



Bench-Scale Development & Testing of a Novel Adsorption Process for Post-Combustion CO₂ Capture

DOE Funding Award DE-FE-007948

Project-Kickoff Meeting

November 22, 2011

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Middlesex, NJ

Executive Summary

- The InnoSeptra process utilizes physical sorption to produce dry CO₂ at high purity (>99%) and high recovery (>90%) from the flue gas taken after the FGD.
- Potential for more than 50% reduction in the capital and more than 40% reduction in parasitic power for CO₂ capture compared to MEA based on lab scale testing
- The process needs to be tested with flue gas containing SO_x, and Hg, and at a bigger scale (>1 tons per day) to address the process risks, and the effect of contaminants
 - This DOE project will address various process risks and scale up issues through lab testing and field testing, process simulation, and detailed economic evaluation

Project Objectives

The overall project objective

- Demonstrate the effectiveness of the InnoSeptra sorbent-based post-combustion CO₂ capture technology, to achieve at least 90% CO₂ removal with a potential pathway for no more than a 35% increase in cost of electricity as a retrofit to coal-fired utility plants

Specific project objectives

- Confirm the design basis for bench-scale testing based on lab scale results and process modeling
- Design, build and test a bench scale unit in the lab
- Test the bench scale unit on actual coal-based flue gas from a power plant
- Perform scale up modeling, process and equipment design, engineering, and costing for installation of the technology at a commercial 550 MW power plant to estimate CO₂ capture cost

Background Information

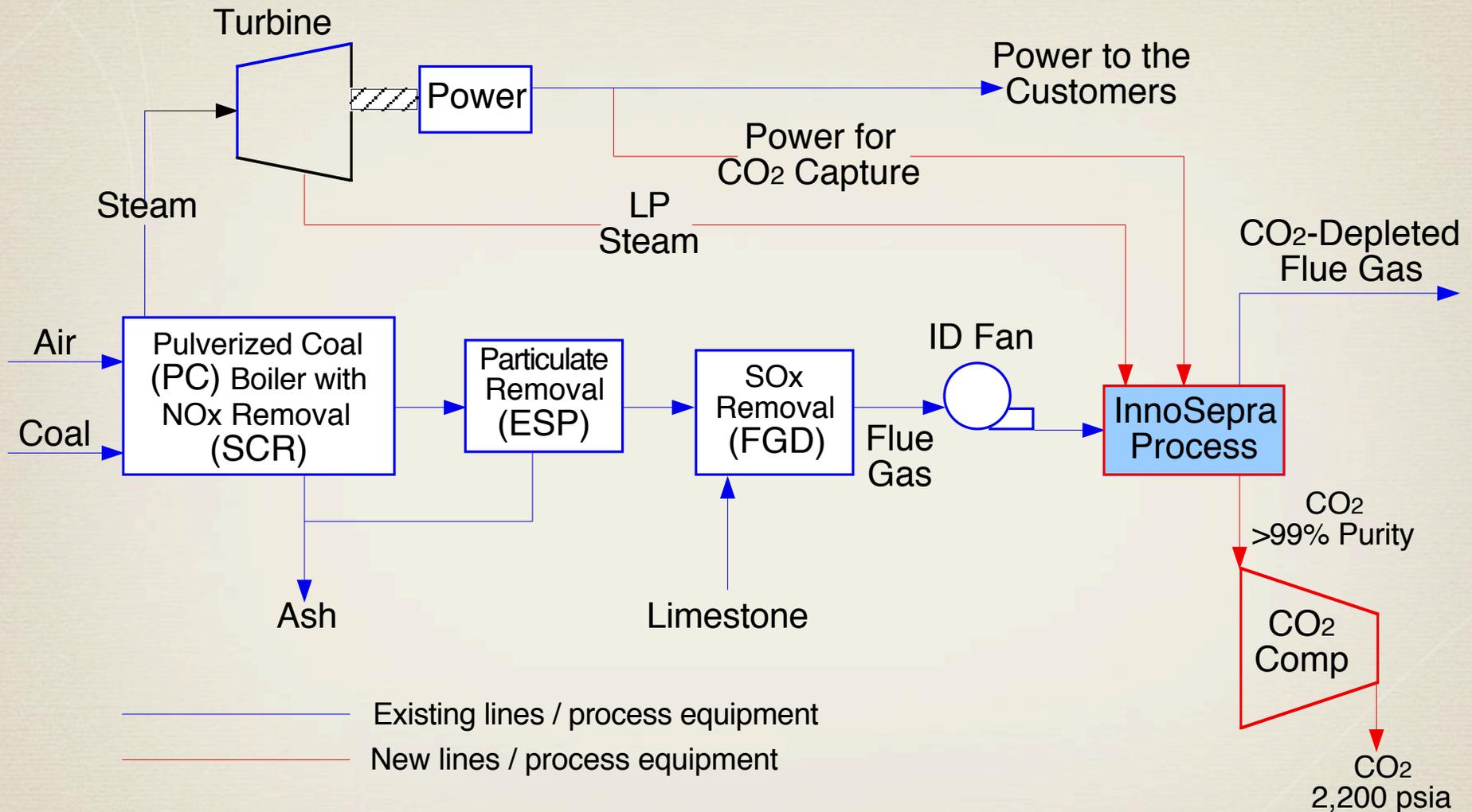
Post-Combustion CO₂ Capture Challenges

- Very large gas volumes at low pressure (~1.05 bara)
- Low CO₂ partial pressure, <150 mbar
- The impurities in the flue gas particularly NO_x, SO_x, Hg, and particulates can have a significant impact on the solvents and sorbents used for CO₂ capture.
- Significant loss in power generation efficiency due to CO₂ capture, 7-10% absolute.

Sorbent-Based CO₂ Capture

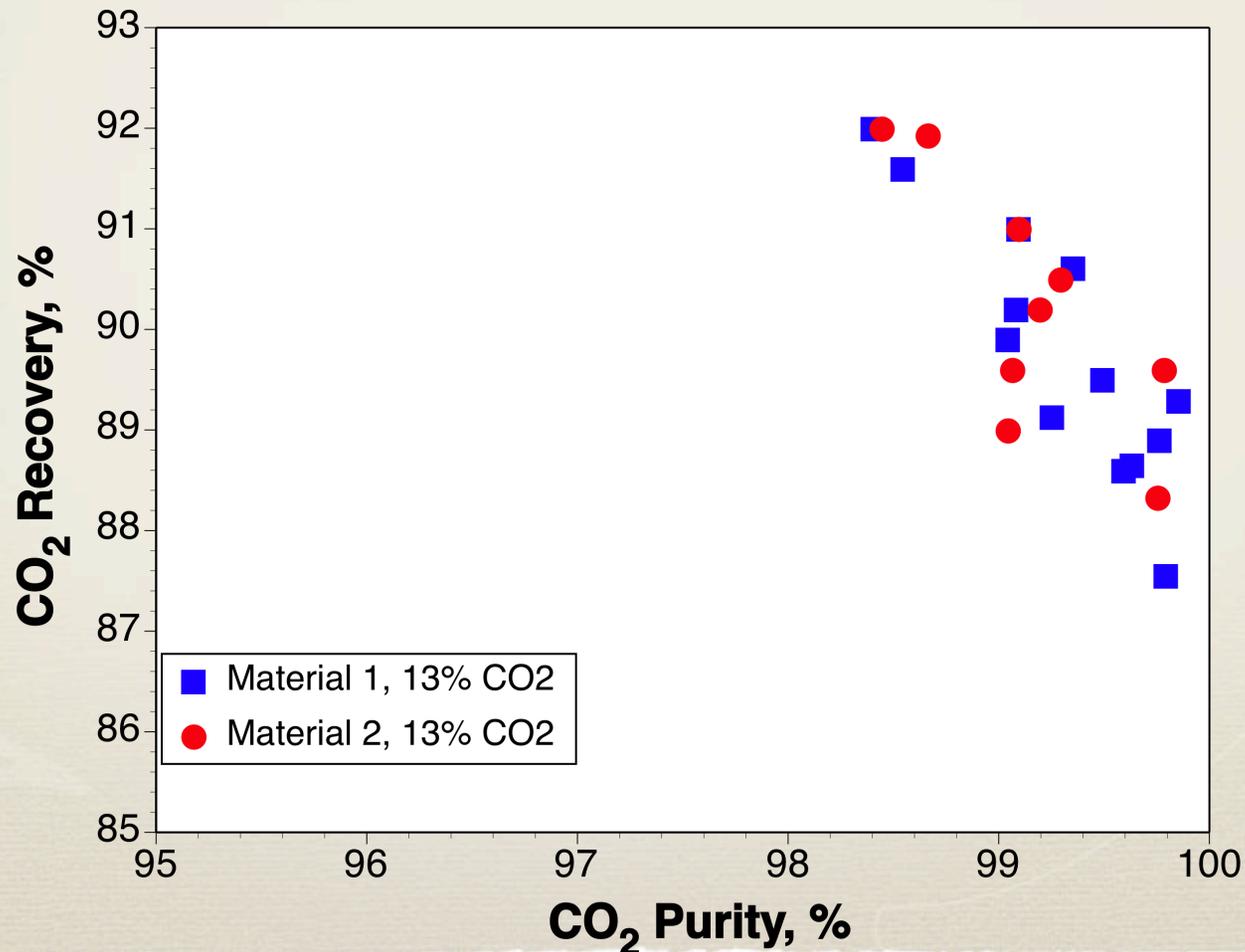
- **Capture CO₂ by physical sorption**
 - 140-240 kcal/kg heats of adsorption
 - Significantly lower than the total energy for amine systems
- **Capture CO₂ by chemical reaction** with amines / carbonates
 - 740-940 kcal/kg heats of reaction
 - Similar to the amine-based absorption systems
 - Ex. $\text{Na}_2\text{CO}_3 + \text{CO}_2 + \text{H}_2\text{O} \text{-----} > 2 \text{NaHCO}_3$
 $\Delta H_{\text{rxn}} = -740 \text{ Kcal/kg of CO}_2$

CO₂ Capture from Power Plants

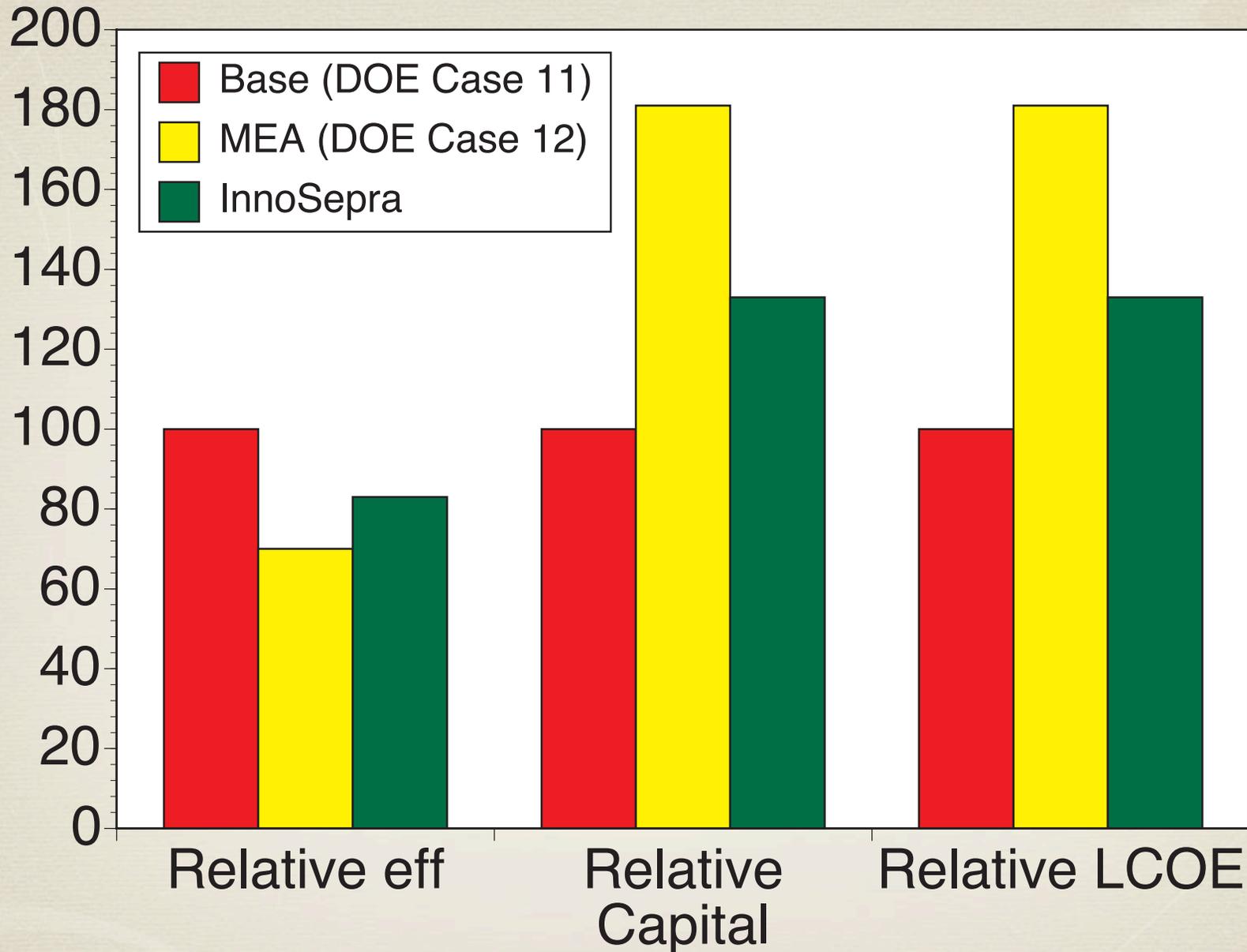


CO₂ Capture Testing Summary

- More than 10 commercial and laboratory materials tested for over 4 years, thousands of complete cycles
- 90% CO₂ recovery and over 99% purity under optimized conditions for a feed containing 13-15% CO₂
- Possible to regenerate below 100°C with potential parasitic power consumption below 450 Kcal/Kg of CO₂.



Comparison with MEA for DOE Baseline Study



“Cost and Performance Baseline for Fossil Energy Plants”, DOE/ NETL-2007/1281, Aug 2007.
(http://www.netl.doe.gov/energyanalyses/pubs/Bituminous%20Baseline_Final%20Report.pdf)

The DOE Project

Project Scope

In the first budget period InnoSeptra will

- Experimentally determine the adsorption isotherms, and measure the heat and mass transfer rates
- Determine the effect of contaminants on the process performance
- Conduct a preliminary technical and economic feasibility study to demonstrate the commercial merits

In the second budget period InnoSeptra will

- Design and construct the bench scale unit
- Commission the bench scale unit in the laboratory and conduct tests using a synthetic flue gas feed

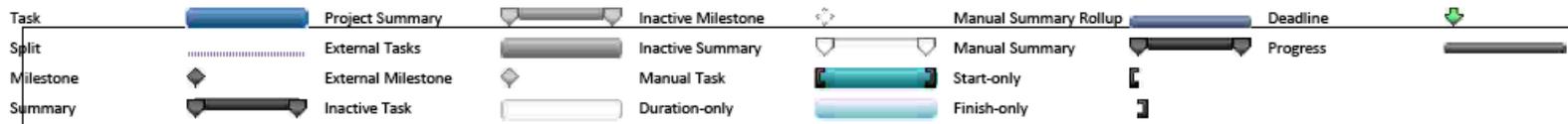
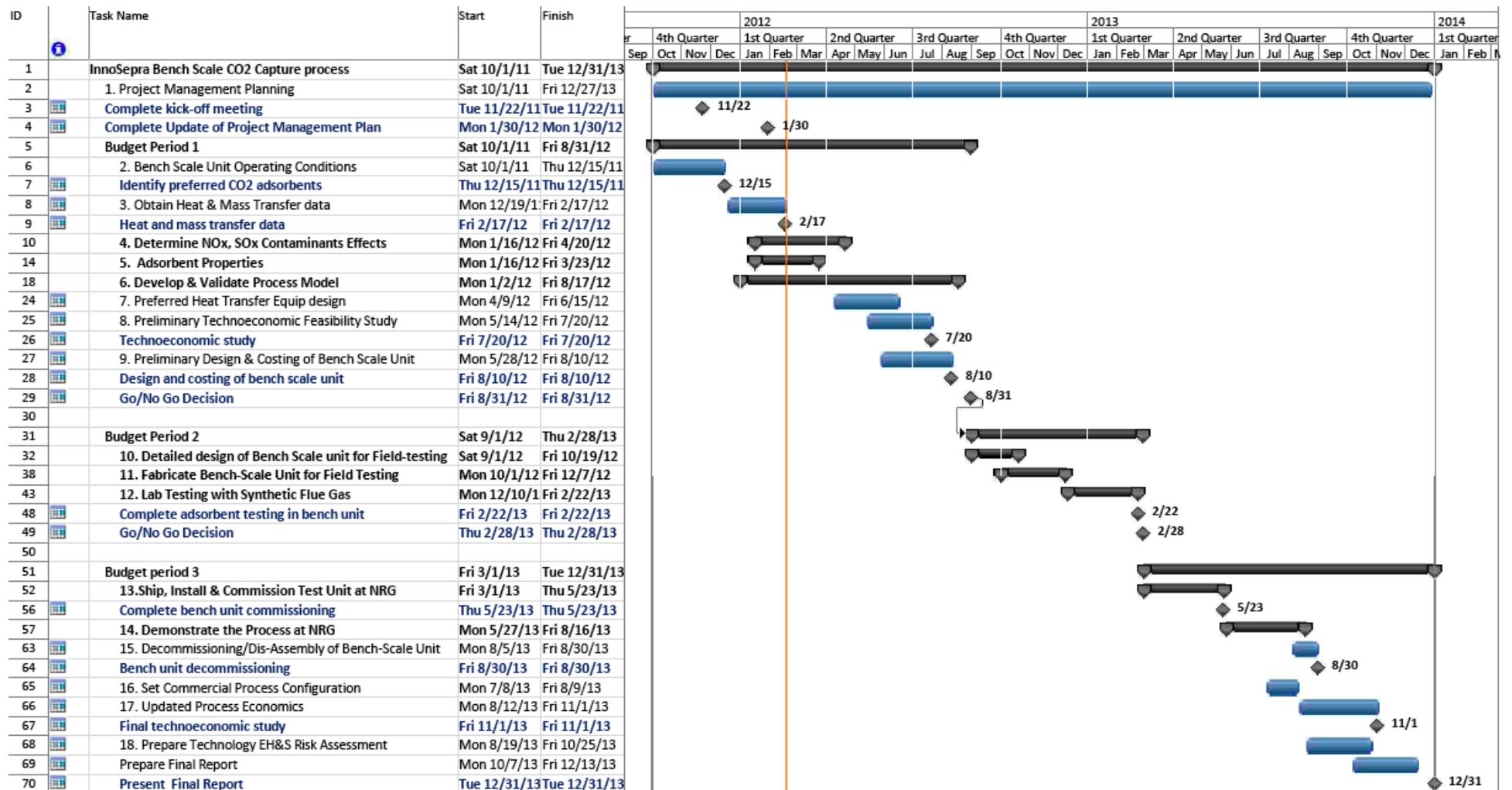
In the third budget period InnoSeptra will

- Commission the unit at the NRG WA Parish coal fired power station and determine the performance of the InnoSeptra process treating a flue gas from the FGD unit
- Update the technical and economic feasibility study based on lab and field tests
- Perform a preliminary technology environmental health and safety (EH&S) risk assessment

Project Budget

Source	BP1 Oct 1, 2011 to Aug 31, 2012	BP2 Sep 1, 2012 to Feb 28, 2012	BP3 Mar 1, 2013 to Dec 31, 2013	Total
Dept of Energy	\$850,187	\$696,204	\$1,048,494	\$2,529,885
Cost Share	\$212,547	\$174,052	\$268,756	\$655,355
Total Project	\$1,062,734	\$870,256	\$1,317,250	\$3,185,240

Project Timeline



Key Project Milestones

Budget Period 1

- Project kickoff meeting with DOE-NETL (11/22/2011)
- Identify two adsorbents with highest performance (12/20/11)
- Heat & mass transfer data, sorption isotherms (3/23/12)
- Preliminary techno-economic evaluation (7/20/12)
- Rigorous process model (8/17/12)
- Design and costing of the bench scale unit (8/10/12)

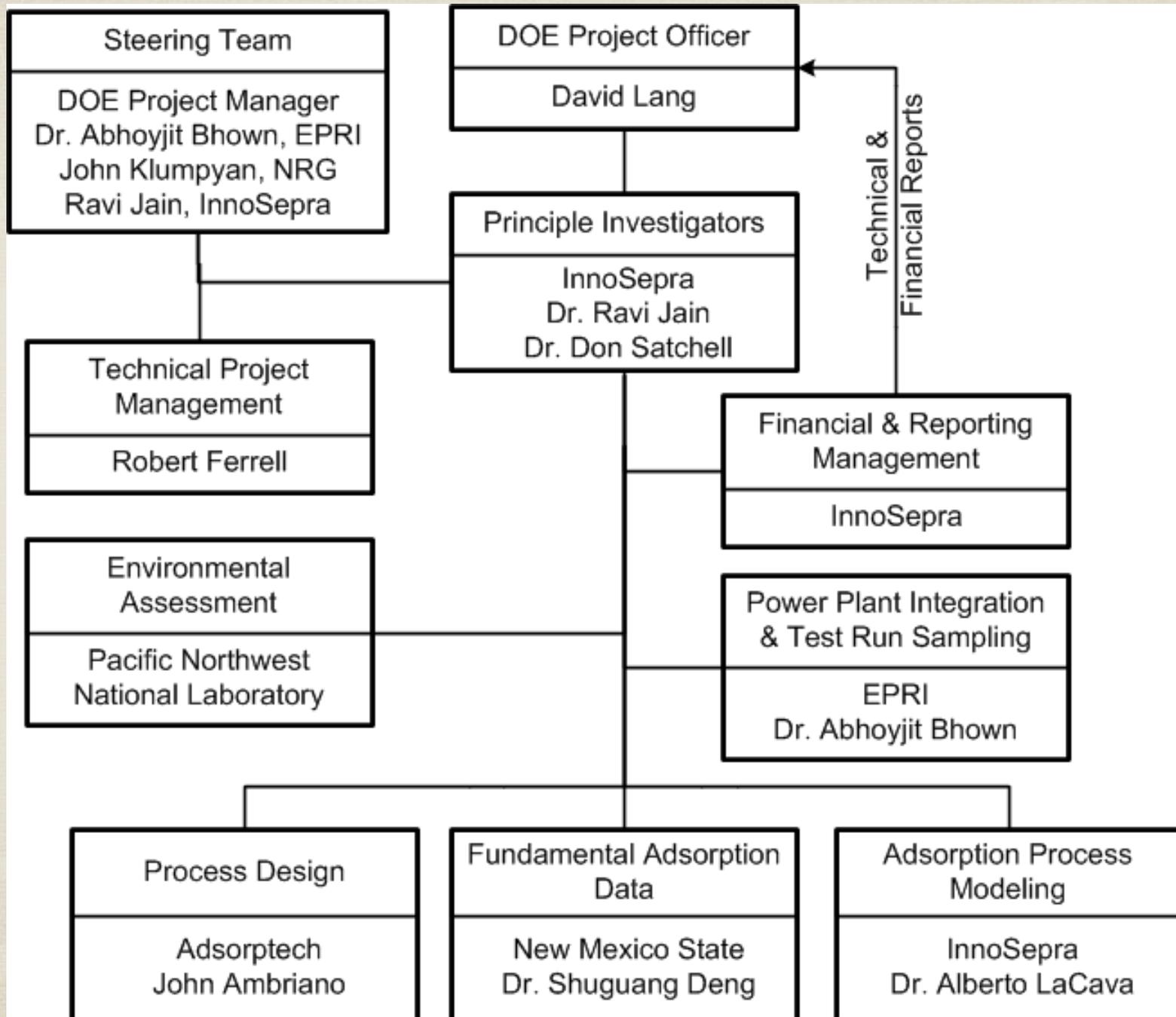
Budget Period 2

- Design and fabrication of the bench scale unit (12/7/12)
- Testing of preferred adsorbents in the bench scale unit (2/22/13)

Budget Period 3

- Commission bench scale unit at the NRG plant (5/23/13)
- Complete field testing of bench scale unit (8/30/13)
- Complete final techno-economic study (11/1/13)

Project Organization Chart



Success Criteria at Decision Points

Decision Point	Date	Success Criteria
Go - No Go decision to build the bench scale unit	8/31/12	<ol style="list-style-type: none">1. Limiting the projected increase in LCOE to below 60% based on lab scale testing and detailed techno-economic evaluation2. Provide a potential pathway for achieving <35% increase in LCOE
Completion of bench scale unit testing in the lab	2/28/13	<ol style="list-style-type: none">1. Complete bench scale testing of preferred adsorbents in the lab and select preferred adsorbent for field testing
Project Closeout	12/31/13	<ol style="list-style-type: none">1. Limiting the projected increase in LCOE to below 60% based on bench scale testing in the field and independent techno-economic evaluation2. Provide a potential pathway for achieving <35% increase in LCOE

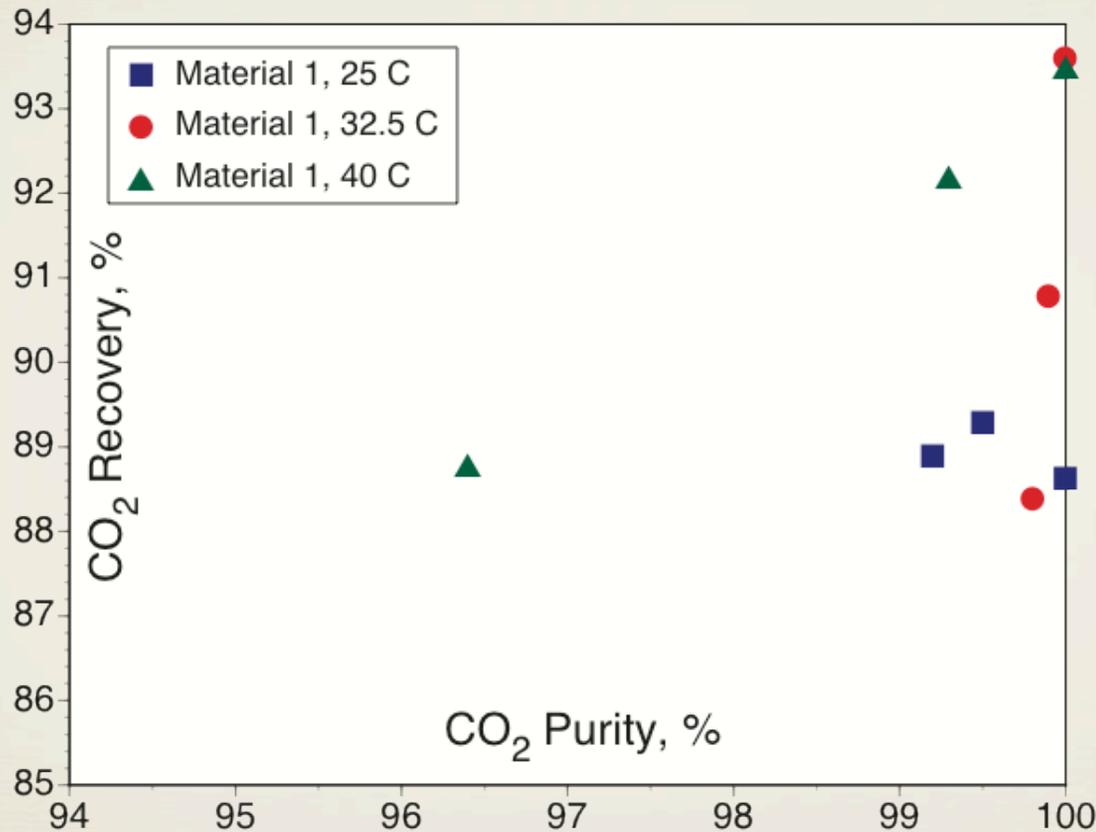
Project Risk Register

Description of Risk	Probability	Impact	Risk management
Technical Risks			
CO ₂ Capture & Regeneration	Moderate	Moderate	Modify process design
Heat Transfer Design & Performance	Moderate	High	Modify heat transfer design
Moisture and Contaminants Removal	Moderate	High	Improve contaminants control steps
Technical Risks			
Project Team Availability	Low	Moderate-High	Identify backup resources
Suitability/ Availability of Sites	Low-Moderate	Low-Moderate	Identify backup sites
Component manufacturing risk	Low	Moderate	Simplify key components design, identify alternate suppliers

Technical Merit and Approach

Key Tasks

- Task 2: Laboratory testing to identify preferred adsorbents
 - Identify two adsorbents with highest productivity, CO₂ recovery, and CO₂ purity



- Task 3: Obtain heat and mass transfer data
 - Heat and mass transfer data for various process configurations

Technical Merit and Approach

- **Task 5: Adsorbent Properties**
 - Determine adsorbent kinetics, isotherms, and physical properties
- **Task 6: Develop and Validate Process Model**
 - Rigorous process simulation model incorporating adsorbent properties, heat transfer equipment, and lab scale process data
- **Task 8: Complete Preliminary Technical and Economic Feasibility Study**
 - Obtain CO₂ capture cost and LCOE based on lab test results and process simulation model
- **Tasks 10 and 11: Design and Fabrication of Bench Scale Unit**
 - Design and fabricate a bench unit capable of processing at least 1 tons per day CO₂ for lab and field testing
- **Task 12: Lab Testing of Bench Scale Unit**
 - Test the bench scale unit in the lab with the preferred adsorbents and synthetic flue gas (moisture-saturated, ~15% CO₂, 50-100 ppm SO₂, 50-100 ppm NO_x)

Technical Merit and Approach

- Task 13: Install and commission the bench scale unit at NRG's W.A. Parish plant
- Task 14: Testing with actual flue gas for up to 8 weeks
 - EPRI sampling to measure process performance
 - Analysis of used adsorbents to determine the effect of contaminants on adsorption capacity, and adsorbent life
- Task 16: Set commercial unit process configuration
- Task 17: Independent techno-economic analysis
 - EPRI will use a contractor for the techno-economic analysis
- Task 18: Prepare EH&S risk assessment (PNNL)

Acknowledge and Disclaimer

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