

# Pilot Test of an Efficient Membrane Process for Post-Combustion CO<sub>2</sub> Capture

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**NETL CO<sub>2</sub> Capture Technology Meeting**  
Monday, August 22, 2011

# Outline

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- Project overview
- Technology background
- Current status of technology
- Project timeline and objectives

# Project Overview

**Award name:** Pilot testing of a membrane system for post-combustion CO<sub>2</sub> capture

**Project period:** 10/1/10 to 9/30/15

**Funding:** \$15 million DOE; \$3.75 million MTR

**DOE program manager:** Jose Figueroa

**Participants:** MTR, Babcock & Wilcox, Southern Company (NCCC), EPRI

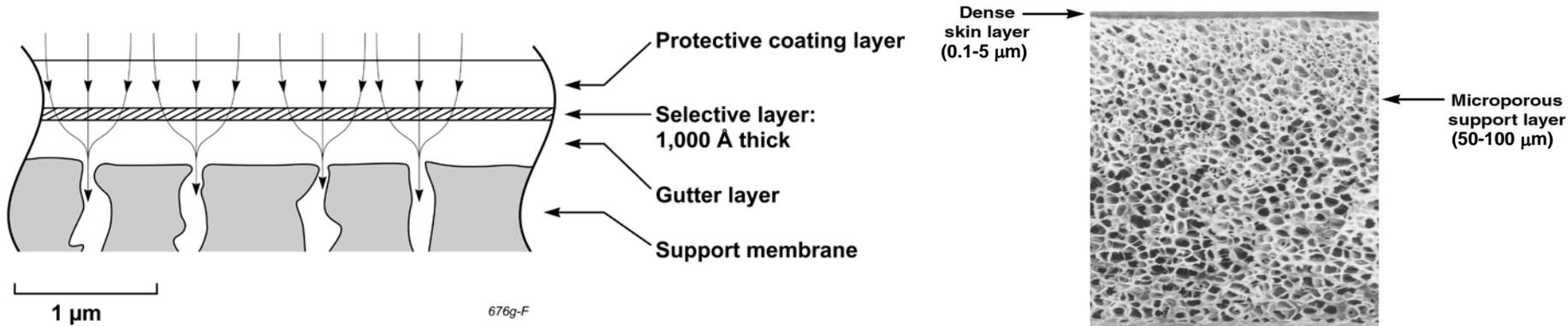
**Project scope:** Demonstrate a membrane process to capture 20 tons of CO<sub>2</sub>/day (20 TPD) from a flue gas slipstream of a coal-fired power plant

**Project plan:** The key project work organized by budget period is as follows:

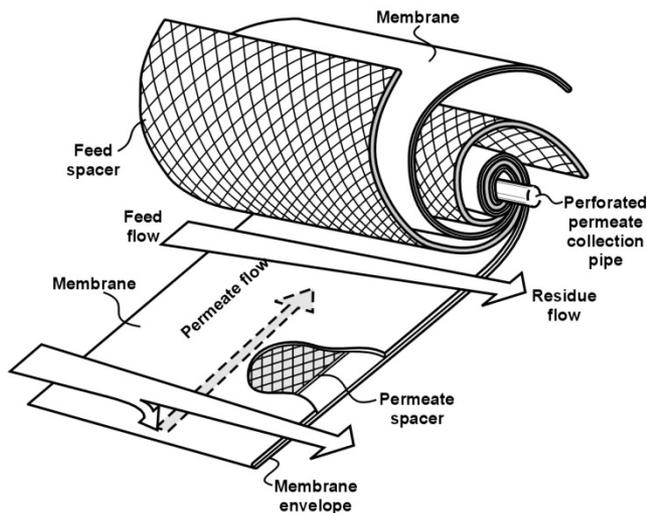
- BP1 – Membrane optimization through continued slipstream testing on the 1 TPD system and evaluation of sweep recycle with B&W
- BP2 – Design and construction of the 20 TPD system
- BP3 – Six-month pilot test of the 20 TPD system and comparative economic analysis

# Membrane Technology Basics

- Membranes have to be thin to provide useful fluxes.



- Membranes are packaged in modules for industrial separations.

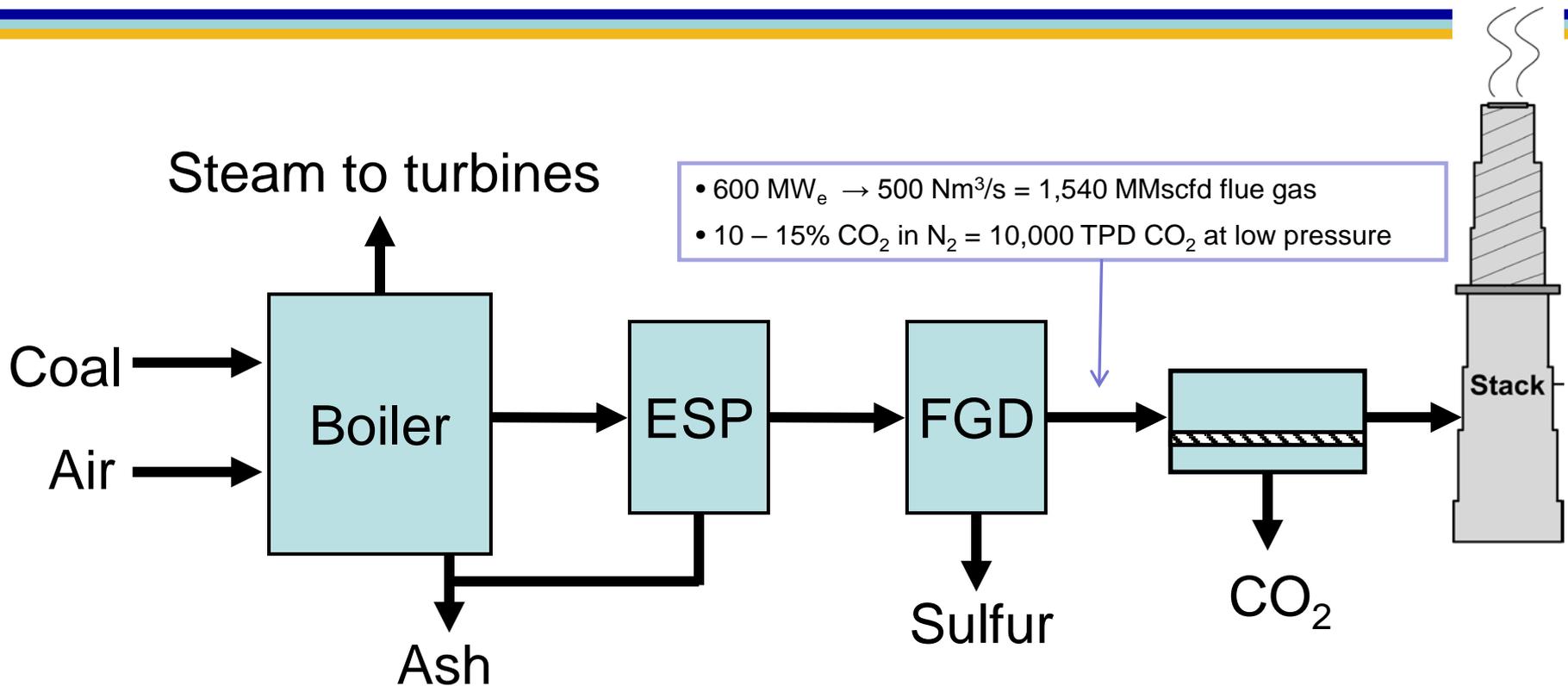


# Advantages of a Membrane Process

- Simple operation; a passive, continuous process
- No use of hazardous chemicals; no chemical handling or disposal issues
- Tolerance to high levels of  $\text{SO}_x$  and  $\text{NO}_x$ ; inert to oxygen
- Compact and modular; easily scalable; easy turndown
- Inherently energy efficient (20% parasitic energy at 90% capture)
- No additional water used (recovers water from flue gas)
- No steam use, so no modifications to existing boiler and steam turbine are needed
- Builds on existing, low-cost technology already used at a similar scale for water desalination and natural gas treatment



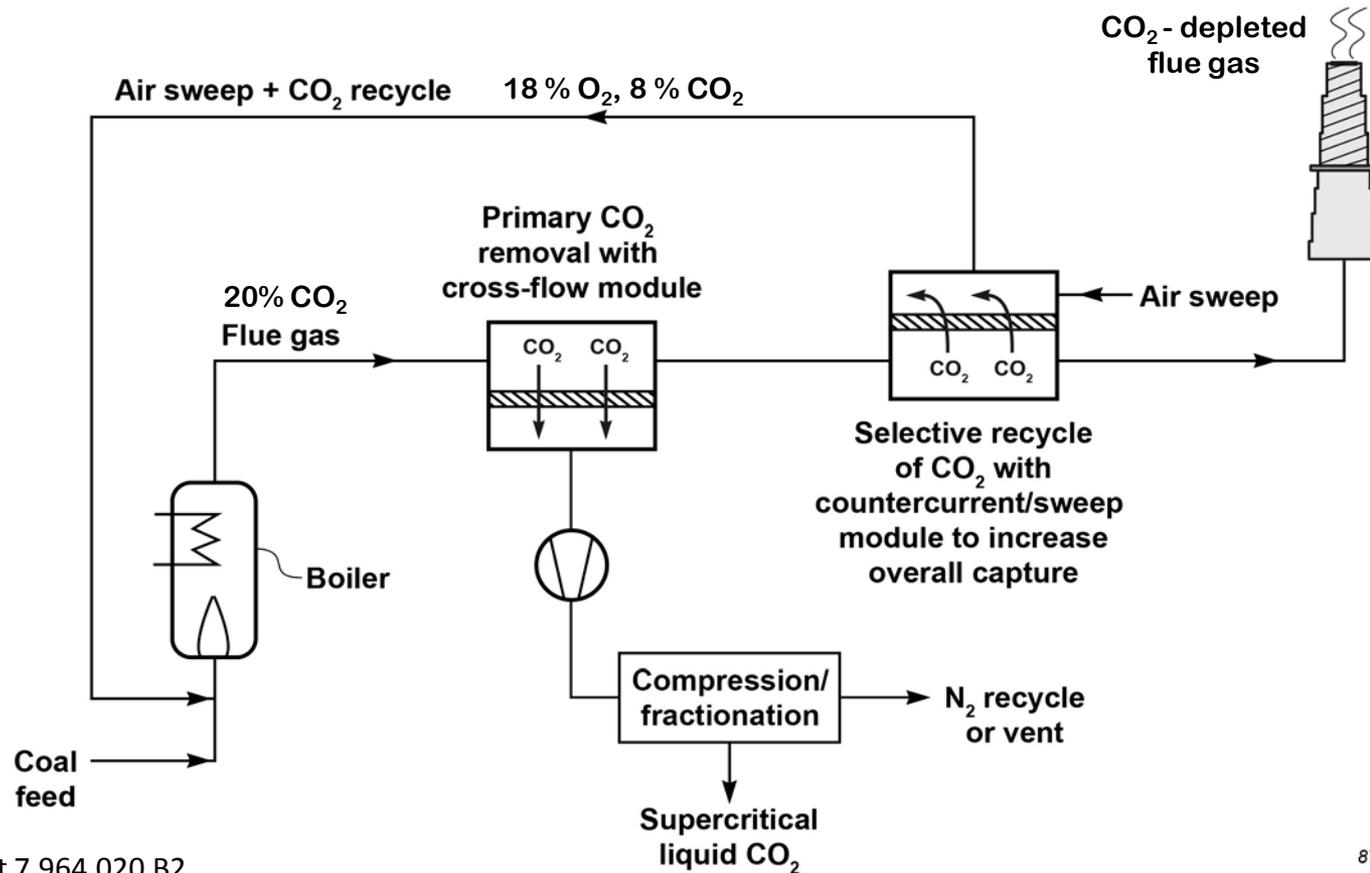
# CO<sub>2</sub> Capture at a Coal-Fired Power Plant



Membrane challenges for treating this large volume of gas include:

- How to generate driving force without using large compression or vacuum power?
- Large membrane area needed → high CO<sub>2</sub> permeance is a must!
- Harmful contaminants (fly ash, SO<sub>2</sub>, NO<sub>x</sub>, water, etc) potentially reduce effectiveness and lifetime.

# An Efficient Membrane CO<sub>2</sub> Capture Process

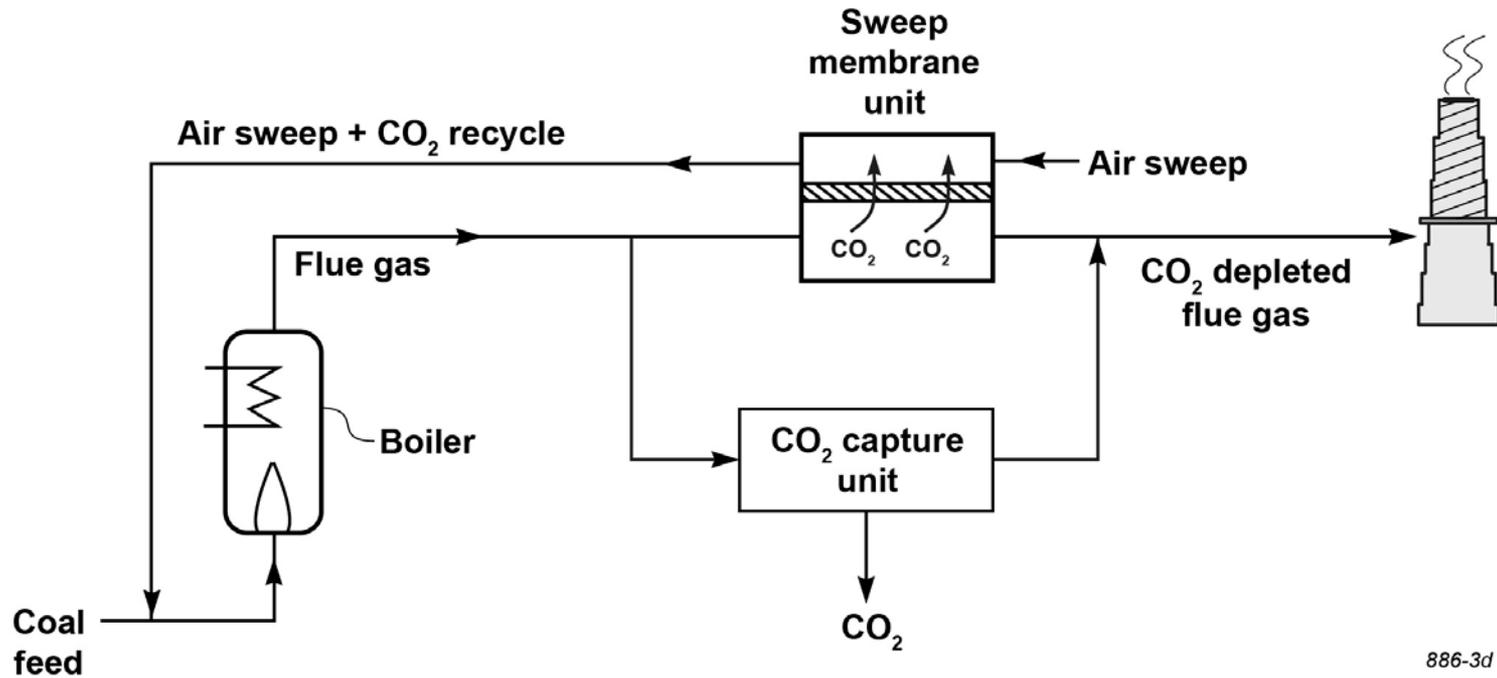


U.S. Patent 7,964,020 B2

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- Countercurrent/sweep with combustion air pre-concentrates CO<sub>2</sub> with little energy input
- An optimized process produces a 50% increase in LCOE at 90% capture

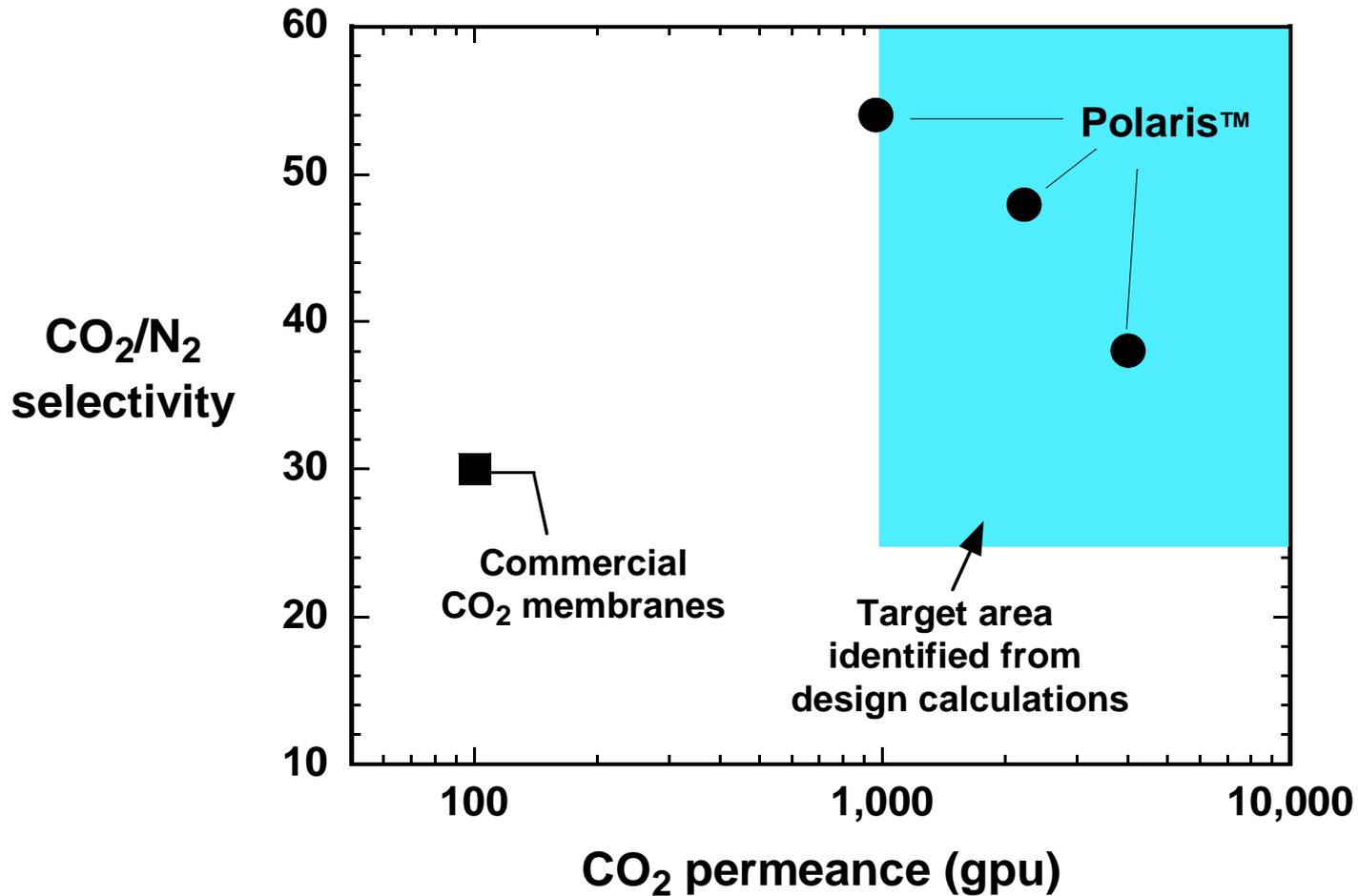
# A Hybrid CO<sub>2</sub> Capture Process



886-3d

- This parallel design avoids the use of any compression or vacuum equipment
- For natural gas, an enrichment factor of 4 to 5 can be achieved with selective exhaust gas recycle

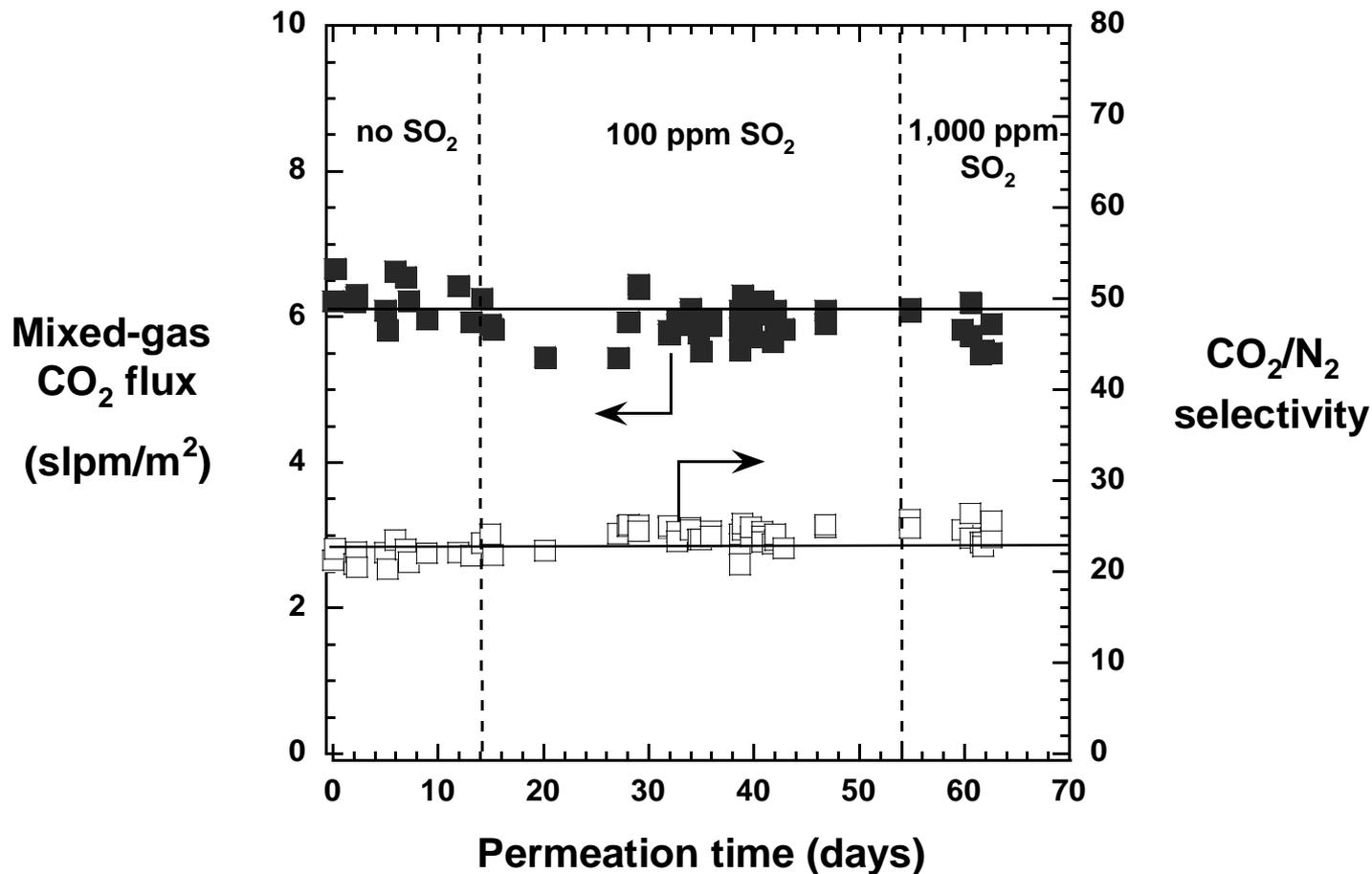
# Polaris™ Membranes



Pure-gas data at 25°C and 50 psig feed pressure

1 gpu =  $10^{-6}$  cm<sup>3</sup>(STP)/(cm<sup>2</sup> s cmHg) =  $3.35 \times 10^{-10}$  mol/(m<sup>2</sup> s Pa)

# Polaris Membranes Are Stable in SO<sub>2</sub>



Feed composition: 18% CO<sub>2</sub> in N<sub>2</sub>; temperature: 50°C

# 1 TPD Slipstream Test at APS Cholla

- Cholla is a 995 MW<sub>e</sub> PC plant using sub-bituminous coal
- Membrane skid houses 8" diameter cross-flow and countercurrent sweep modules
- System captures 1 TPD CO<sub>2</sub>



- Field test ran from April – July 2010
- Purpose of test was:
  - to evaluate membrane lifetime with real flue gas
  - Demonstrate sweep modules

# Cholla Test Results: Modules Are Stable

Fresh module

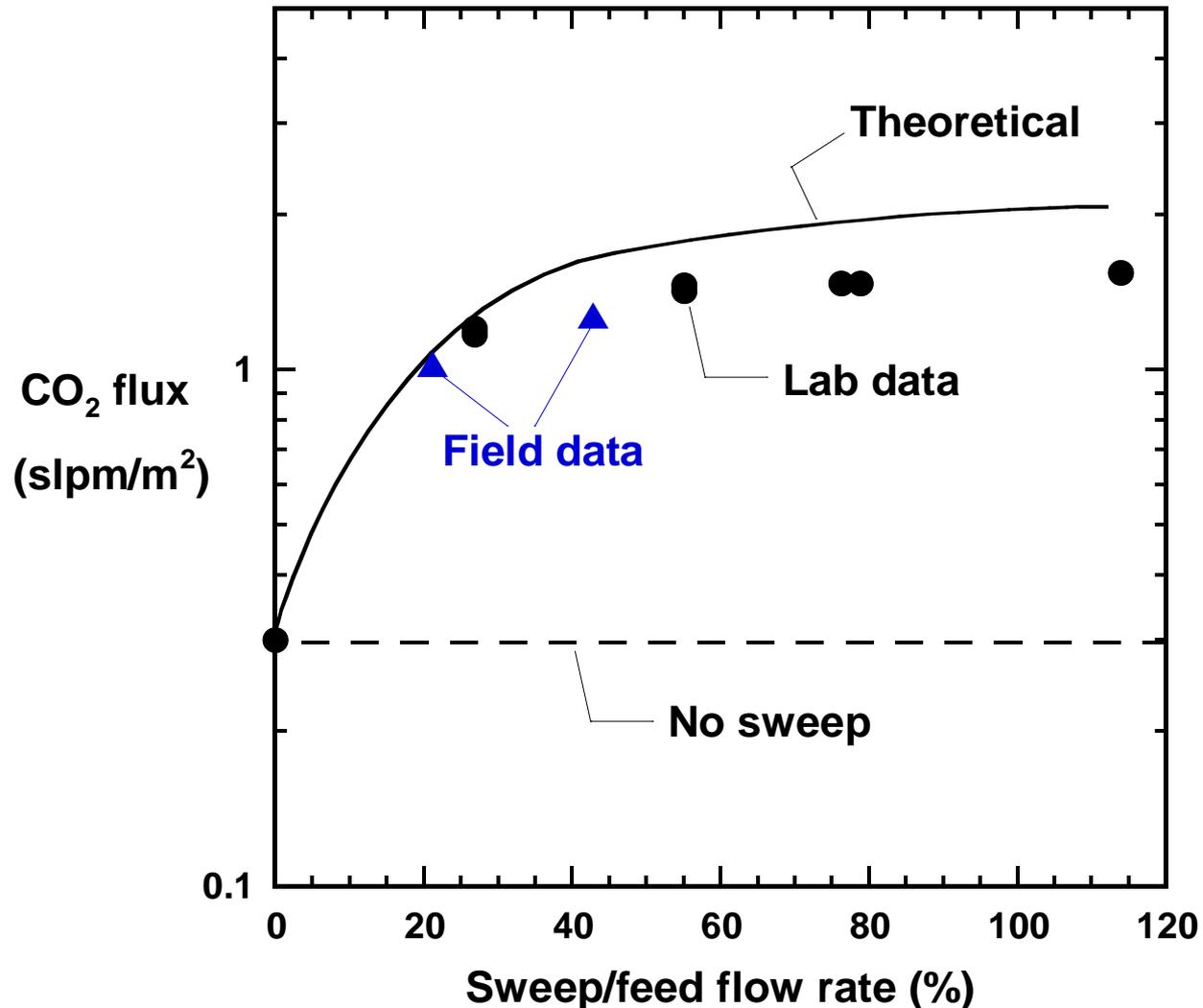


After 45 days of operation at Cholla



Module Number	Normalized CO <sub>2</sub> Permeance		Normalized CO <sub>2</sub> /N <sub>2</sub> Selectivity	
	Before	After	Before	After
5839 (Cross-flow)	100%	110%	100%	118%
5879 (Sweep)	100%	108%	100%	96%

# Cholla Test Results: Sweep Operation Works



# Next Steps: 20 TPD Project Timeline



BP1

BP2

BP3



## Cholla I (1 TPD)

- DOE project NT0005312 (completed 3/31/11)
- Collaboration with APS and EPRI
- Slipstream testing at Cholla plant

## Complete a Preliminary Systems and Economic Analysis



## Continue Membrane Optimization on 1 TPD System

- Run continuous tests at National Carbon Capture Center (NCCC)
- Improve membrane/module performance
- Investigate low-fouling module geometries



## Boiler Recycle / Water Recovery Study

- Evaluate CO<sub>2</sub> recycle and plant integration with B&W
- Investigate flue gas water recovery/management with EPRI



## Design and Install 20 TPD Demo (1 MW<sub>e</sub>)

- Design, build, and install the 20 TPD test system at NCCC



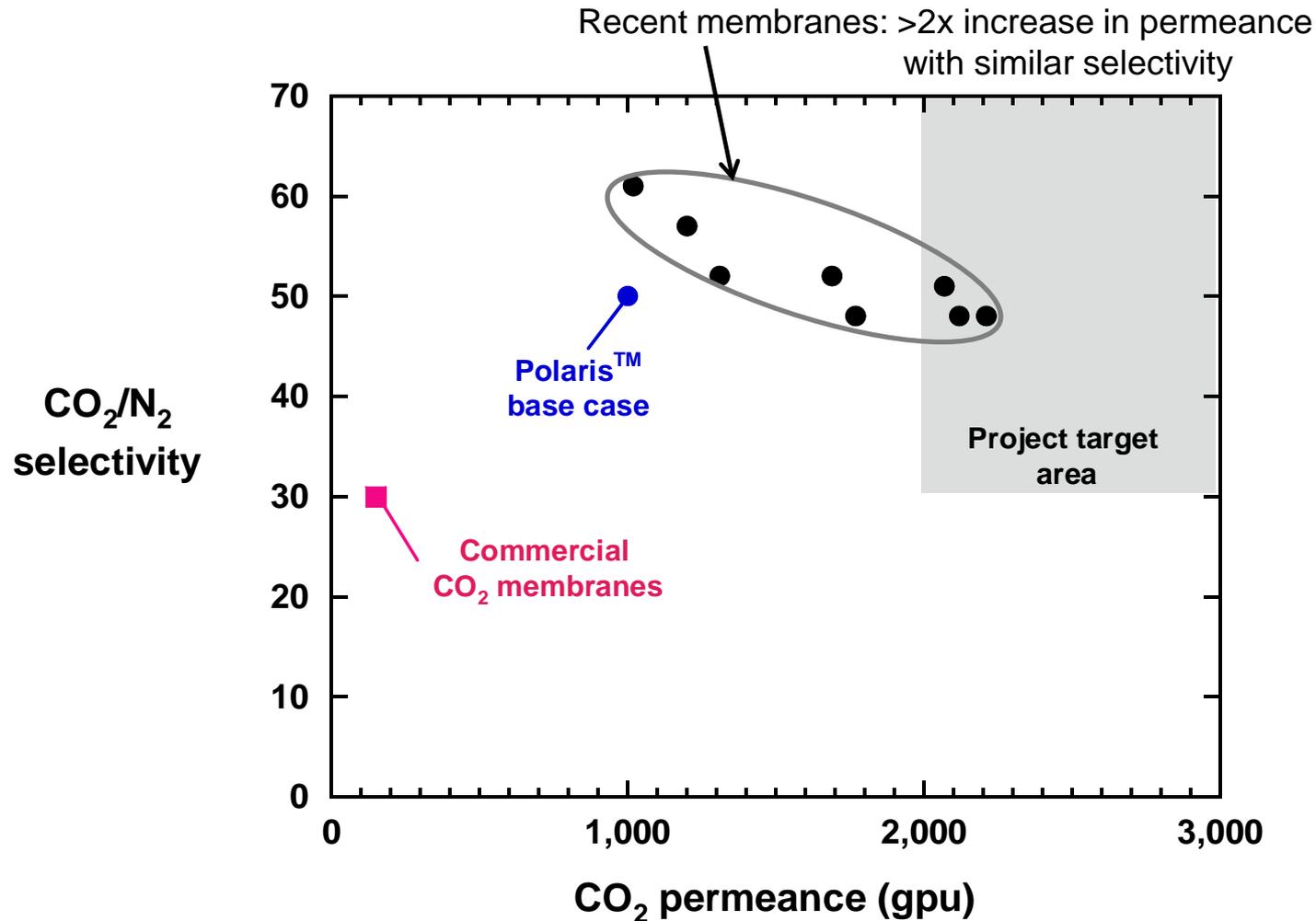
## Operate 20 TPD Demo (1 MW<sub>e</sub>)

- Run 6 month test
- Analyze results and prepare a comparative systems analysis

Blue arrow = DE-NT0005312  
Green arrows = DE-FE0005795



# Membranes Are Getting Better

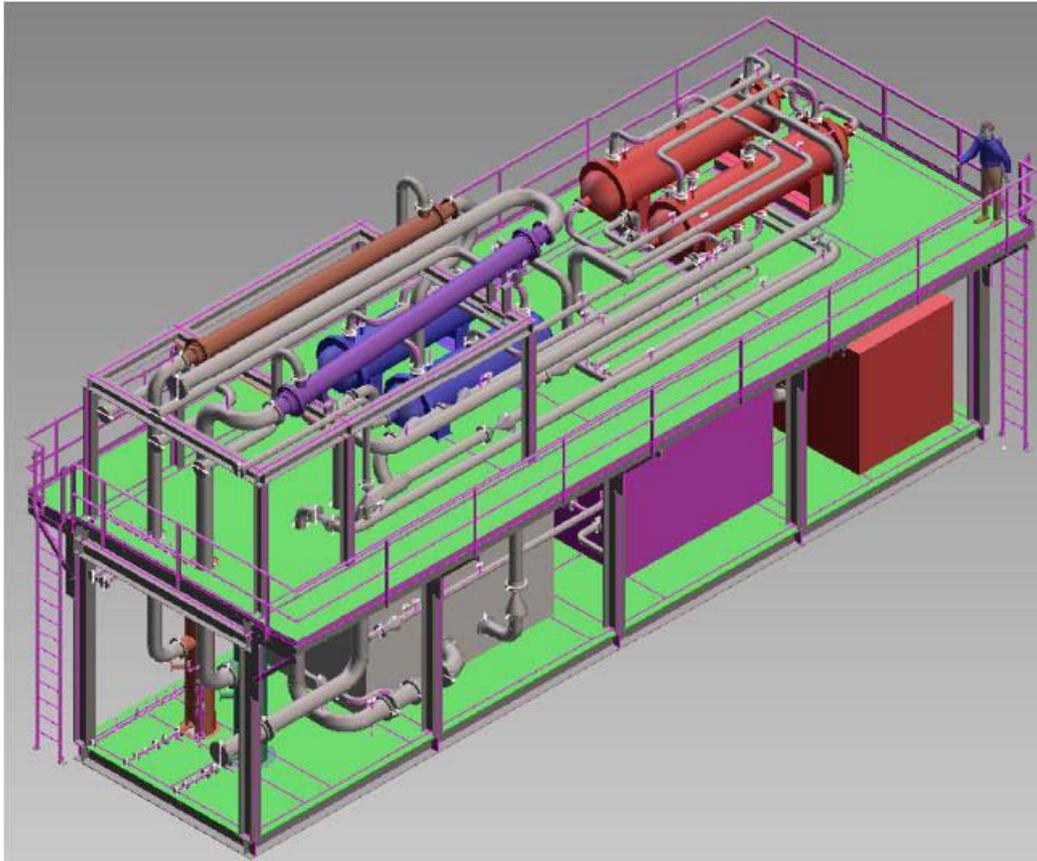


# 1 TPD System Testing at NCCC

1 TPD test system is a valuable field laboratory. System startup at NCCC is scheduled for September 2011. Items to study include:

- Performance and lifetime of rotating equipment and other system components
- New high performance membranes
- Low pressure drop module configurations
- New low-fouling module designs; compare with current baseline module
- Disposition of contaminants in membrane process

# Preliminary Design of 20 TPD System



- 20 TPD skid (or 1 MW<sub>e</sub>) will begin operation in 2013
- Uses commercial-sized membrane modules
- Approximate skid dimensions are 50 ft x 18 ft x 26 ft (l x w x h)

# 20 TPD System at NCCC/PC4



Picture courtesy of Mr. Tony Wu, Southern Company

# What Would a Large Membrane System Look Like?

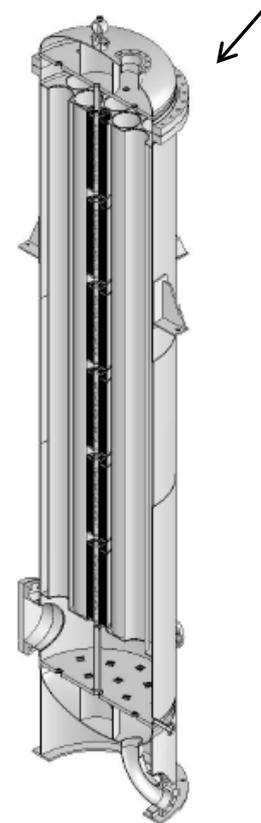


## Ashkelon desalination plant

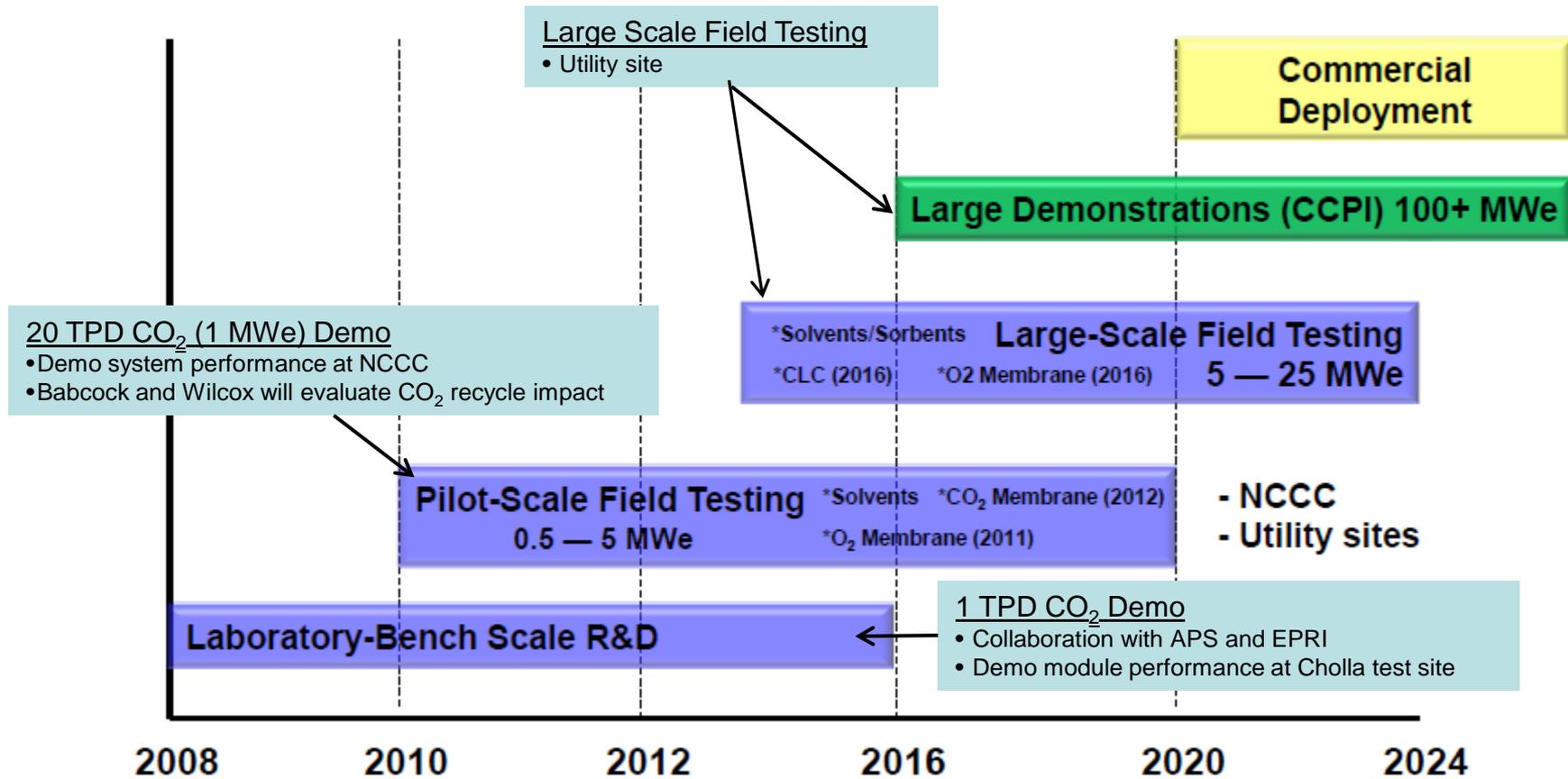
- 40,000 spiral-wound RO membrane modules (Dow Filmtec®)
- 1.5 million m<sup>2</sup> membrane area

## Flue gas membrane vessels

- ~100 vessels required for 550 MW<sub>e</sub> plant with current membranes
- Double the permeance → halve the vessels



# DOE CO<sub>2</sub> Capture Timeline



# Summary

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- Membranes have some advantages and can play a role in post-combustion CO<sub>2</sub> capture
- Process design is important to address how to provide affordable pressure ratio
- Membranes are getting better and have significant potential for further improvements
- Membrane technology is at the slipstream test stage; this testing is key to work out real world problems

# Acknowledgements

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