

Low-Pressure Membrane Contactors for CO₂ Capture (DE-FE0007553)

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Membrane Technology and Research, Inc.

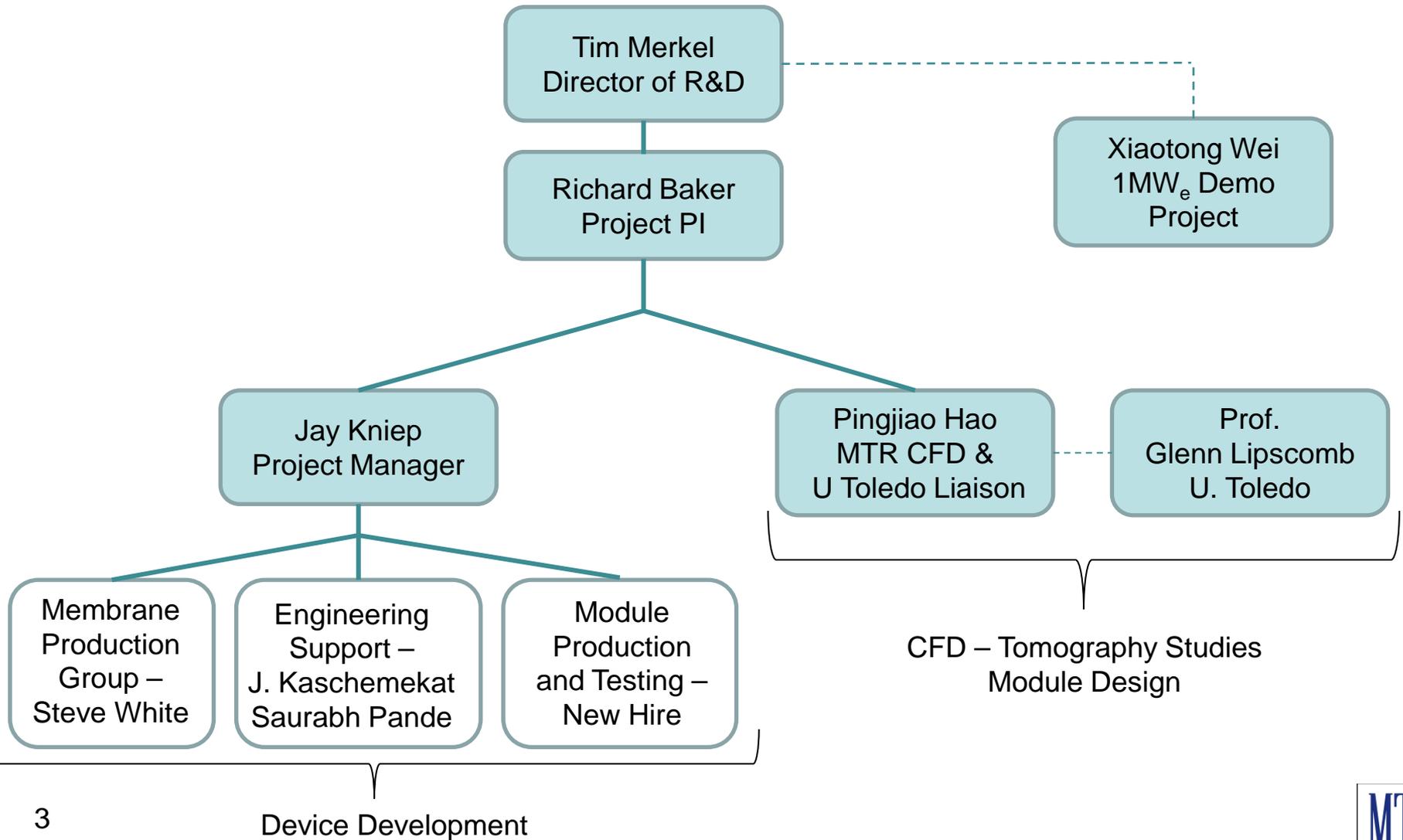
Project Kickoff Meeting

Tuesday, November 29, 2011

Program Objectives

- Low Cost, Large Area Modules (500 m² +)
- Smaller Foot Print, Less Manifolds
- Reduce Energy Cost by Lowering Module Pressure Drop
 - Pressure Drop in Modules = Parasitic Energy Loss
 - 1 PSI Pressure Drop = 2.5 MW_e of Compression Power for a 500 MW_e Coal-Fired Power Plant
- Year 1- 5 PSI , Year 2- 2.5 PSI , Year 3- 1.5 PSI

The Project Team



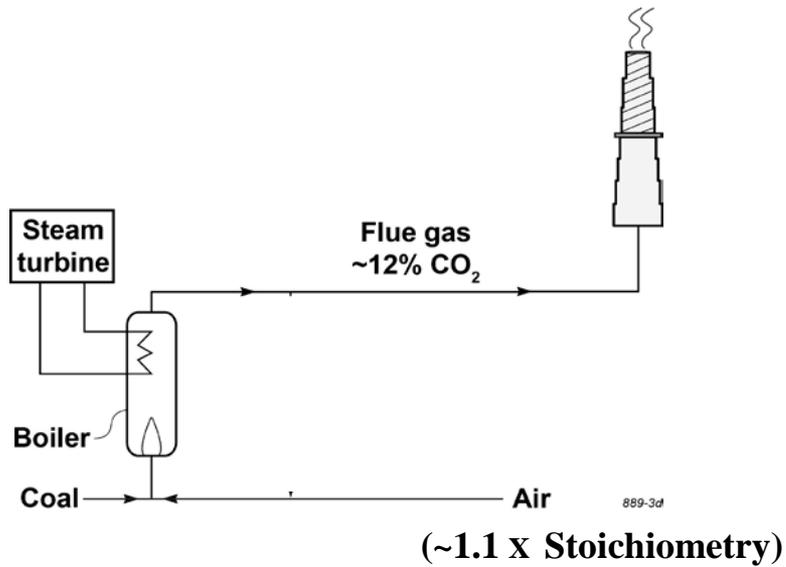
Program Overview

- Process Introduction
- Our Current Approach
- Issues
- Program Approach
- CFD and Tomography Measurements
- Tasks, Schedule, Budget

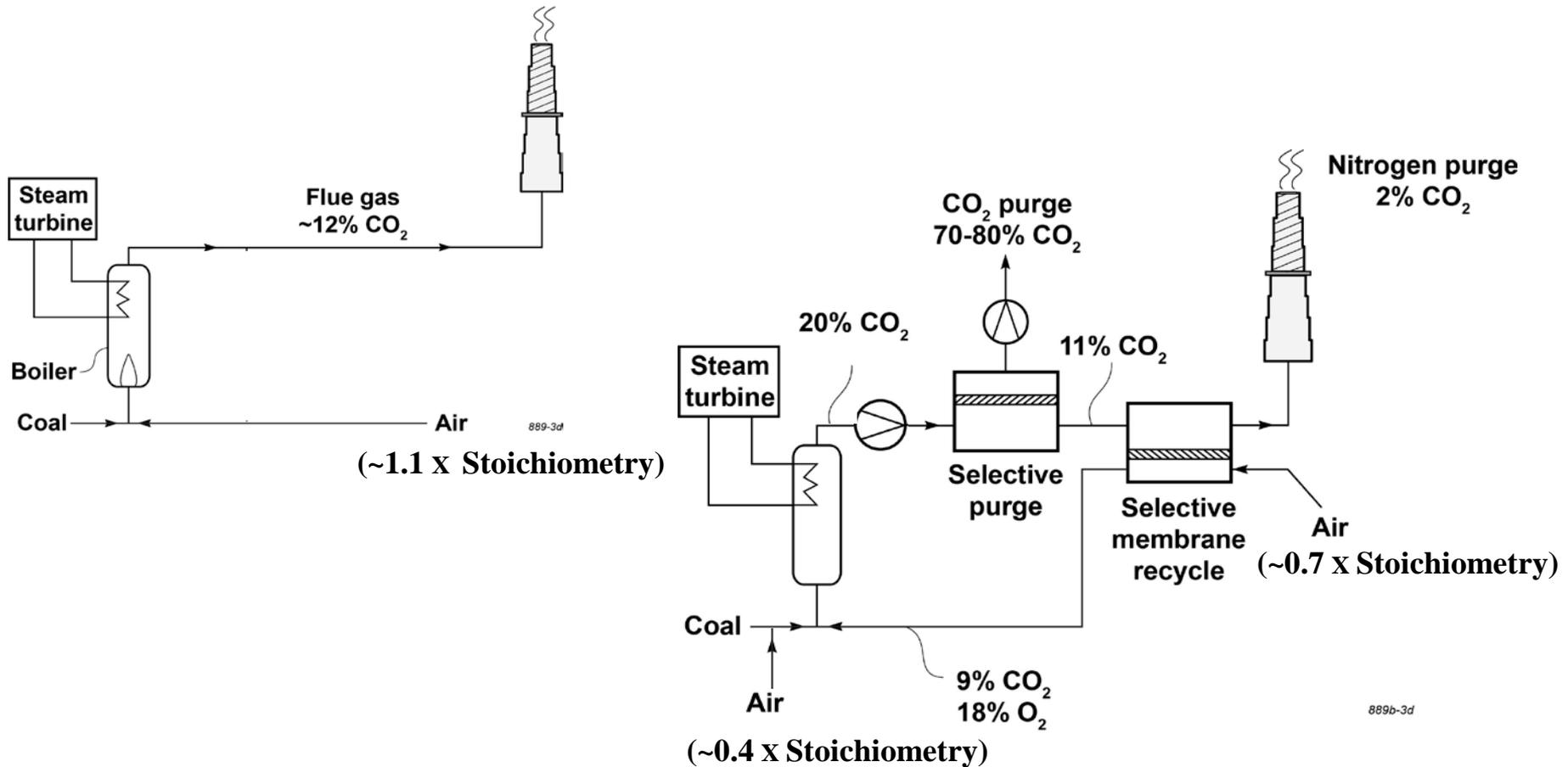
Program Overview

- Process Introduction
 - Coal
 - Gas Turbine
 - Our Vision
- Our Current Approach
 - Nested Spiral-Wound Modules
 - Large Plate and Frame Modules

CO₂ Separation from Coal Flue Gas

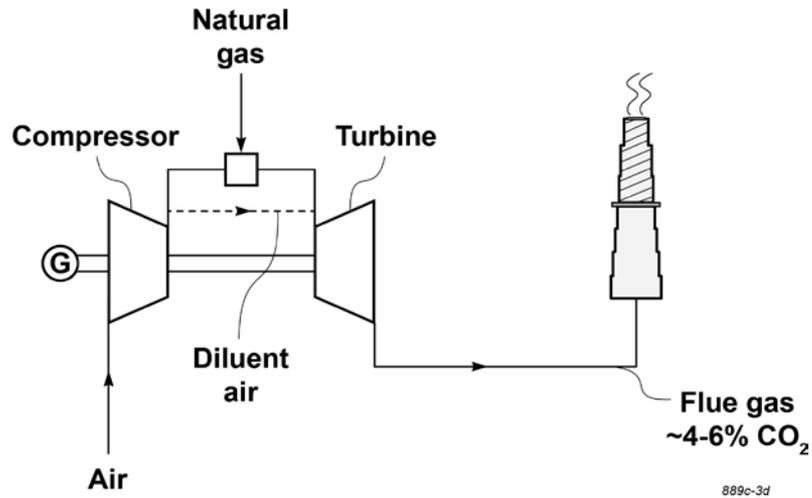


CO₂ Separation from Coal Flue Gas



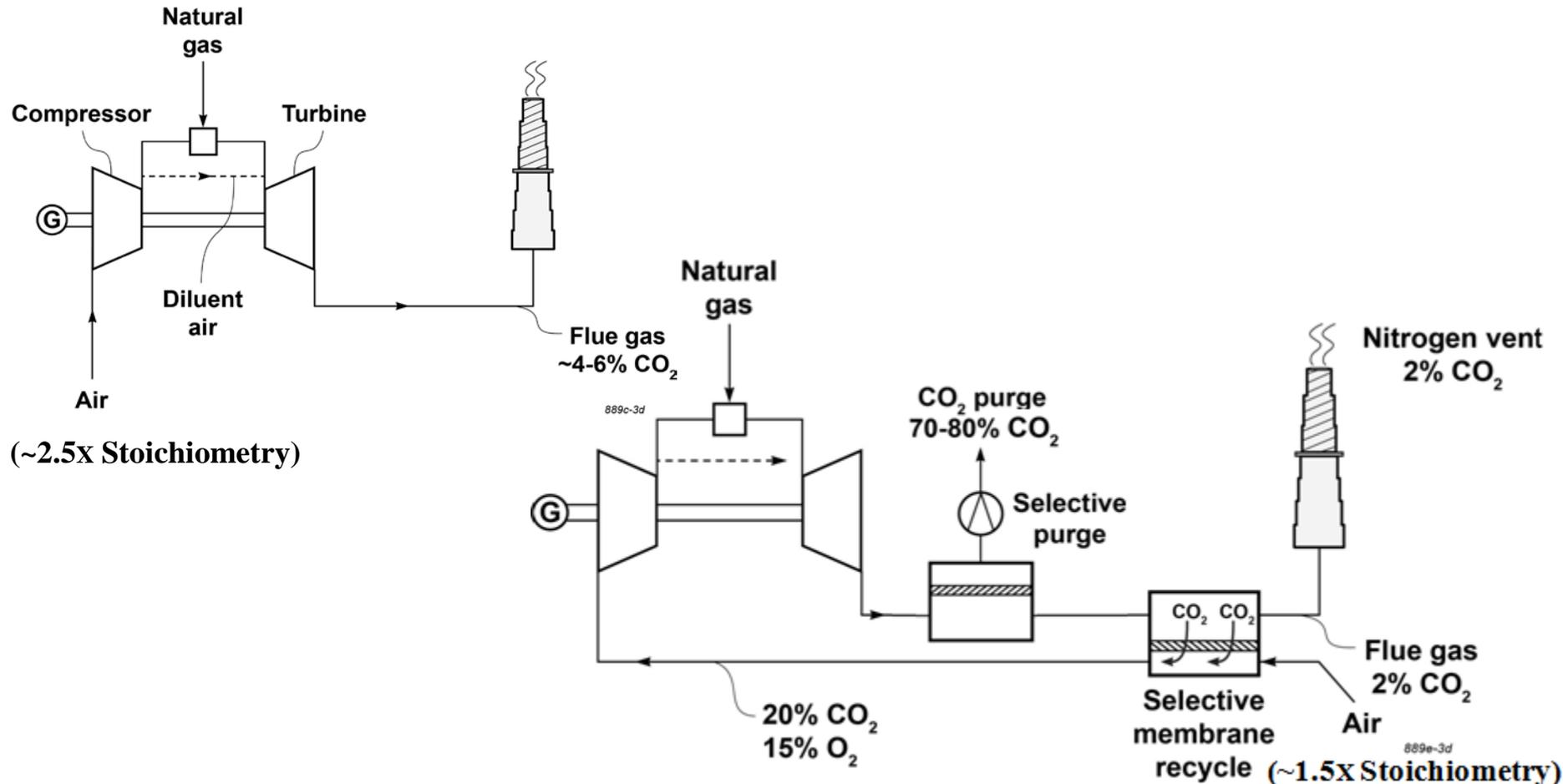
Sweep ratio for a coal contactor is ~ 0.7

CO₂ Separation from Gas Turbine Flue Gas



(~2.5x Stoichiometry)

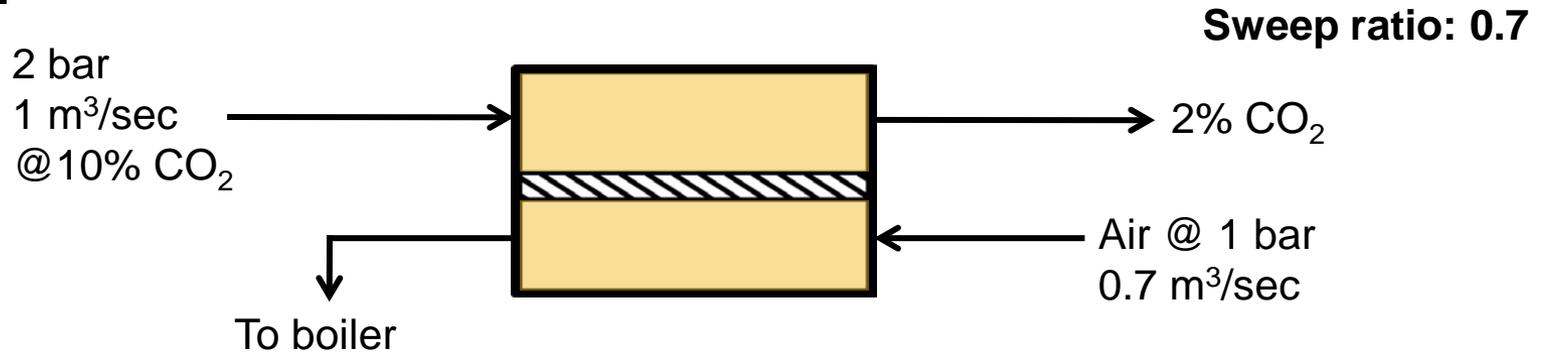
CO₂ Separation from Gas Turbine Flue Gas



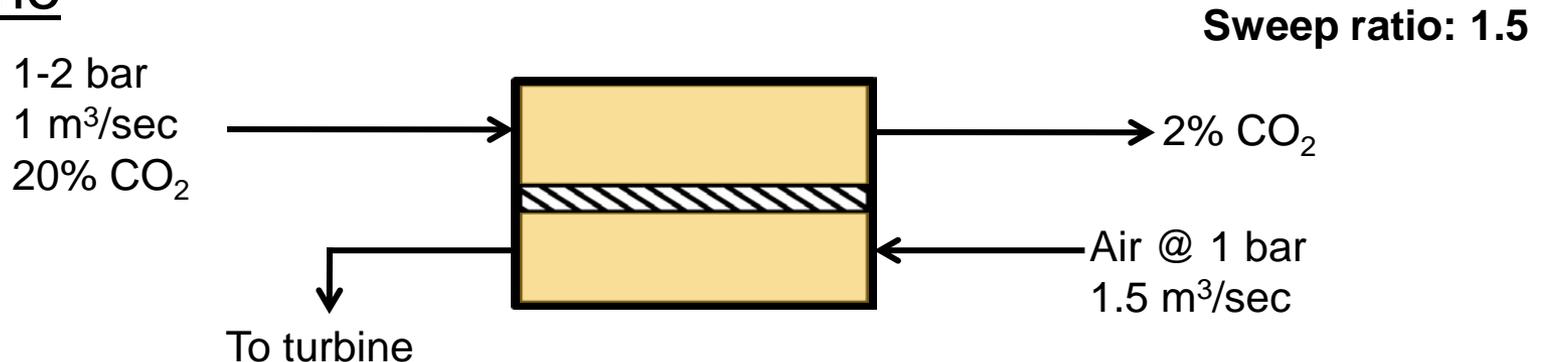
9 Sweep ratio for a gas turbine contactor is ~ 1.5

Base Case Operating Conditions

Coal



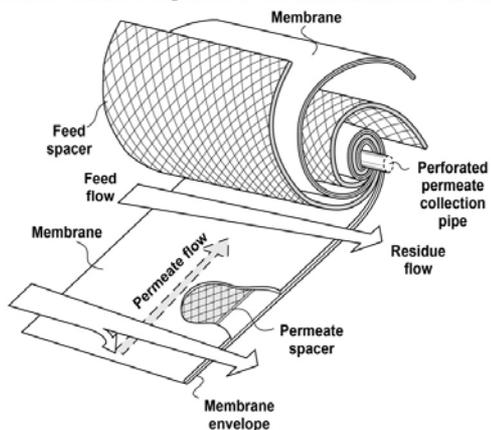
Gas Turbine



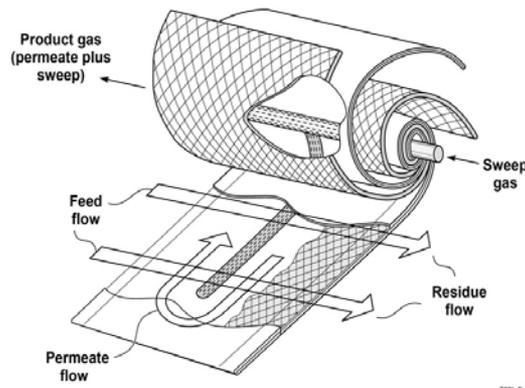
Depending on the operating conditions and membrane permeance, a 500 MWe power plant will need 0.5 – 1.0 million m² of membrane

Current Approach Uses Modified Spiral-Wound Modules in Nested Bundles

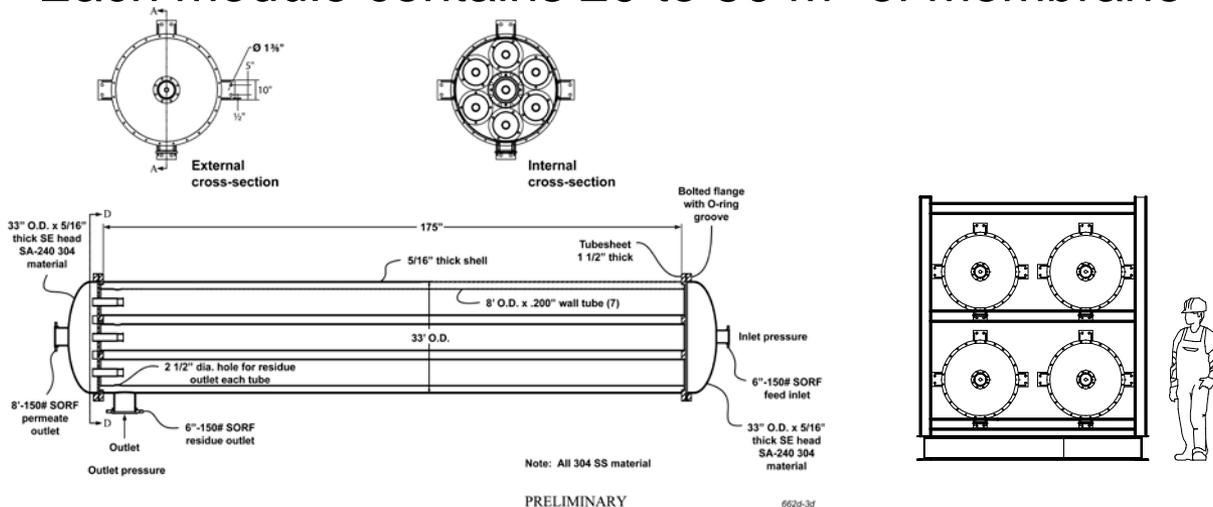
Conventional spiral-wound module



Spiral-wound countercurrent/sweep module

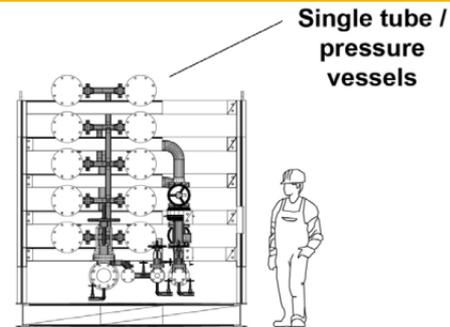
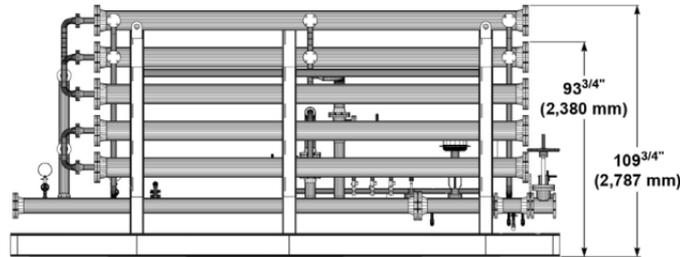


Each module contains 20 to 50 m² of membrane

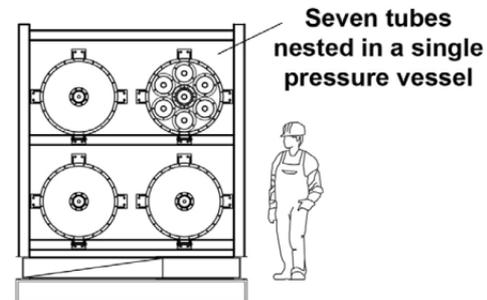
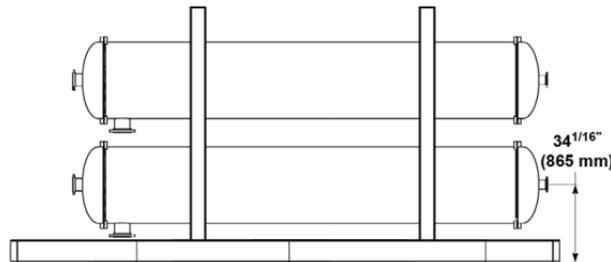


A Comparison of Skid Designs

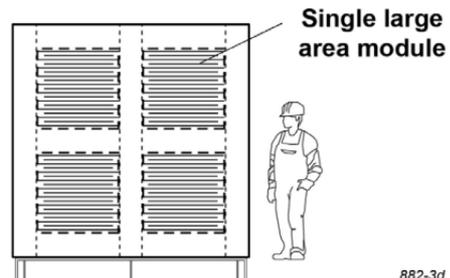
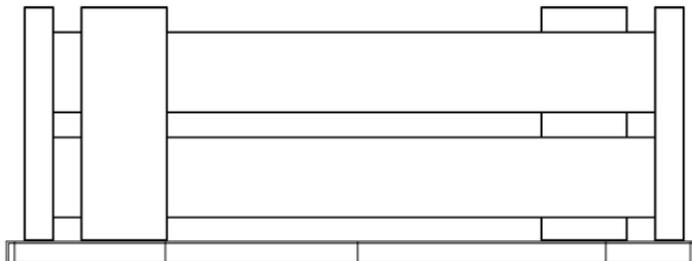
4 x 10 (8 inch modules) @ 20 m²/modules = 800 m²



4 x 4 x 7 (8 inch modules) @ 20 m²/modules = 2,240 m²



4 x (1 x 1 x 5 m) modules @ 2,500 m²/modules = 10,000 m²



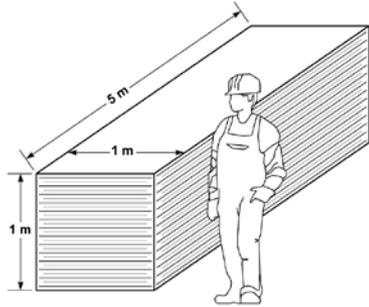
A Comparison of Skid Designs

| Module Configuration | Membrane Packing Efficiency Contactor Module Only (m ² /m ³) | Packing Efficiency Total Contactor Module Skid (m ² /m ³) | Housings Needed for a 100 MWe Plant* | Volume of 100 MWe Plant (m ³) |
|---|---|--|--------------------------------------|---|
| 8" Spirals (20 m ² each), 4 modules/tube | 600 | 19 | 2,500 | 10,500 |
| 8" Spirals (20 m ² each), 4 modules/tube, 7 nested tubes/pressure vessel | 600 | 54 | 360 | 3,700 |
| 2,500 m ² large area contactor (1m x 1m x 5m) | 500 | 240 | 80 | 830 |

* 100 MWe requires about 200,000 m² of membrane

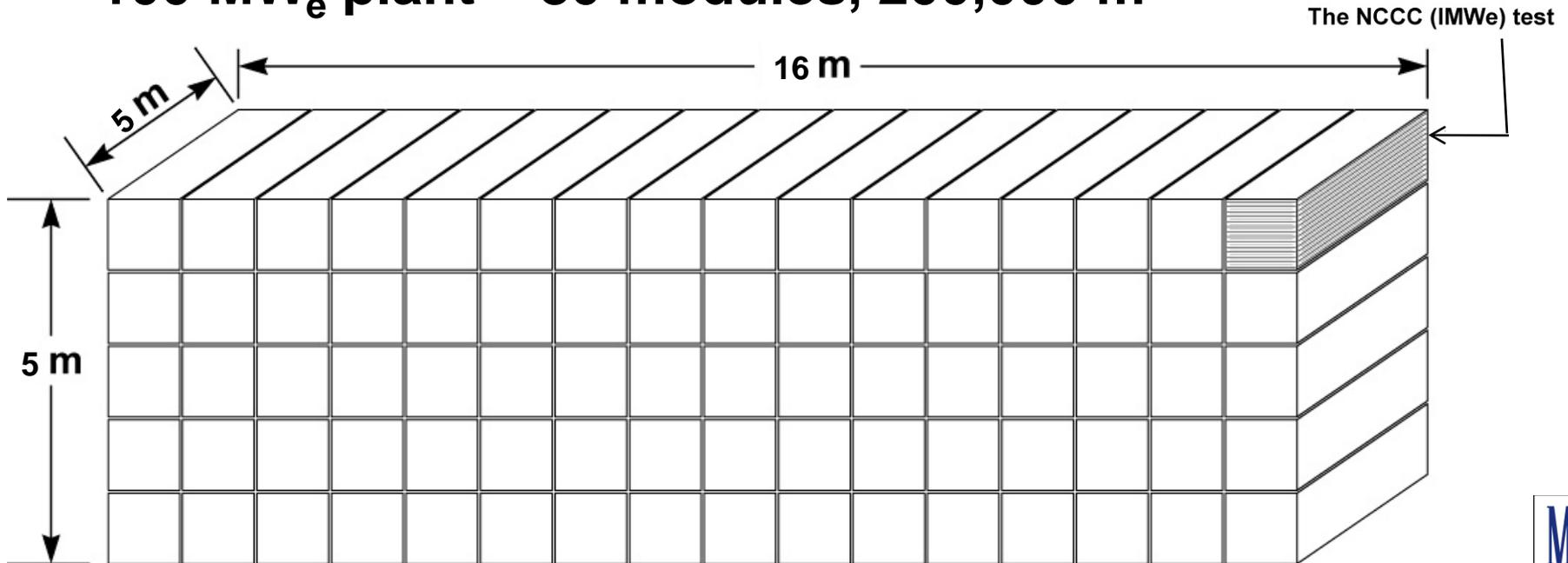
Large-area modules reduce manifolding and plant footprint

Membrane Unit Size



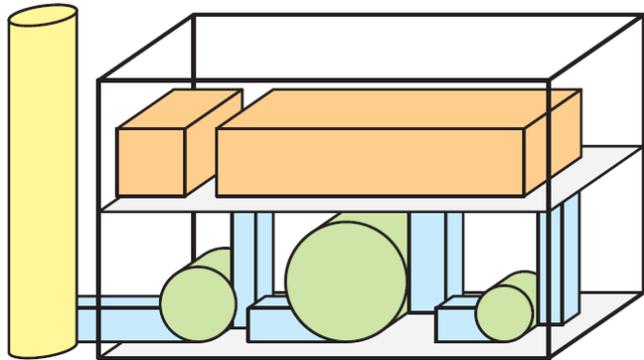
One module skid, 2500 m²

100 MW_e plant ~ 80 modules, 200,000 m²

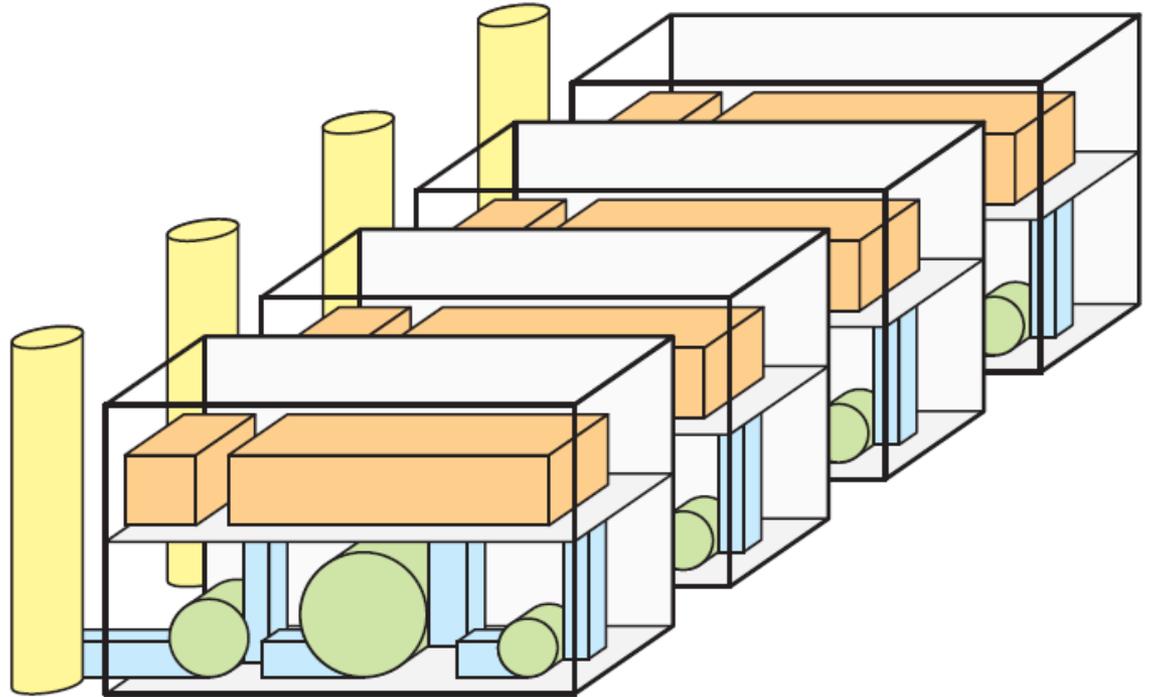


Membrane Skid Scale Up

25m



100 MW_e plant

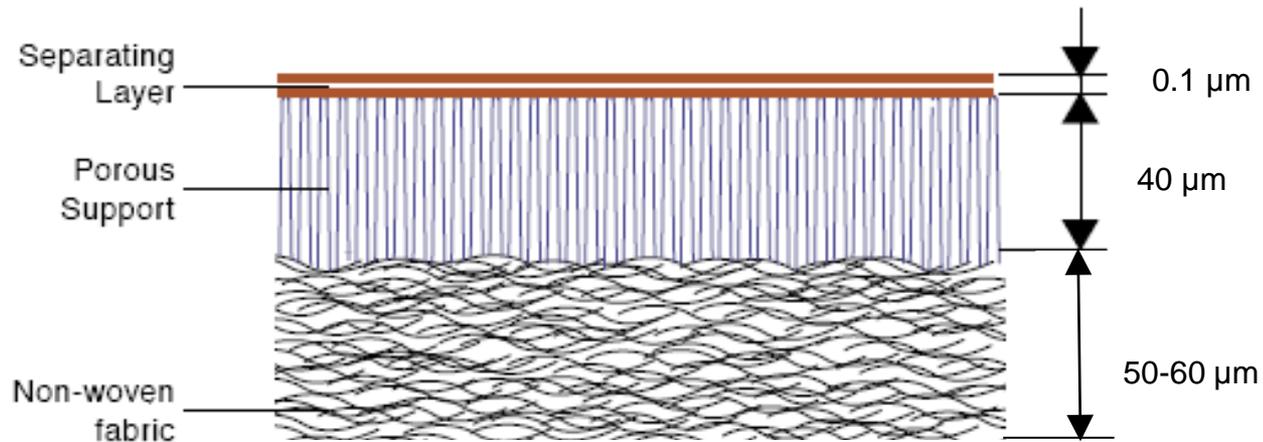


400 MW_e plant

Program Overview

- Issues
 - The Membrane
 - Concentration Polarization/Bypass/Flow Maldistribution
 - Module Pressure Drop
 - Does Sweep Work?
 - Counter-Flow Sweep
 - Cross-Flow Sweep

The Issues: The Membrane



Current standard:

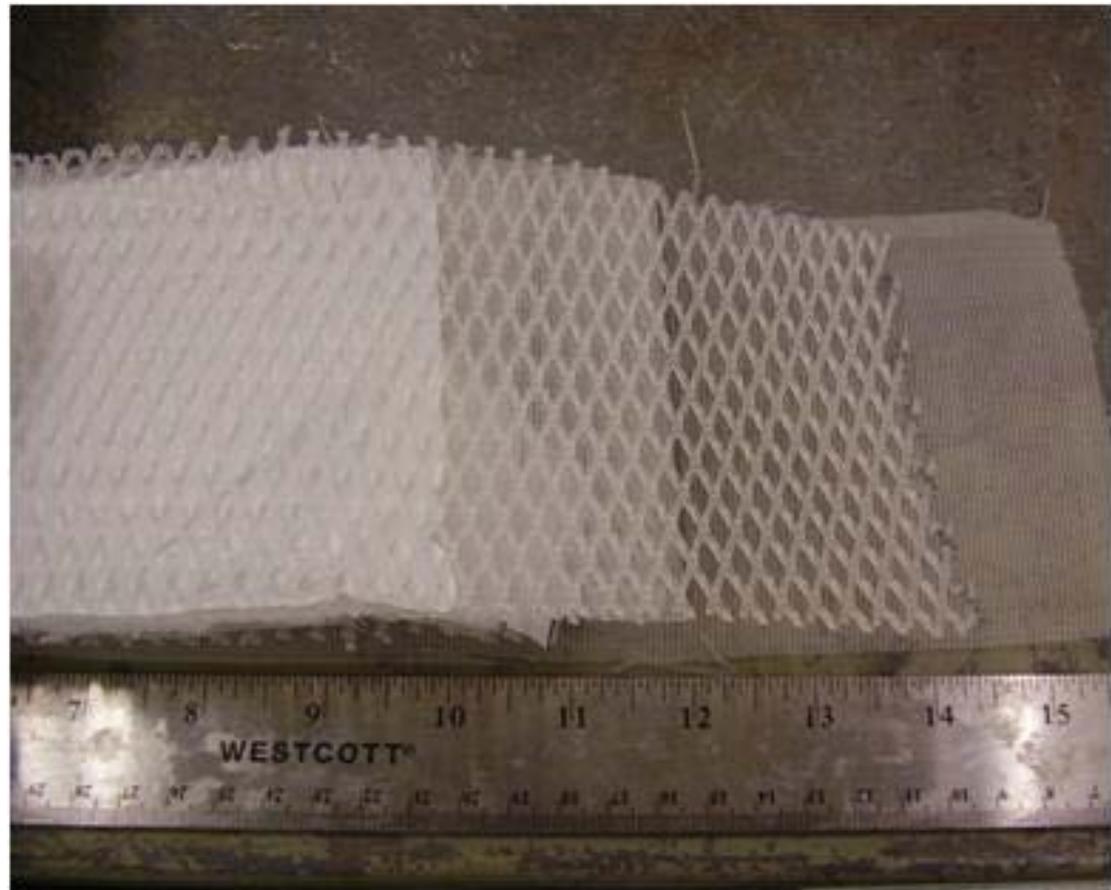
CO_2 permeance = 1000 gpu , $\alpha = 40$

Target:

CO_2 permeance = 2500 gpu , $\alpha = 40$

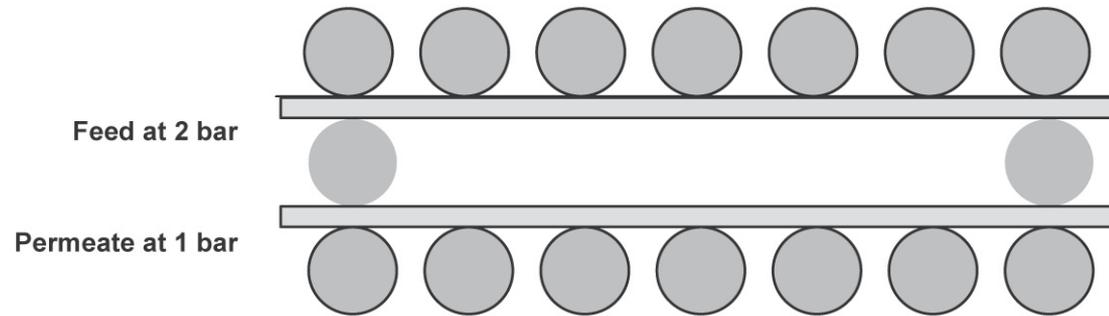
The Issues: Spacer Selection and Design

- Wide Range of Commercially Available Spacers
 - Material
 - Geometry
 - Weave
 - Thickness

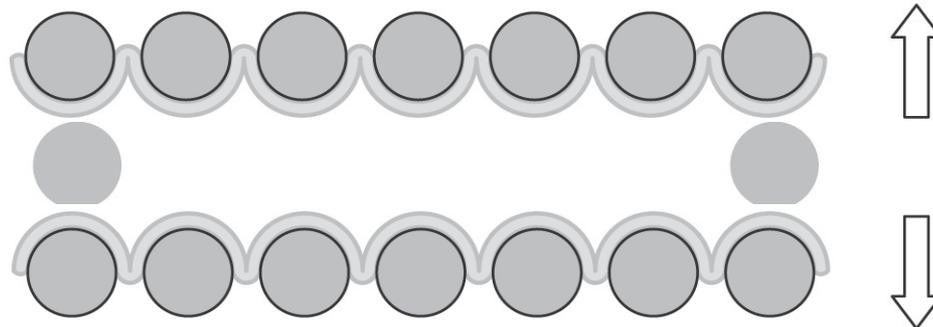


The Issues:

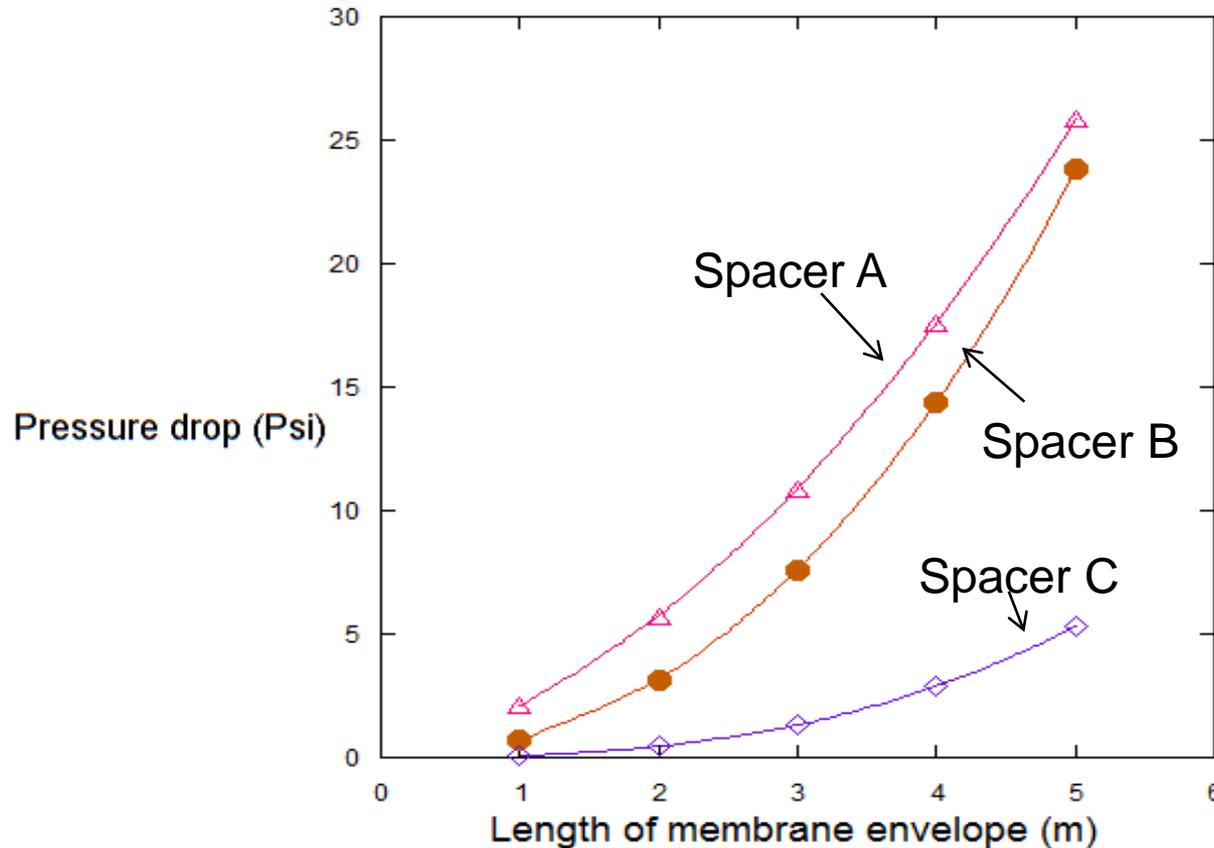
Mechanical Damage to The Membrane



Under compression,
the membrane is damaged
by the permeate spacer

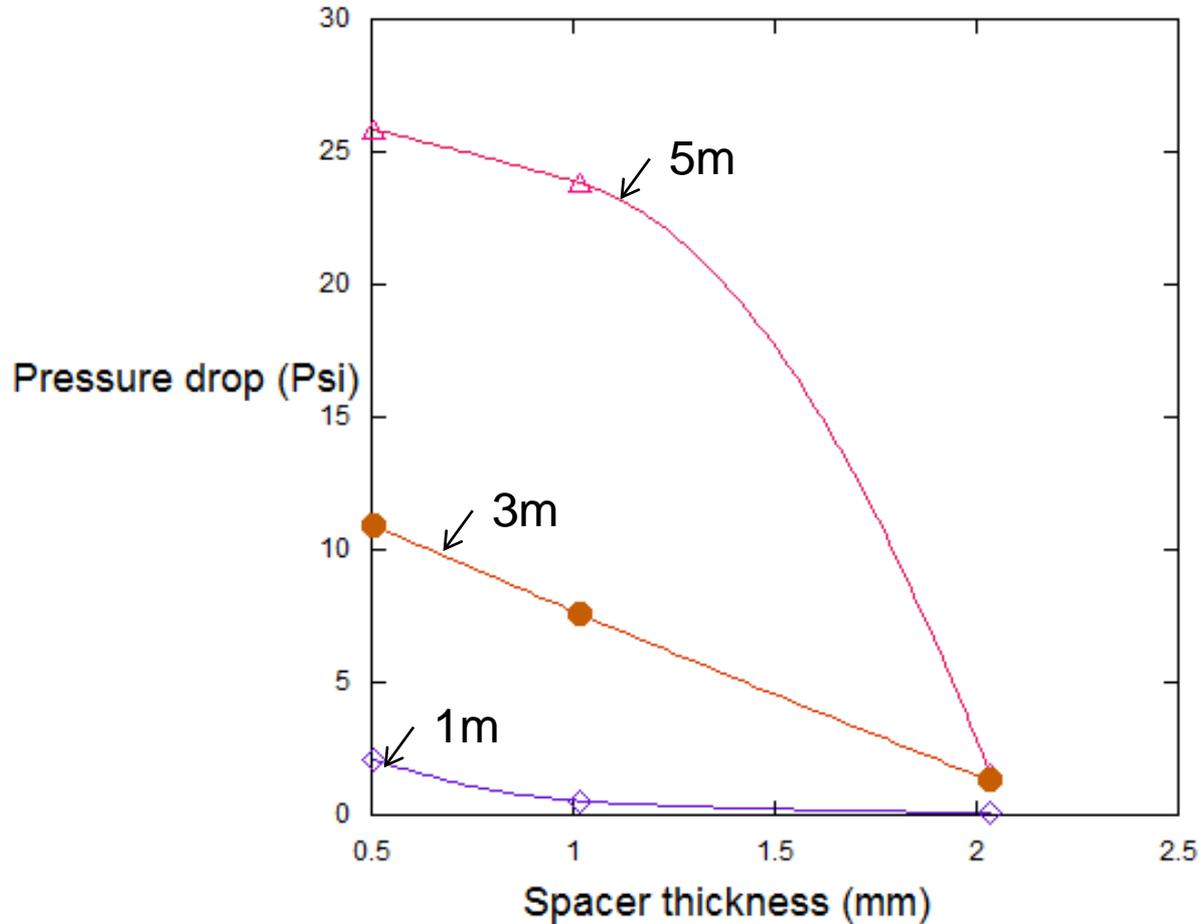


Spacer Pressure Drop



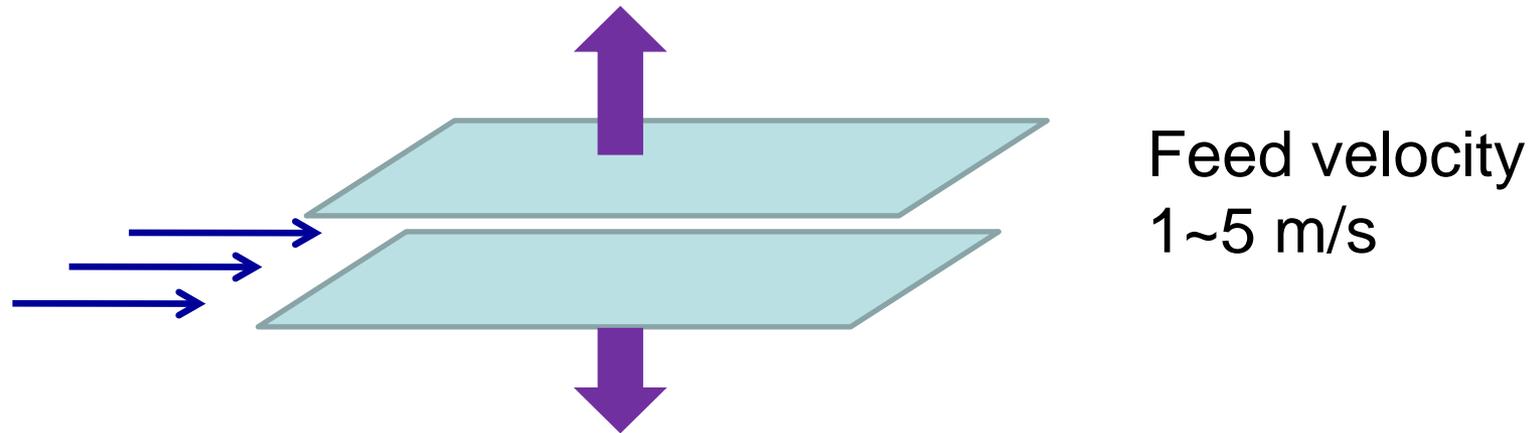
- Pressure drop goes up as the square of the envelope length
- Pressure drop is a function of weave & orientation

Spacer Pressure Drop



– Pressure drop goes down as the spacer thickness increases

Concentration Polarization/Bypass/ Flow Maldistribution

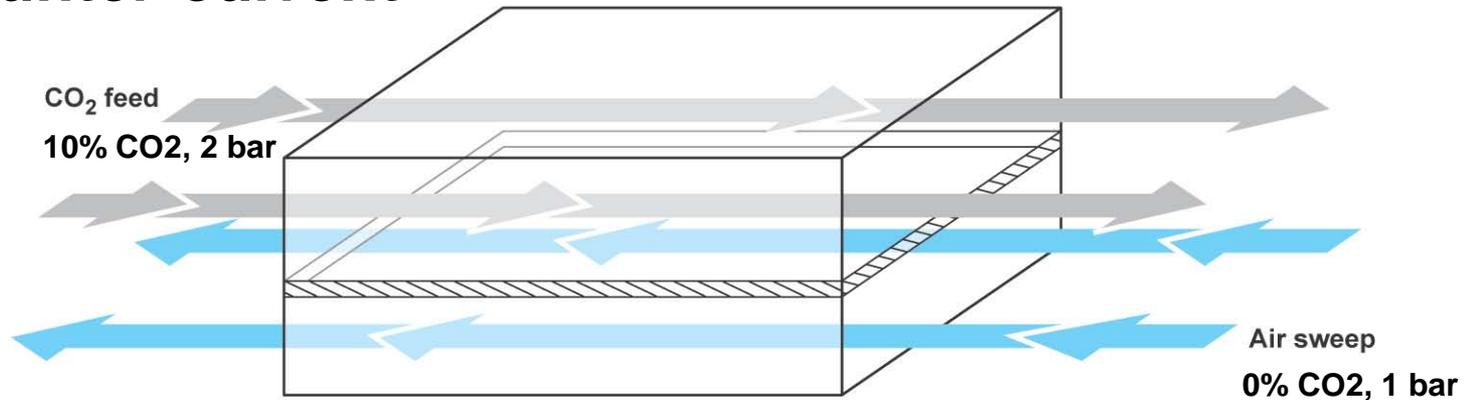


Permeate velocity through the membrane
~ 0.005 cm/sec

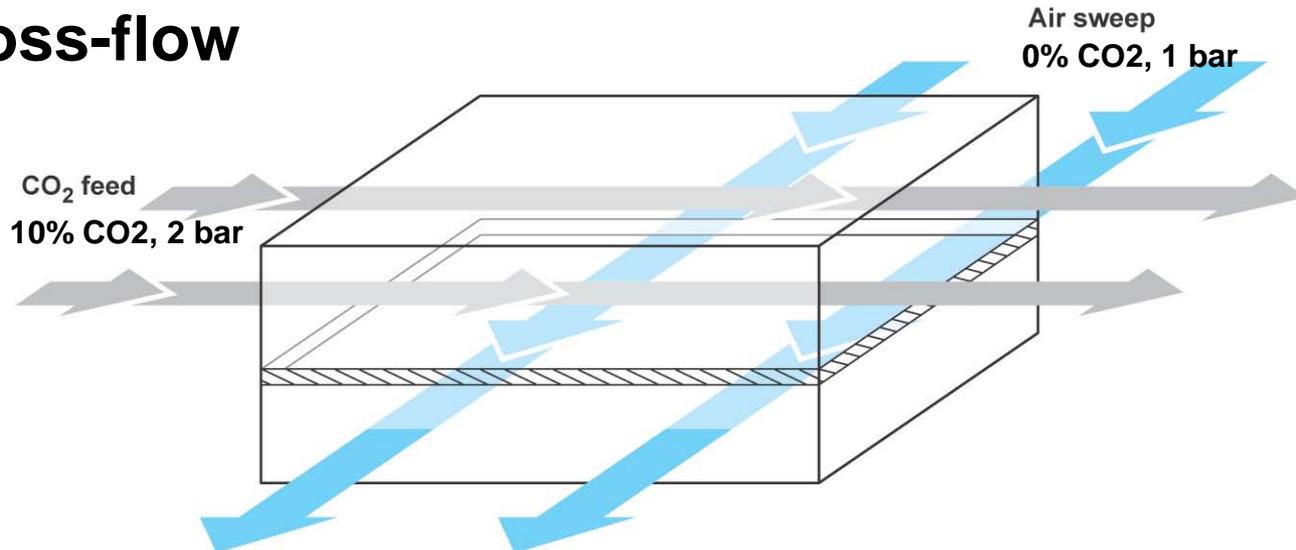
- Concentration polarization with the membrane unlikely to be a problem (Peclet $\sim 1 \times 10^{-3}$)
- Bypass and maldistribution will be more important

The Issues: Does Sweep Work?

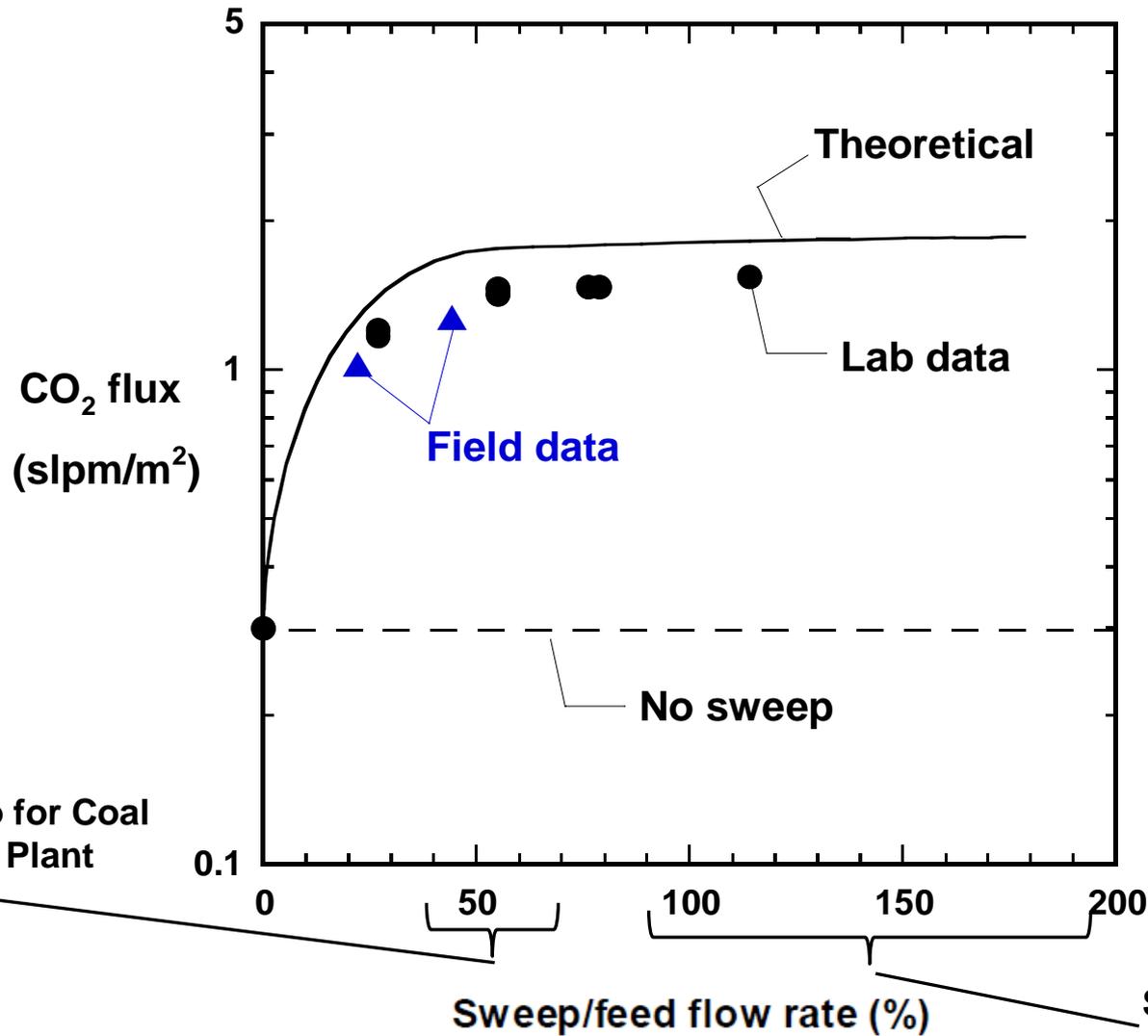
Counter-current



Cross-flow

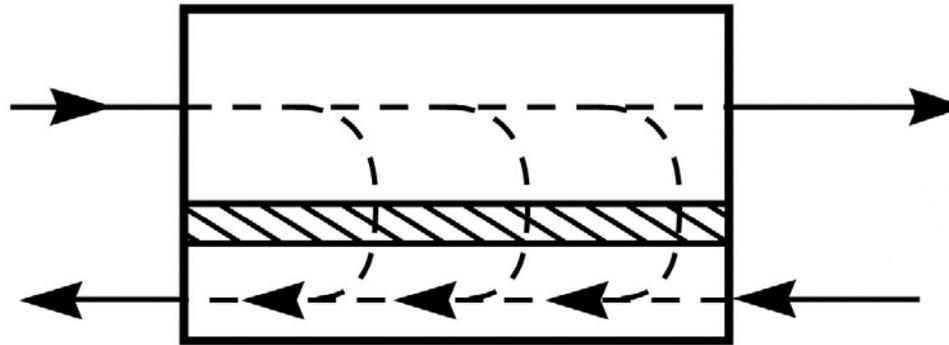


Sweep Does Work!



Counter Current Sweep: The Effect of Sweep Ratio

Feed
-1 m³/s
-10% CO₂
-1 bar

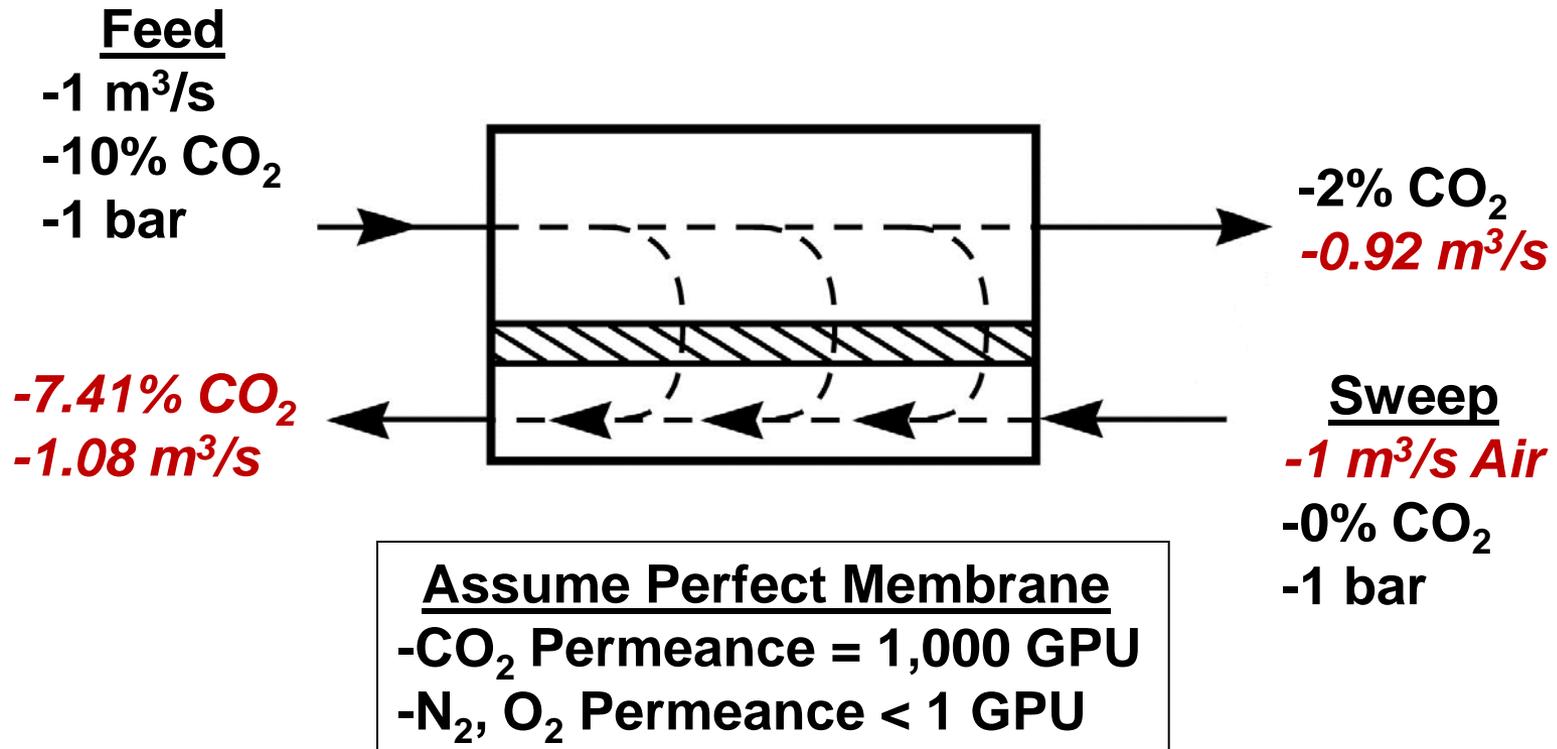


-2% CO₂

Sweep
-1 m³/s Air
-0% CO₂
-1 bar

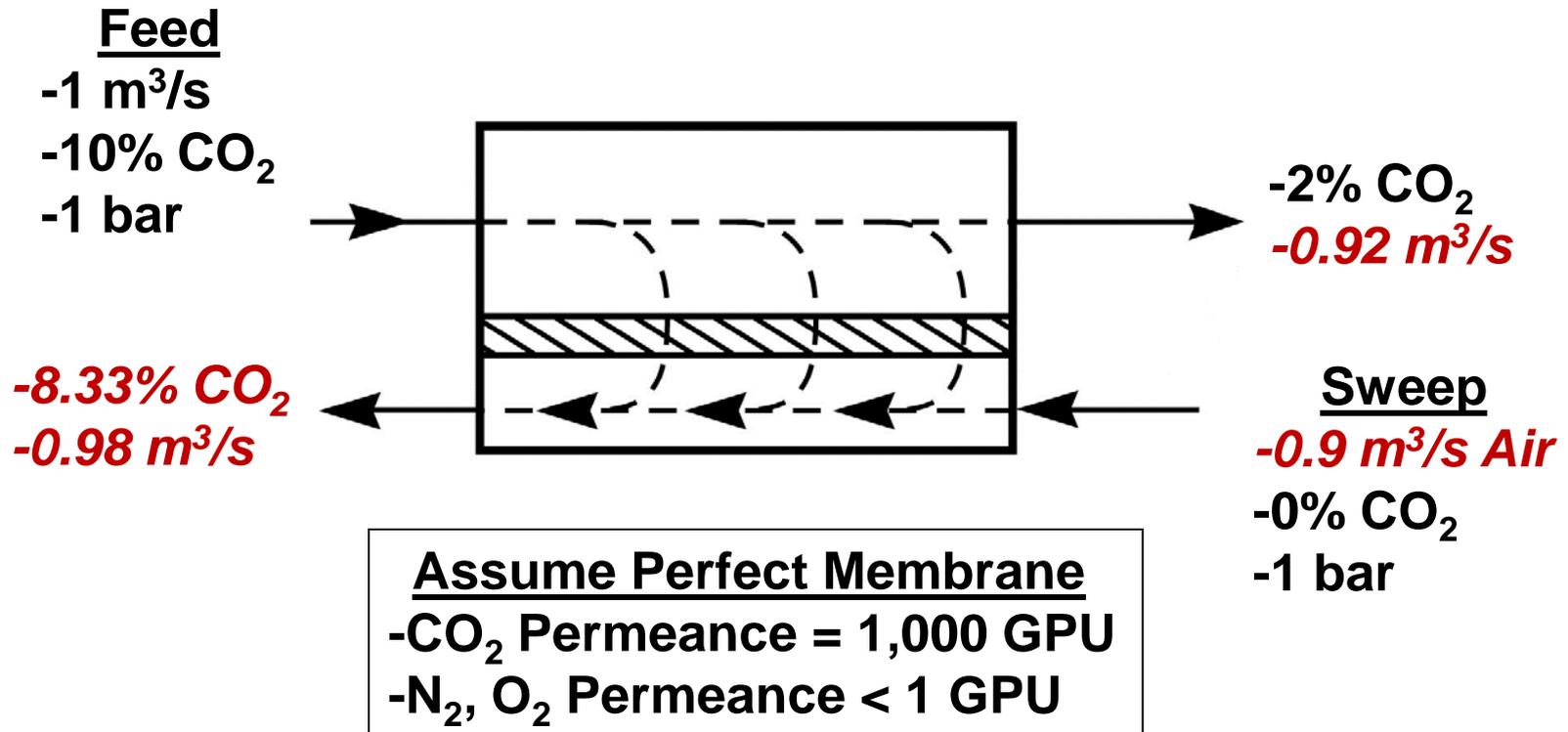
Assume Perfect Membrane
-CO₂ Permeance = 1,000 GPU
-N₂, O₂ Permeance < 1 GPU

Counter Current Sweep: The Effect of Sweep Ratio



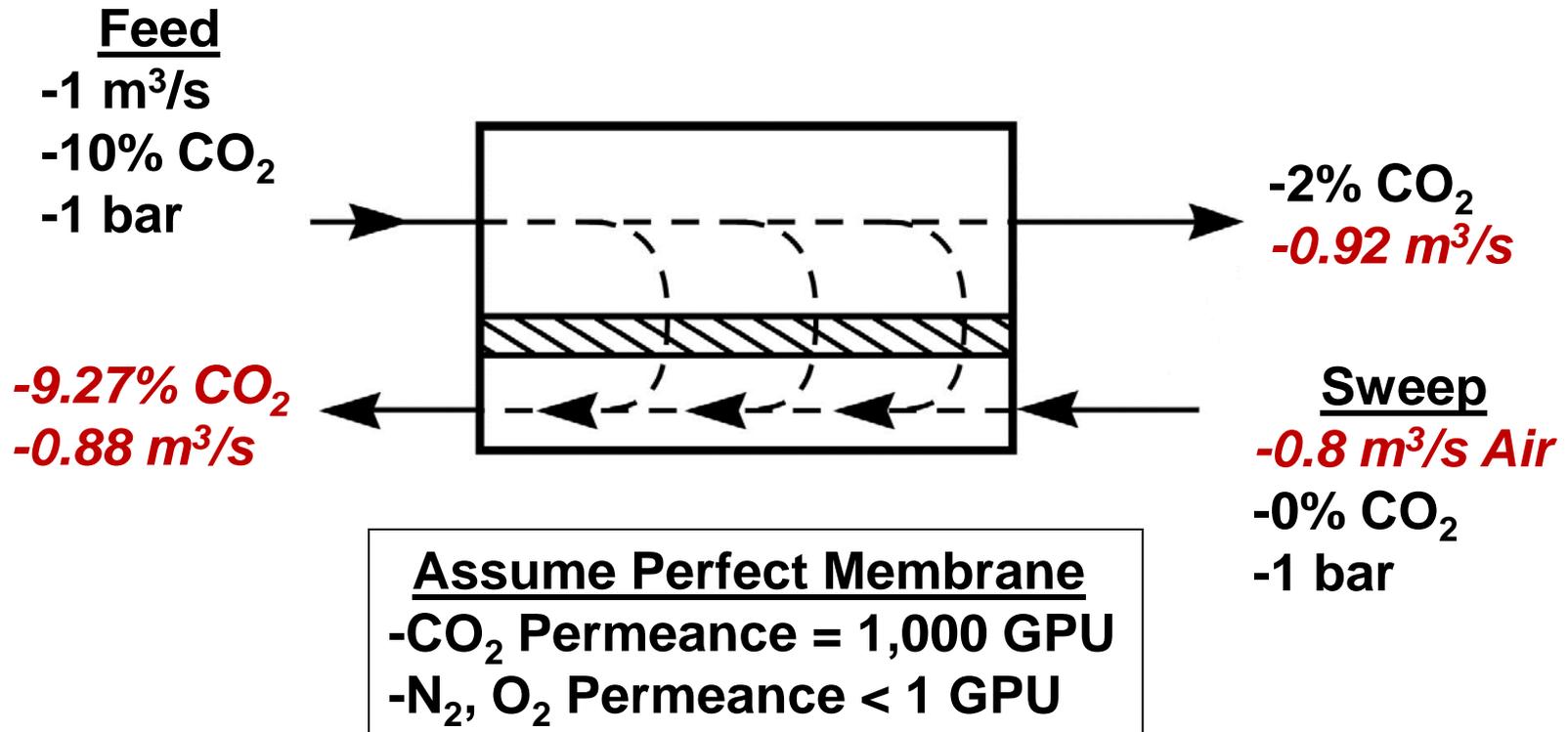
Sweep Ratio: 1.0
Membrane Area: 5,000 m²

Counter Current Sweep: The Effect of Sweep Ratio



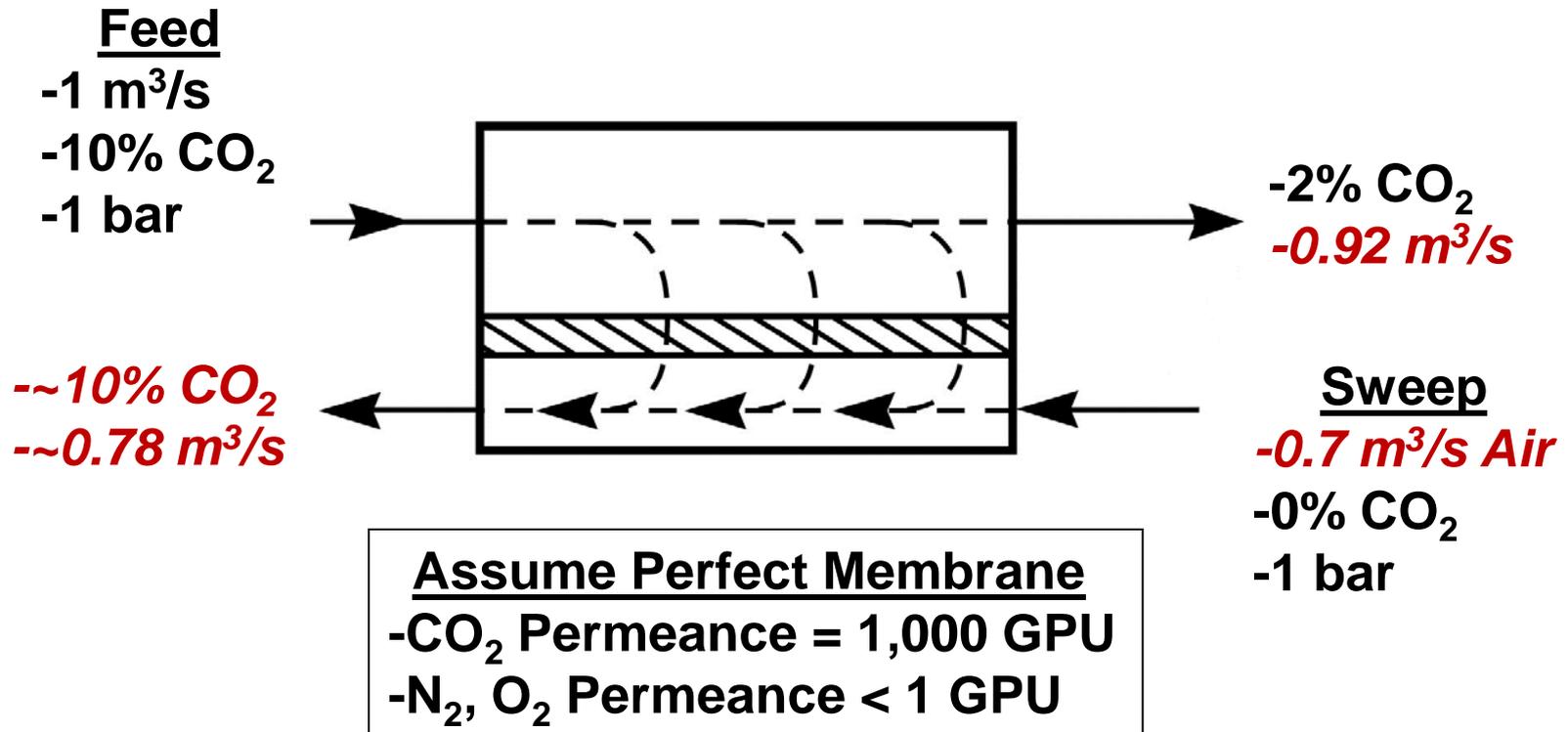
Sweep Ratio: 0.9
Membrane Area: 6,000 m²

Counter Current Sweep: The Effect of Sweep Ratio



Sweep Ratio: 0.8
Membrane Area: 8,500 m²

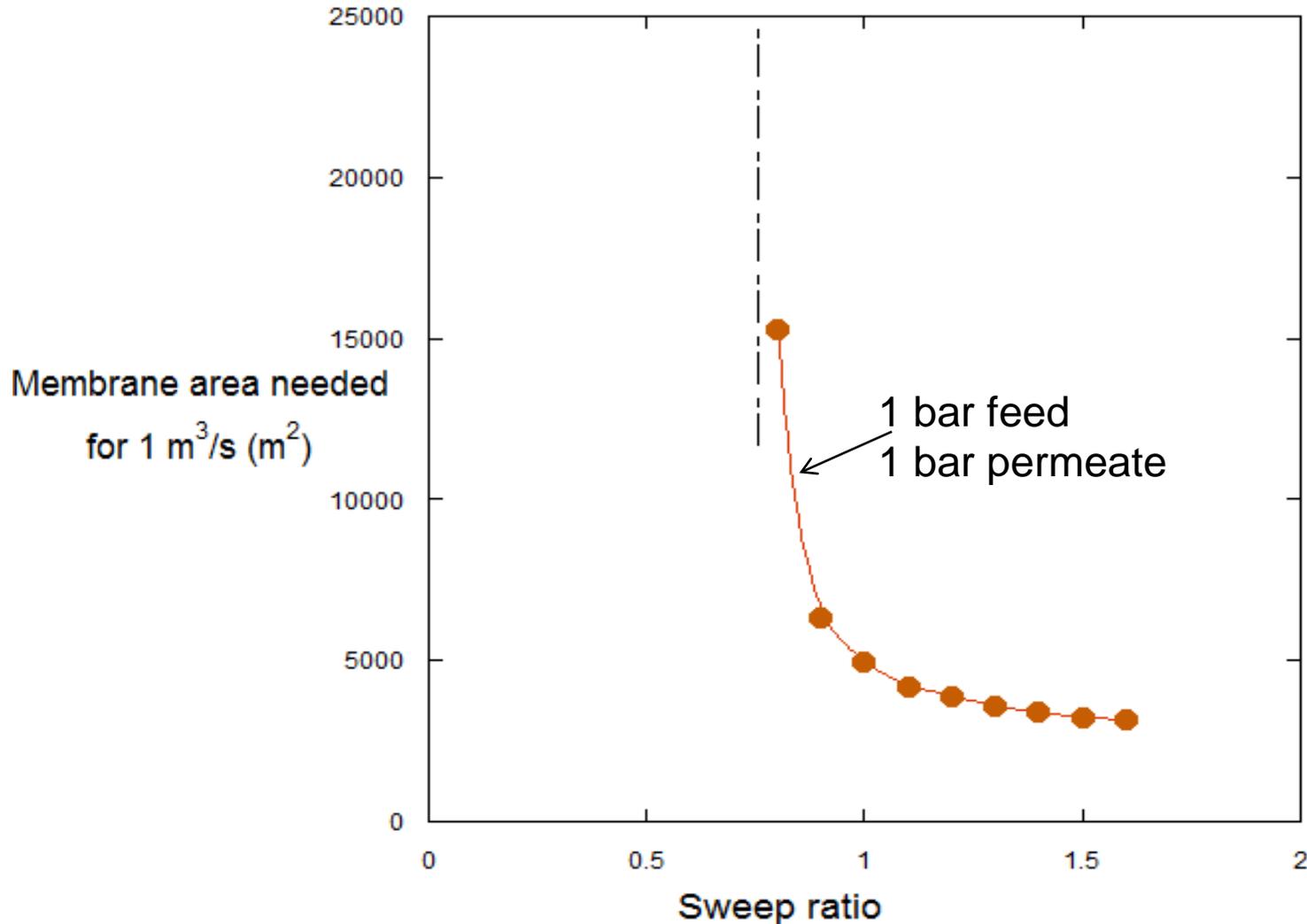
Counter Current Sweep: The Effect of Sweep Ratio



Sweep Ratio: 0.7
Membrane Area: INFINITE!!

Counter Current Sweep

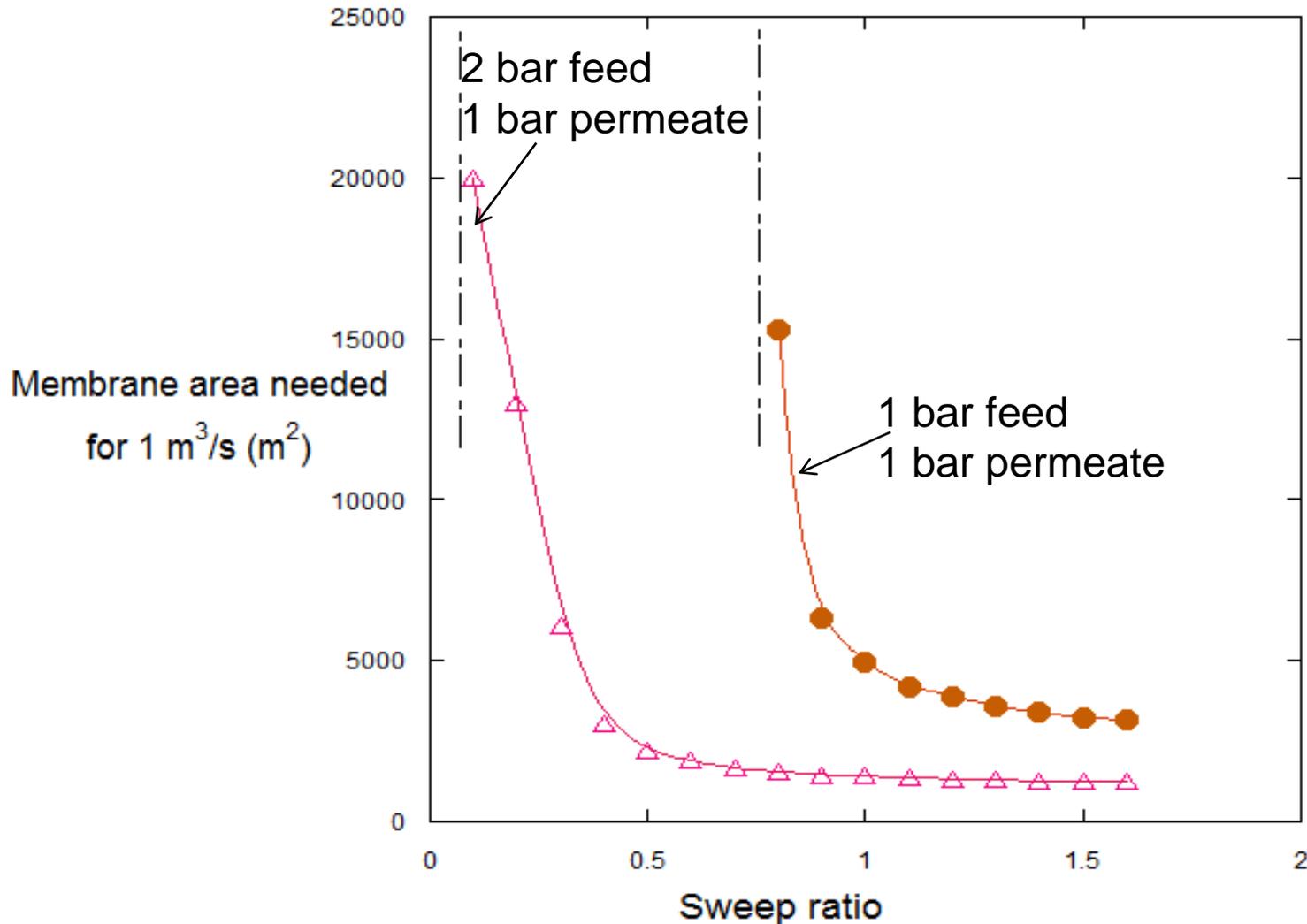
The Effect of Sweep Ratio



30 – At low sweep ratios, pressurized feed is needed

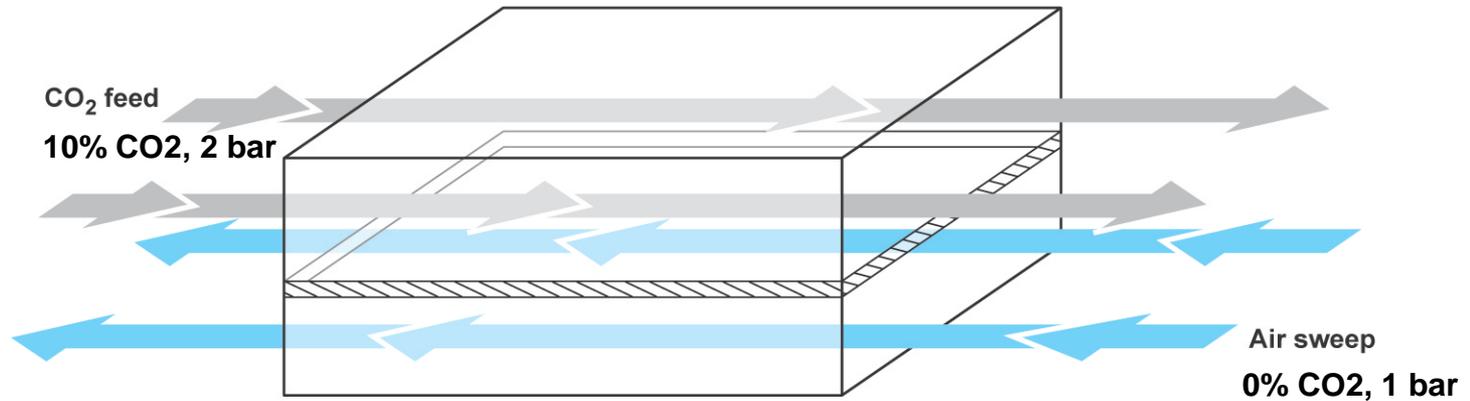
Counter Current Sweep

The Effect of Sweep Ratio



31 At low sweep ratios, pressurized feed is needed

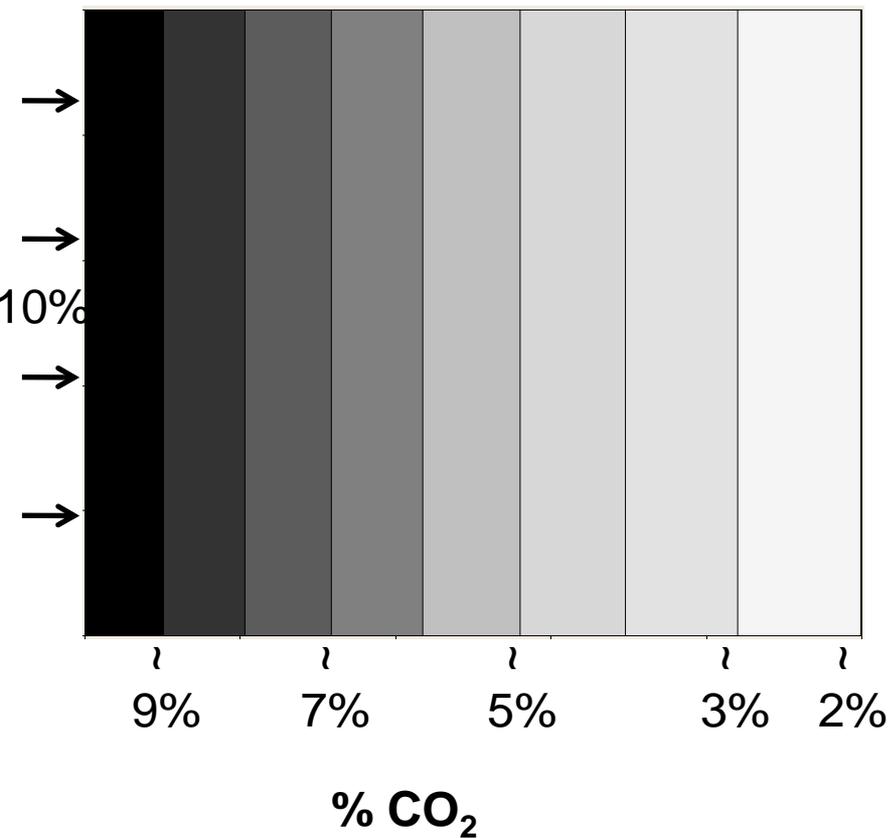
Counter-Current Sweep



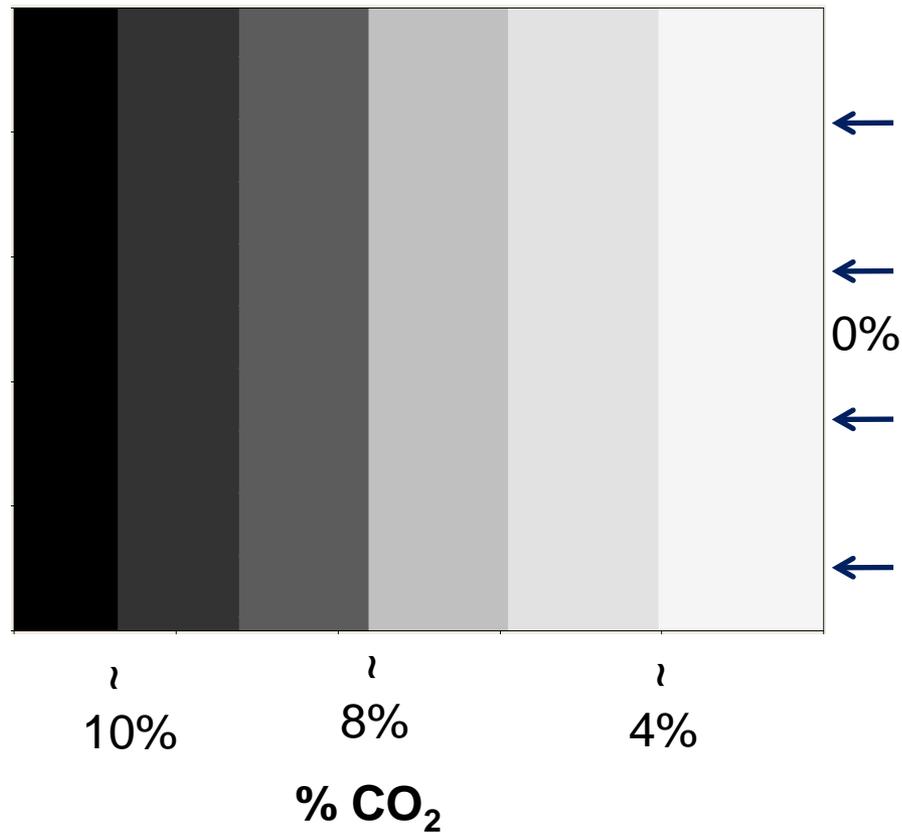
Counter-current sweep is the most efficient design but most difficult to make.

Counter-Current Sweep

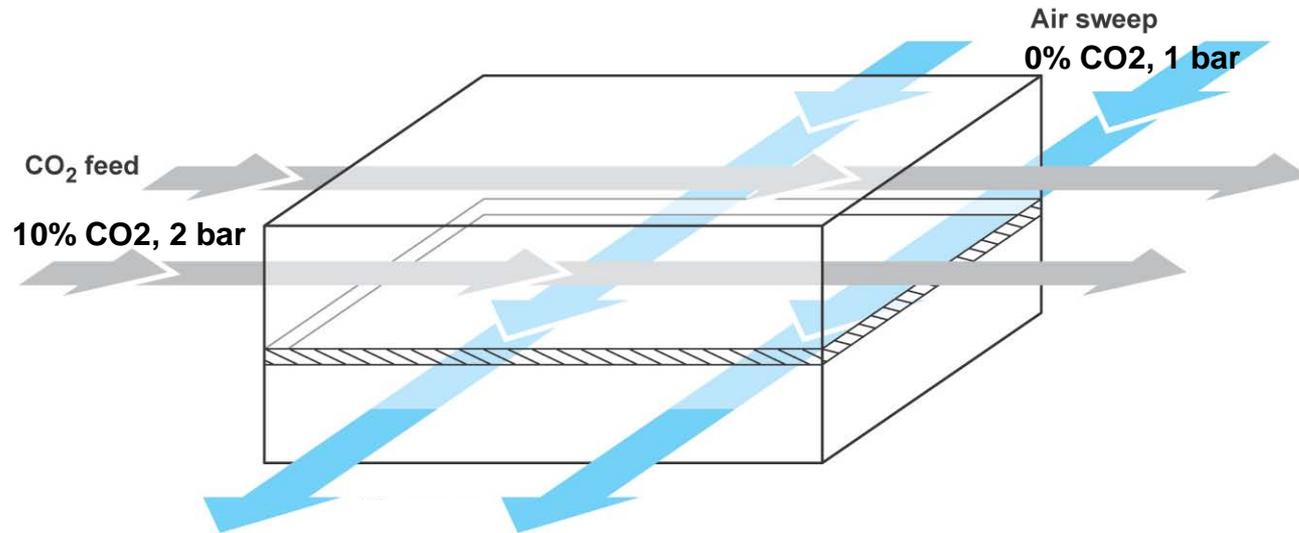
Feed side, 2 bar



Permeate side, 1 bar



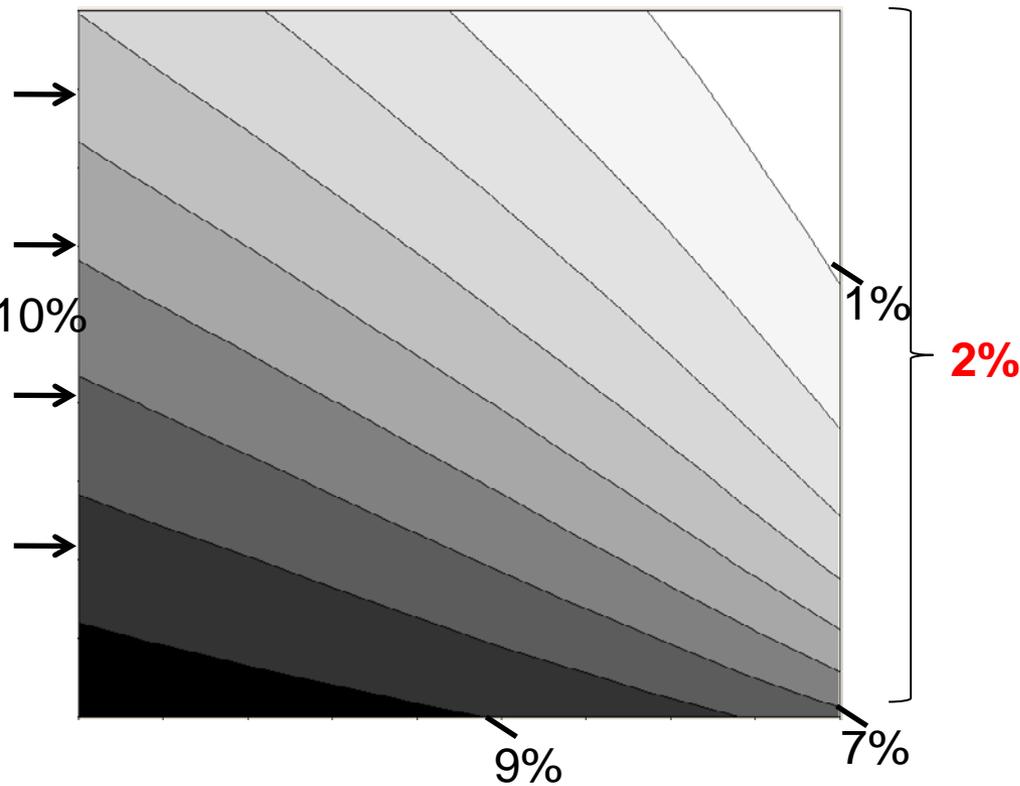
Cross-Flow Sweep



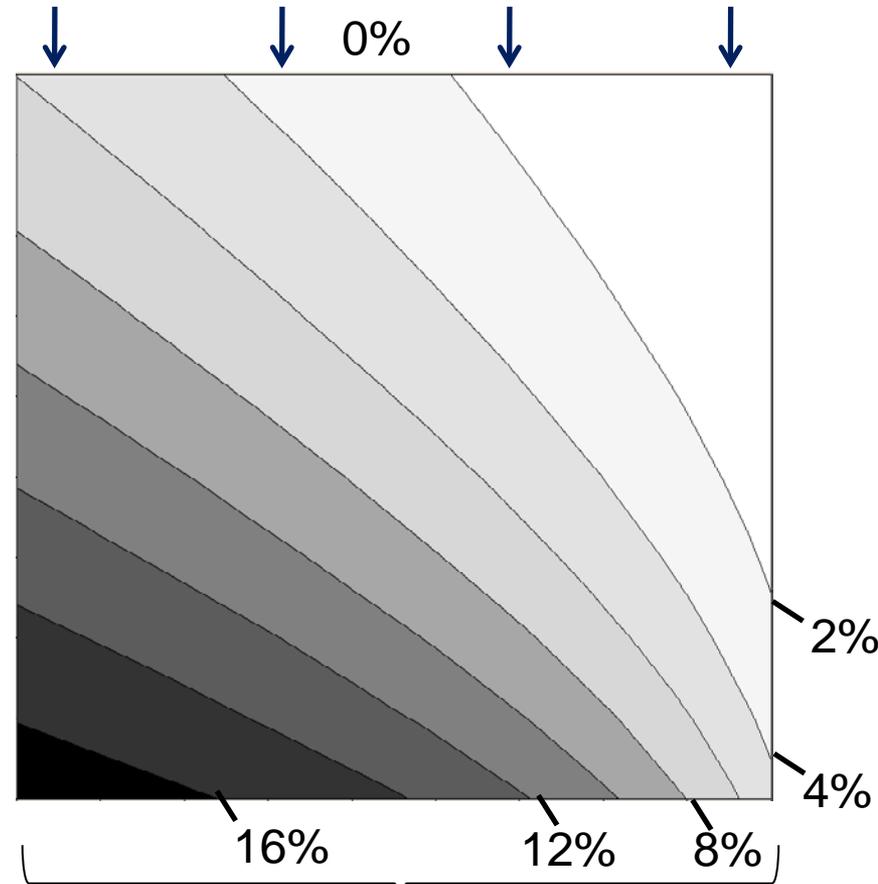
Cross-flow sweep is a less efficient design but easier to make and has less pressure drop on the permeate side.

Cross-Flow Sweep

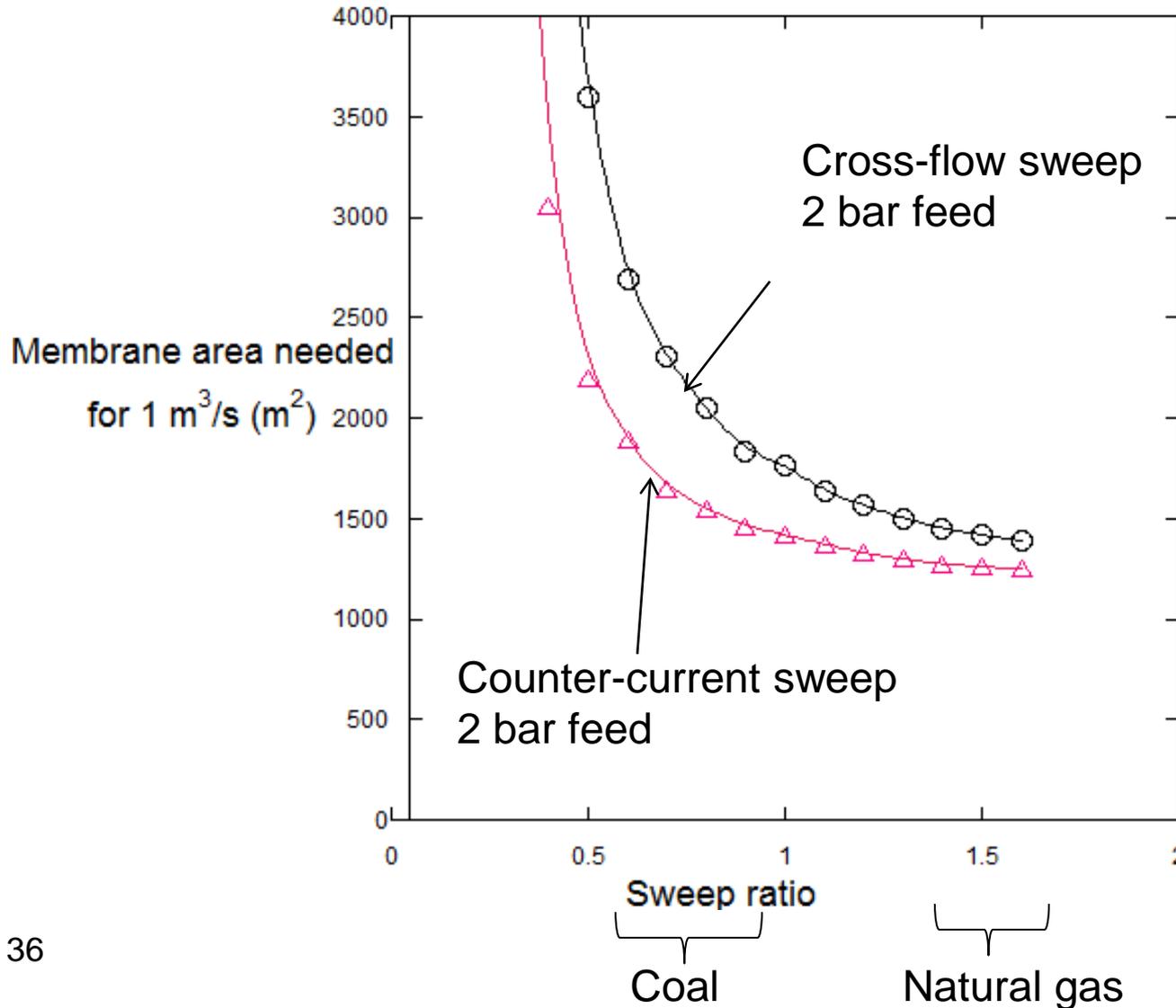
Feed side, 2 bar



Permeate side, 1 bar



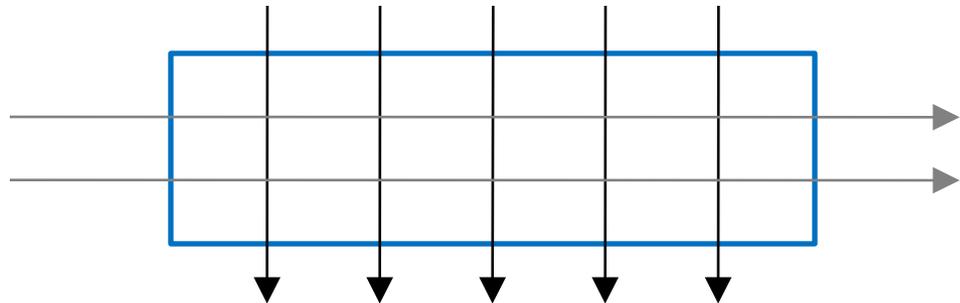
Comparison Between Counter-Current Sweep And Cross-Flow Sweep



Sweep ratio @ 0.7, 40% more membrane area is needed for cross-flow module

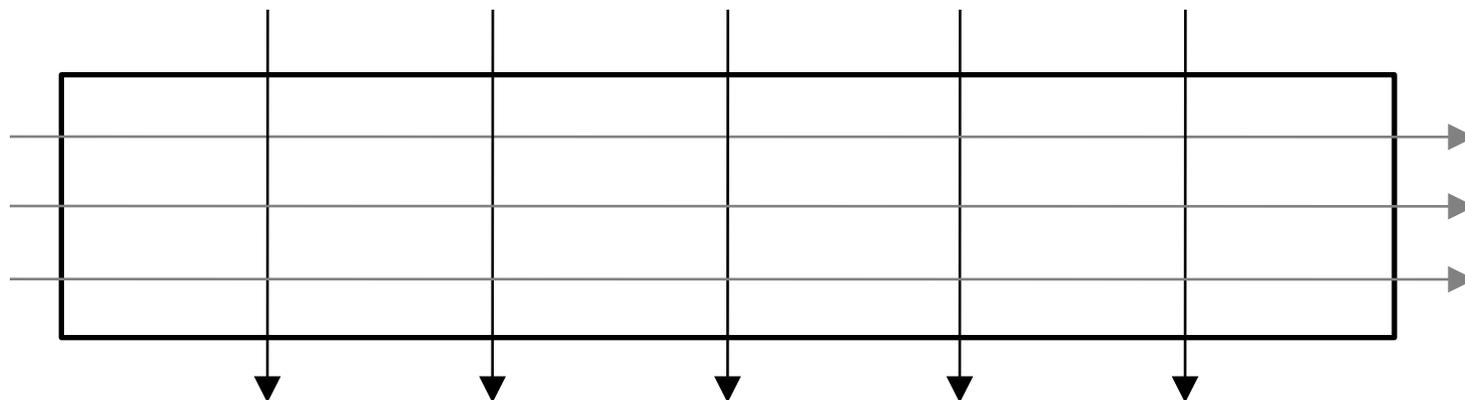
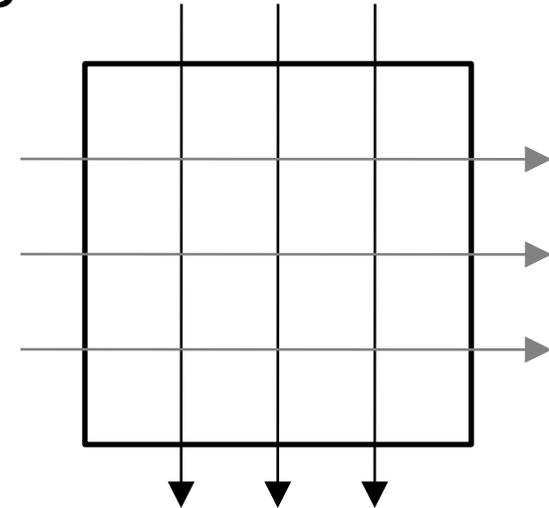
Our Approach

- Develop the Module in Stages
 - Increasing Module Size
 - Moving from Cross-Flow to Counter-Flow
- Year 1
 - Develop Sealing Techniques
 - Select the Optimum Spacers
 - Pressure Drop Milestone: < 5 PSI
 - Cross-Flow Modules (~20 m²)
 - 0.3 m X 1.0 m Sheets



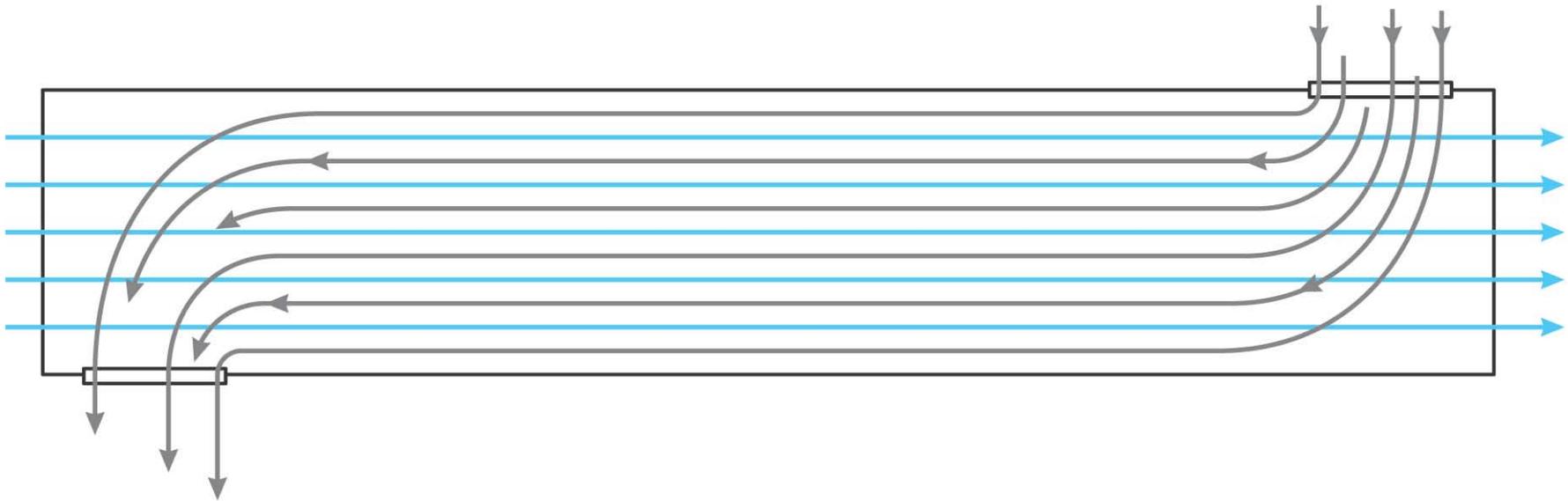
Our Approach - Year 2

- Solve Scale-Up Issues
- Develop Larger Cross-Flow Modules
 - 1 m X 1 m ($\sim 100 \text{ m}^2$)
 - 1 m X 5 m ($\sim 100 \text{ m}^2$)
- Pressure Drop Milestone: $< 2.5 \text{ PSI}$
- Test at MTR and
on the 1 TPD NCCC Skid



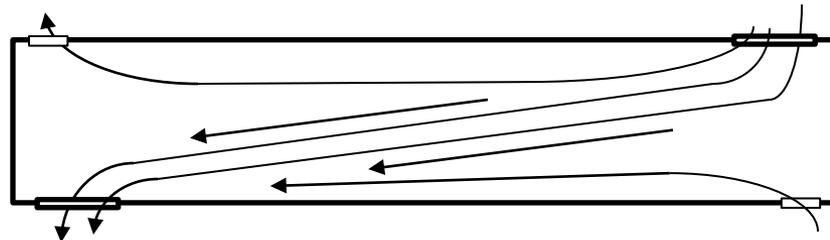
Our Approach - Year 3

- Develop Counter-Flow, Full Scale Modules
 - 1 m X 5 m (500 m²)
- Evaluate Different Spacer and Flow Configurations
- Pressure Drop Milestone: ≤ 1.5 PSI
- Test on the 20 TPD NCCC Skid (?)



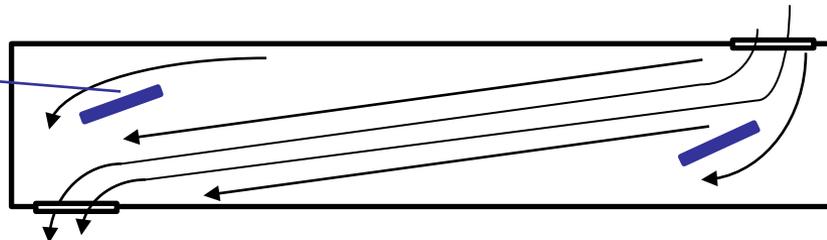
CFD Calculations and Tomography Measurements

- Use CFD Calculations to Analyze Various Spacers and Membrane Sheet Aspect Ratio
- Make Model Modules and Evaluate with Tomography Measurements



**Small Side Ports
to Eliminate
Low Flow Areas**

**Flow Directing
Baffles**



**Use Baffles to
Even Out Flow**

Program Plan/Schedule – See proposal

| Task # | Task Description | Year 1 | Year 2 | Year 3 |
|--------|---|--------|--------|--------|
| 1 | Project Management | ————— | | |
| 2 | Make Modules | ——— | | |
| 3 | Make Small Modules | ————— | | |
| 4 | Construct Test Unit | ——— | | |
| 5 | Test Modules | ——— | | |
| 6 | Initial CFD Design | ————— | | |
| 7 | Make Membrane | | ——— | |
| 8 | Make Full Footprint Modules | | ————— | |
| 9 | Prepare Tooling for Large-Scale Modules | | ——— | |
| 10 | Refine CFD/Tomography | | ————— | |
| 11 | Evaluate Process Designs | | ——— | |
| 12 | Make Membrane | | | ——— |
| 13 | Prepare Full-Scale Modules | | | ————— |
| 14 | Test Full-Scale Modules | | | ——— |
| 15 | Evaluate and Cost Process Designs | | | ————— |
| 16 | Select and Prepare Best Integrated Scheme | | | ——— |