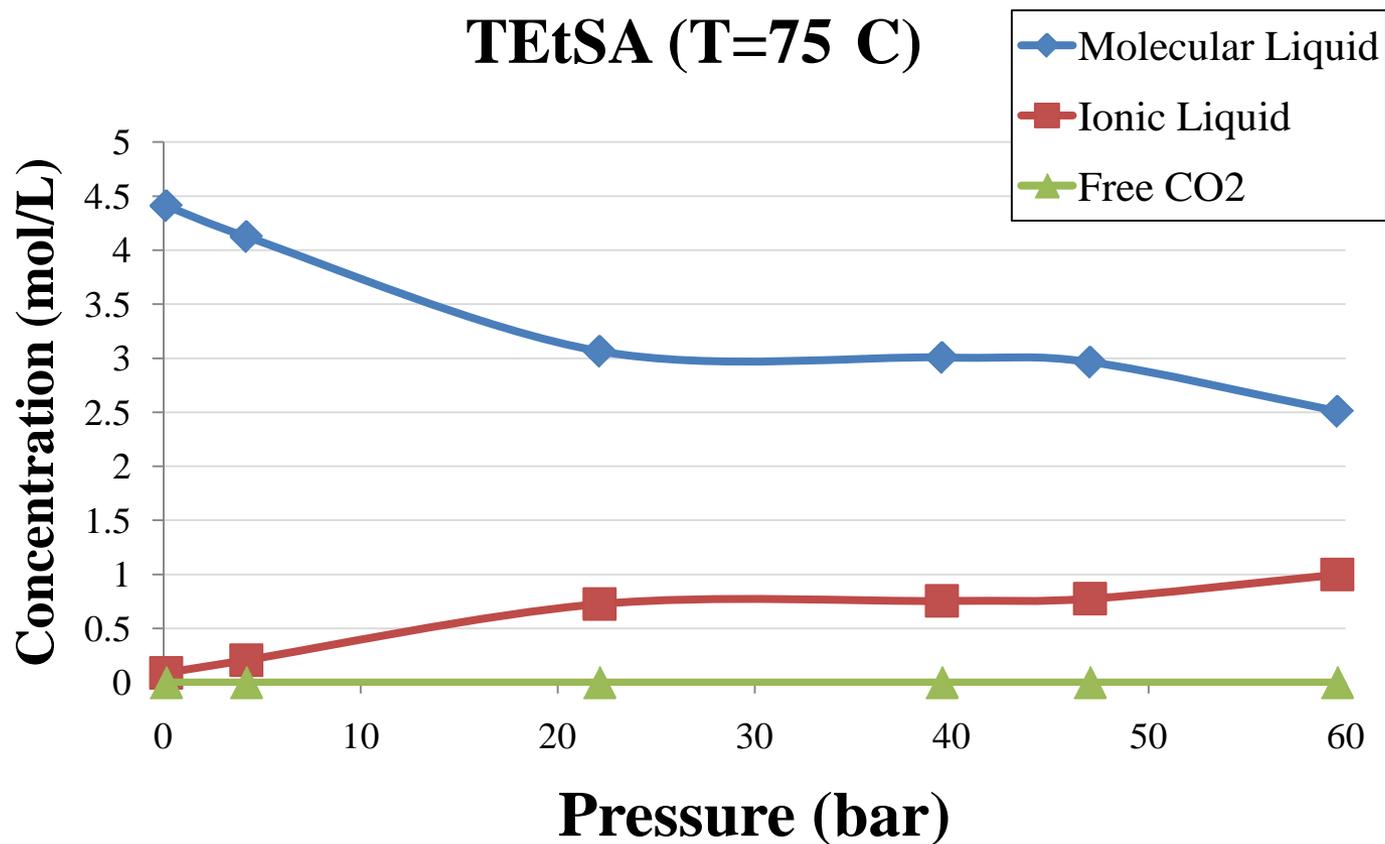
# *Project Methodology*

- Synthesis and Characterization of Novel Compounds
  - ✓ 1-Comp. Silyl Guanidine-Based ILs
  - ✓ 1-Comp. Silyl Amine-Based ILs
- Thermodynamics of IL Formation with CO<sub>2</sub>
- Rates of Uptake/Release
- Optimize Solvent Structure for CO<sub>2</sub> Capture
- Process Design & Economic Analysis

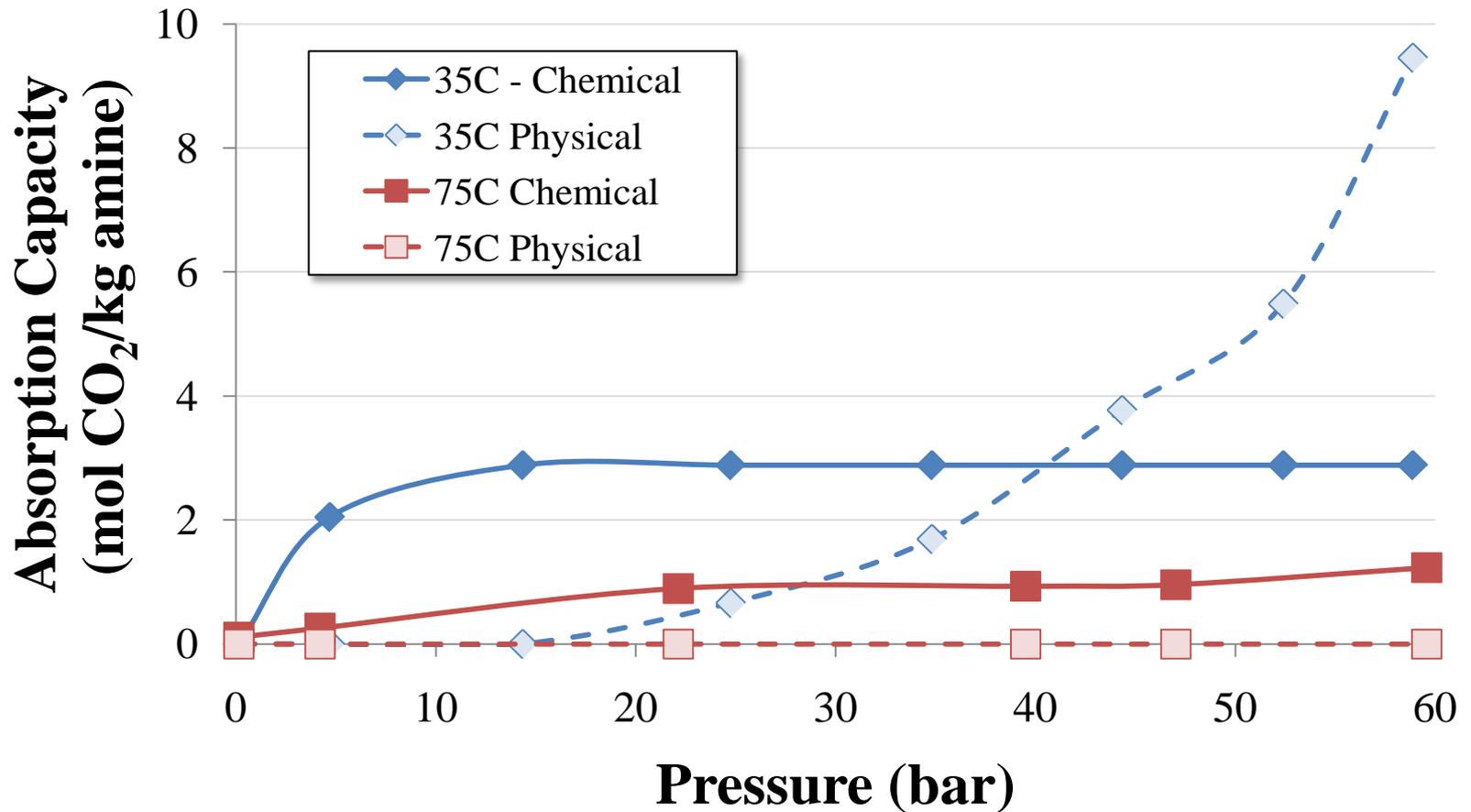
# *Ionic Liquid Formation Favored at Low Temperatures*



# *At 75°C, Much Different Equilibrium*



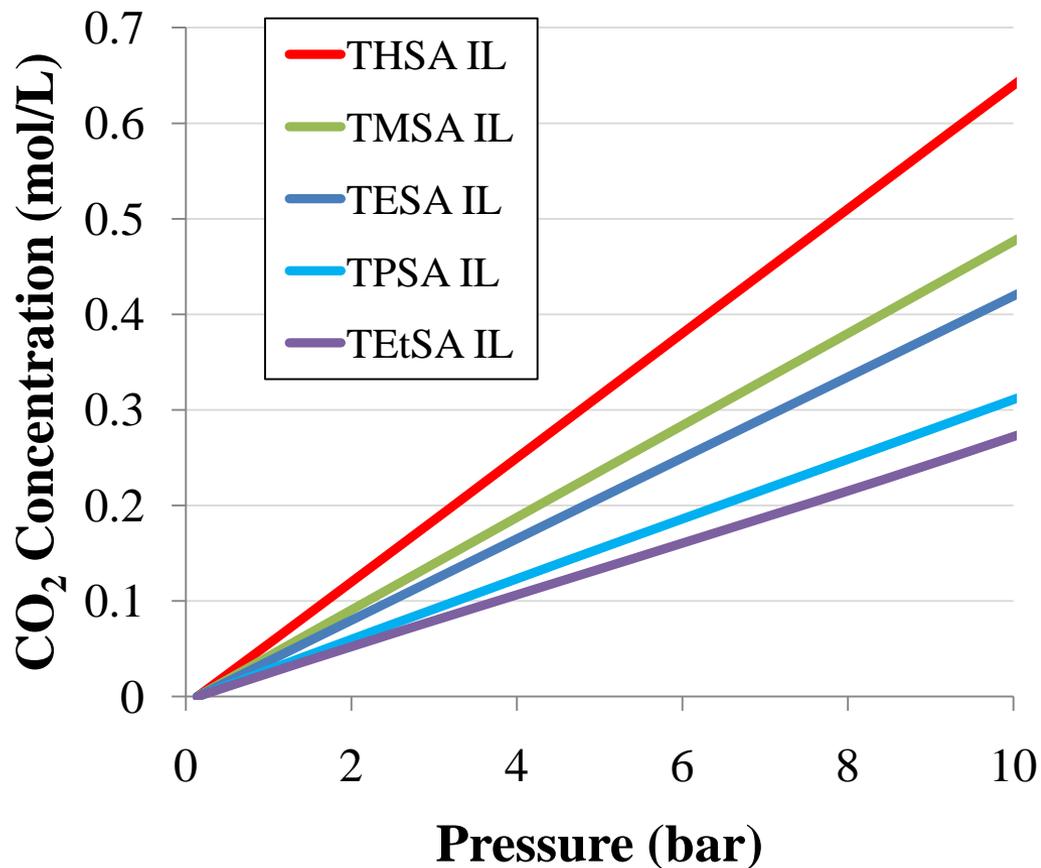
# *ATR FT-IR Reveals Capacities and Equilibrium*



\* Physical Absorption Detection Limit = 0.5 mol/L

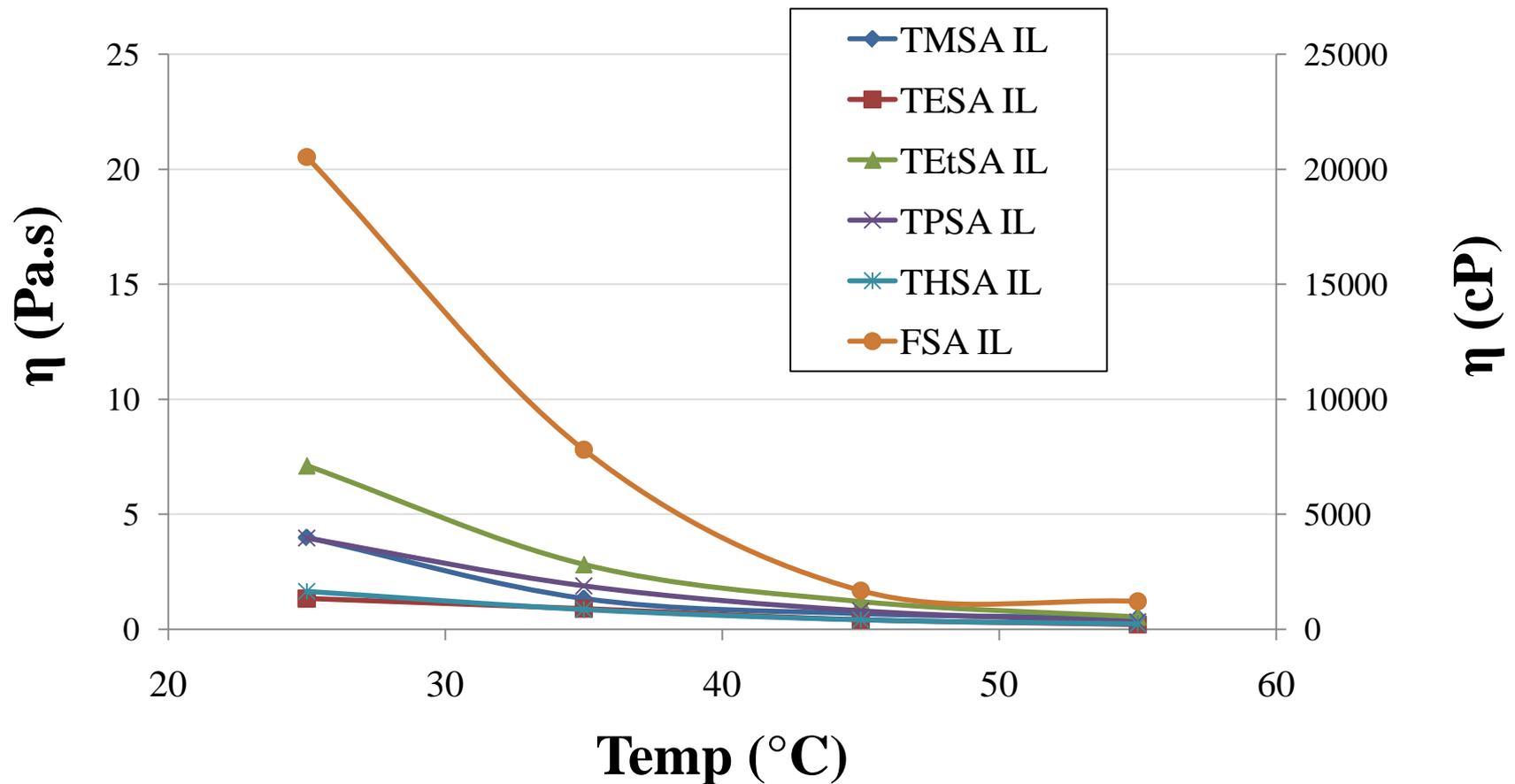
# Enhancement of Physical Absorption in Ionic Liquids ( $T=35^{\circ}\text{C}$ )

**Double the capacity for alkyl amines!**



Compound	Void Volume (L/mol)	Henry's Law Constant (L·bar/mol)
TMSA	0.357	20.8
TESA	0.466	23.8
TEtSA	0.423	37.0
TPSA	0.520	32.3
THSA	0.822	15.6

# *Project Challenge: Viscosity of Ionic Liquids*



# *Final Process Optimization*

- Solvent with Optimum Balance of Properties
  - ✓ Synthesize and Characterize
  - ✓ Use in Process Design
  - ✓ Determine Best by Energy, Economics
- Optimum Solvent
  - ✓ Demonstrate on Lab Scale
  - ✓ Design Pilot Scale Process
  - ✓ Develop Scalable Process for Synthesis
- **Bottom Line:** Superior Process for CO<sub>2</sub> Capture from Coal-Fired Power Plants

## *Economic Evaluation – Path Forward*

- Setup complete process diagram
- Important variables
  - ✓ Input compounds/models
  - ✓ Setup general reaction in absorber
- Use to calculate targets
- Evaluate compounds synthesized in lab
  - ✓ Information communicated through website,  
<http://www.chbe.gatech.edu/eckert/doeindex.html>

# *Support From DOE Has Generated...*

- 3 Publications
- Presentations:
  - ✓ 8 Invited (1 Student Authored)
  - ✓ 8 Conferences (5 Student Authored)
- 1 Invention Disclosure
- 7 Collaborations:
  - ✓ 4 Academic
  - ✓ 3 Industrial
- 2 Students Graduated
  - ✓ Vittoria Blasucci, PhD ChBE (Exxon)
  - ✓ Hillary Huttenhower, PhD Chem (Pratt and Whitney)
- To Graduate this Term
  - ✓ Ryan Hart, PhD ChBE
  - ✓ Ali Fadhel, PhD ChBE
  - ✓ Melissa Burlager, BS ChBE

# *Project Objectives and Timing: Milestones*

<b>Milestone Title</b>	<b>Finish</b>	<b>Verification Method</b>
A Complete Project Management Plan	9/30/08	PMP approved by DOE COR
B 1-Comp. Silyl Amine-Based ILs	06/30/10	Successful Synthesis and Characterization
C 1-Comp. Silyl Guanidine-Based ILs	02/28/11	Successful Synthesis and Characterization
D Thermo & Rates of IL Formation	6/30/11	Successful Measurements
E Optimize CO <sub>2</sub> Capture Solvent Structure	10/31/11	Optimal Solvent Identified
F Process Design and Economic Analysis	10/31/11	Design and Scaleup Completed
G Write Final Report	12/31/11	Final Report Submitted

# *Future Testing & Development*

- This Project
  - ✓ Develop and Test for Optimum RevIL
  - ✓ Design and Economic Analysis
- Next Project
  - ✓ IL Scaleup for Economic Manufacture
  - ✓ Address Rates, Transport Issues
- Scale-Up Potential
  - ✓ Already Working with Industrial Partner  
ConocoPhillips