

# **Syngas & Hydrogen Combustion Reduced Order Reactions: Flame speeds, Mechanism validation, Reduced Mechanism**

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# Research goal: Gas Turbine Engines Using Hydrogen Syngas

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- Validated, reduced order kinetic mechanism
- Understanding kinetics at engine conditions

- High pressure ( $\sim 10\text{-}30$  atm)
- Lean/rich conditions for low  $\text{NO}_x$  (3ppm)
- Preheated temperature ( $\sim 650\text{K}$ )
- High levels of diluents ( $\text{N}_2$ ,  $\text{H}_2\text{O}$ , or  $\text{CO}_2$ )



# Research Tasks

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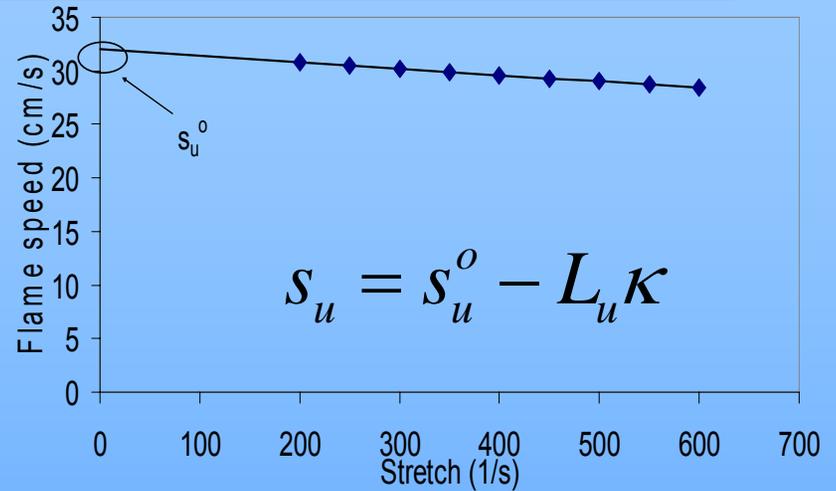
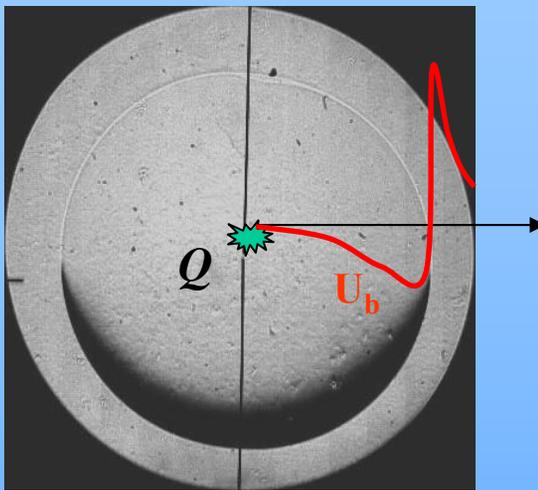
- **Methodology to measure flame speeds at high pressure**
- **Flame speed measurements and mechanism validation**
- **Dynamic multiscale (AMS) kinetic reduction algorithm**



# 1. Methodology to measure rigorous flame speeds



# Flame speed measurement using spherical flames



**Assumption: Burned gas velocity is zero!**

$$S_u = V_f \rho_b / \rho_u \quad (1)$$

**What if the burned gas velocity is not zero?**

Flame speed error will be:

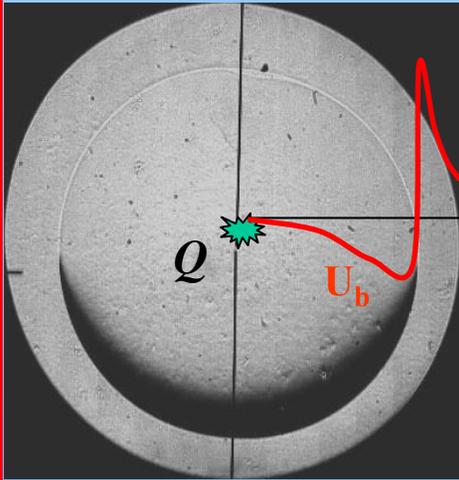
$$\varepsilon \equiv \frac{S_u - \hat{S}_u}{\hat{S}_u} = \frac{u_b}{V_f} \quad (2)$$

**What causes non-zero burned gas velocity?**

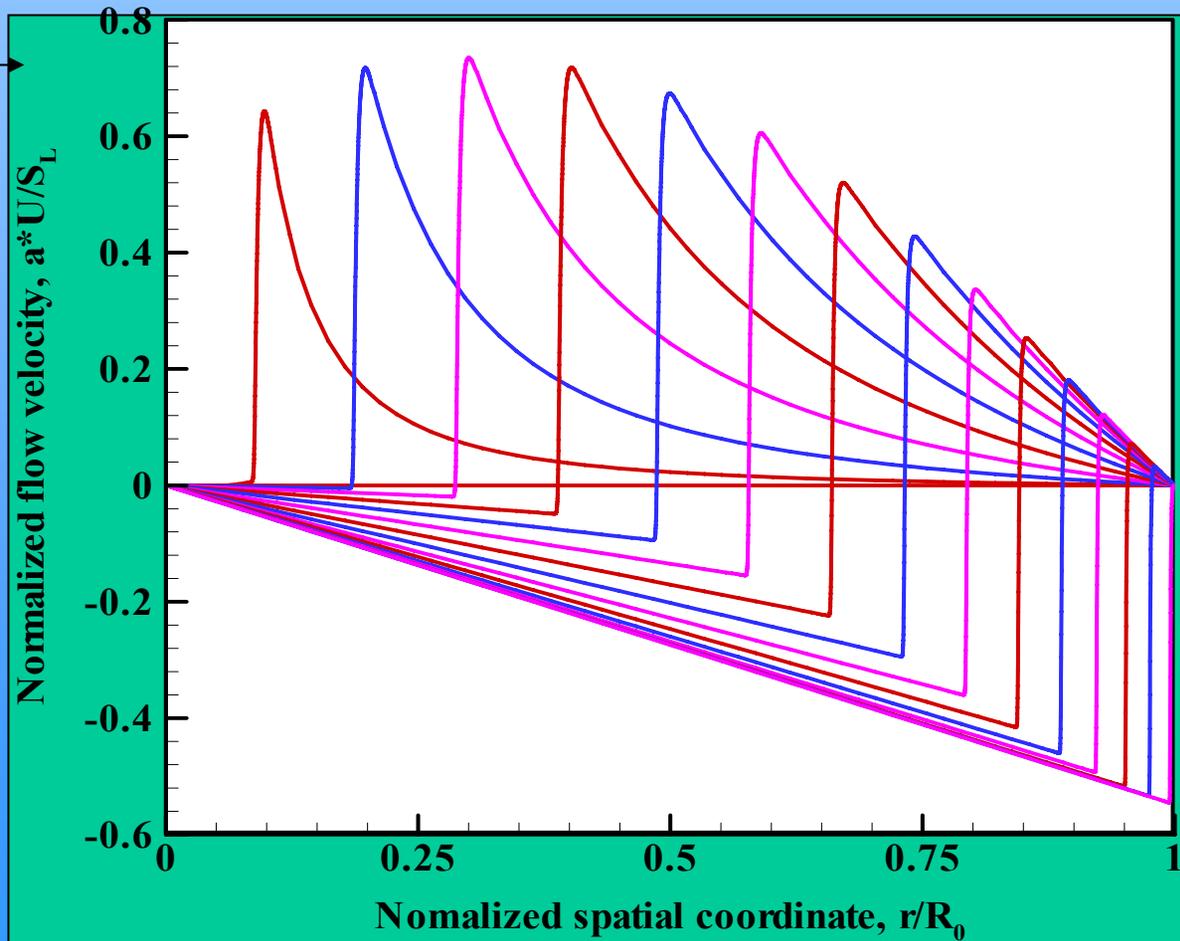
Compression, non-symmetric flow, radiation...



# Flame speed measurement using a spherical bomb: *Compression induced burned gas velocity*



## Velocity distribution $V(r,t)$

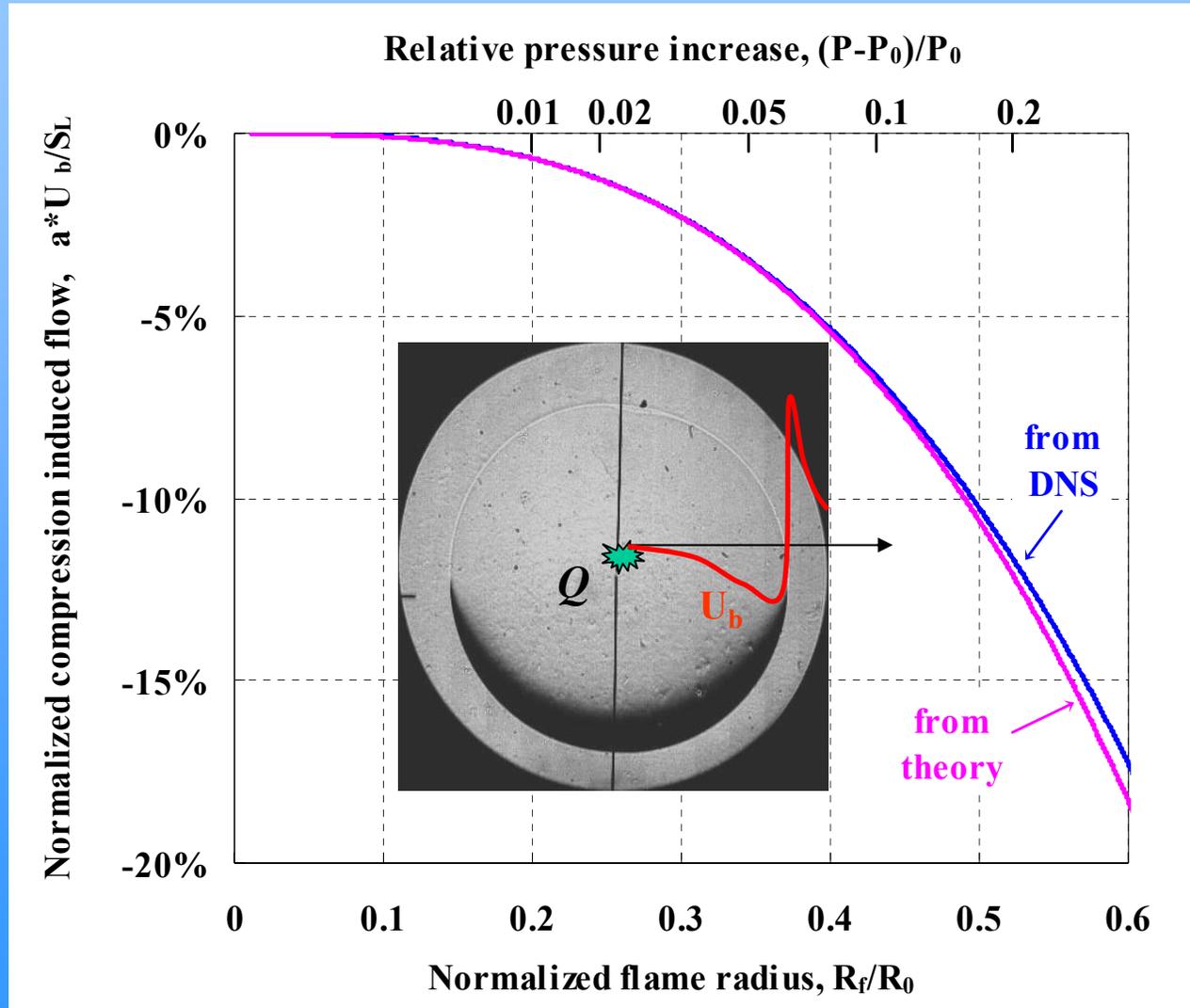


Chen & Ju 2007

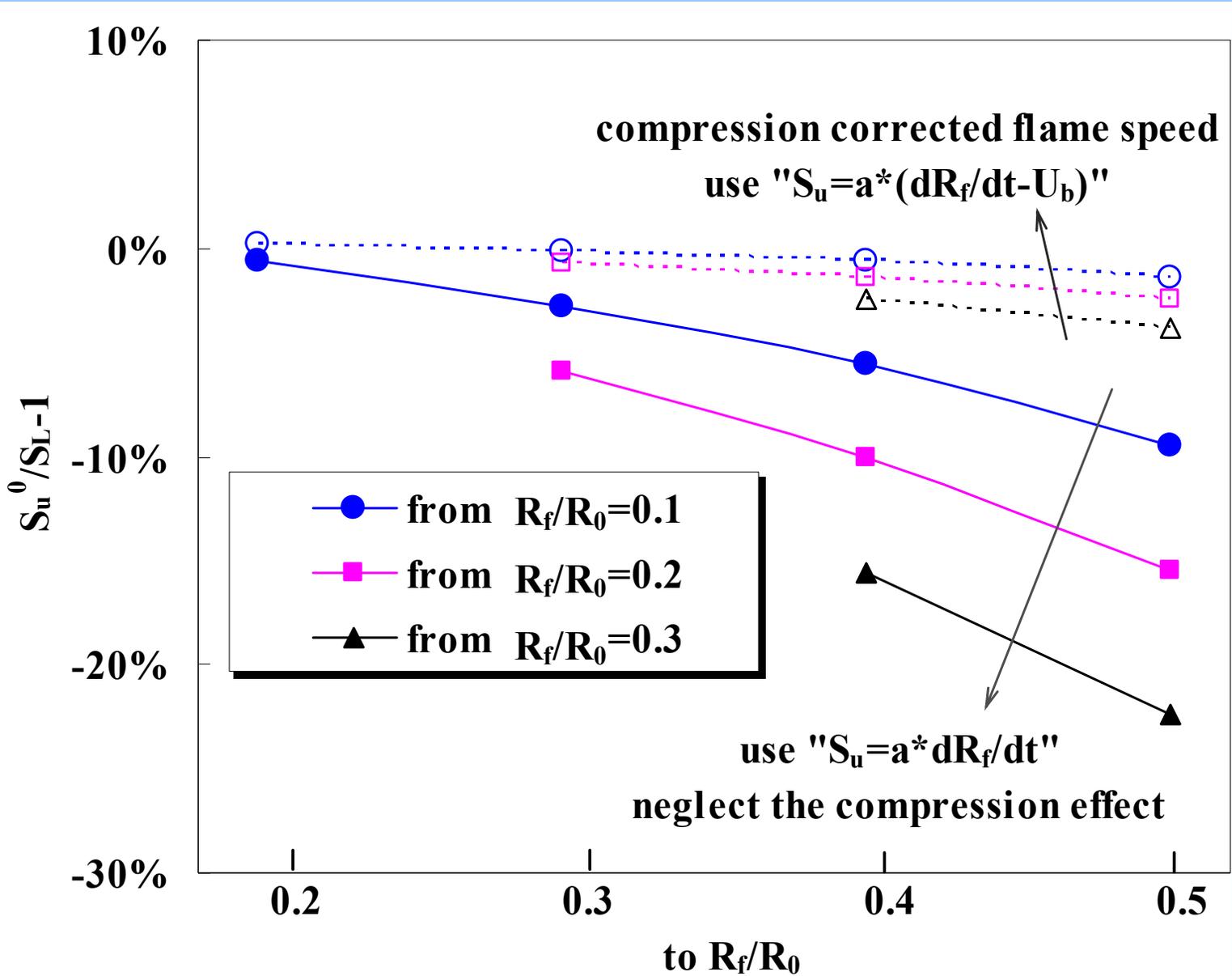


Constant pressure method: *Compression induced burned gas velocity*

Theoretical estimation:



# Constant Pressure Method: *Compression Corrected Flame Speed (CCFS)*



# What if a cylindrical chamber is used?

Princeton University

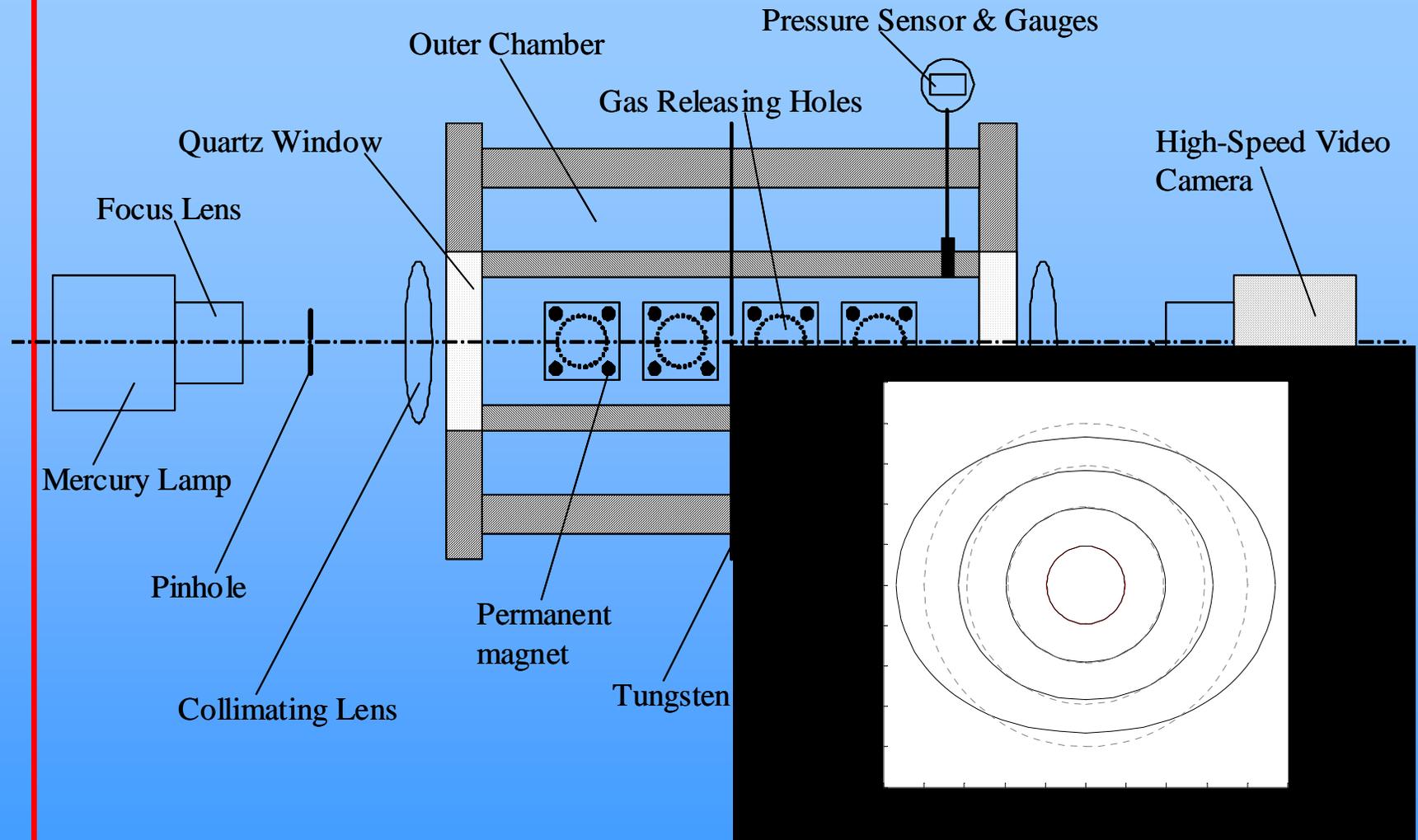


Princeton 8.3 cm dia by 13 cm length (Law),  
10 cm dia by 15 cm length (Ju)

Other groups too!



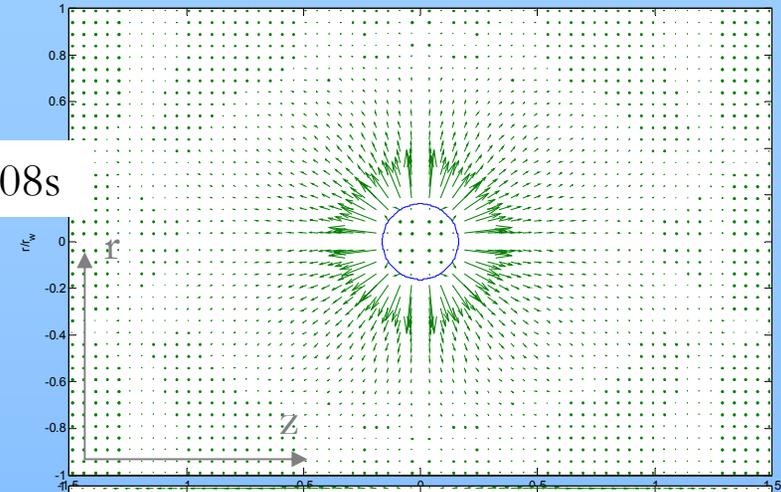
# What if a cylindrical chamber is used?



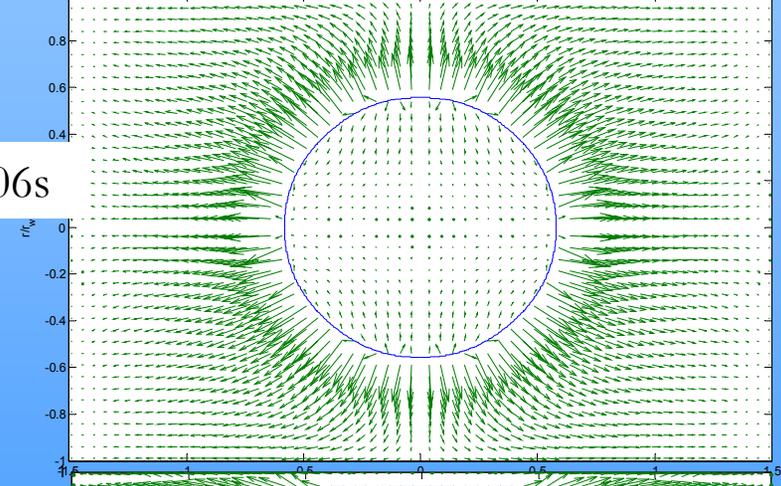
*Non-symmetrical flow induced burned gas velocity!*



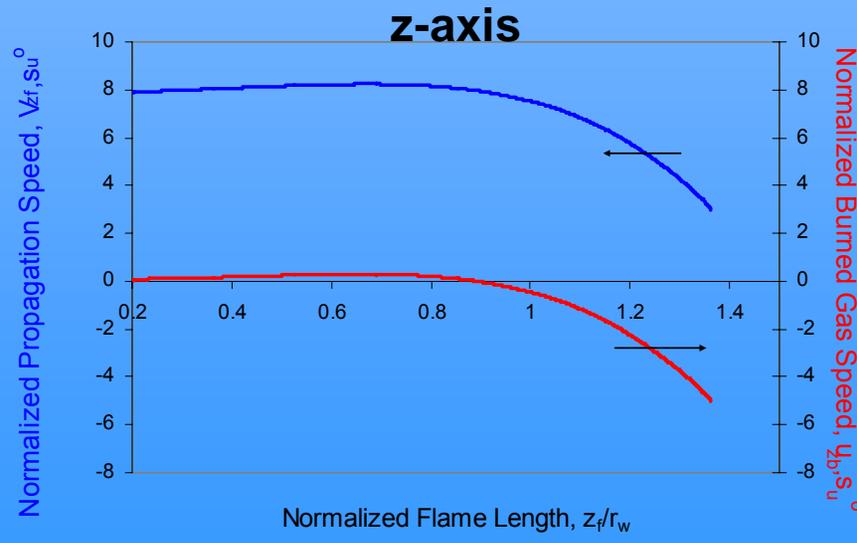
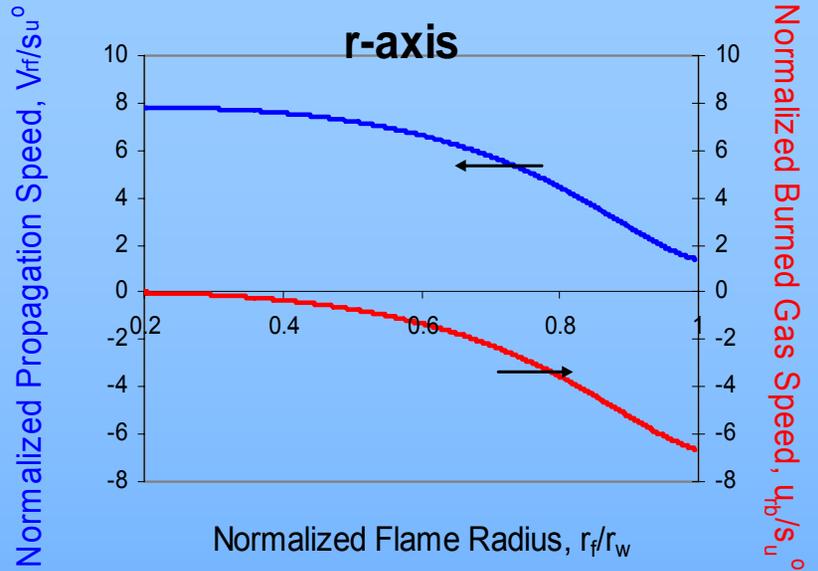
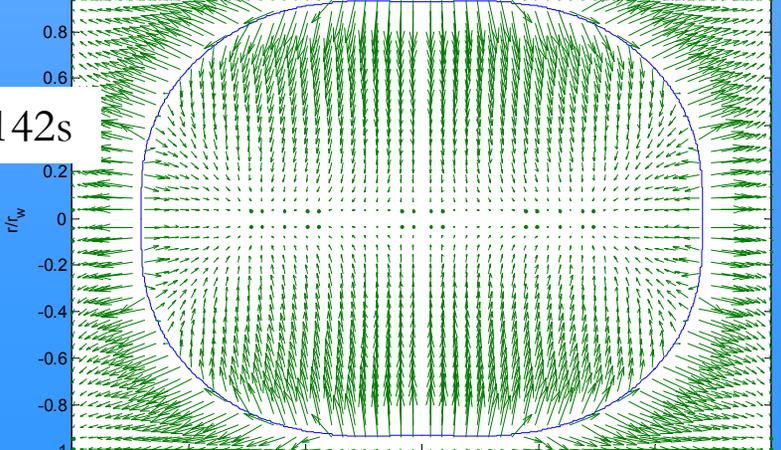
t=0.008s



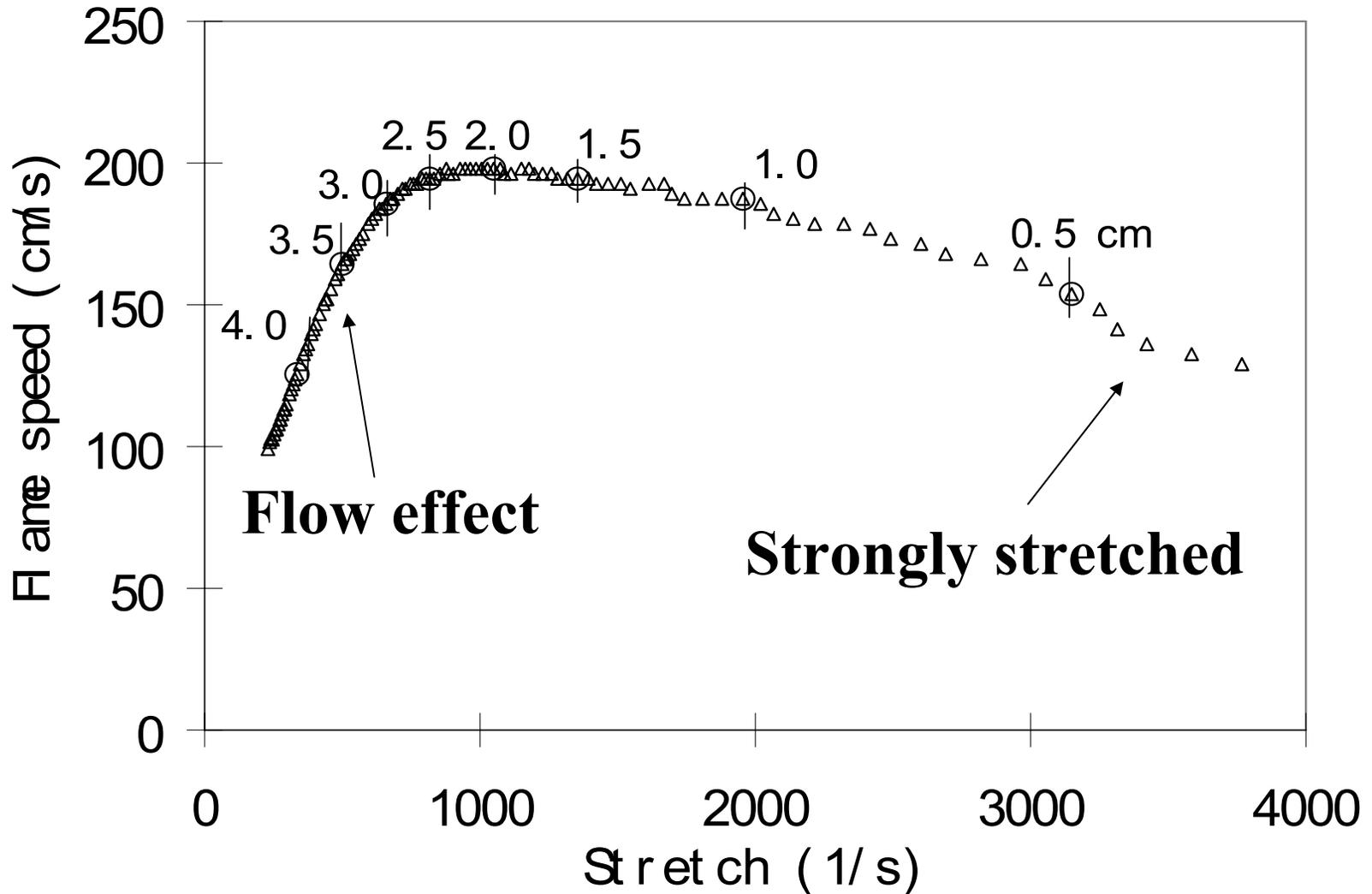
t=0.06s



t=0.142s



# Flame speed history in a cylindrical chamber



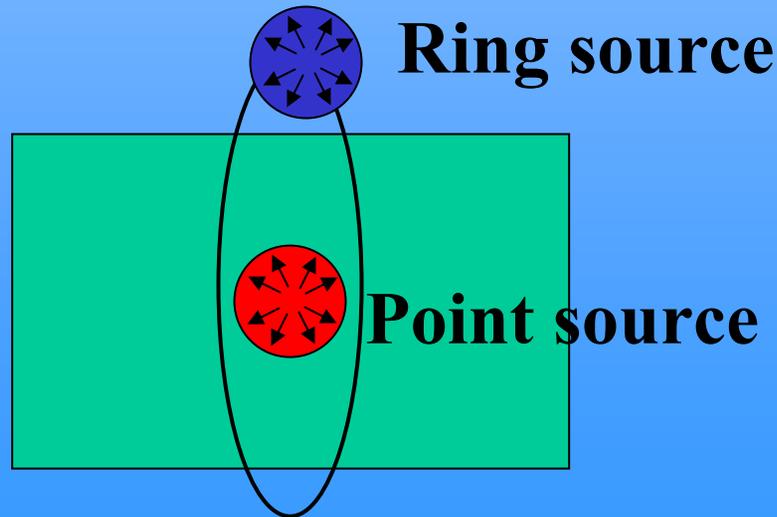
**Difficulty in linear extrapolation!**



# How to improve the measurements

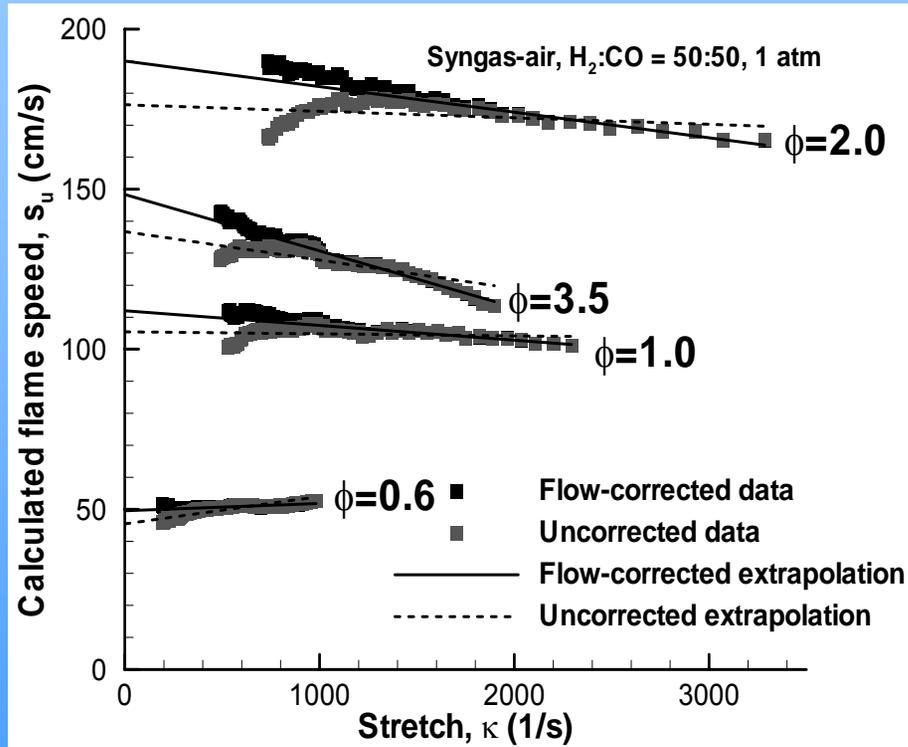
**Potential flow:**

$$\phi = \frac{m(t)}{4\pi \cdot r} + \int_0^{2\pi} \frac{q(t)}{\left\{ [x - \eta \cdot \cos(\gamma)]^2 + [y - \eta \cdot \sin(\gamma)]^2 + z^2 \right\}^{1/2}} \cdot d\gamma$$



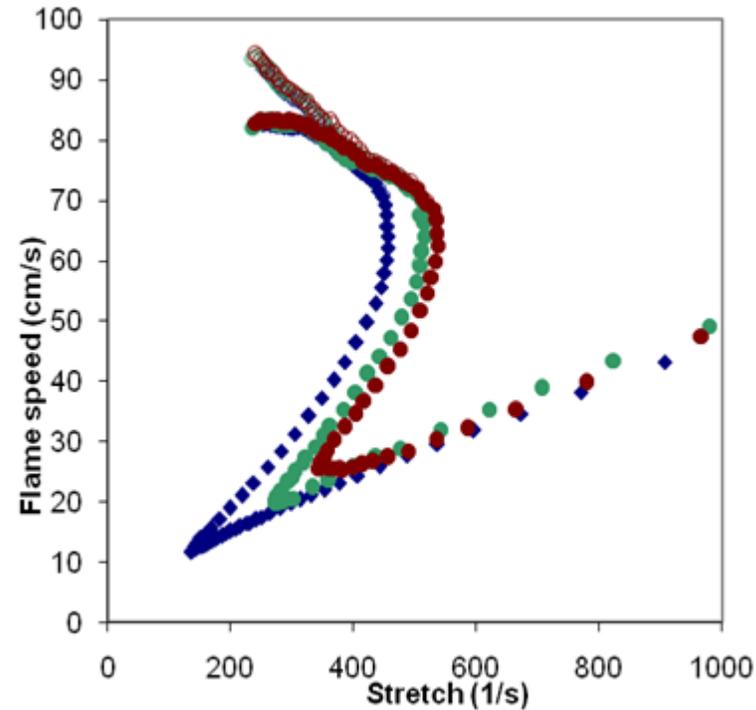
# Flow correction of flame speeds

## Syngas-air



Improves accuracy and extends range of flame radii that can be used for extrapolation

## Rich hydrogen-air



Allows for flame speed determination for flames with long ignition transients

Burke, Chen, Ju, Dryer, submitted for publication

Chen, Burke, Ju,  
Proc. Comb. Inst. (2009)

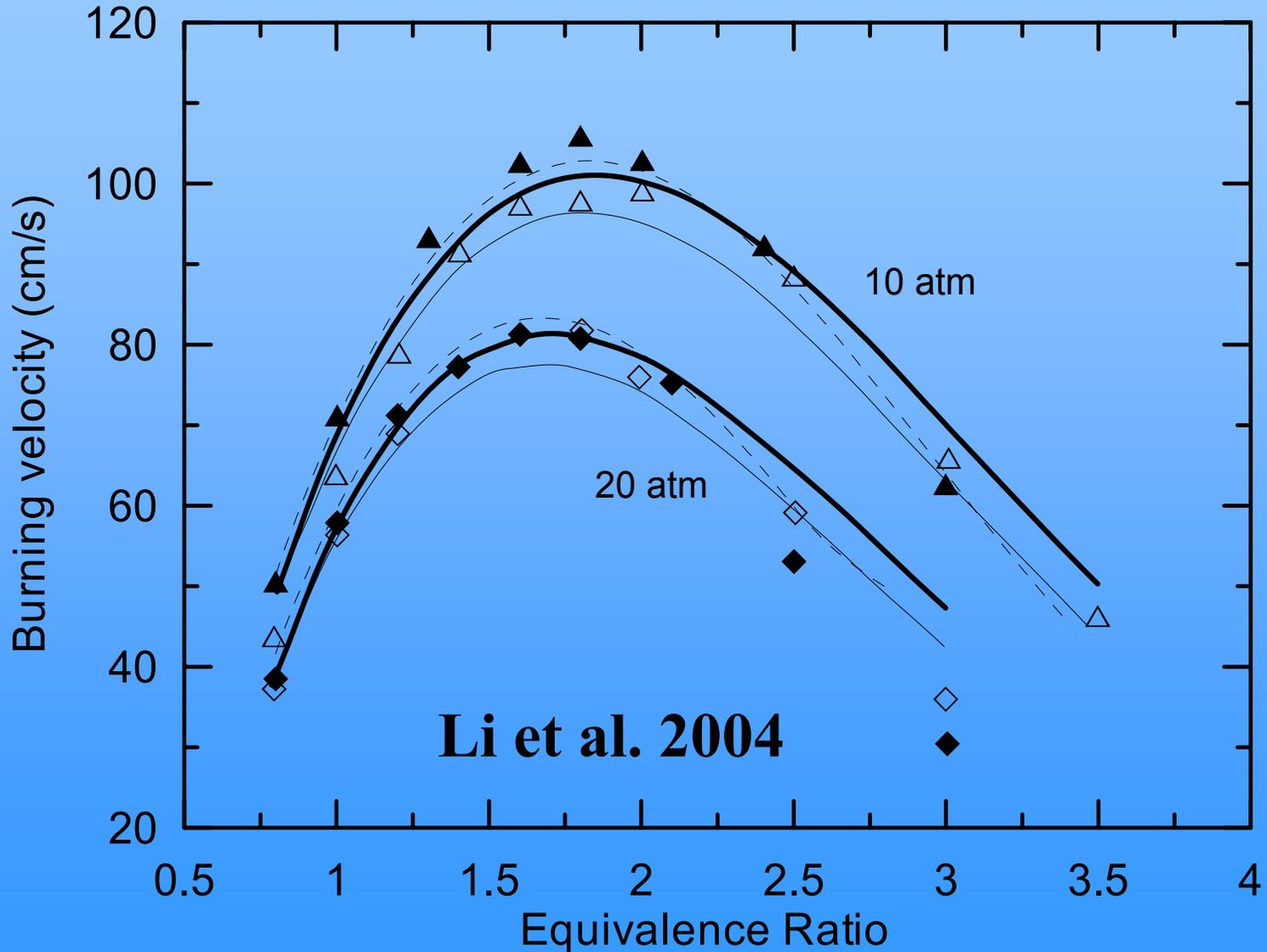


## 2. Flame speed measurements & kinetic mechanism



# Experimental data: Syngas flame speed at 10, 20 atm

H<sub>2</sub>-CO = 25:75 syngas mixture in O<sub>2</sub>+7He



Li et al. 2004

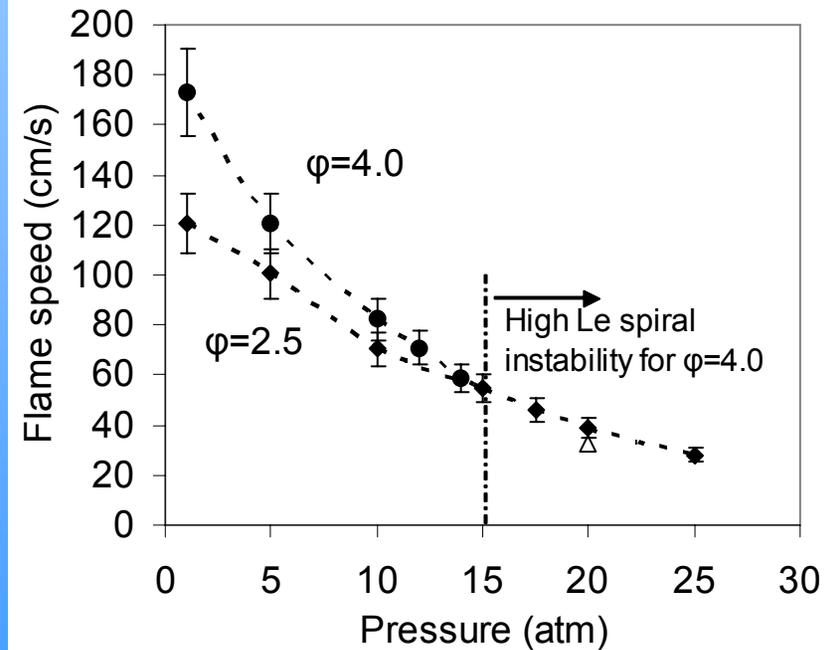
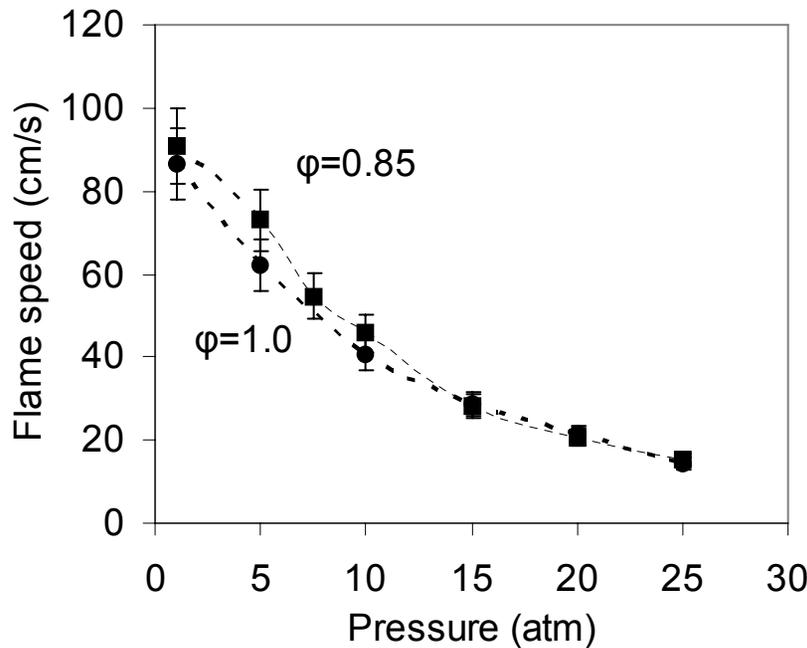
Discrepancy in rich conditions



# Experimental Data (hydrogen-air): Flame speed vs. Pressure

Lean  $\text{H}_2/\text{O}_2/\text{He}$  of Flame Temp=1600K

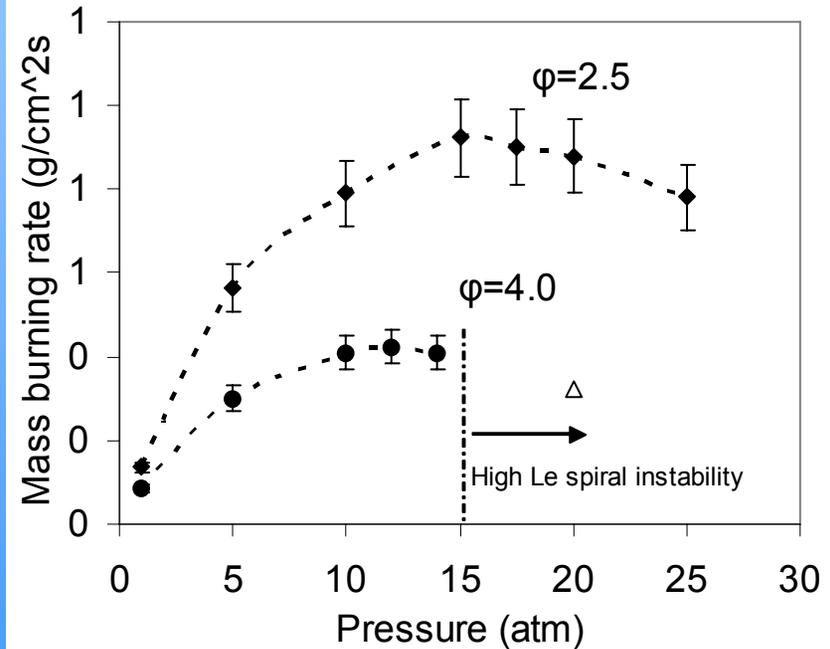
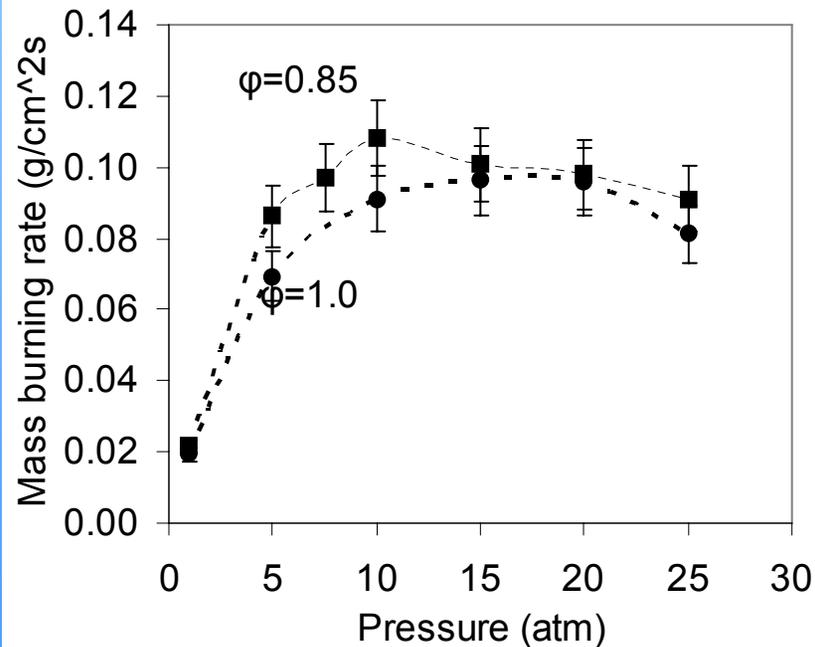
Rich  $\text{H}_2/\text{O}_2/\text{Ar}$  or  $\text{N}_2$  of Flame Temp=1600K



- Flame speed decreases uniformly with pressure
- Flame speed becomes insensitive to mixture composition, but only to temperature at high Pressure

# Experimental data: Mass Burning Rate vs. Pressure

Lean  $H_2/O_2/He$  of Flame Temp=1600K    Rich  $H_2/O_2/Ar$  or  $N_2$  of Flame Temp=1600K



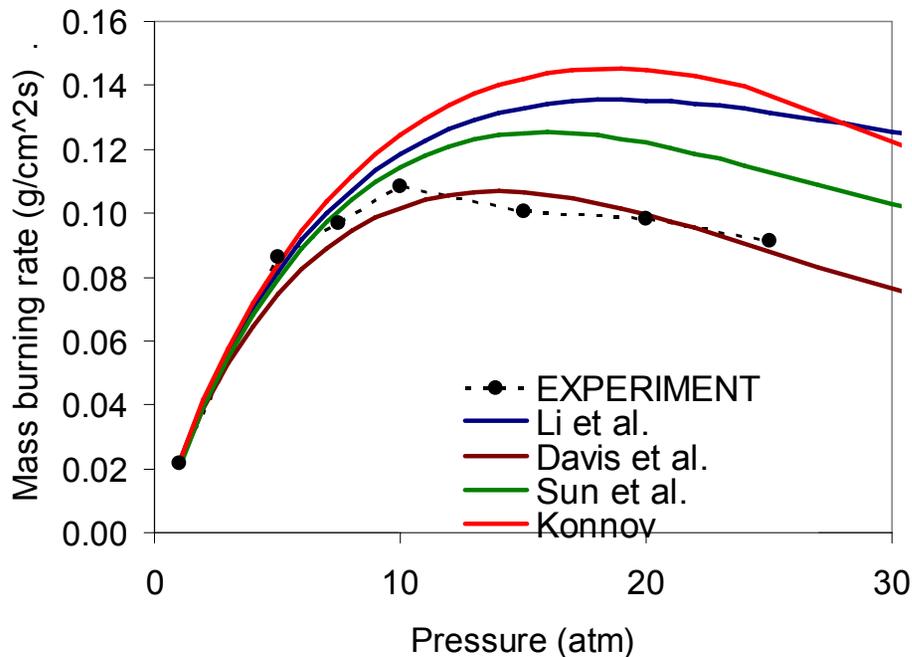
- Mass burning rate increases with pressure until 15 atm, then decreases with pressure



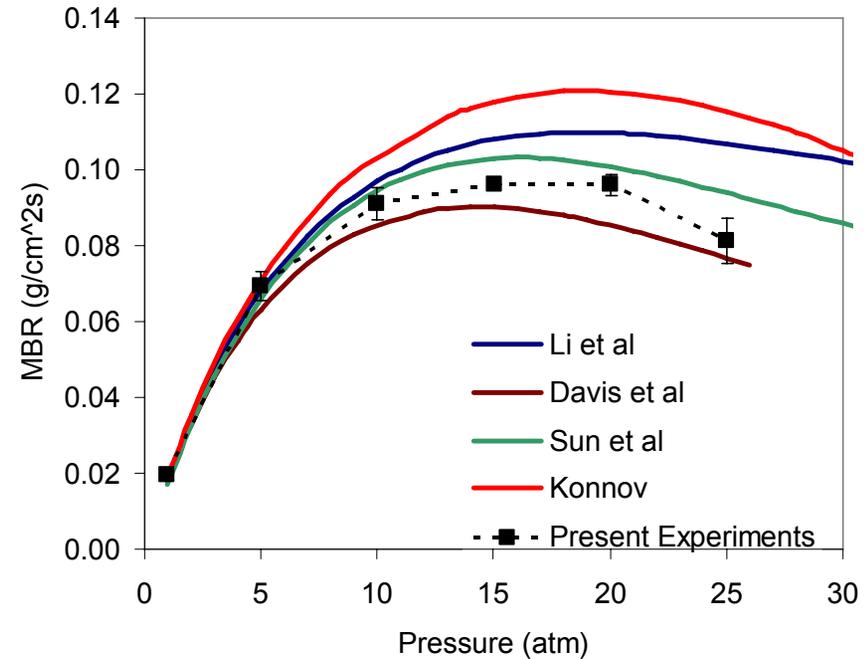
# Validation of kinetic mechanism

## Lean mixtures at high pressures

H2 in O2+11.5He of equivalence ratio 0.85



H2/O2/He, Phi=1.0, He=82.3%, Tf=1600K

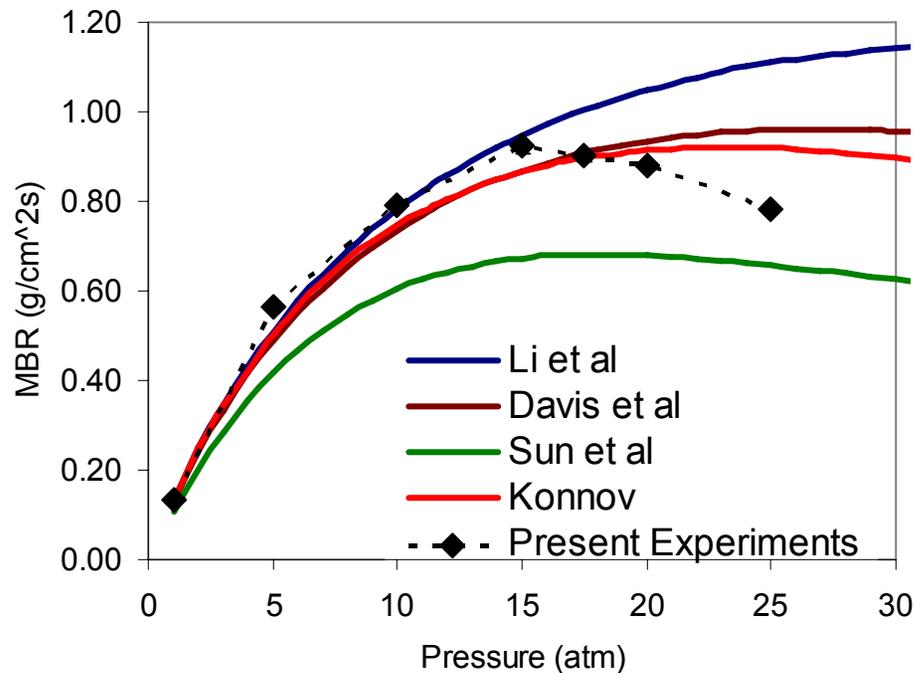


- Mechanism of Davis et al. outperforms the other models
- Other models disagree by up to ~40%

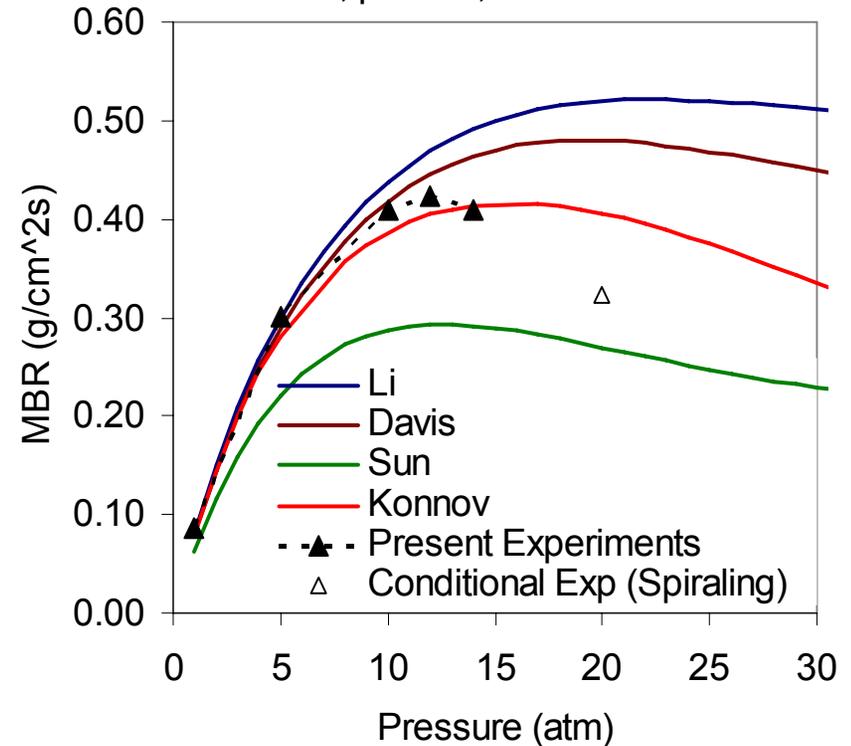
# Validation of kinetic mechanism

## Rich mixtures at high pressures

H<sub>2</sub>/O<sub>2</sub>/Ar,  $\phi=2.5$ , Ar=61.3%, T<sub>f</sub>=1600K



H<sub>2</sub>-air,  $\phi=4.0$ , T<sub>f</sub>=1560K



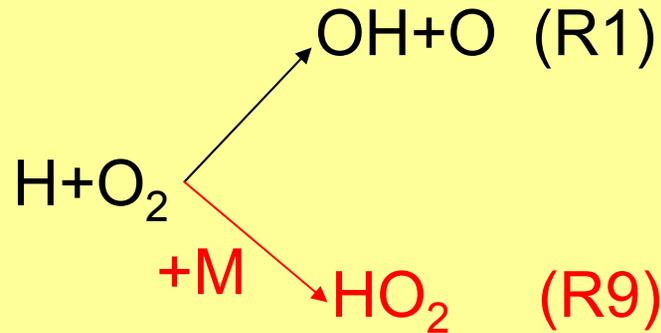
P

- No model accurately predicts trends above 15 atm
- Differences among models reach about a factor of 2

# What happens kinetically when the pressure increases?

- Three-body reactions favored

– e.g.



\*chain-branching

\*favored at lower pressures and higher temperatures

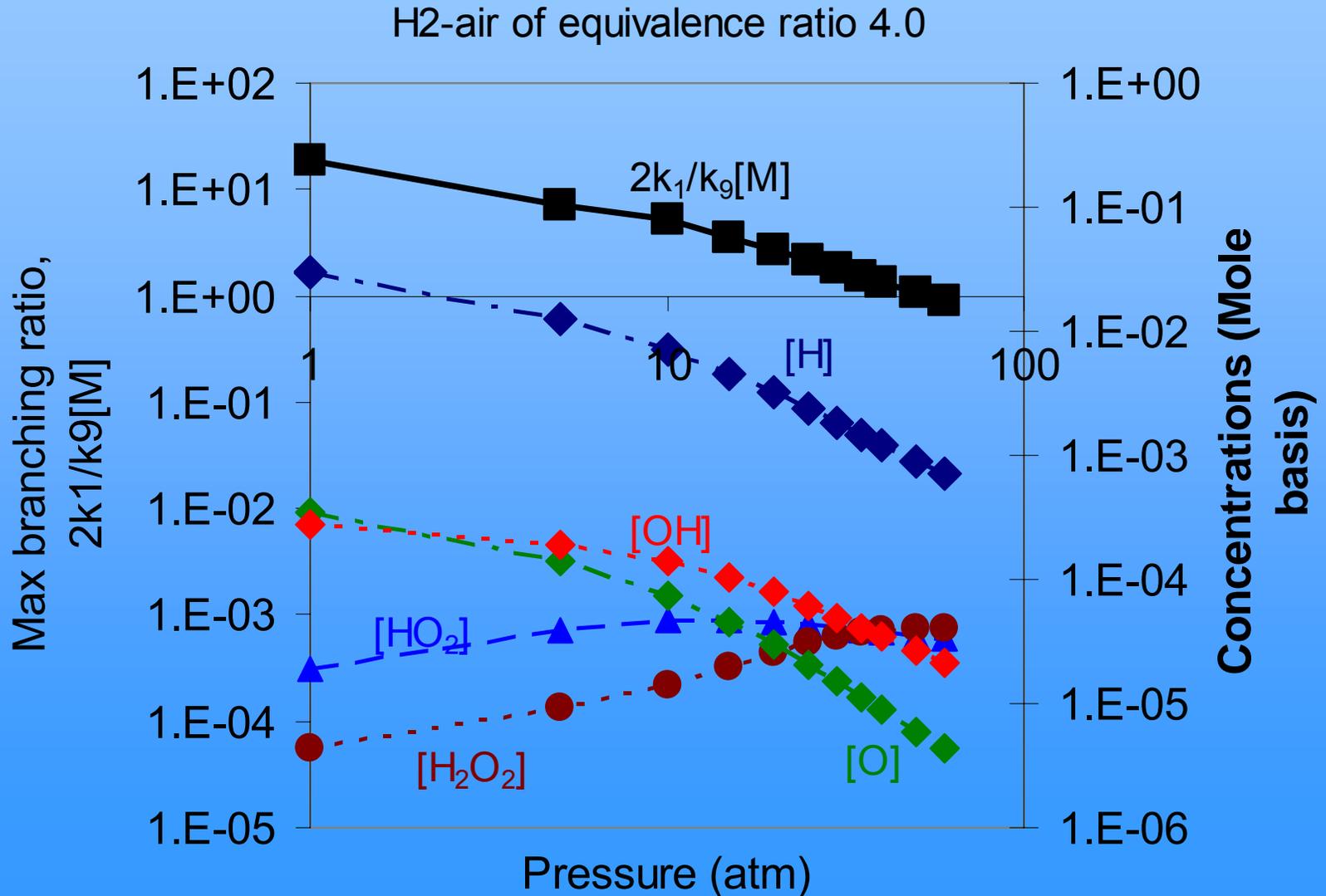
\*chain-termination

\*favored at higher pressures and lower temperatures

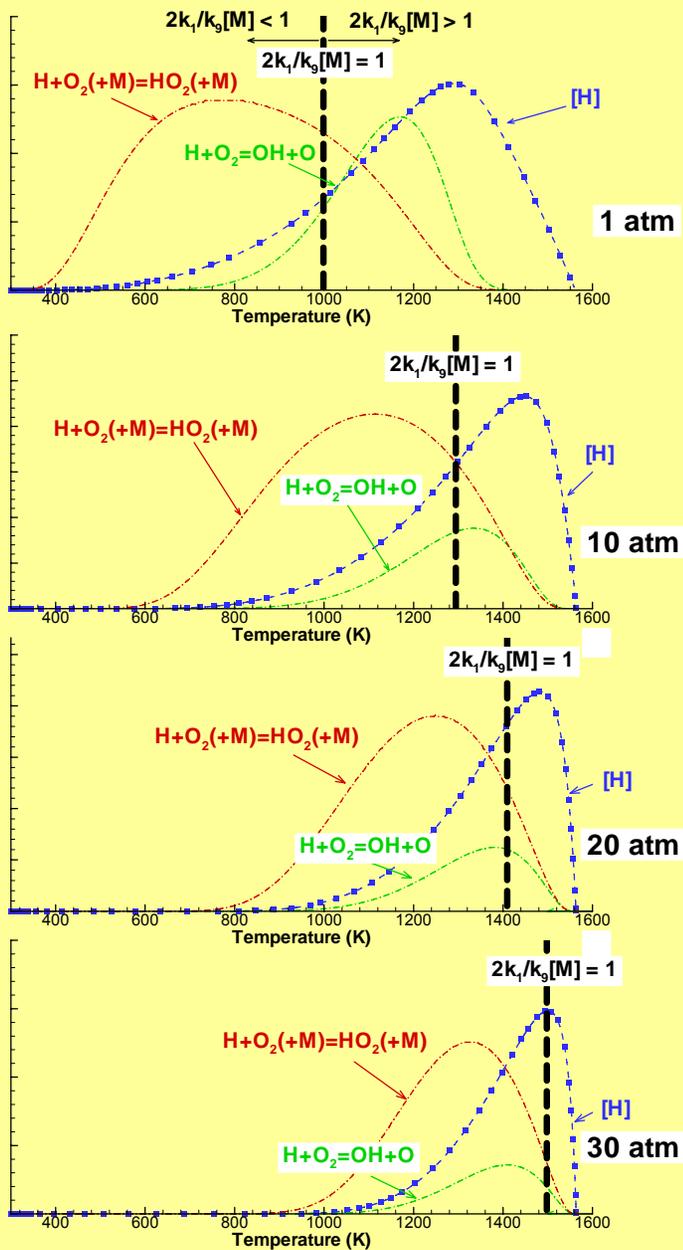
- Extended Second Limit – demarcates 2 distinct kinetic regimes

$$\frac{2k_1}{k_9[M]} < 1 \longrightarrow \text{Overall mechanism is chain branching} \qquad \frac{2k_1}{k_9[M]} > 1 \longrightarrow \text{Overall mechanism is chain terminating}$$

# Branching Ratios and Radical Pool Decrease with Pressure



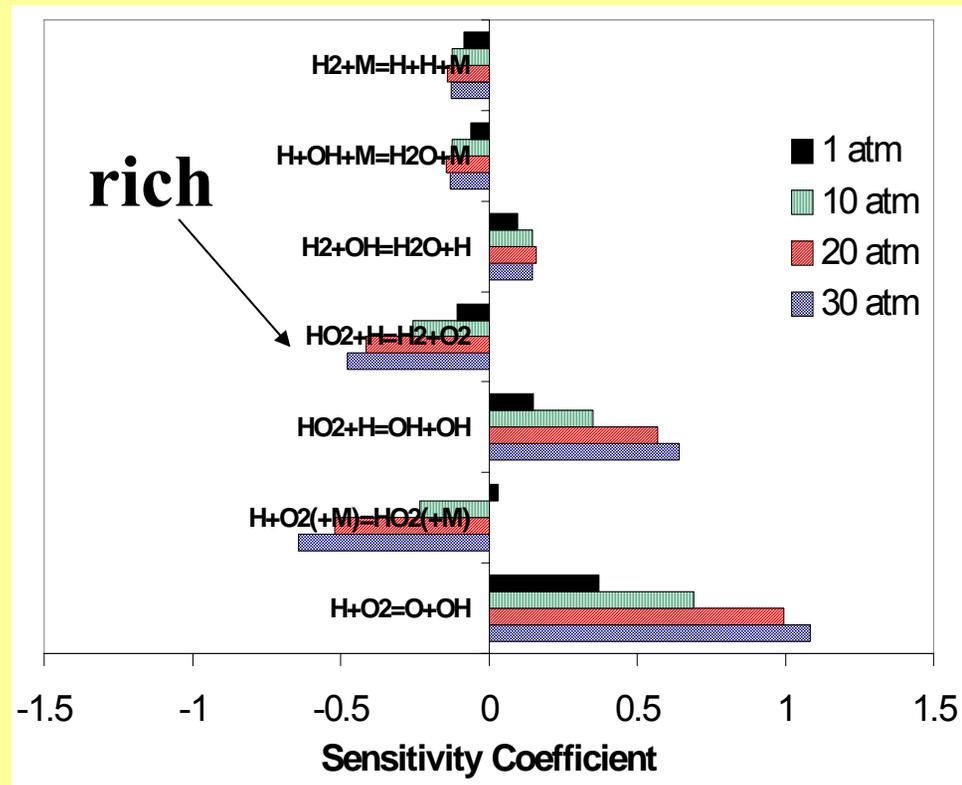
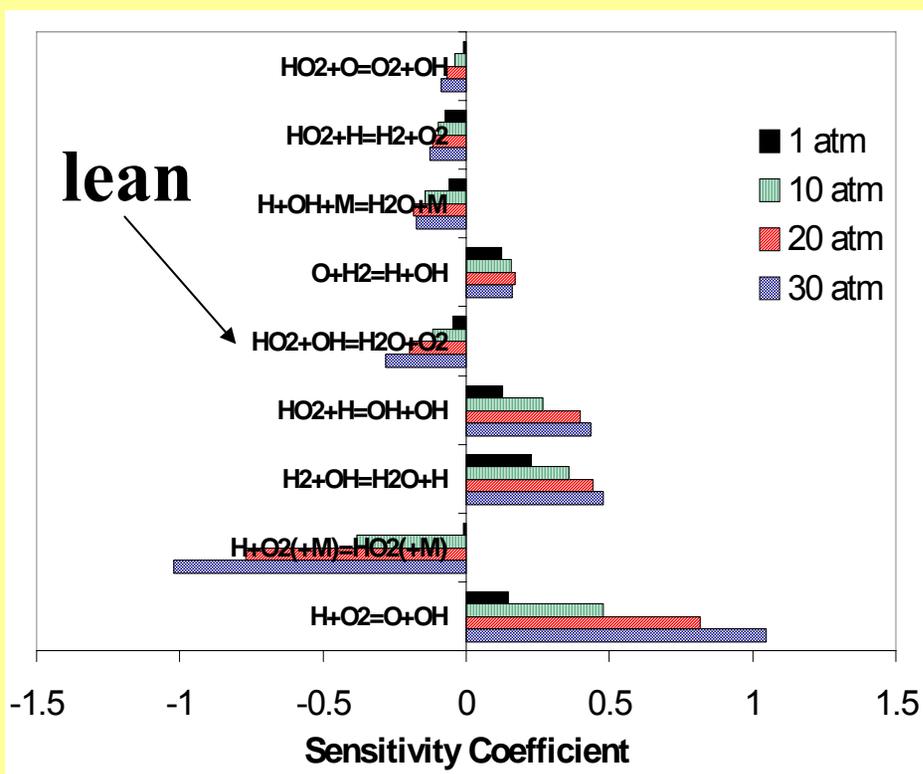
# Flux Analysis



- Extended Second Limit,  $2k_1/k_9[\text{M}] = 1$ , pushed to higher temperatures with increasing pressure
  - Raises the overall activation energy
    - Pushes the radical concentration and reaction flux profiles toward the back end of the flame
  - Extended second limit as a chemical singularity
    - Sensitivity to rate parameters blows up
    - Small differences in parameters make a big difference

Extended Second Limit →

# Sensitivity Analysis

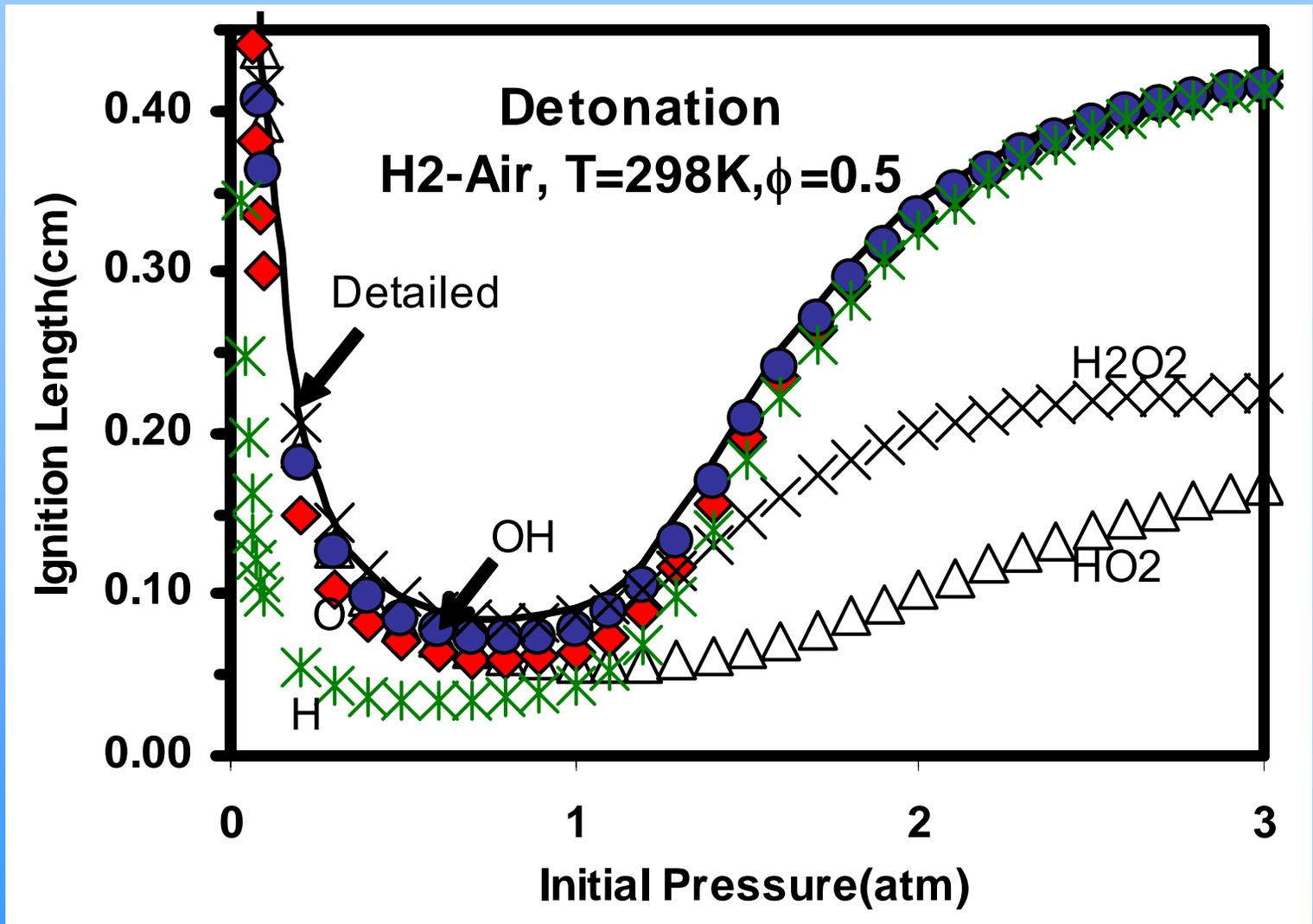


- Competition of  $\text{H} + \text{O}_2$  and  $\text{H} + \text{O}_2 + \text{M}$  becomes more sensitive with increasing pressure
- $\text{HO}_2 + \text{H}/\text{OH}$  reactions become more sensitive with increasing pressure at rich and lean conditions.
- No simple fix of the kinetic mechanism.

### 3. Development of reduced order kinetic mechanism



# A close look at hydrogen mechanism vs. QSS species

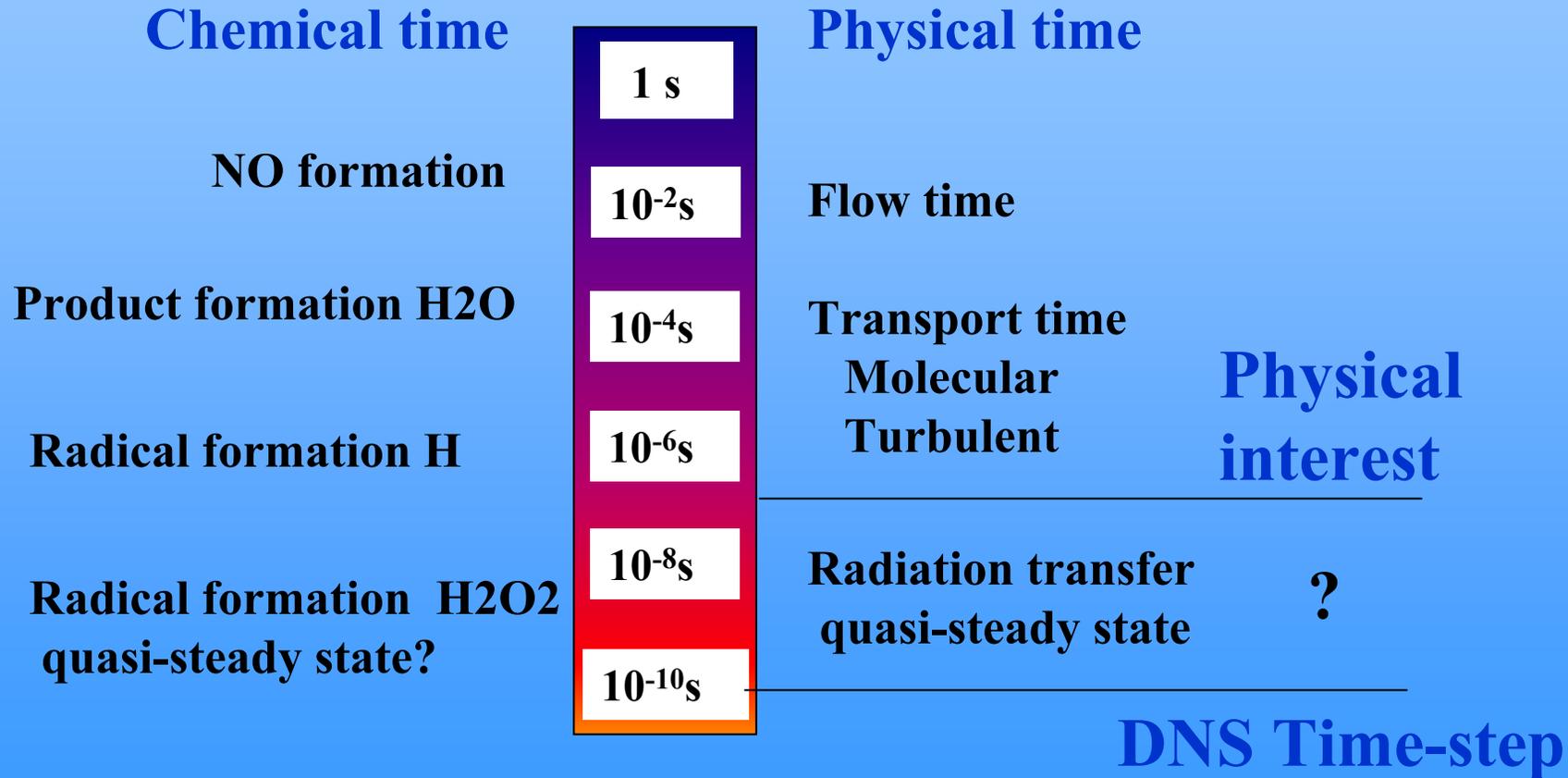


**No species can be reduced! How to reduce chemistry size?**

**Time scales are very different!**

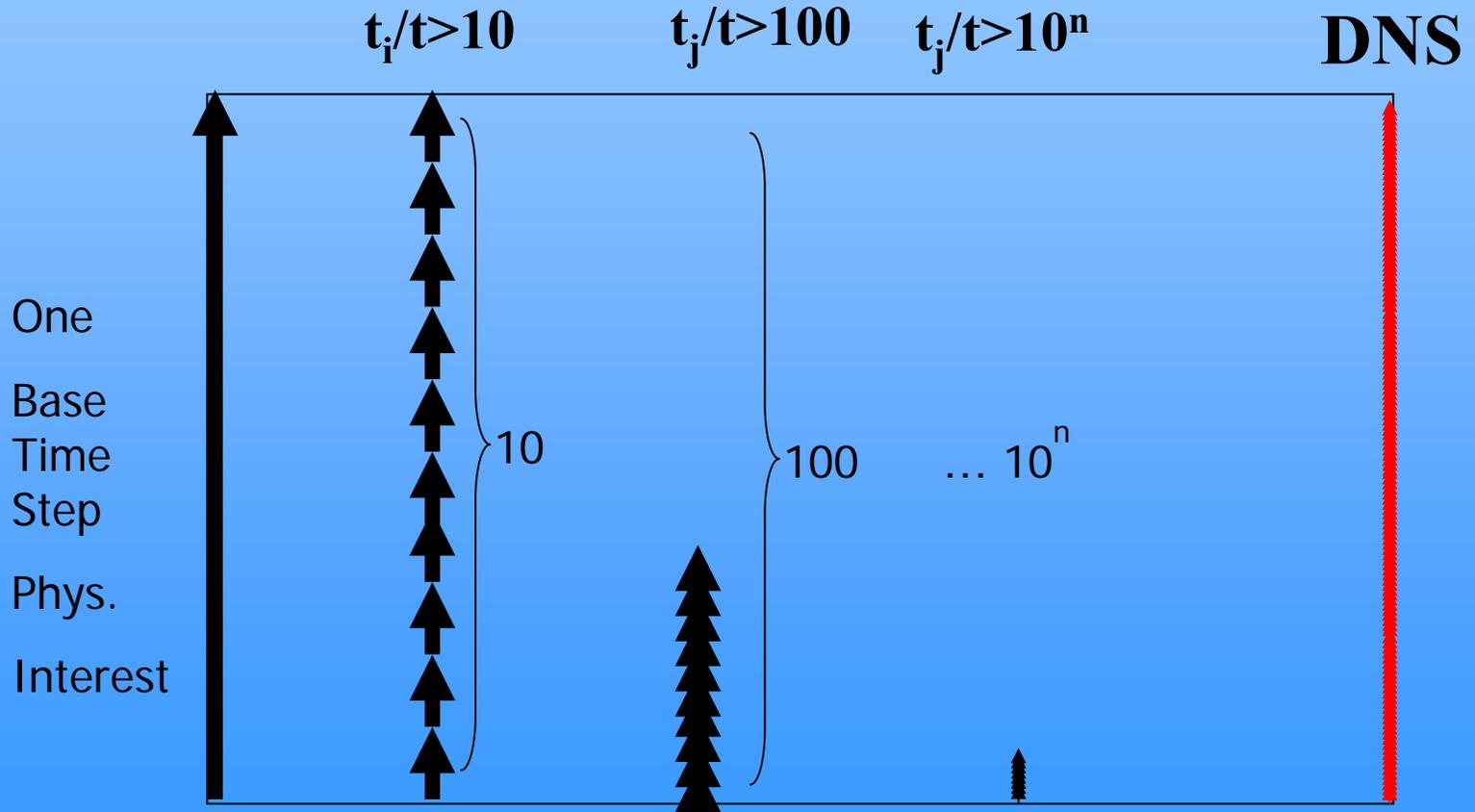
# A dynamic multi-scale (DMS) kinetic reduction model

## Time scales in reactive flow

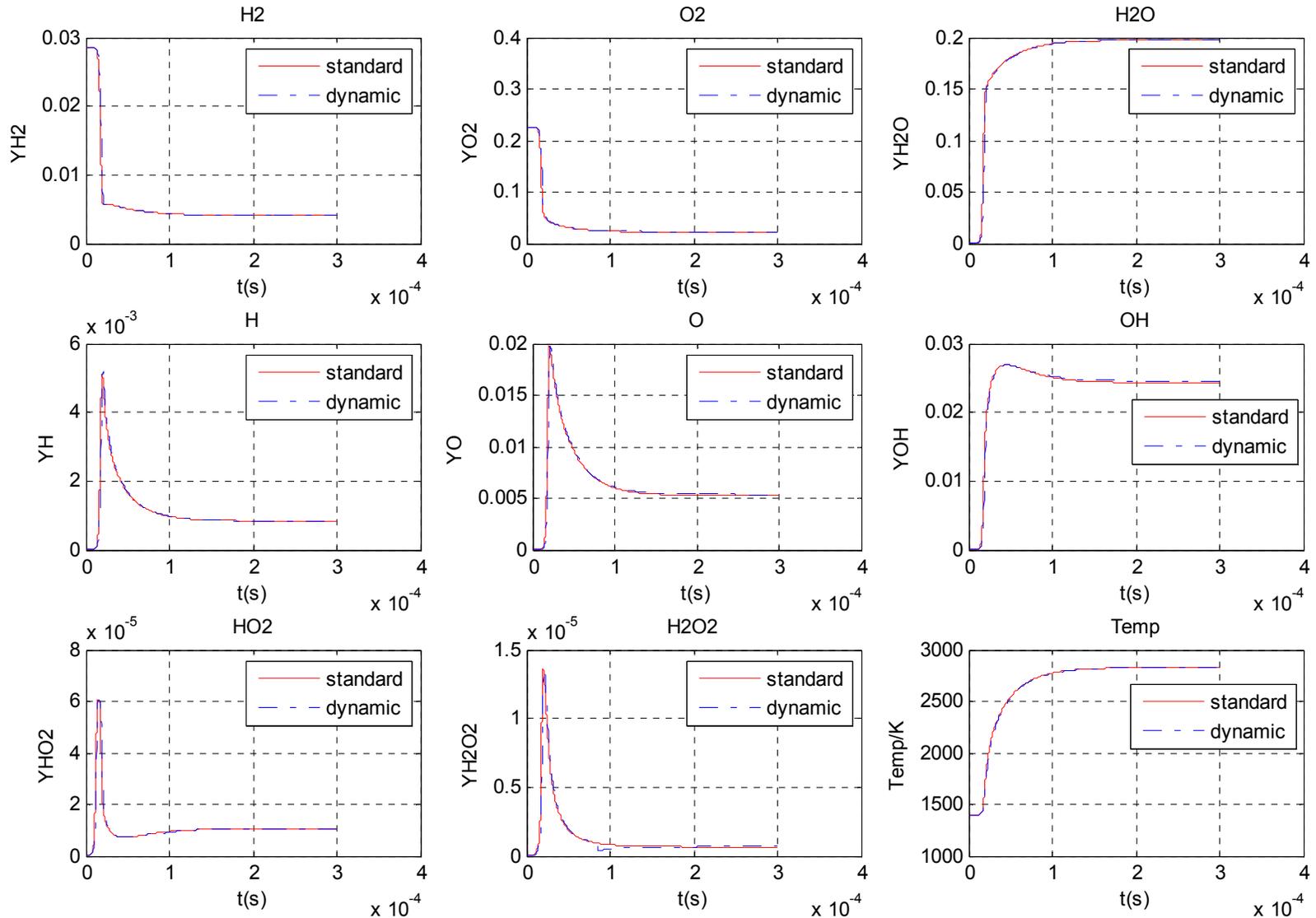


# Algorithm of Dynamic Multi-Scale (DMS) Modeling

Every species decays at its own time scale:  $Y_i = Y_{i0} e^{-\frac{t}{\tau_i}}$



# Validation of DMS method (hydrogen)



# Computational efficiency of DMS method

## Hydrogen/air ignition

No.	Max. calculation times for groups	Base time step	Average calculation time (s)	Figure No.
<b>For fix time step Euler</b>				
1	1	Step=Min. characteristic time	5.8	
<b>For Static Multi-scale(2 Groups)</b>				
1	9	Min. characteristic time	5.3	
2	5	Min. characteristic time	3.8	
3	3	Min. characteristic time	2.9	
4	2	Min. characteristic time	1.9	
<b>For Dynamic Multi-scale method vs. Direct numerical simulation of Euler equation, 6.66 s needed</b>				
1	50%	Min. characteristic time*100	0.57 s	DMTS-11

**With a detailed mechanism and no QSS assumption,  
Computation is speeded 10 times!**

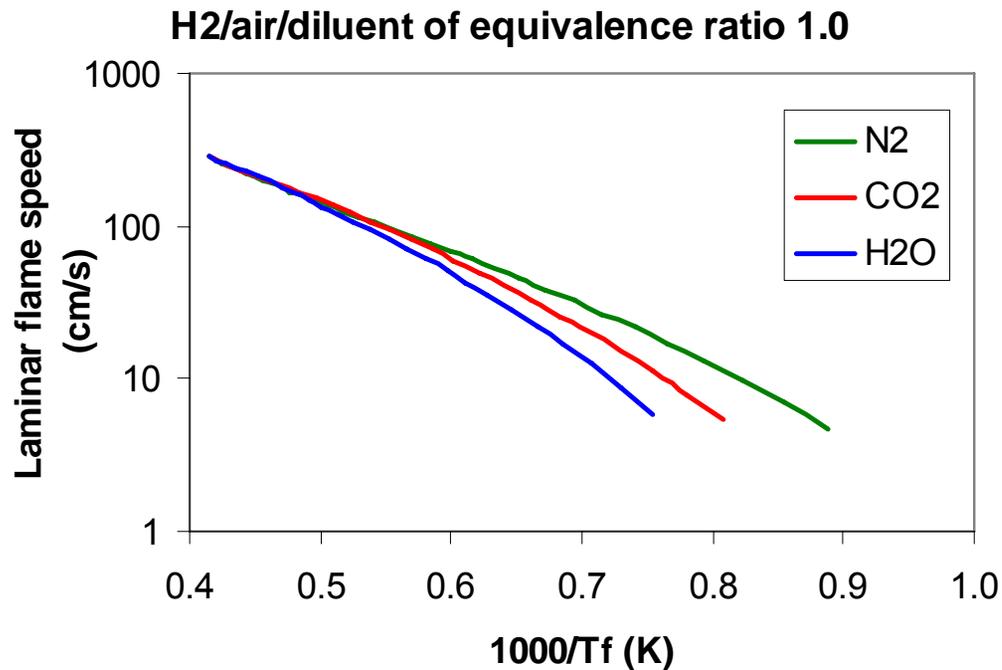


## Conclusions

- **A rigorous experimental approach for flame speed measurement at high pressures was developed.**
- **Hydrogen flame speed has a positive dependence on pressure up to 15 atm, but a negative dependence at higher pressures.**
- **No existing models reproduce measured flame speeds of high pressure rich hydrogen flames.**
- **A dynamic multiscale model is developed to reduce computational time by one order.**



# Flame Speeds with Preheat and H<sub>2</sub>O dilution (with Counterflow Flames)



Methane diffusion flame with 26% H<sub>2</sub>O dilution in fuel stream

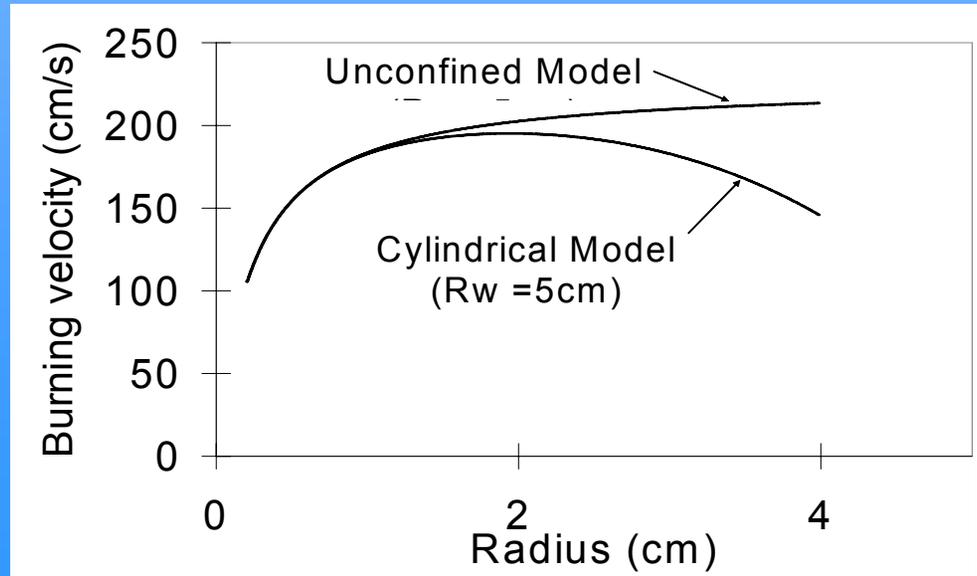
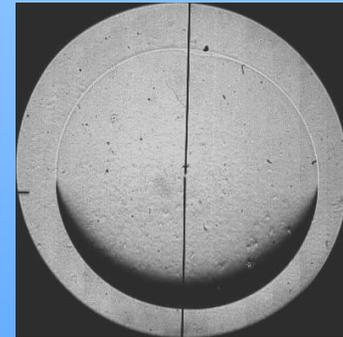
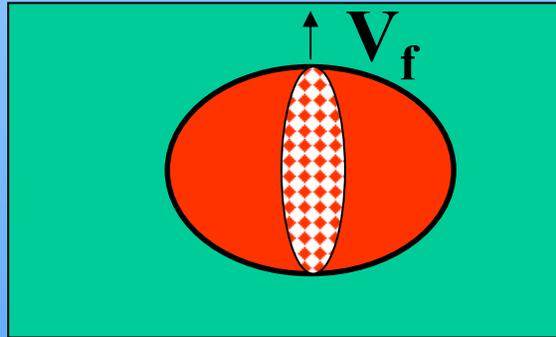
- Performed preliminary tests with PIV system and evaporator
- Currently refining the system to prepare for gathering data

# High pressure flame speed ( $S_u$ ) measurement

## Effect of non-spherical flow, $u_b \neq 0$

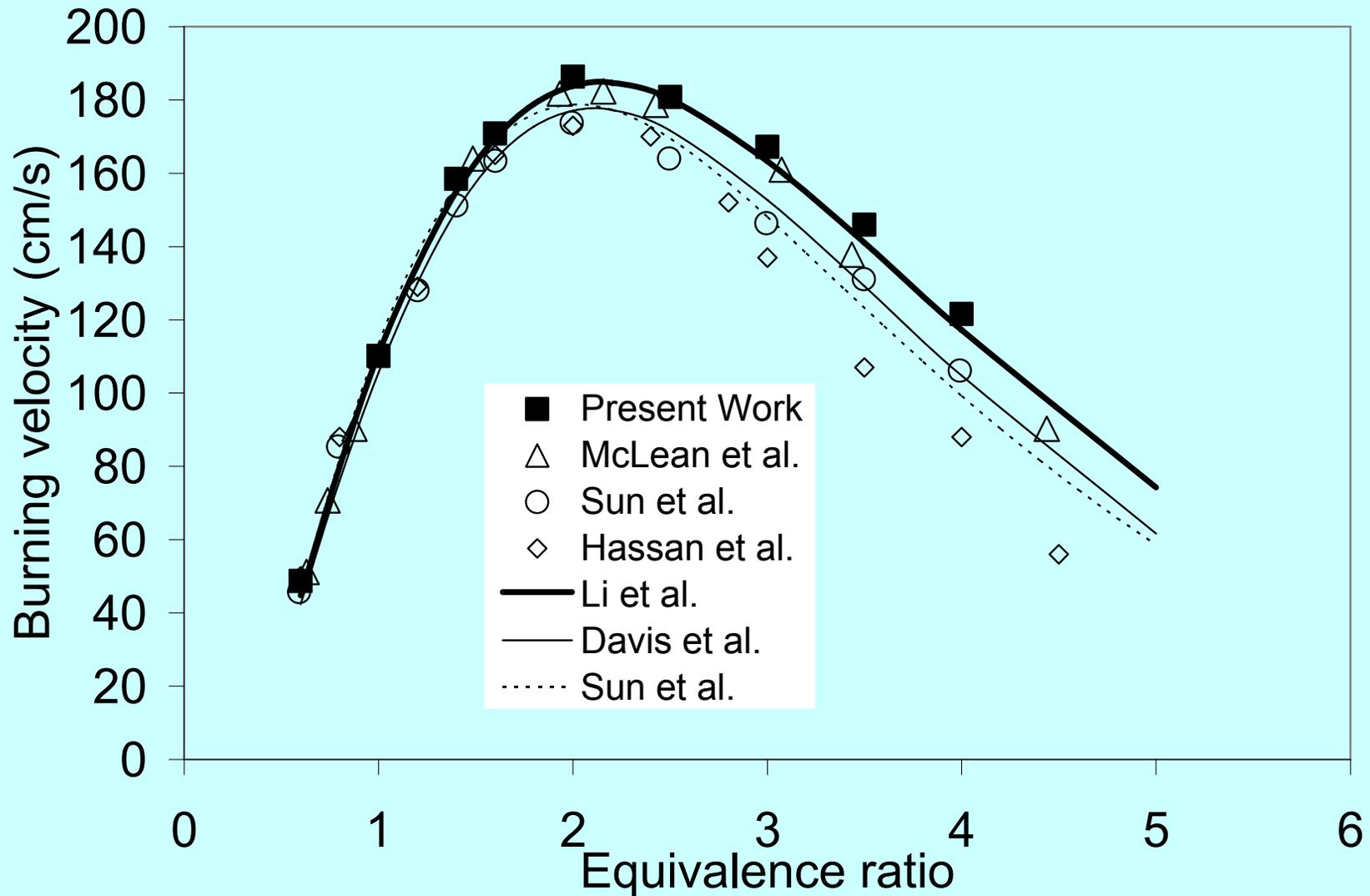
$$\frac{S_u^* - S_u}{S_u} = (\sigma - 1) \cdot \frac{\Delta u_f}{u_f} = ?$$

→  
Collimated  
beam



# Compression of measured hydrogen syngas flame speed

H<sub>2</sub>-CO = 50:50 syngas mixture in air at 1 atm



Burke, Qin, Ju & Dryer 2007

