

Comparative Assessments of PC, NGCC and IGCC Power Plants With and Without CO₂ Capture and Storage

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Objectives

- Compare the performance and cost of **current** fossil fuel power systems with and without CO₂ capture and storage (CCS)
 - Pulverized coal combustion (PC)
 - Integrated coal gasification combined cycle (IGCC)
 - Natural gas combined cycle (NGCC)

What's New Here?

- We explore a broader range of conditions that influence comparisons among these technologies
- We highlight the implications of CCS energy penalties on resource requirements, multi-pollutant emissions, and cross-media environmental impacts
- We use the (publicly available) IECM computer model to systematically evaluate all three systems

The Integrated Environmental Control Model (IECM)

- Estimates the performance, emissions, and cost of power generation and emissions control for a single facility (based on user-specified configuration and parameters)
- Developed for DOE/NETL, originally to model options for controlling air pollutants at coal-fired power plants
- Expanded in recent years to include CCS technologies, and a broader array of fossil fuel power systems
- Provides users with a flexible and systematic framework to evaluate and compare alternative options (including effects of uncertainties, if desired)

IECM Software Package

Fuel Properties

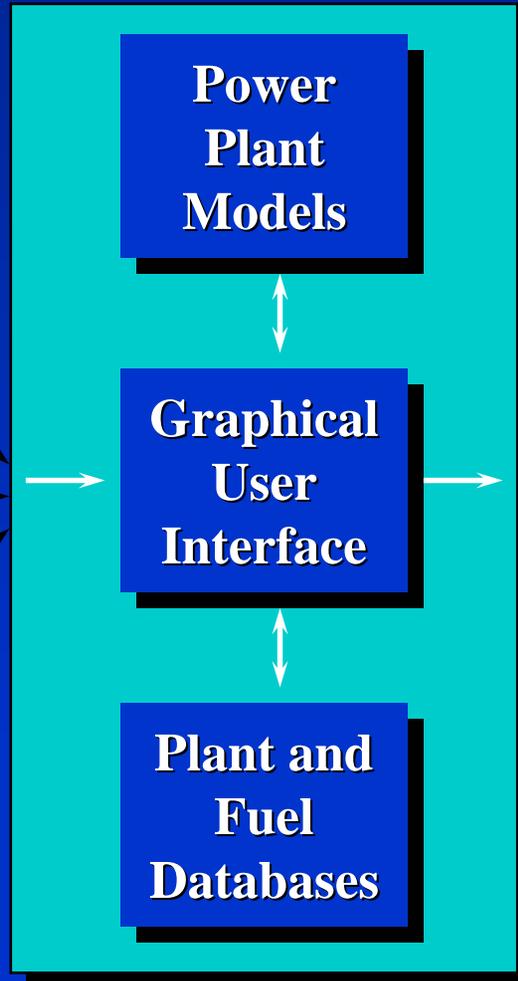
Heating Value
Composition
Delivered Cost

Plant Design

Conversion Process
Emission Controls
Solid Waste Mgmt
Chemical Inputs

Cost Data

O&M Costs
Capital Costs
Financial Factors



Plant & Process Performance

- Efficiency
- Resource use

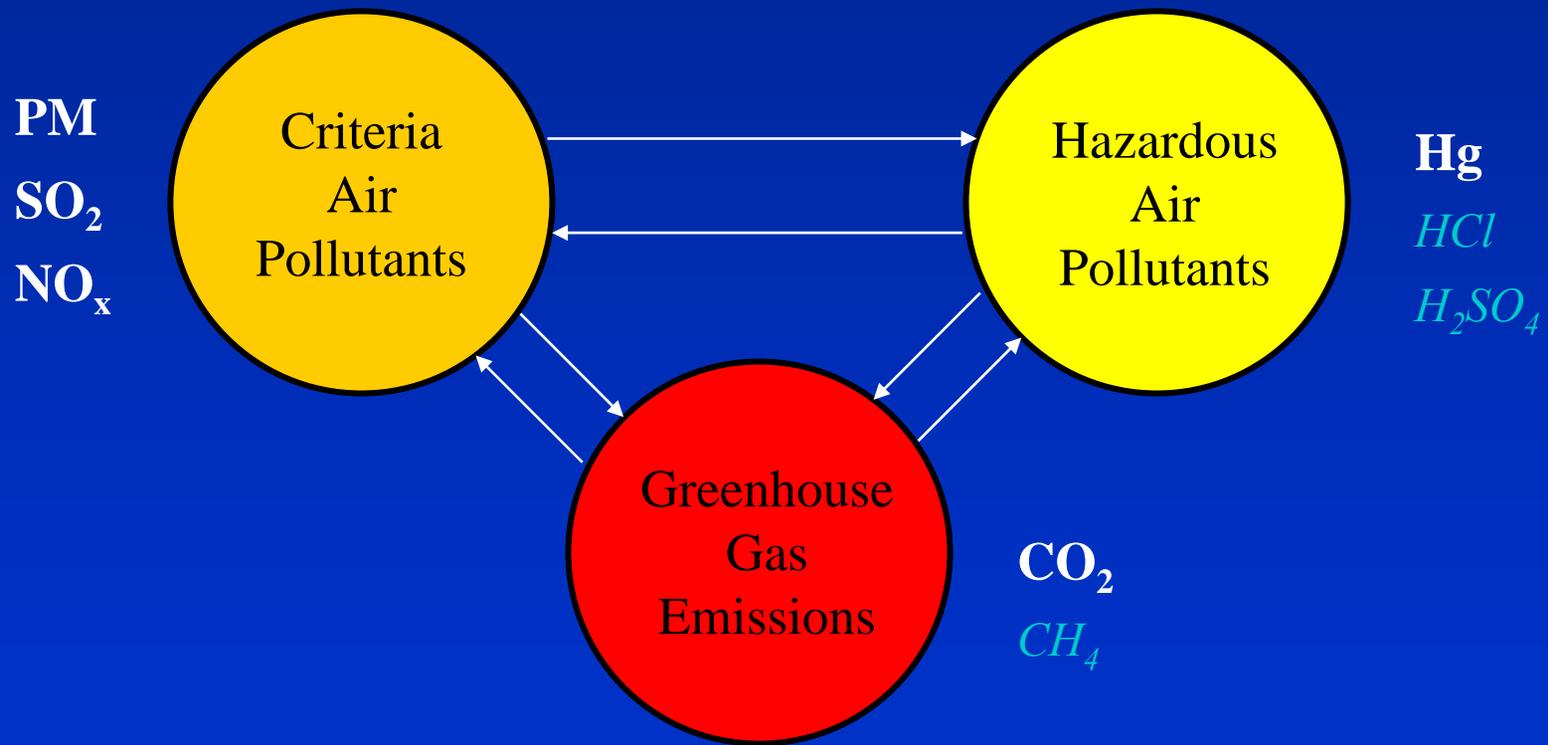
Environmental Emissions

- Air, water, land

Plant & Process Costs

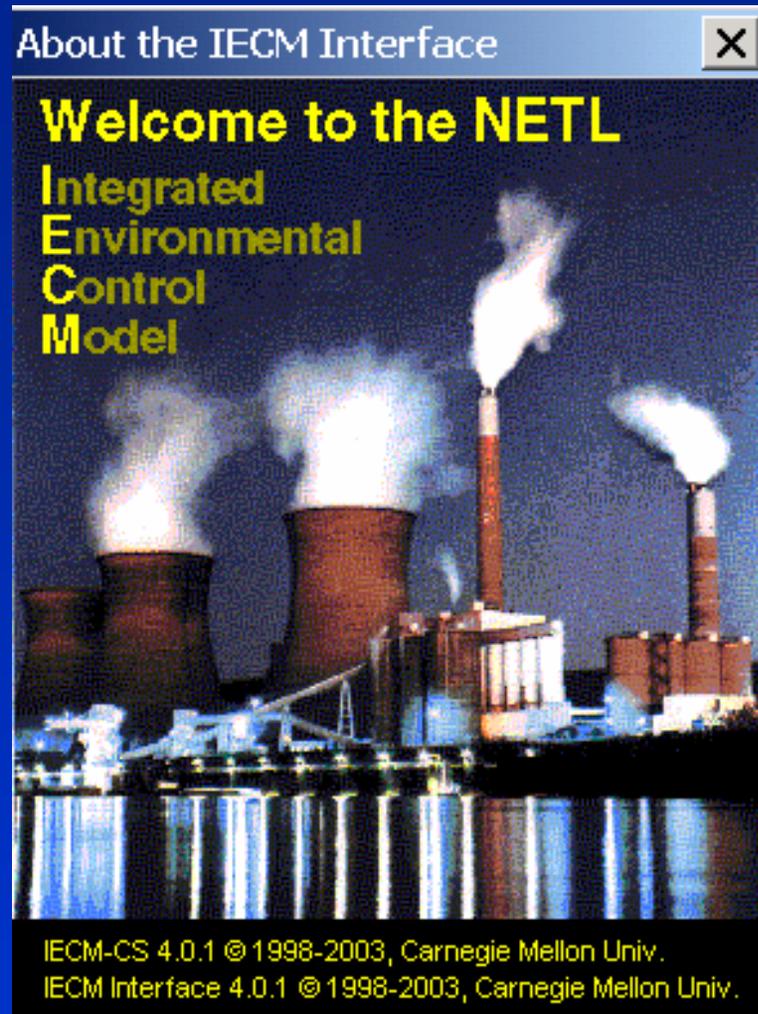
- Capital
- O&M
- COE

Multi-Pollutant Interactions

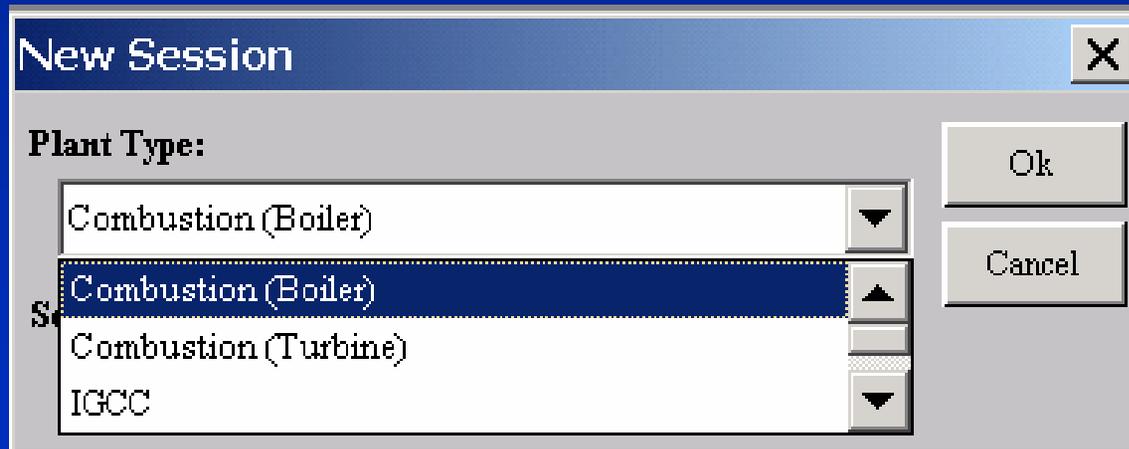


*Sample
Screens from
the User
Interface*

(IECM 4.0.1)



Select Plant Type



PC Plant with CO₂ Capture

IEA Case Study*

Configure Plant Set Parameters Get Results

Combustion Controls

Fuel Type: Coal

NOx Control: None

Post-Combustion Controls

NOx Control: Hot-Side SCR

Particulates: Cold-Side ESP

SO₂ Control: Wet FGD

Mercury: None

CO₂ Capture: Amine System

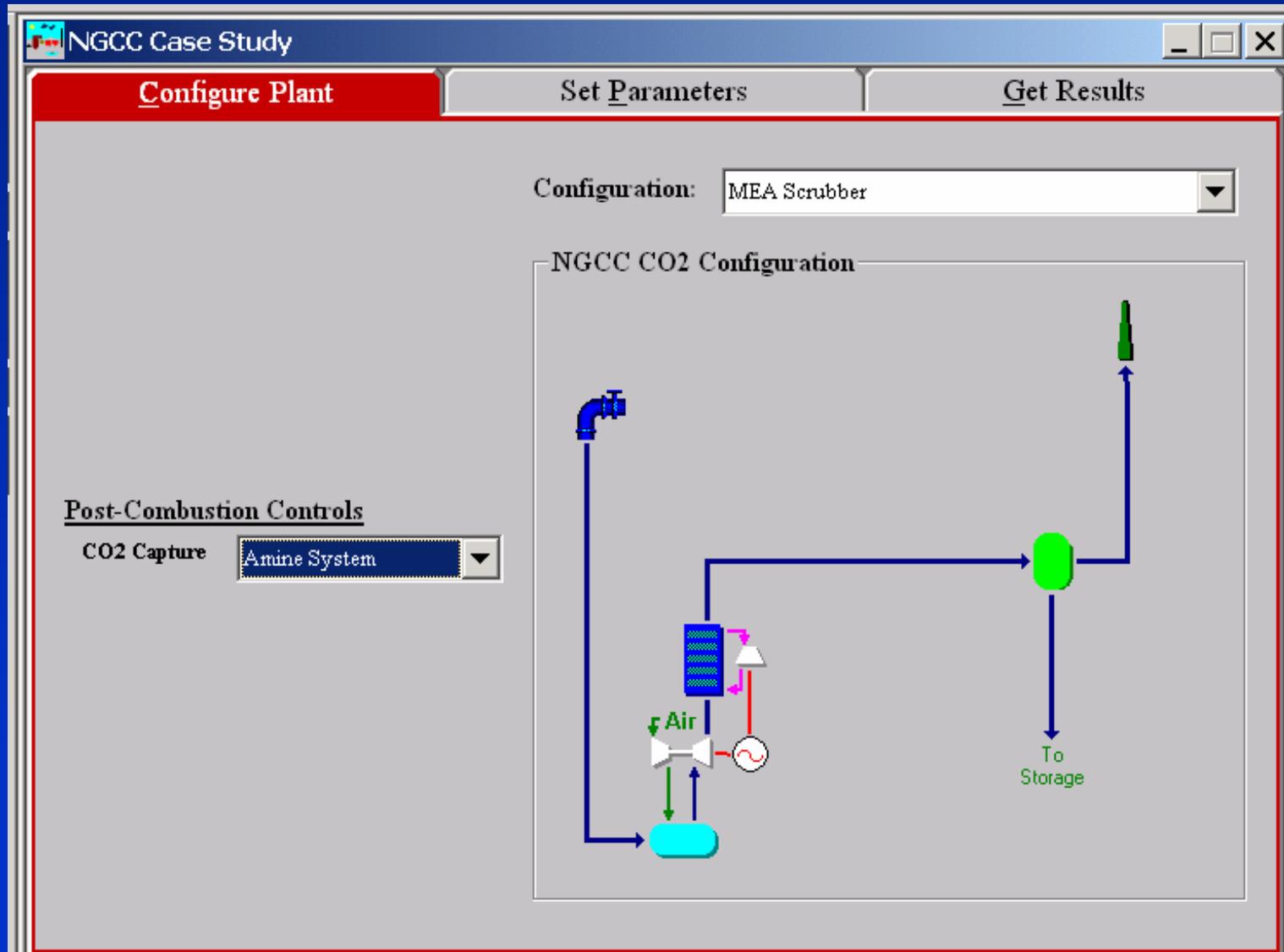
Solids Management

Disposal: mixed w/ Landfill

Plant Diagram

The diagram illustrates the flow of gas and solids through the plant. It starts with a boiler (red) that emits smoke. The gas then passes through a cold-side ESP (green), a hot-side SCR (pink), and a wet FGD (blue). The amine system (red) is connected to a CO₂ storage tank (green) labeled 'To Storage'. The final exhaust goes to a stack (green). Solids are collected in two bins (yellow and blue).

NGCC Plant with CO₂ Capture



IGCC Plant with CO₂ Capture

IGCC Case Study*

Configure Plant | Set Parameters | Get Results

Configuration: Sour Shift + Selexol

Gasification Options

Gasifier: Texaco (Oxygen-blown)

Gas Cleanup: Cold-gas

CO₂ Control: Sour Shift + Selexol

Combustion Controls

NO_x Control: None

Solids Management

Slag: Landfill

Sulfur: Sulfur Recovery

IGCC Base Configuration

Air

To Storage

Set Financial Parameters

IGCC Case Study*

Configure Plant **Set Parameters** Get Results

Overall Plant Fuel Air Separation Gasifier Area Sulfur Removal CO₂ Capture Power Block By-Prod. Mgmt Stack

	Title	Units	Unc	Value	Calc	Min	Max	Default
1	Year Costs Reported			2000	▼	Menu	Menu	2000
2	Constant or Current Dollars?			Constant	▼	Menu	Menu	Constant
3	Fixed Charge Factor (FCF)	fraction		0.1480	<input checked="" type="checkbox"/>	0.0	1.000	calc
4	Discount Rate (Before Taxes)	fraction		0.1030	<input checked="" type="checkbox"/>	0.0	2.000	calc
5	<i>Or, specify all the following:</i>							
6	Inflation Rate	%/yr		0.0	<input checked="" type="checkbox"/>	0.0	20.00	calc
7	Plant or Project Book Life	years		30.00		5.000	60.00	30.00
8	Real Bond Interest Rate	%		9.000		0.0	15.00	9.000
9	Real Preferred Stock Return	%		8.500		0.0	20.00	8.500
10	Real Common Stock Return	%		12.00		0.0	25.00	12.00
11	Percent Debt	%		45.00		0.0	100.0	45.00
12	Percent Equity (Preferred Stock)	%		10.00		0.0	100.0	10.00
13	Percent Equity (Common Stock)	%		45.00	<input checked="" type="checkbox"/>	0.0	100.0	calc
14								
15	Federal Tax Rate	%		35.00		15.00	50.00	35.00
16	State Tax Rate	%		4.000		0.0	10.00	4.000
17	Property Tax Rate	%		2.000		0.0	5.000	2.000
18	Investment Tax Credit	%		0.0		0.0	20.00	0.0

Process Type: Overall Plant

1. Diagram 2. Performance **3. Financing**

Specify Fuel Properties

IGCC Case Study*

Configure Plant | **Set Parameters** | Get Results

Overall Plant | **Fuel** | Air Separation | Gasifier Area | Sulfur Removal | CO₂ Capture | Power Block | By-Prod. Mgmt | Stack

Current Fuel

Name:

Rank:

Source:

Composition (wt% as received) and Higher Heating Value (Btu/lb)

Tot %:

	Property	Value
1	Heating Value	13260
2	Carbon	73.81
3	Hydrogen	4.88
4	Oxygen	5.41
5	Chlorine	0.06
6	Sulfur	2.13
7	Nitrogen	1.42
8	Ash	7.24
9	Moisture	5.05
10		
11		

Save For All...

Plant Types

Fuel Types

Save In Database

Use Default Ash Properties

View Ash Properties

Fuel Databases

Fuel:

Rank:

Source:

Show All Plant Types

Show All Fuel Types

	Property	Value
1	Heating Value	1.308e+04
2	Carbon	71.74
3	Hydrogen	4.620
4	Oxygen	6.090
5	Chlorine	7.000e-02
6	Sulfur	0.6400
7	Nitrogen	1.420
8	Ash	9.790
9	Moisture	5.630
10	Plant Type	<Any>
11	Fuel Type	Coal

Open Database

New Database

Use This Fuel

Delete This Fuel

View Ash Properties

Process Type:

1. Properties | 2. Cost

Set Power Block Performance Parameters

IGCC Case Study*

Configure Plant | **Set Parameters** | Get Results

Overall Plant | Fuel | Air Separation | Gasifier Area | Sulfur Removal | CO2 Capture | **Power Block** | By-Prod. Mgmt | Stack

	Title	Units	Unc	Value	Calc	Min	Max	Default
1	<u>Gas Turbine/Generator</u>							
2	Gas Turbine Model			GE 7FA+ ▼		Menu	Menu	GE 7FA+e
3	Gas Turbine Size (Nominal)	MW		410.5	<input checked="" type="checkbox"/>	0.0	5000	calc
4	No. of Gas Turbines	integer		2 ▼		Menu	Menu	2
5	Inlet Water Content	vol %		33.00	<input checked="" type="checkbox"/>	0.0	100.0	calc
6	Turbine Inlet Temperature	deg. F		2420	<input checked="" type="checkbox"/>	2000	2500	calc
7	Turbine Back Pressure	psia		2.000		0.0	10.00	2.000
8	Adiabatic Turbine Efficiency	%		95.00		0.0	100.0	95.00
9	Shaft/Generator Efficiency	%		98.00		0.0	100.0	98.00
10	<u>Air Compressor</u>							
11	Pressure Ratio (outlet/inlet)	ratio		15.70		1.000	25.00	15.70
12	Adiabatic Compressor Efficiency	%		70.00		0.0	100.0	70.00
13	Ambient Air Temperature	deg. F		77.00		-50.00	130.0	77.00
14	Ambient Air Pressure	psia		14.70		12.00	15.00	14.70
15	<u>Combustor</u>							
16	Combustor Inlet Pressure	psia		294.0		0.0	350.0	294.0
17	Combustor Pressure Drop	psia		4.000		0.0	10.00	4.000
18	Excess Air For Combustor	% stoich.		177.8	<input checked="" type="checkbox"/>	0.0	400.0	calc

Process Type: Power Block ▼

1. Gas Turbine | 2. Steam Cycle | 3. Emis. Factors | 4. Retrofit Cost | 5. Capital Cost | 6. O&M Cost

Get Results for Overall Plant

IGCC Case Study*

Configure Plant **Set Parameters** **Get Results**

Overall Plant Fuel Air Separation Gasifier Area Sulfur Removal CO2 Capture Power Block By-Prod. Mgmt Stack

IGCC Sour Shift CO2 Config

Gasification Options

Gasifier:	Texaco (Oxygen-blown)
Gas Cleanup:	Cold-gas
CO2 Control:	Sour Shift + Selexol

Post-Combustion Controls

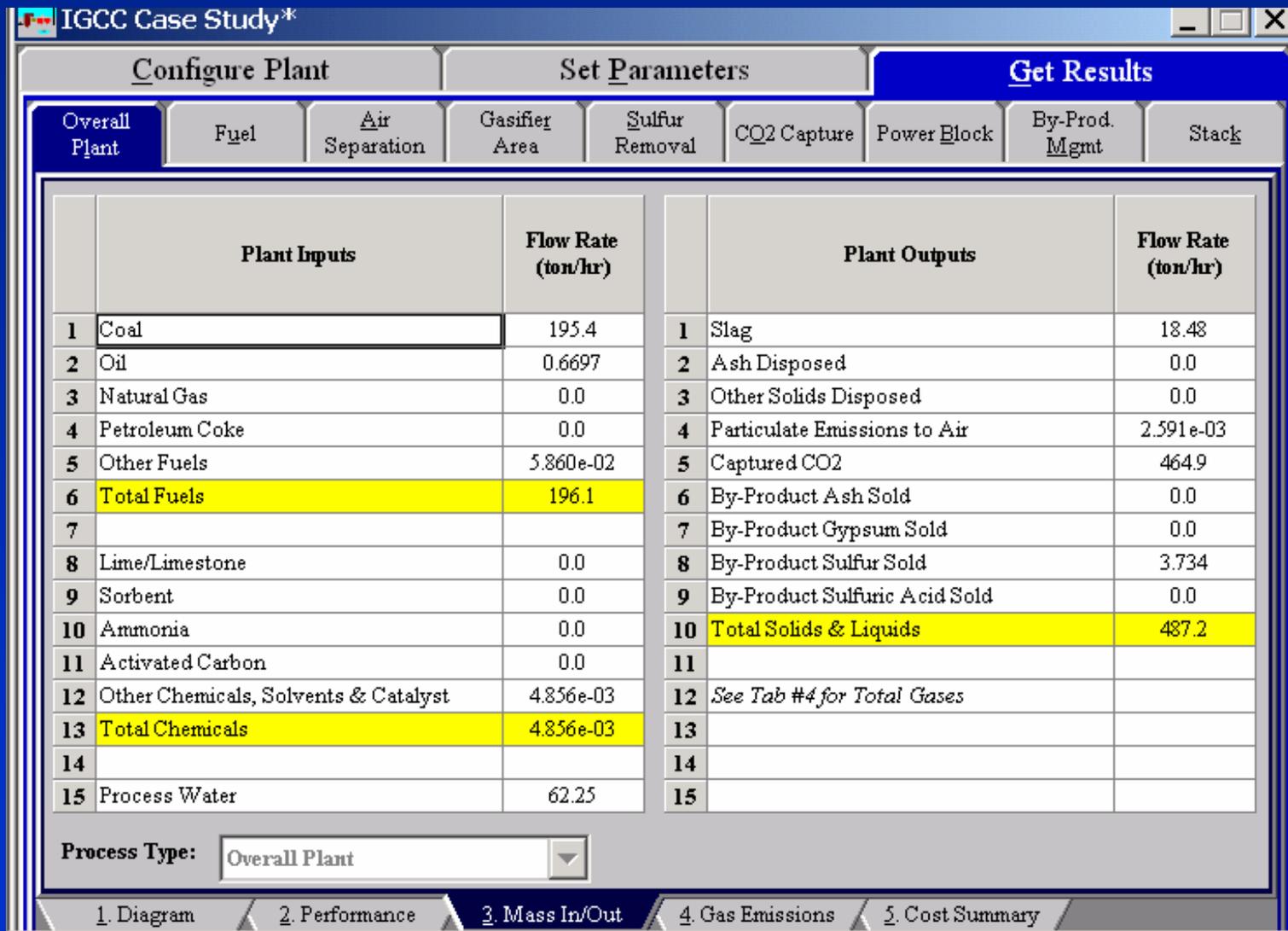
NOx Control:	None
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Solids Management

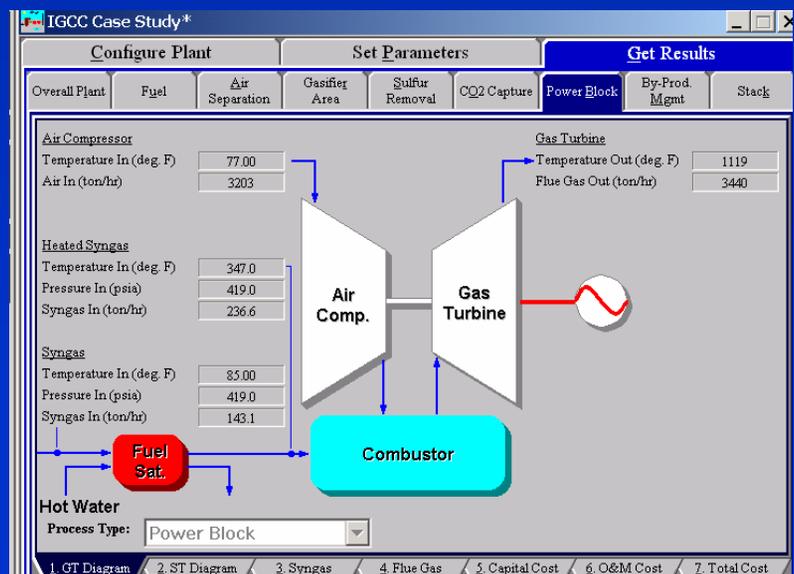
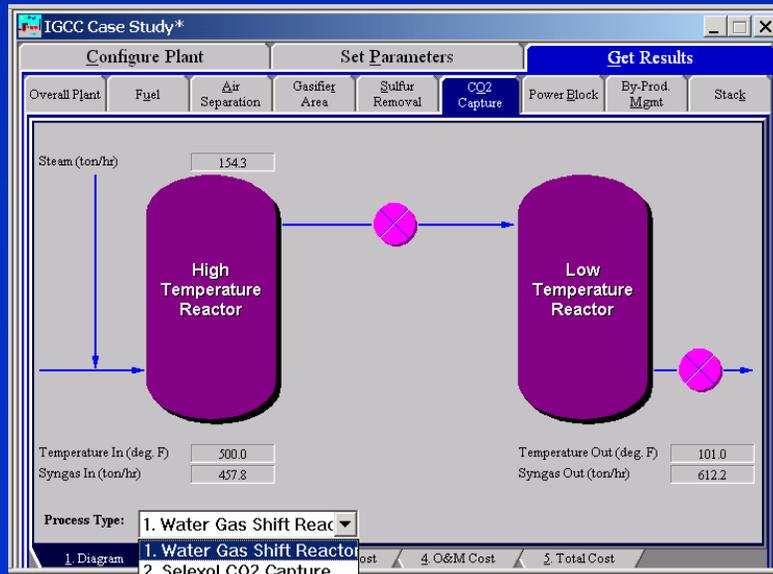
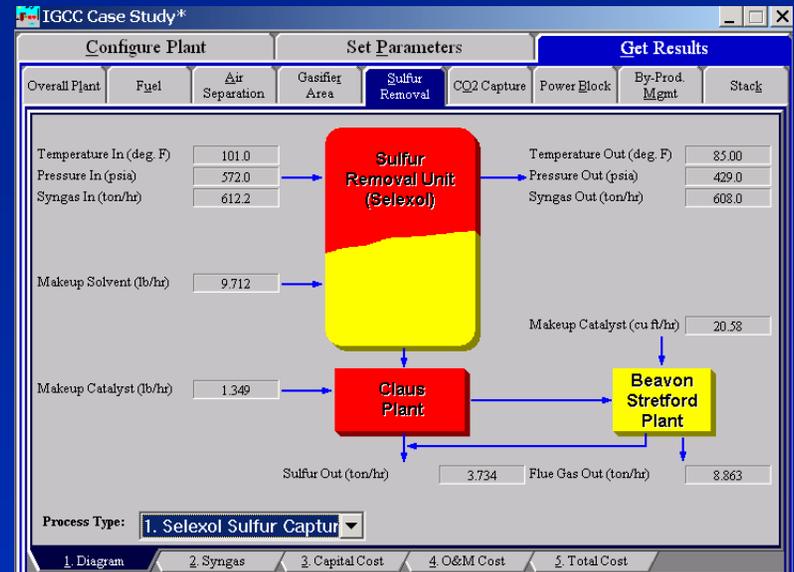
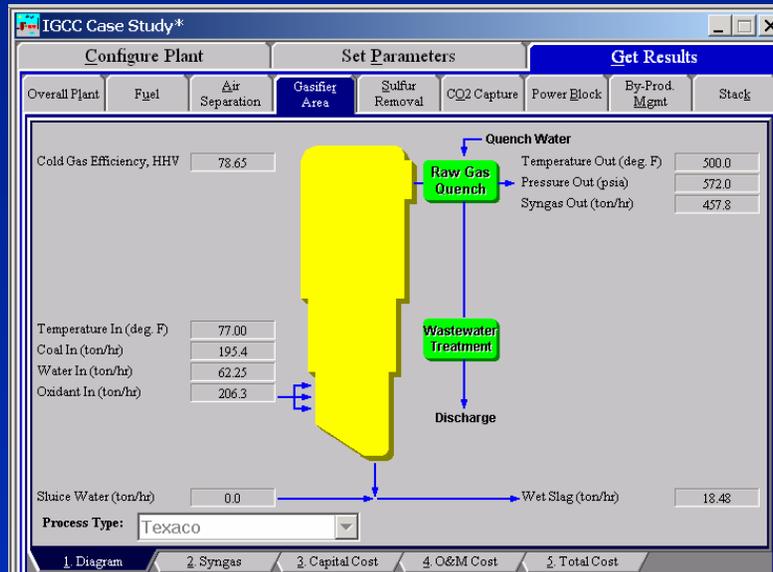
Slag:	Landfill
Sulfur:	Sulfur Plant

1. Diagram 2. Performance 3. Mass In/Out 4. Gas Emissions 5. Cost Summary

Get Results for Plant Mass Balance

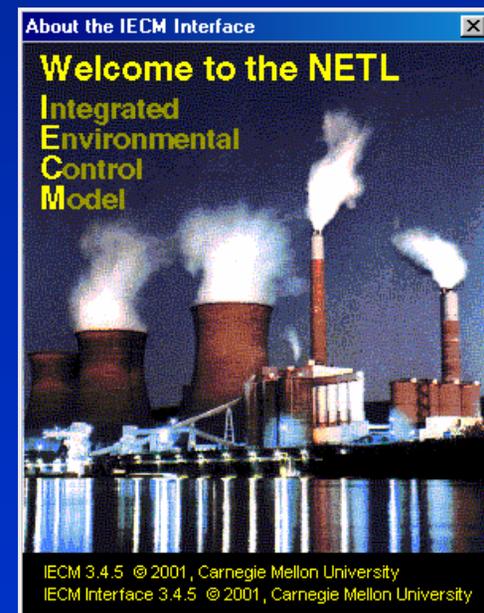


Get Results for Specific Components



The IECM is Available At . . .

- **CO₂ Version (Beta):**
 - Contacts: rubin@cmu.edu
mikeb@cmu.edu
- **Web Access :**
 - www.iecm-online.com
- **Technical Support:**
 - PED.modeling@netl.doe.gov



Case 1:

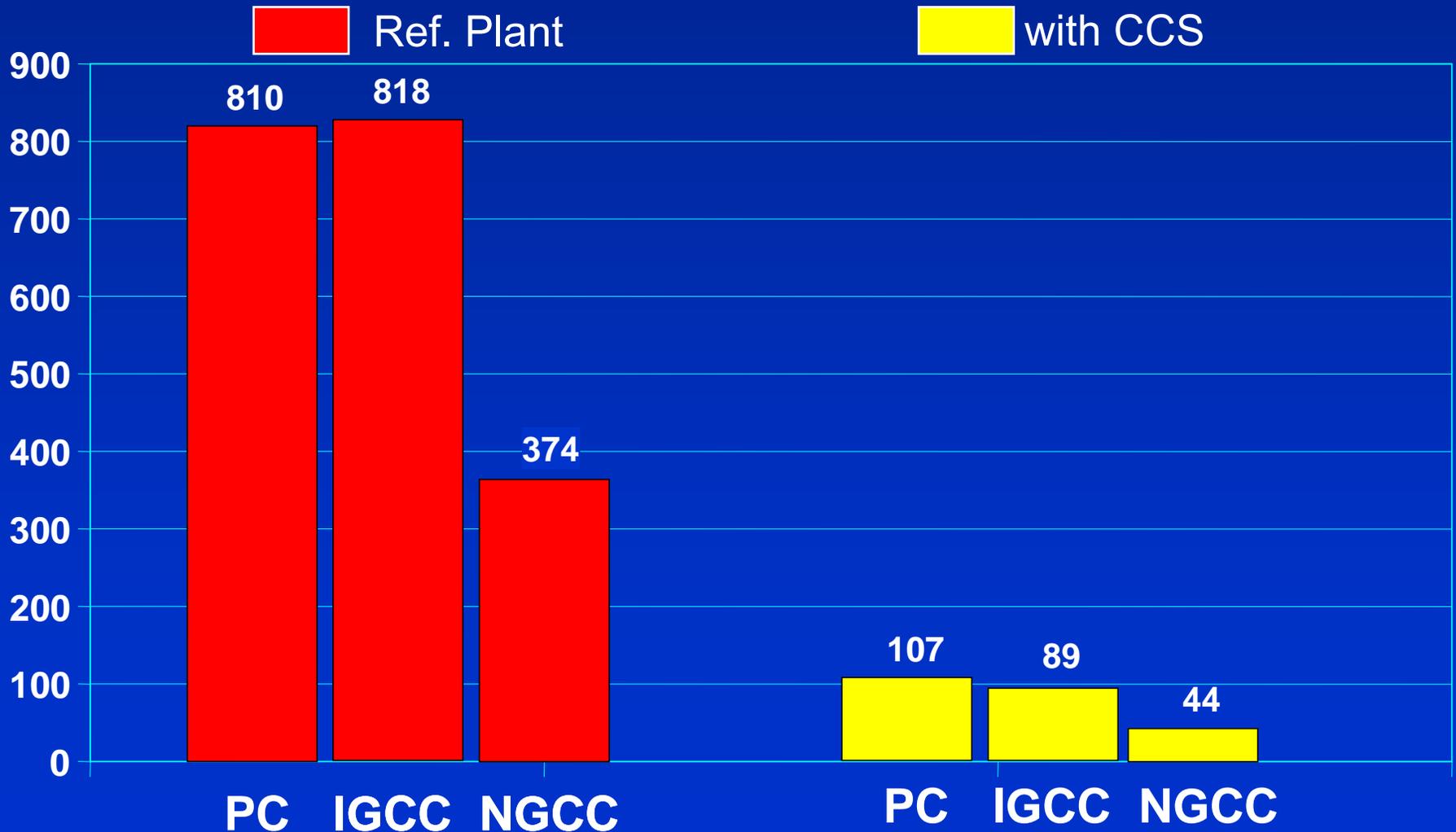
Nominal Assumptions

Nominal Case Study Assumptions

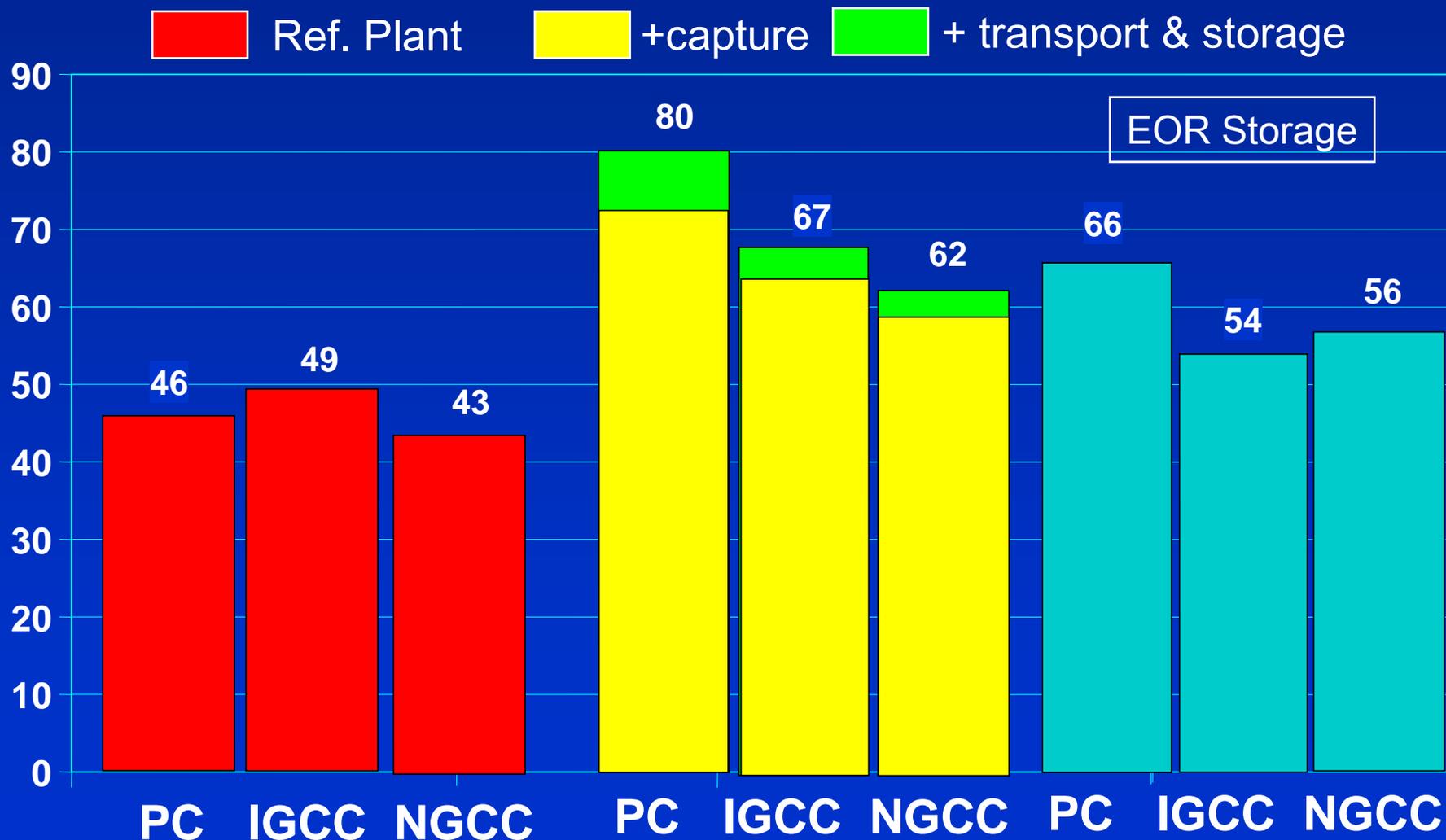
Parameter	NGCC	PC	IGCC
Reference Plant (~500 MW)	2 x 7FA	Supercritical	Texaco quench
Fuel Type	Nat. Gas	2%S Bit	2%S Bit
Net HHV Efficiency (%)	50.3	39.3	37.5
Capacity Factor (%)	75	75	75
Fuel Cost, HHV (\$/GJ)	3.92	1.27	1.27
CCS Plant (~500 MW)			
CO ₂ Capture System	Amine	Amine	Shift+Selexol
CO ₂ Removal (%)	90	90	90
Pipeline Pressure (MPa)	13.8	13.8	13.8
Geologic Storage Option	Aquifer	Aquifer	Aquifer

Also: fixed charge factor = 0.148; all costs in constant 2002 US\$

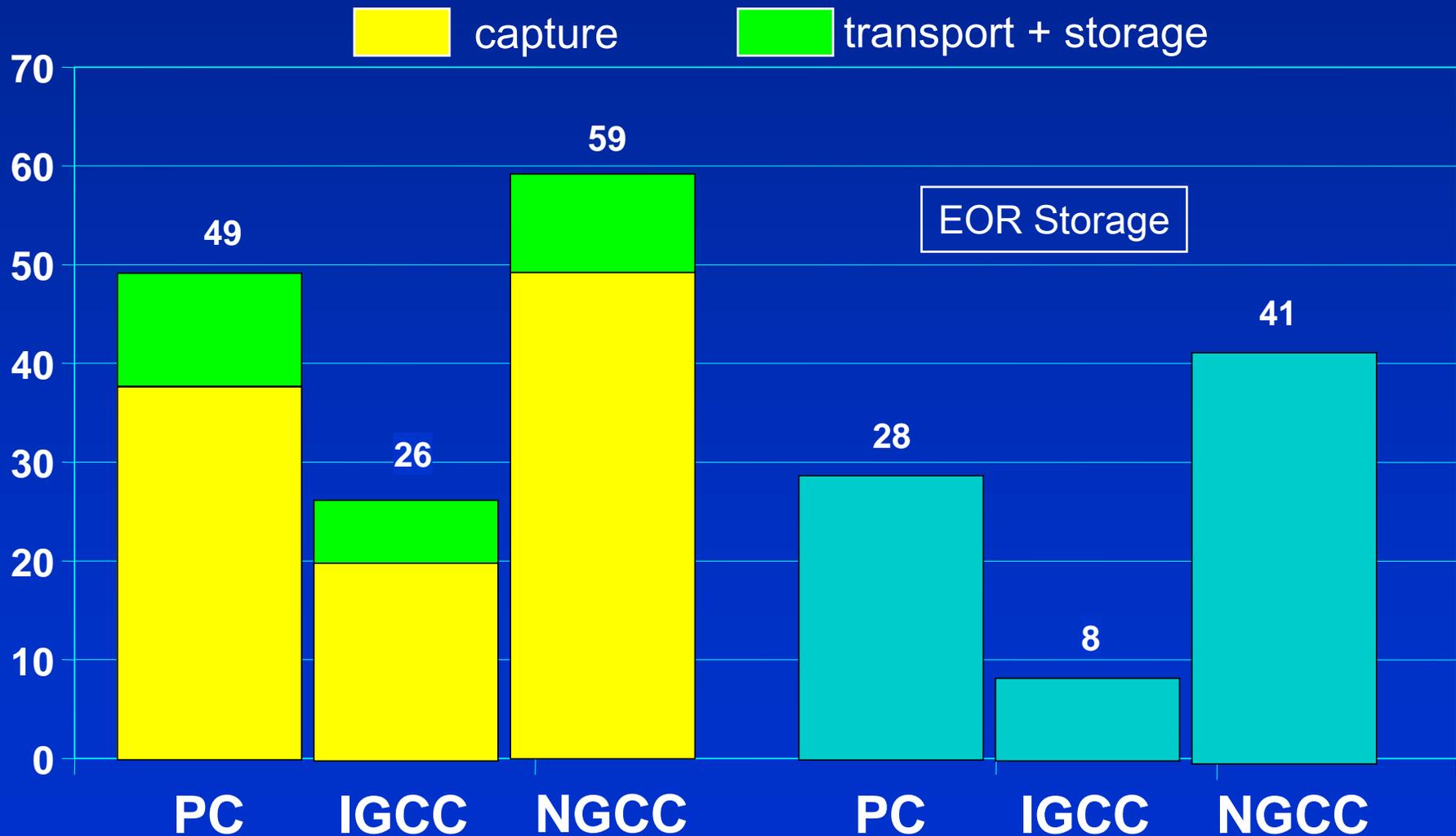
CO₂ Emission Rates (kg/MWh)



Cost of Electricity (COE) (Levelized \$/MWh)



Cost of CO₂ Avoided (\$/tonne CO₂)



Case 2:

*Effects of Fuel Price
and Plant Dispatch*

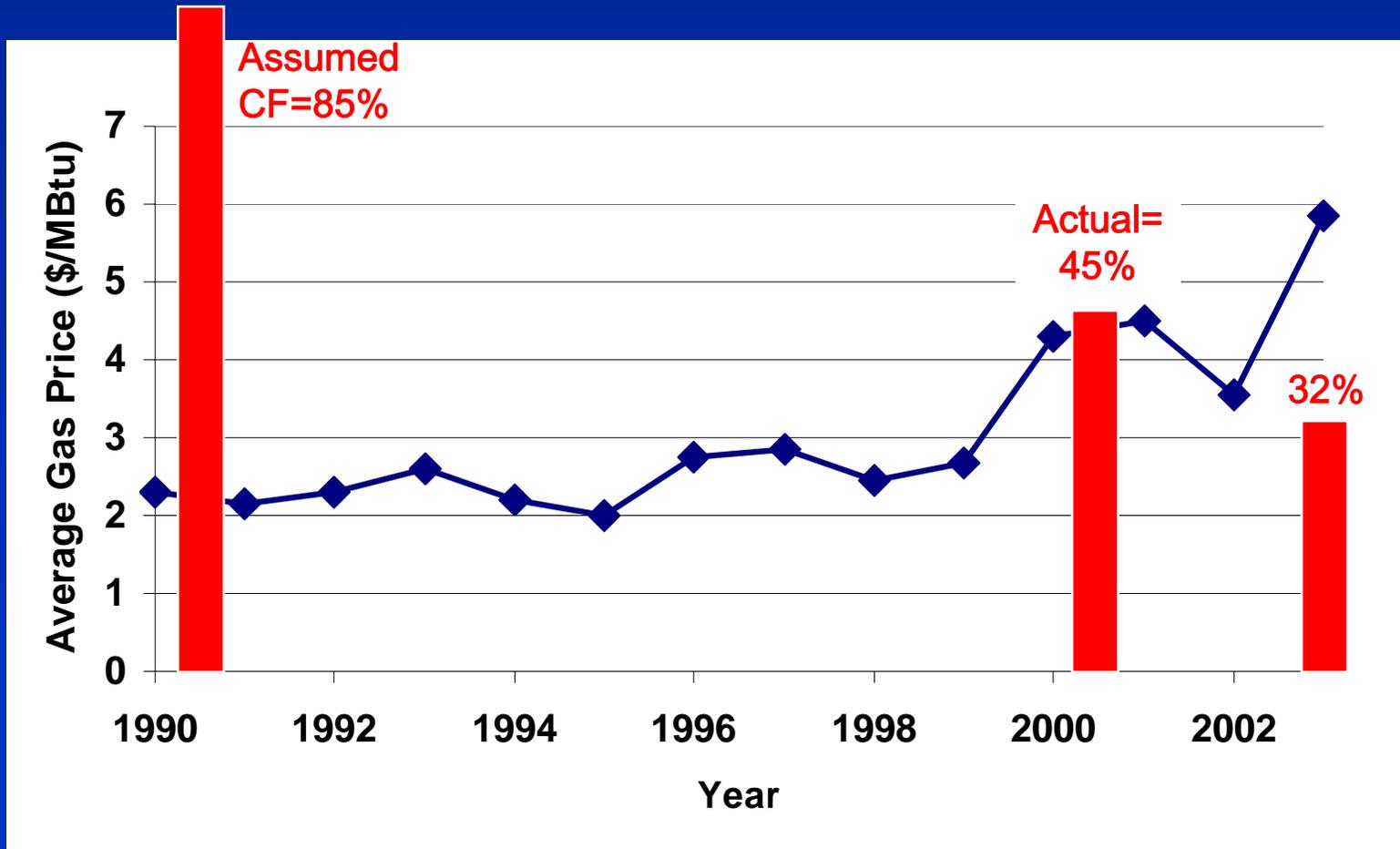
Differences in Total Variable Operating Cost (\$/MWh)

(Includes fuel, chemicals, utilities, wastes and byproducts)

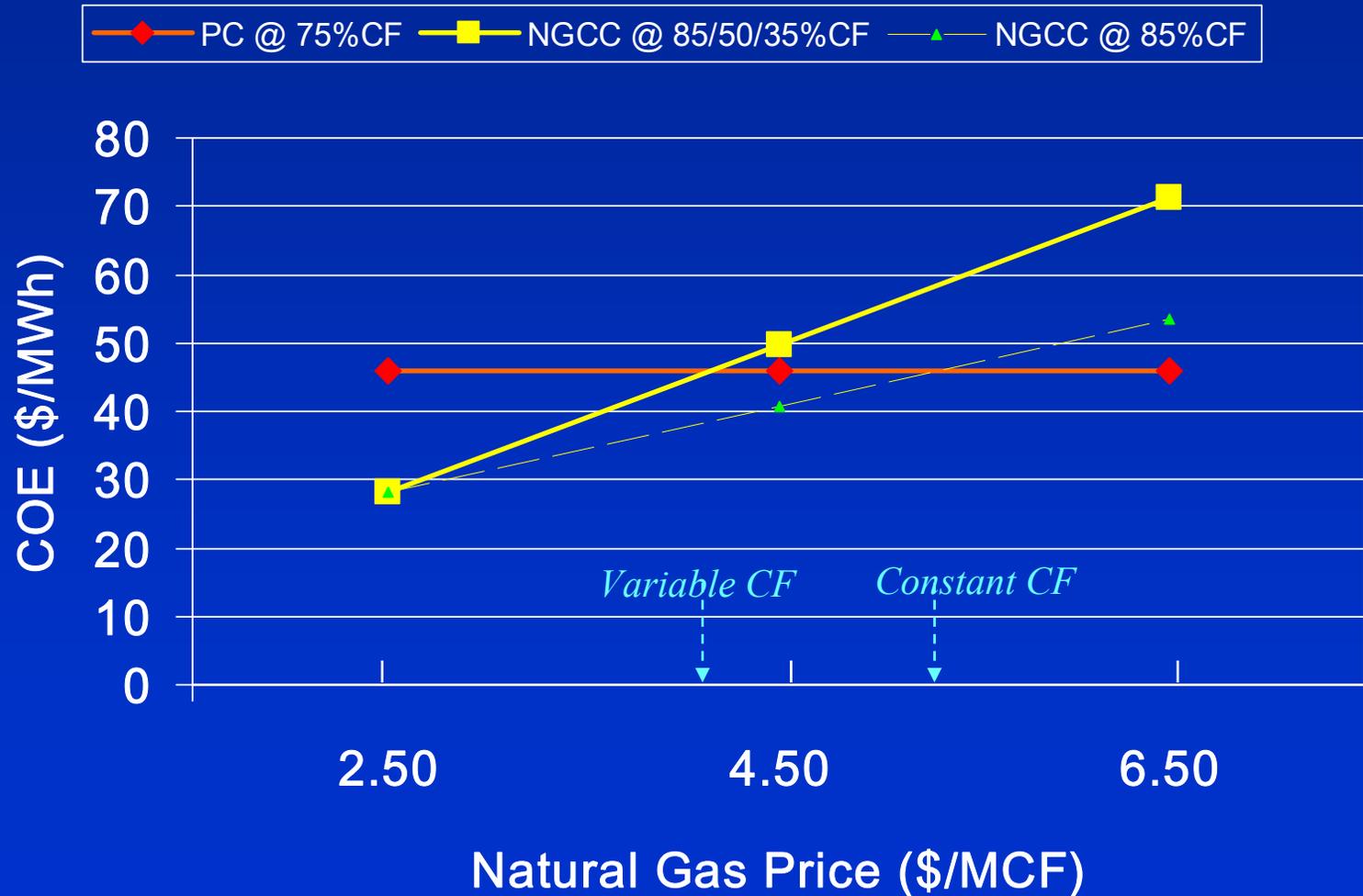
Plant	Fuel Price	Ref. Plant
PC	\$1.27/ MBtu	(Base case)
IGCC	\$1.27/ MBtu	~ 0
NGCC	\$2.50/MCF	+ 3
	\$4.50	+15
	\$6.50	+27

Implication: *Decreasing dispatch of NGCC at higher gas prices if coal plants are available*

Recent Trends for NGCC Plants



Effect of Variable Capacity Factor on Breakeven NG Price



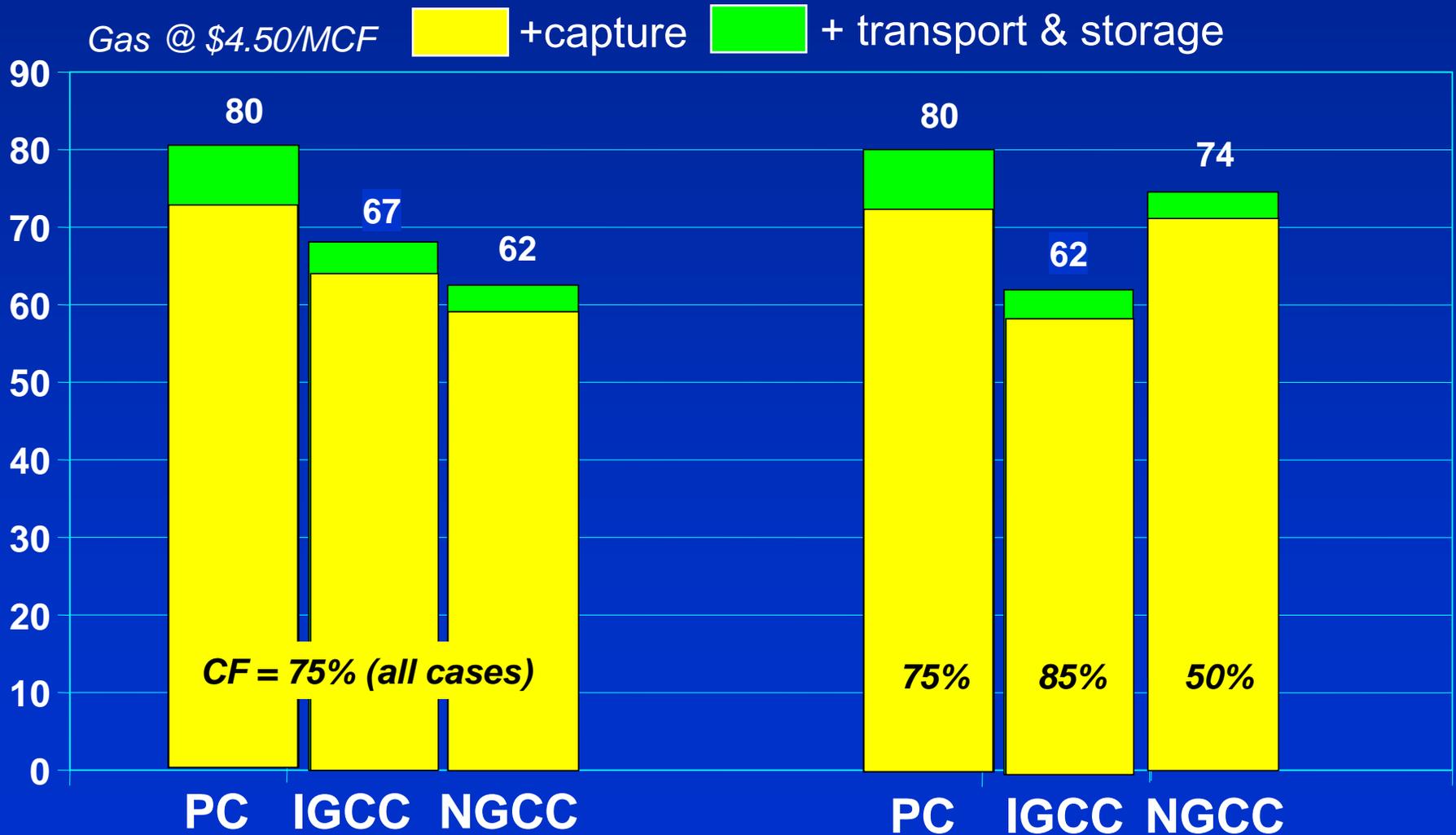
Differences in Total Variable Operating Cost w/ CCS (\$/MWh)

(Includes fuel, chemicals, utilities, wastes and byproducts)

Plant	Fuel Price	CCS Plant
PC	\$1.27/ MBtu	(Base case)
IGCC	\$1.27/ MBtu	- 10
NGCC	\$2.50/MCF	- 7
	\$4.50	+ 8
	\$6.50	+38

Implication: Increasing dispatch of IGCC

Cost of Electricity (\$/MWh) w/ Differential Capacity Factors



Case 3:

*Effects of IGCC
Financing & Operation*

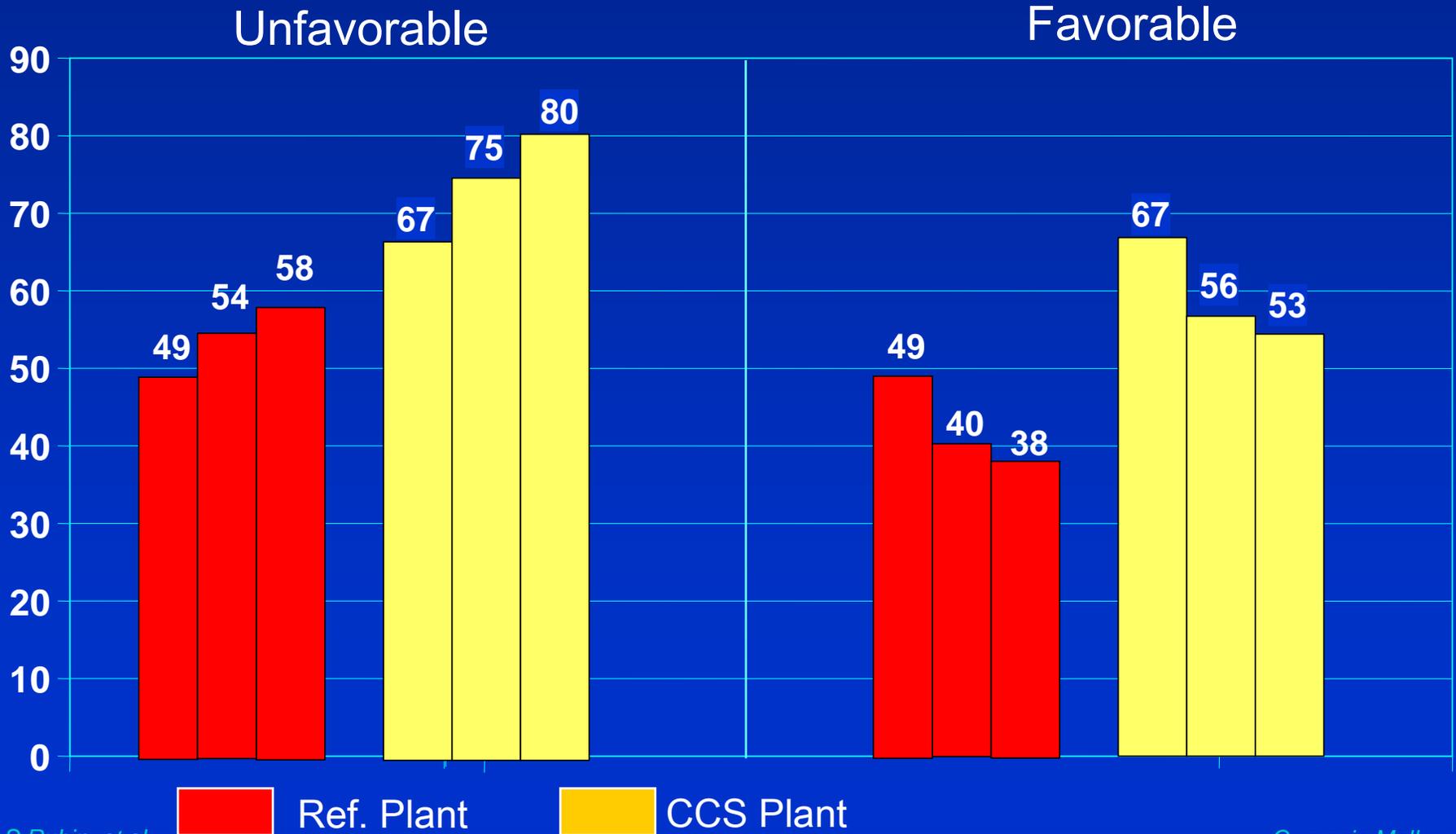
IGCC — Can You Build It?

- Today, IGCC plants are generally more expensive than conventional PC plants, based on expected COE
- IGCC technology is also perceived as “riskier” by the financial community, and by many utility companies
- Several efforts underway to develop more attractive financing and ownership arrangements to facilitate deployment of IGCC in the U.S. power market

Two New Scenarios for IGCC Financing and Operation

- *Unfavorable*
 - Higher fixed charge rate of 17.3%
(20% risk premium on rates of return)
 - Lower plant utilization (CF=70%)
- *Favorable*
 - Lower fixed charge rate of 10.4%
(e.g., Harvard 3-Party Covenant)
 - Higher plant utilization (CF=80%)

Cost of Electricity (\$/MWh) for the Two New Scenarios



Case 4:

*CCS Energy Penalty Impacts
on Resource Consumption and
Multi-media Emissions*

Energy Penalty Defined

- Commonly defined as the reduction in plant output for a constant fuel input (i.e., plant derating) due to CCS
- More general definition is based on change in net plant heat rate or efficiency (η):

$$EP = 1 - (\eta_{\text{CCS}} / \eta_{\text{ref}})$$

Case study energy penalties:

PC = 24%, IGCC = 14%, NGCC = 15%

An Alternative Definition

- An alternative definition of the energy penalty is the increase in plant inputs per unit of output (EP*):

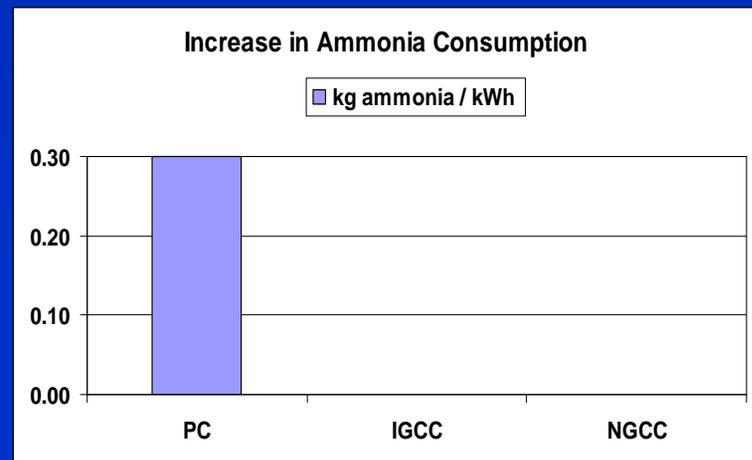
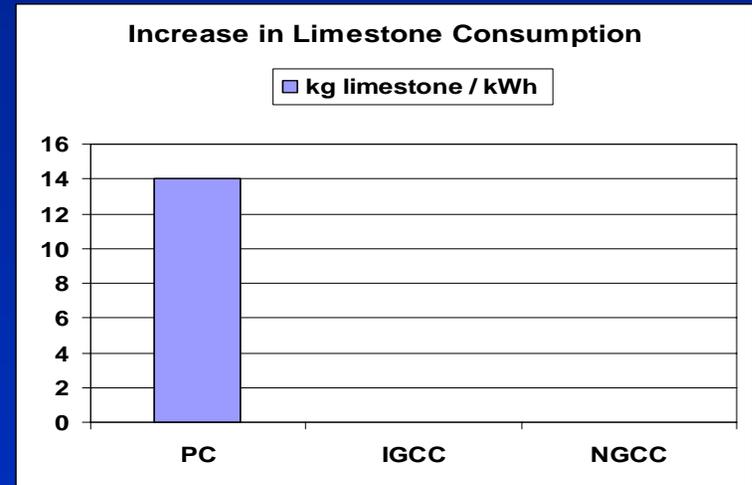
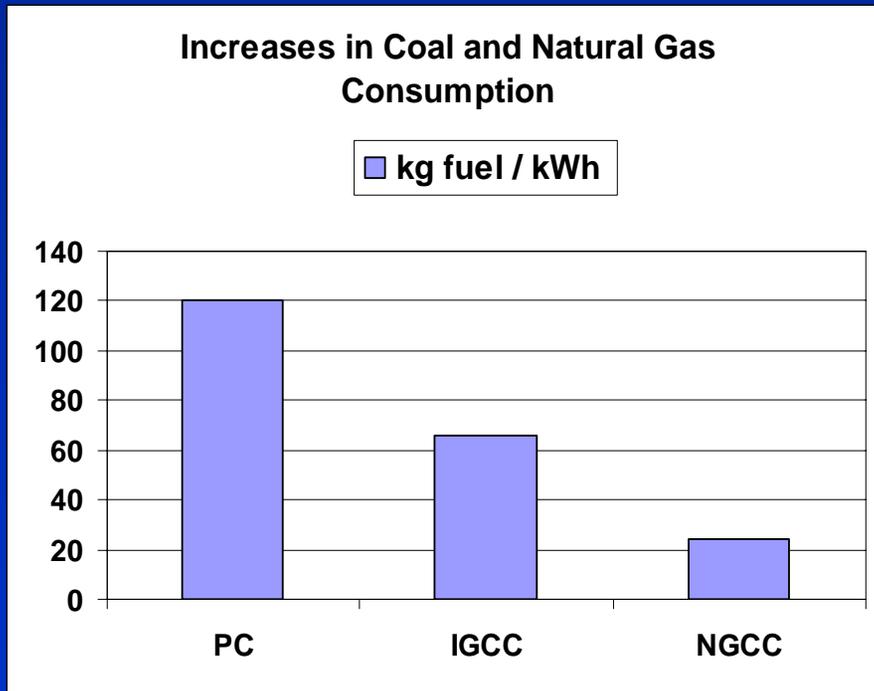
$$EP^* = EP / (1 - EP)$$

- This measure reflects increases per unit of product for:
 - Plant fuel consumption
 - Other resource requirements
 - Solid and liquid wastes
 - Air pollutants not captured by CCS
 - Upstream (life cycle) impacts

CCS Energy Penalties

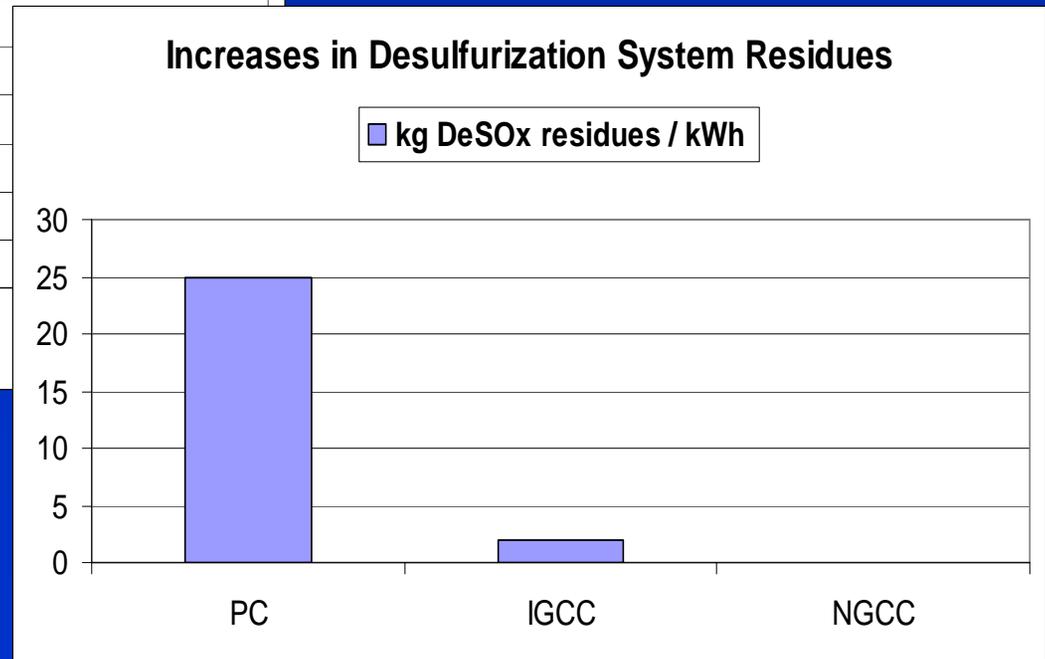
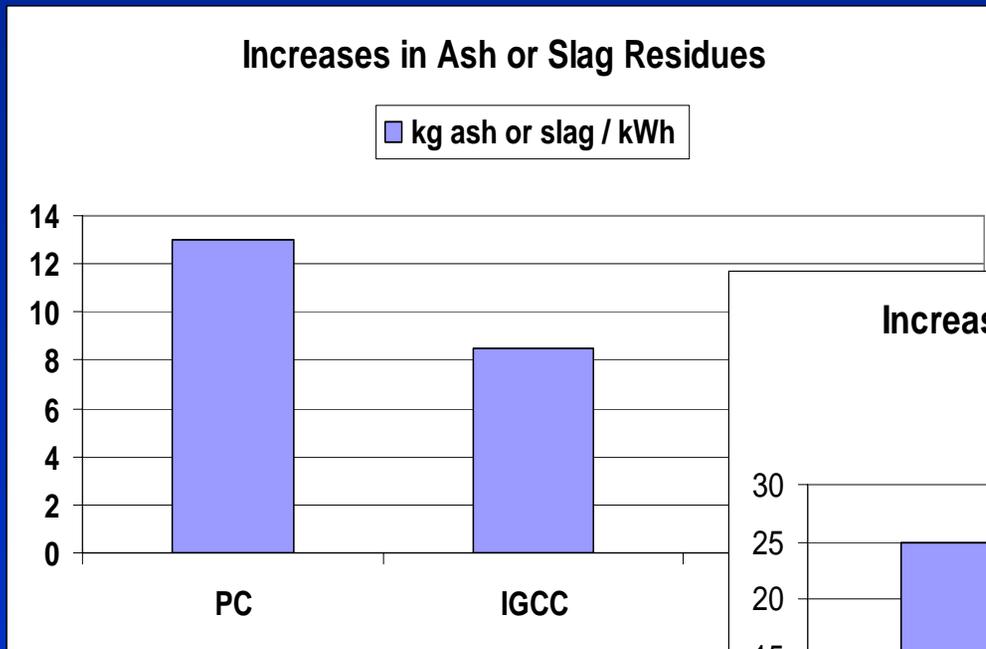
- Case study energy penalties for current technologies based on EP*:
 - PC = 31 %
 - IGCC = 16%
 - NGCC = 18%

Increases in Fuel and Reagent Consumption*



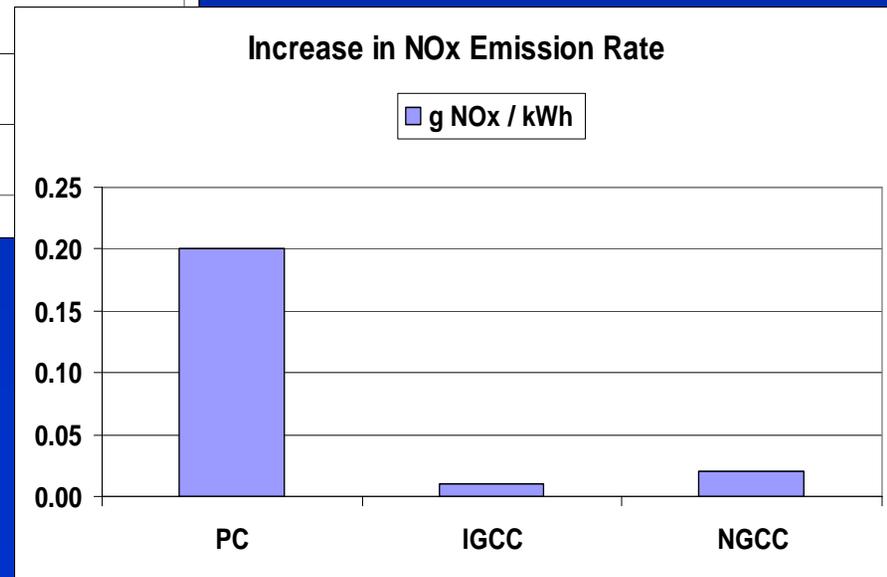
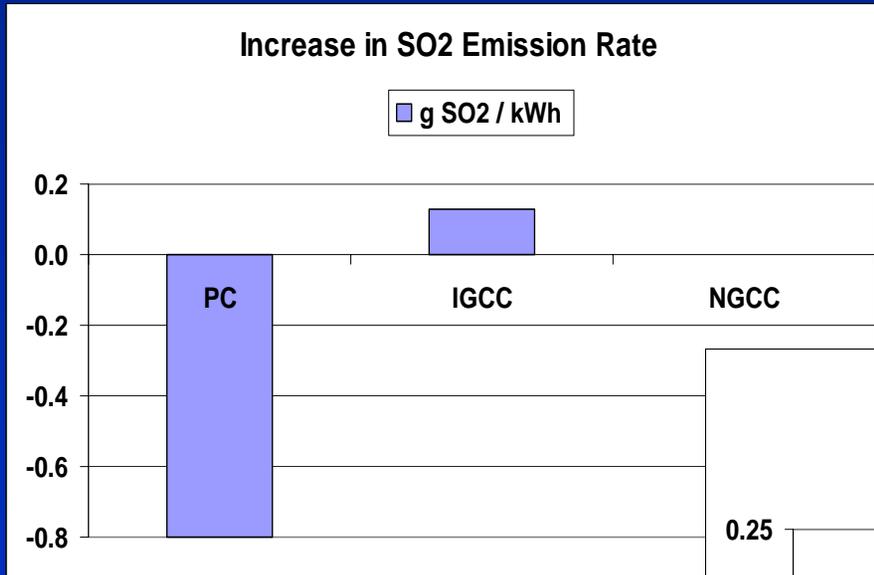
*Based on Illinois #6 coal

Increases in Solid Wastes & Plant Byproducts*



*Based on Illinois #6 coal

Increases in Air Emission Rates*



*Based on Illinois #6 coal

The Critical Importance of Technology Innovation

- New or improved technologies for power generation and CO₂ capture can lower the cost of CCS, *and* significantly reduce adverse secondary impacts by:
 - Improving overall plant efficiency
 - Reducing CCS energy penalties
 - Maximizing co-capture of other pollutants

Work in Progress at CMU

- *Incorporate performance and cost models of advanced power systems and CO₂ capture options:*
 - Oxyfuel combustion
 - ITM oxygen production
 - Advanced IGCC designs
 - Advanced NGCC
- *Expand and regionalize transport & storage models*
- *Comparative analyses of CO₂ capture options for new and existing power plants*
 - Advanced PC, NGCC and IGCC systems
 - Repowering or rebuild of existing units
- *Assessments of R&D Benefits*