

# Effects of Exhaust Gas Recirculation (EGR) on Turbulent Combustion Emissions in Advanced Gas Turbine Combustors with High Hydrogen Content (HHC) Fuels

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# Outline of the Presentation

- **Yiguang Ju - Chemical kinetics with EGR effects, Reactor Assisted Turbulent Slot (RATS) burner studies at atmospheric pressure**
- **Bob Lucht and Jay Gore: High-pressure Premixed Axisymmetric Reactor Assisted Turbulent (PARAT) burner, initial measurements**
- **Michael Mueller – Advanced numerical modeling of the RATS and PARAT burners**

# Effects of CO<sub>2</sub> and H<sub>2</sub>O Diluents on

## Laminar & turbulent flame speeds, Chemical kinetics, Emissions

- What happens to the burning rate when diluents (CO<sub>2</sub>, H<sub>2</sub>O, etc.) are introduced? Four effects:
  - **Dilution** – Reduce reactant concentrations, reduce reaction *rates*
  - **Thermal** – Reduce flame temperature, reducing rate *coefficients*
  - **Transport** – thermal/mass diffusivity (**Lewis number**) and **Radiation**
  - **Chemical** – Reactions of “diluent” with fuel, oxidizer, and intermediates (e.g. **CO<sub>2</sub>+H→CO+OH** and **HCO+M=H+CO**, **H<sub>2</sub>O+O=2OH**)

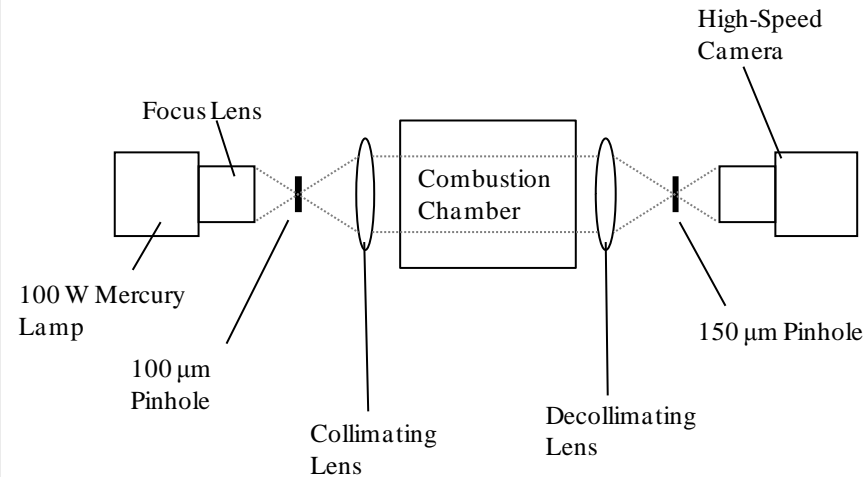
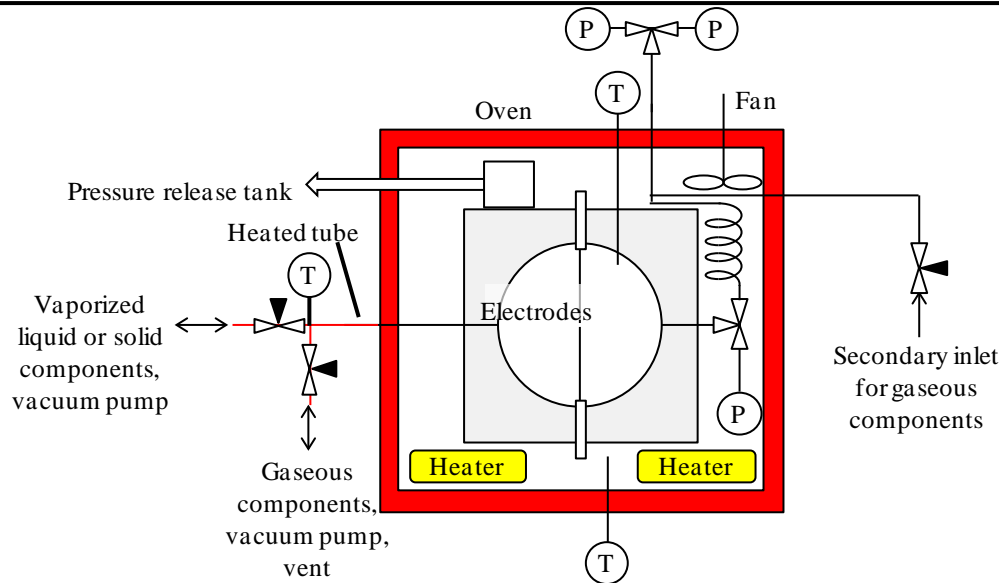
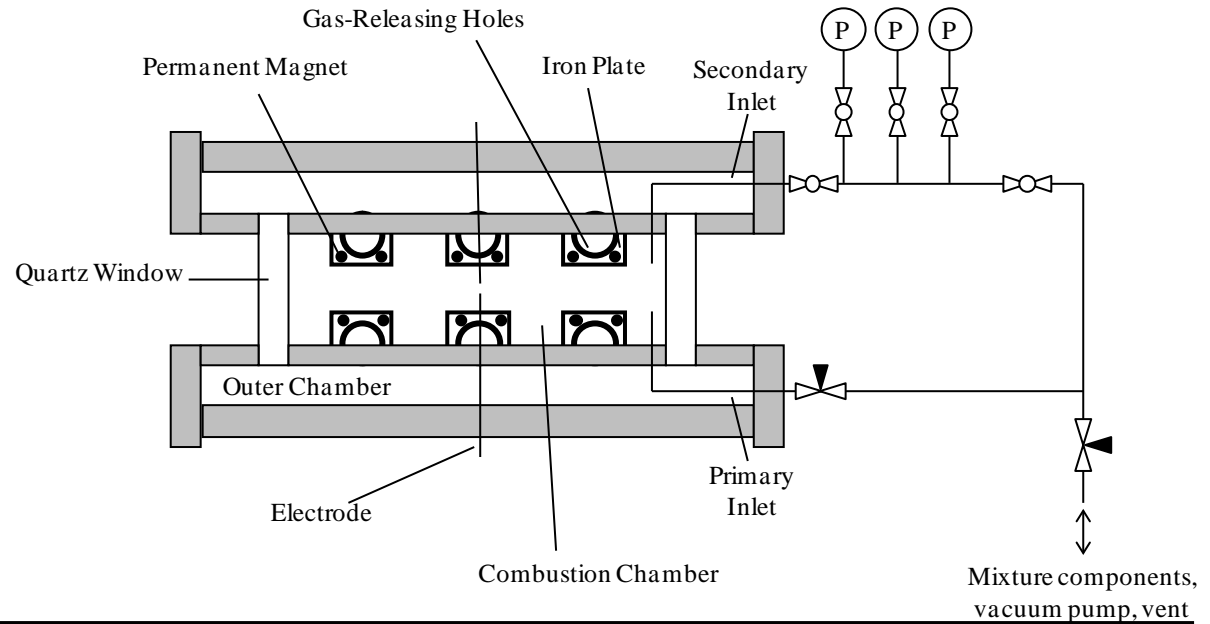
## Research accomplishments

- Flame speed measurements of HHC fuels with CO<sub>2</sub>/H<sub>2</sub>O additions
- High pressure kinetic mechanism (HP-Mech) for HHC fuels with EGR
- Turbulent flame speed and structure measurements with H<sub>2</sub>O/CO<sub>2</sub> dilution
- Radiation effect of CO<sub>2</sub>/H<sub>2</sub>O
- HO<sub>2</sub> diagnostics using Faraday Rotational Spectroscopy

# Laminar flame speeds: Experimental Design

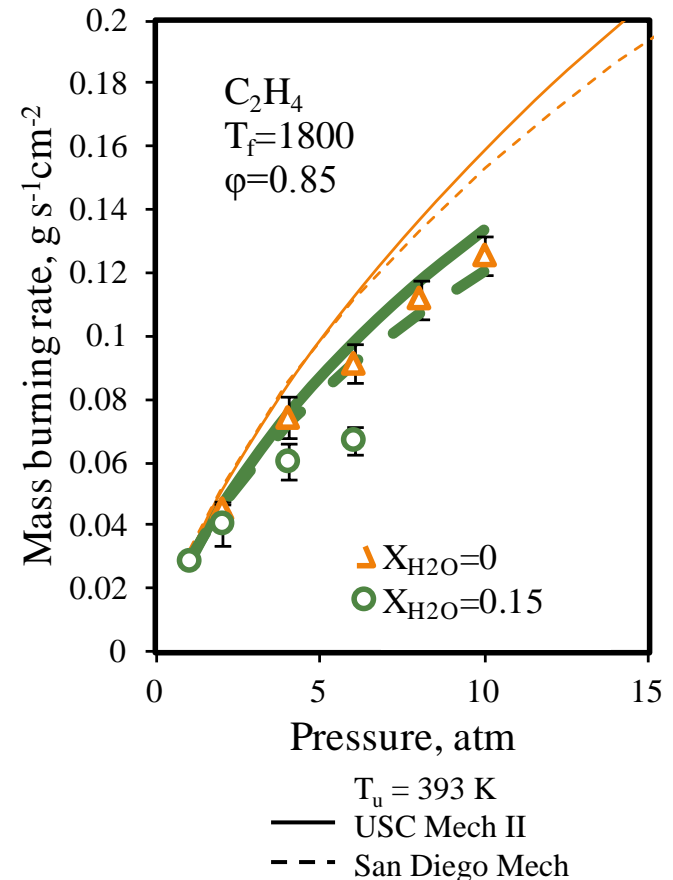
H<sub>2</sub>, CH<sub>4</sub>, CH<sub>2</sub>O, C<sub>2</sub>H<sub>2</sub>, C<sub>2</sub>H<sub>4</sub>, and C<sub>2</sub>H<sub>6</sub> fuels with H<sub>2</sub>O or CO<sub>2</sub> dilutions

- Two validated experiments
  - Cylindrical, room temperature chamber for CO<sub>2</sub> dilution from 1-20 atm
  - Spherical, heated chamber for H<sub>2</sub>O dilution from 1-10 atm
- Both experiments:
  - Centrally ignited spherically expanding flame
  - High speed schlieren imaging
  - Passive custom pressure-release valves



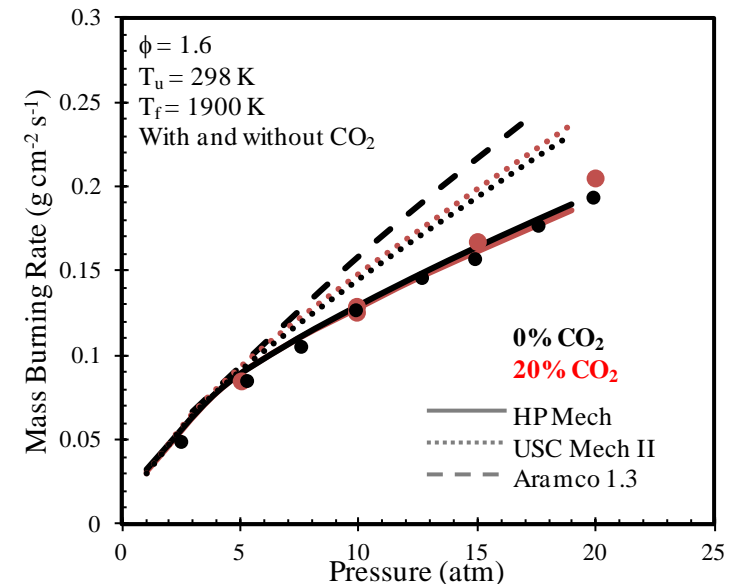
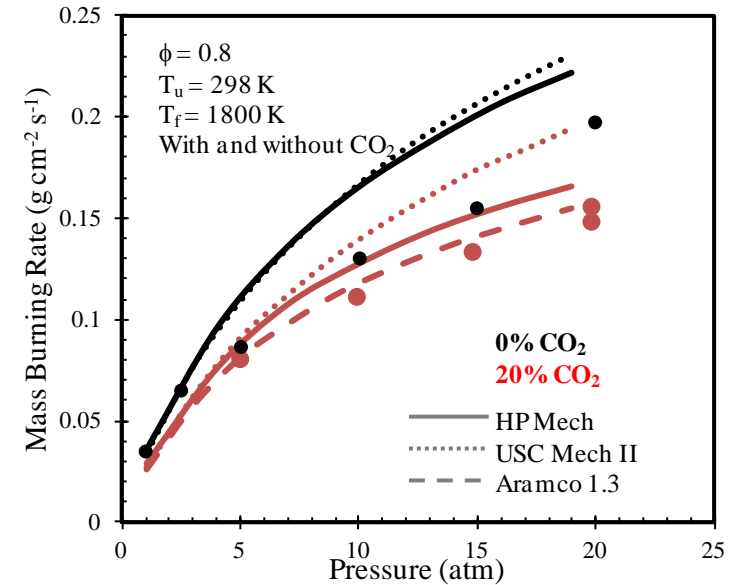
# For example: $C_2H_4$ with $H_2O$ dilution

- Water vapor decreases the mass burning rate, more at high pressure
- Models disagree with experiments and each other, more at high pressure
- Similar for hydrogen and syngas flames with water vapor\*



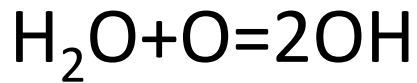
# C<sub>2</sub>H<sub>2</sub> Flames with CO<sub>2</sub> dilution

- CO<sub>2</sub> dilution decreases burning rate for lean conditions – but doesn't affect rich conditions
- Typically, CO<sub>2</sub> slows flame by decreasing H through reverse reaction of CO+OH=CO<sub>2</sub>+H
- Existing models do not have a good prediction. HP-Mech improves prediction.



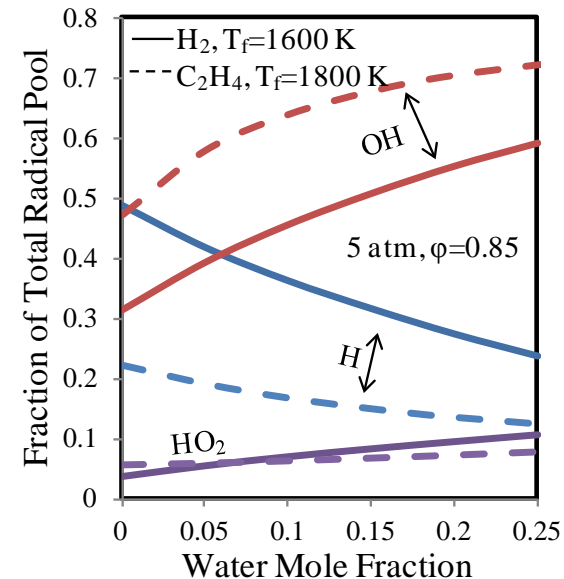
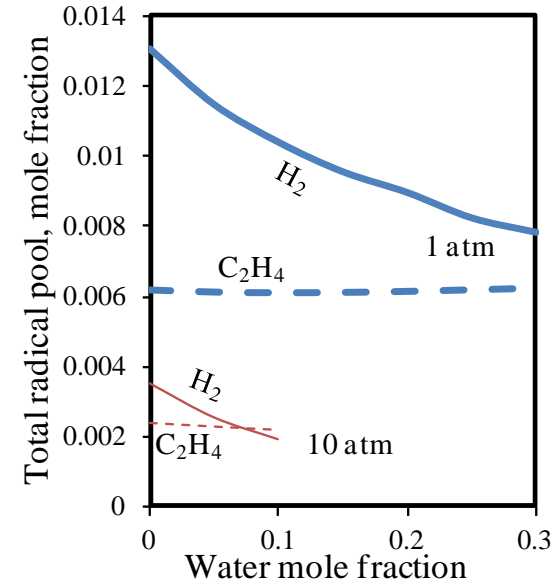
# Chemical effect of H<sub>2</sub>, C<sub>2</sub>H<sub>4</sub> Flames with H<sub>2</sub>O dilution

- Water addition decreases H and O radicals relative to OH and HO<sub>2</sub>



- High collisional efficiency of H<sub>2</sub>O
  - Increased HO<sub>2</sub> from  $\text{H} + \text{O}_2 + \text{M} = \text{HO}_2 + \text{M}$
  - Increased H from  $\text{HCO} + \text{M} = \text{H} + \text{CO} + \text{M}$

- Chemical effect increases with pressure



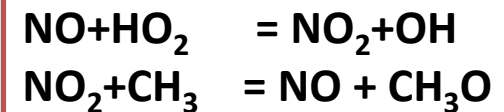
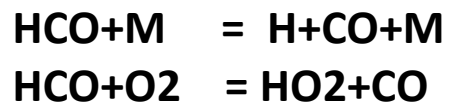
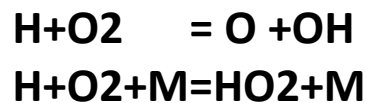
## Task 2a A high pressure mechanism (HP-Mech) for C<sub>0</sub>-C<sub>2</sub> hydrocarbon fuel with H<sub>2</sub>O and CO<sub>2</sub>

- Many models available, but... not for EGR, pressure dependency...
  - Most widely ones.: GRI-Mech, USC Mech II, optimization based, off-design problem
  - Dryer models: small hydrocarbons: H<sub>2</sub>, CO/CH<sub>4</sub>, CH<sub>2</sub>O, CH<sub>3</sub>OH, CH<sub>3</sub>CH<sub>2</sub>OH, not focused on EGR
  - Curran models: also try to optimize the experiments such as ignition delay and flame speed
  - ...

### HP-Mech

- Addressing the pressure dependence of reactions
- EGR effect
- Using the elementary rates with high level quantum computation and/or experimentally determined, *no optimization!*
- Update the thermochemistry database (e.g. Burcat and Ruscic database).

Key reactions:  
For example



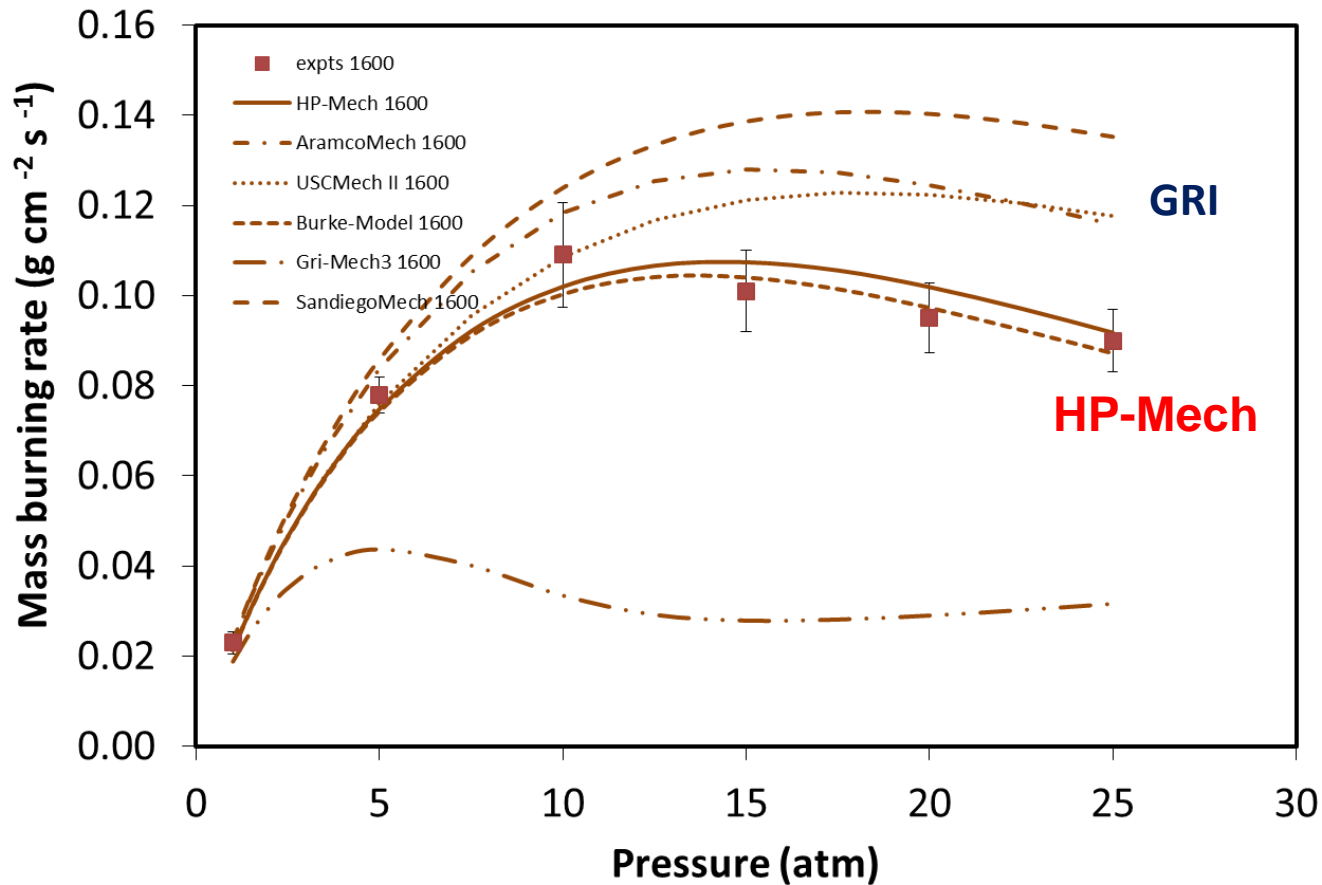


# High pressure mechanism (HP-Mech) development

- **Thermochemistry:** Active Thermochemical Tables
- **Transport:** chemkin library: H, H<sub>2</sub> and HE from Hai Wang USC Mech II
- **Reaction set:** up to C<sub>6</sub> - reflecting the most recent advance of rate determinations
  - H<sub>2</sub>-O<sub>2</sub> model (Burke et al, Int. J. Chem. Kinet. 44(2012), 444–474, update or modification)
  - CO+OH=CO<sub>2</sub>+H (Joshi et al, Int. J. Chem. Kinet. 38 (2006), 57-73)
  - HCO decomposition (Yang et al, 8<sup>th</sup> US National Combustion Meeting, Park City, Utah 2013)
  - HCO+O<sub>2</sub>=HO<sub>2</sub>+CO (Klippenstein private communication)
  - CH+O<sub>2</sub> reactions (Rohrig et al, Int. J. Chem. Kinet. 29(1997), 781-789; Bergeat et al, *Faraday Discuss.*, 119(2002), 67-77)
  - CH<sub>2</sub>+O<sub>2</sub> reactions (Lee et al, *J. Phys. Chem. A*, 116 (2012), pp 9245–9254; Blitz et al, *Z. Phys. Chem.* 225 (2011), 957–967)
  - CH<sub>2</sub> relaxations (Gannon et al, *J. Chem. Phys.* 132(2010), 024302)
  - H+CH<sub>3</sub>+M=CH<sub>4</sub>+M (Troe et al, *J. Chem. Phys.* 136(2012), 214309; Brouard et al, *J. Phys. Chem.* **93**(1989), 4047 )
  - CH<sub>3</sub>+HO<sub>2</sub> (Jasper et al Proc. Combust. Inst. 32, 279 (2009))
  - CH<sub>3</sub>+OH and CH<sub>3</sub>OH decomposition ( Jasper et al, *J. Phys. Chem. A* 111, 3932 (2007))
  - H+C<sub>2</sub>H<sub>2</sub>+M=C<sub>2</sub>H<sub>3</sub>+M and H+C<sub>2</sub>H<sub>4</sub>+M=C<sub>2</sub>H<sub>5</sub>+M (Miller and Klippenstein, *Phys. Chem. Chem. Phys.*, 6(2004), 1192 –1202)
  - CH<sub>2</sub>(S)+C<sub>2</sub>H<sub>2</sub>=C<sub>3</sub>H<sub>3</sub>+H (Gannon et al *J. Phys. Chem. A* 114(2010) 9413–9424; Polino et al, *J. Phys. Chem. A*. 117(2013):12677-92)
  - HCCO+O<sub>2</sub> (Klippenstein et al., Proc. Combust. Inst. 29 (2002), 1209; Zou et al., *Phys. Chem. Chem. Phys.*, 6(2004), 1697-1705)
  - C<sub>2</sub>H<sub>2</sub>+OH (Senosiain et al., *J. Phys. Chem. A* 109(2005) 6045-6055)
  - C<sub>2</sub>H<sub>3</sub>+O<sub>2</sub> (Klippenstein private communication; Matsugi et al, Int. J. Chem. Kinet. 46: 260–274, 2014)
  - HCCO+OH=HCOH+CO (Mai et al, *Chem. Phys. Lett.* 592(2014) 175-181)
  - C<sub>2</sub>H<sub>4</sub>+O (Nguyen, et al., *J. Phys. Chem. A* 109(2005) 7489-7499)
  - ....

# Hydrogen flames-1

Mass burning rate of H<sub>2</sub>/O<sub>2</sub>/He phi=0.85

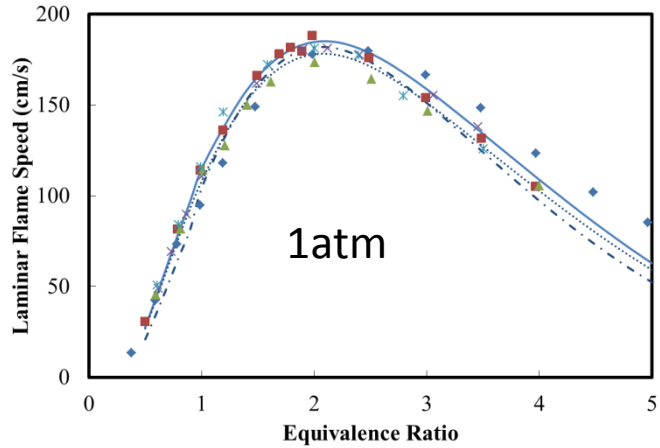


H+O<sub>2</sub>+M dominate pressure dependence

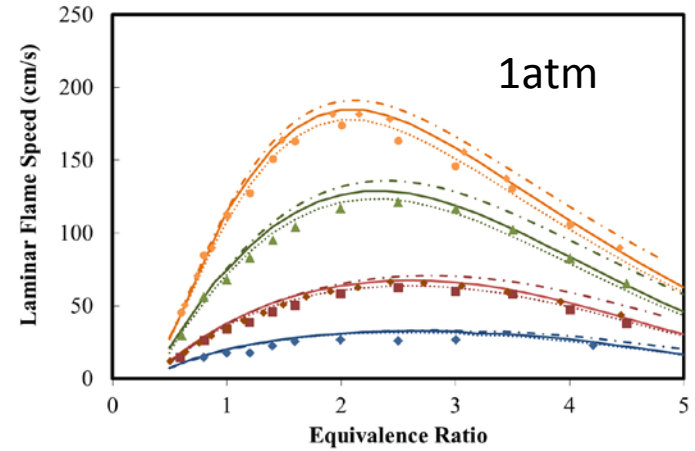
# H2/CO flames

HP-Mech —  
 USC Mech II .....  
 Aramco Mech ····-

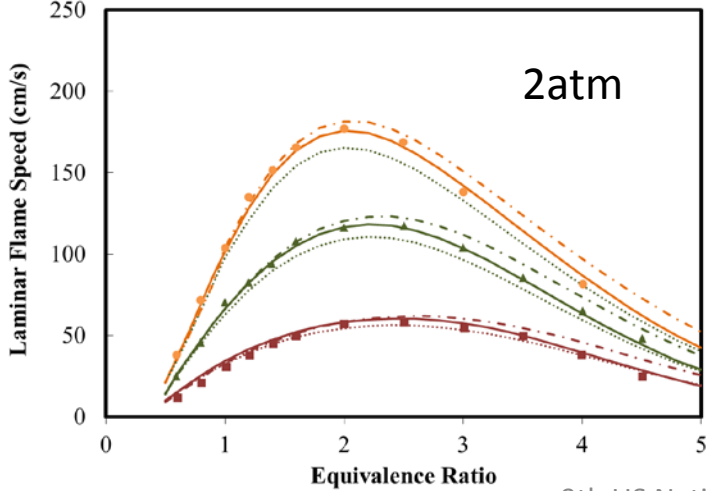
50H2-50CO-air-flame



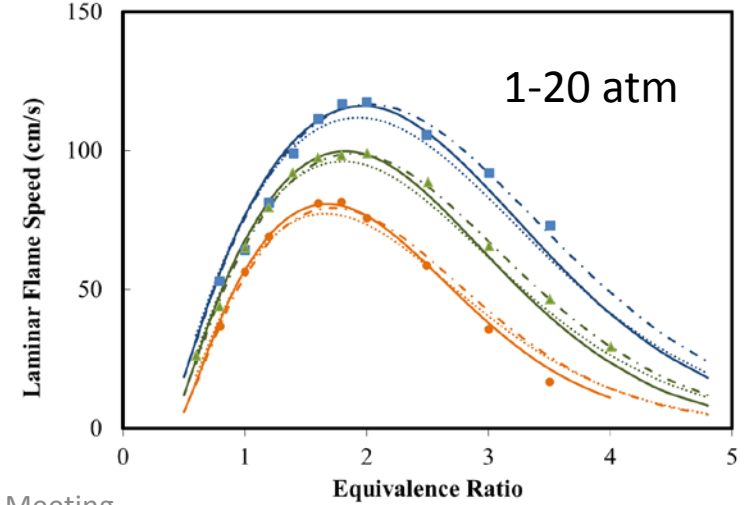
Mixture composition effect at 1 atm  
 $x\%H_2$  and  $1-x\%CO$   $x=1,5,25,50$



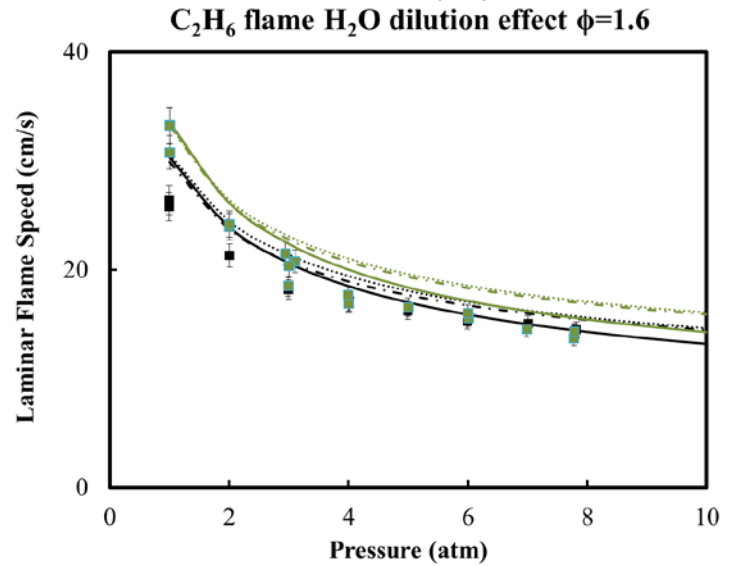
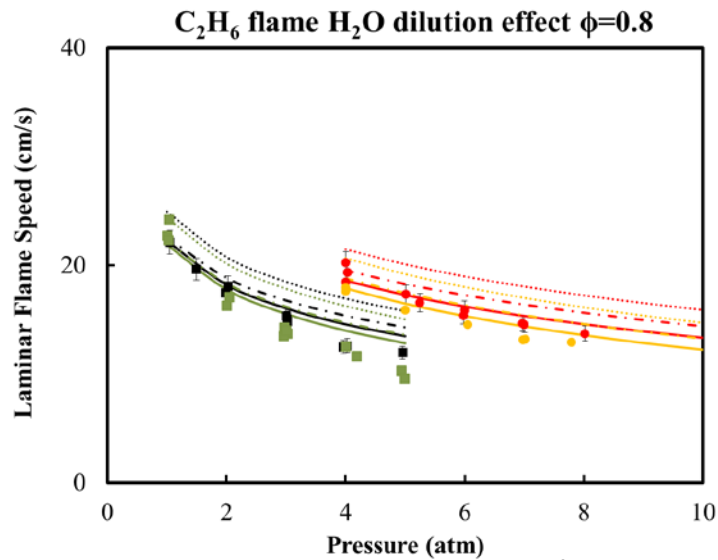
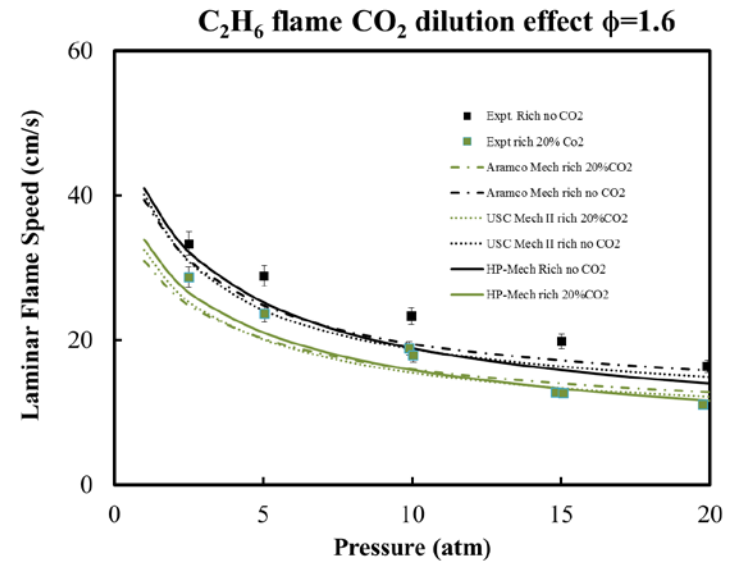
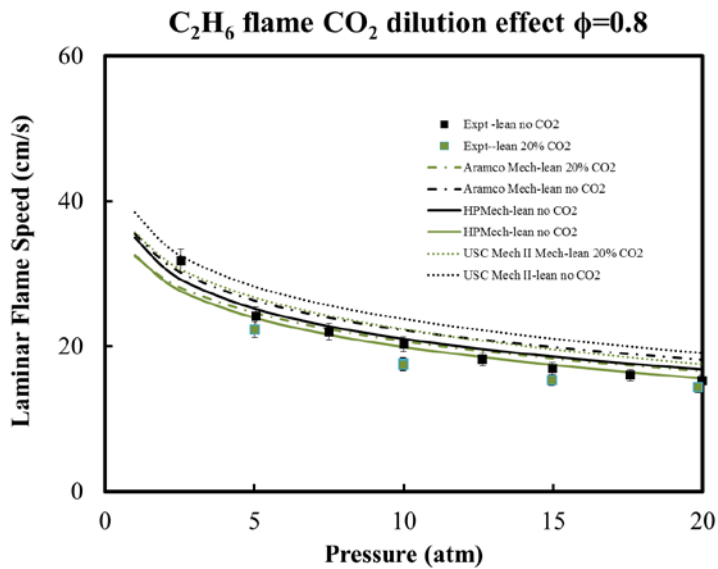
Mixture composition effect at 2 atm  
 $x\%H_2$  and  $1-x\%CO$   $x=5, 25, 50$



Pressure of 25% H2-75% CO  
 $P=5, 10, 20$  atm



# Ethane flame



# Task 4. EGR Kinetic Effect on Turbulent CH<sub>4</sub> Flames

## Investigation of EGR Effects on Turbulent Flame Structure in RATS Burner

### Objectives

- Investigate turbulent burning velocity and flame structures
  - At EGR conditions and elevated temperature
  - Systematic measurements of H<sub>2</sub>O and CO<sub>2</sub> dilution
    - Effects of H<sub>2</sub>O<sup>1</sup> and CO<sub>2</sub><sup>2</sup> dilution were investigated separately in previous studies only with methane/air.
- Identify **chemistry/thermal/transport effects** on turbulent premixed flames<sup>3</sup> in EGR conditions.

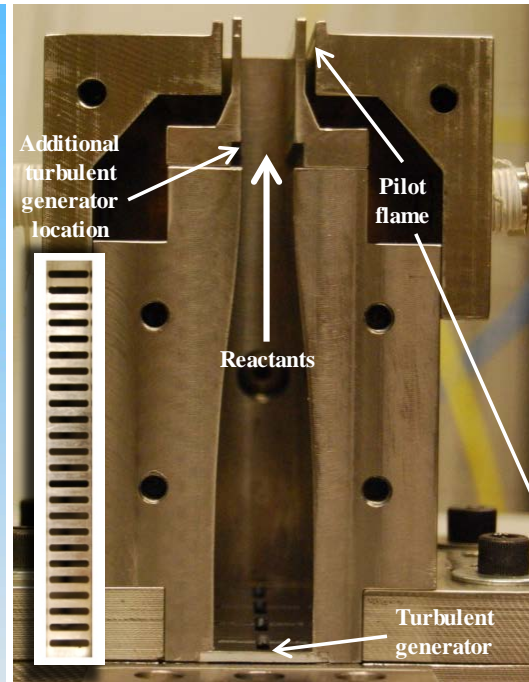
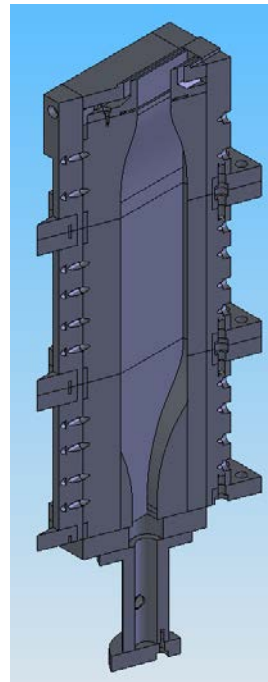
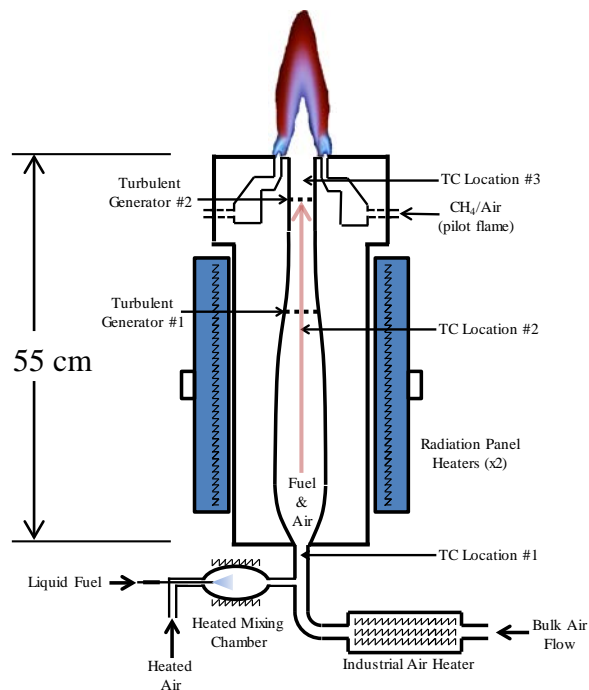
<sup>1</sup> H. Kobayashi, et al., Proc. Combust. Inst. 32 (2009) 2067-2614.

<sup>2</sup> H. Kobayashi, et al., Proc. Combust. Inst. 31 (2007) 1451-1458.

<sup>3</sup> J. F. Driscoll, Prog. Energy Combust. Sci. 34 (2008) 91-134.

# Experiment, RATS Burner

- **Reactor Assisted Turbulent Slot burner (RATS burner)<sup>1</sup>**
  - Heat large flow rates (1000 LPM) up to 700 K with CO<sub>2</sub>/H<sub>2</sub>O/N<sub>2</sub> dilutions
  - ~ 55 cm heated length, 100 × 10 mm exit cross-section ( $D_H \approx 18$  mm)
  - Two turbulence generators<sup>2,3</sup>, homogeneous isotropic turbulence confirmed by hot-wire anemometry
  - High Reynolds number ( $Re_{\text{bulk}} > 10,000$ )

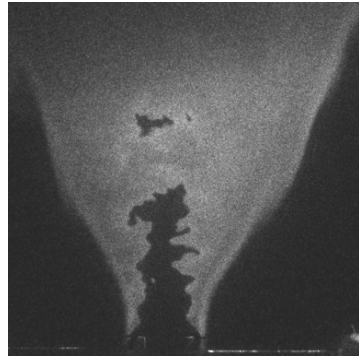


<sup>1</sup>S. H. Won, B. Windom et al, *Combust. Flame* 161 (2014) 475-483.

<sup>2</sup>Coppola, G., and Gomez, A., *Experimental Thermal and Fluid Science*, Vol. 33, 2009, pp. 1037-1048.

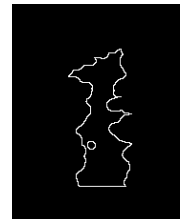
<sup>3</sup>Venkateswaran, P. et al., *Combustion and Flame.*, 158, 2011, 1602-1614

# Determination of turbulent flame speed, $S_T$



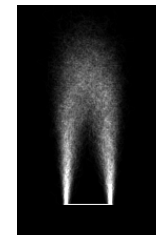
Single Image of OH PLIF

Find inner edge

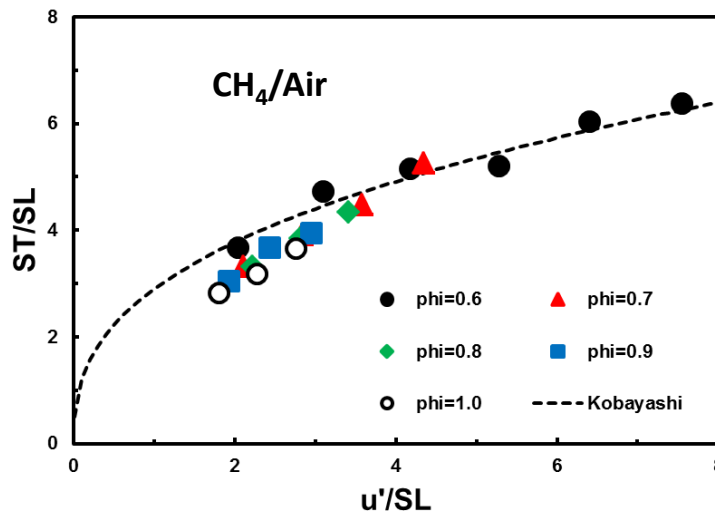


Flame perimeter from single image

Stack perimeters from 500 images



PDF of Flame Perimeters

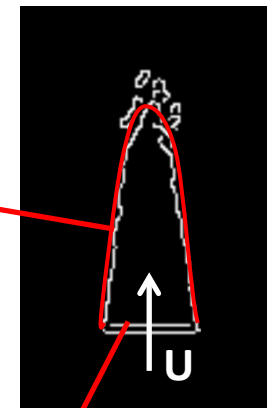


$$S_T = \frac{Uw}{L_p}$$

Find inner edge



$L_p$   
(4<sup>th</sup> order polynomial fit)

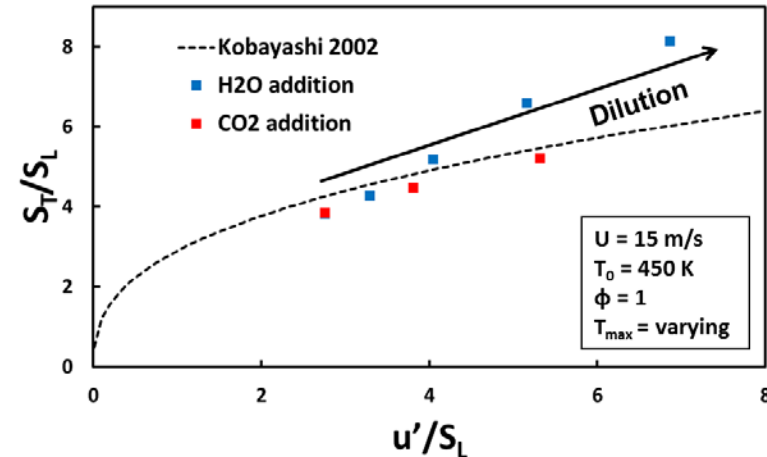
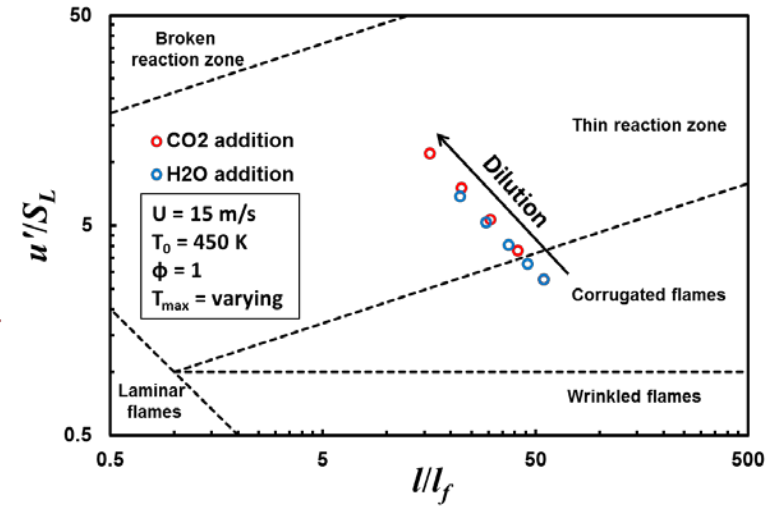
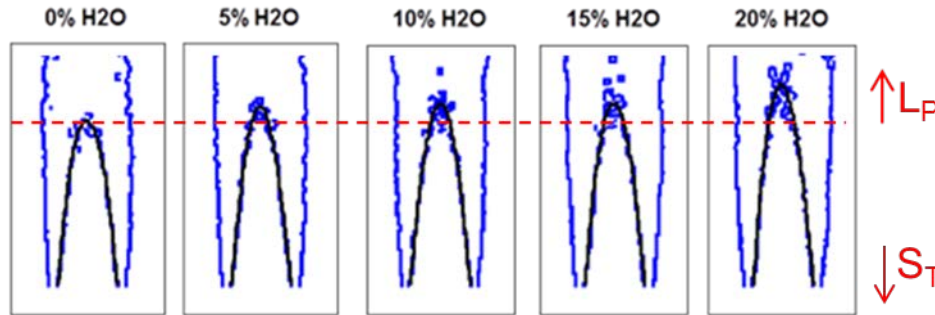


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“PDF method” gives similar results to method seen in H. Kobayashi, *Exp. Therm. Fluid Sci.* 26 (2002) 375-387

# Effects on flame speed with EGR dilution

$$S_T = \frac{Uw}{L_P}$$



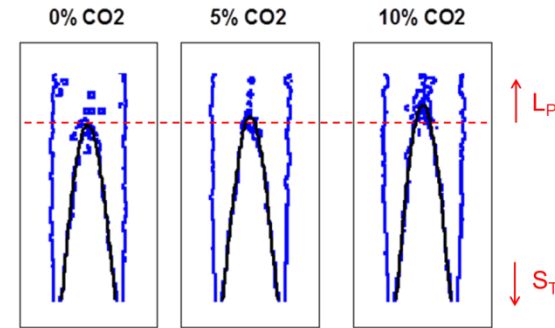
- Both CO<sub>2</sub> and H<sub>2</sub>O addition decrease turbulent burning velocity,  $S_T$
- Strong decrease in laminar flame speed  $S_L$ 
  - Drop from 70.6 cm/s to 28.4 cm/s for 20% H<sub>2</sub>O
  - Drop from 70.6 cm/s to 36.8 cm/s for 10% CO<sub>2</sub>
- $S_T/S_L$  increases with dilution for both CO<sub>2</sub> and H<sub>2</sub>O addition
  - More pronounced increase for CO<sub>2</sub>, however

- Why does normally  $S_T/S_L$  increases with dilution?
- How do we know the effects are thermal or kinetic?



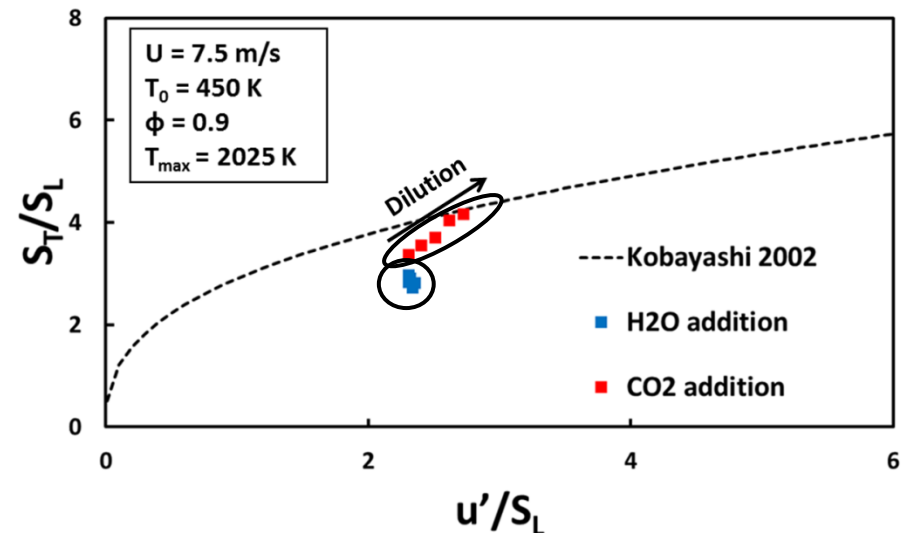
# EGR Dilution effect at **Constant Temperature:** Corrugated Flames

- H<sub>2</sub>O dilution has almost no discernable effect on L<sub>p</sub>, S<sub>T</sub>, or S<sub>T</sub>/S<sub>L</sub>
- Thermal effects were clearly the dominant factor for H<sub>2</sub>O dilution
- CO<sub>2</sub> dilution produces (~10%) decrease in S<sub>T</sub>, **kinetic effect**
- Turbulence **reduces the kinetic effect** of CO<sub>2</sub> on burning velocity
- CO<sub>2</sub> dilution increases turbulence-turbulent flame speed coupling due to the combined chemistry and transport effect (Le). (Promoted instability)



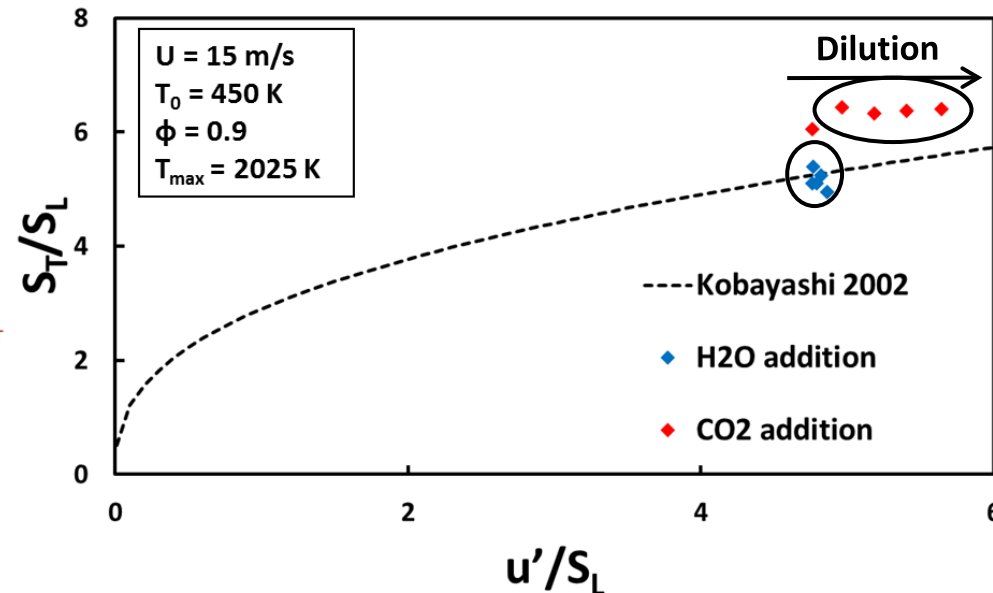
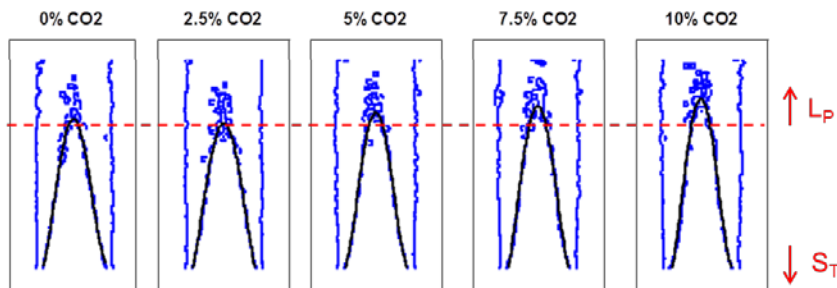
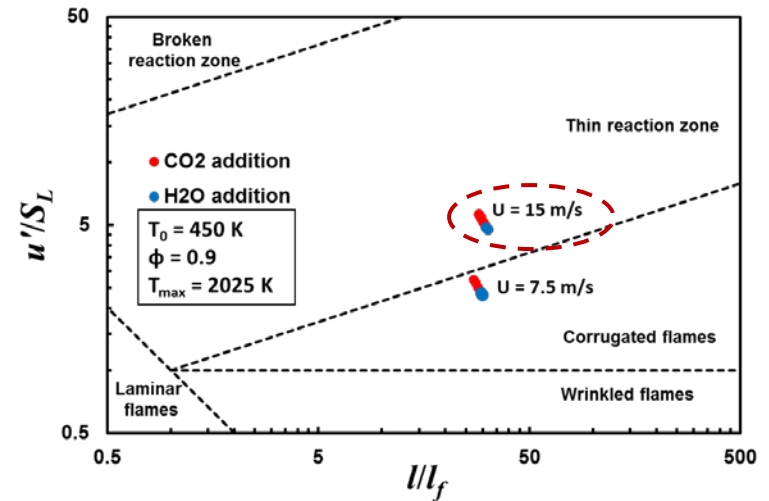
$$\frac{S_T}{S_L} \sim \left(\frac{u'}{S_L}\right)^{0.5} \left(\frac{1}{Le}\right)^{0.5}$$

- ↑ 10% H<sub>2</sub>O results in u'/S<sub>L</sub> ↑ 2% and 1/Le ↓ 8%
- ↑ 10% CO<sub>2</sub> results in u'/S<sub>L</sub> ↑ 18% and 1/Le ↑ 8%



# EGR Dilution at Constant Temperature: Thin Reaction Zone

- H<sub>2</sub>O again has no significant effect on  $L_p$ ,  $S_T$ , or  $S_L$
- Turbulence increases the decrease of  $S_T$  with CO<sub>2</sub> addition, enhance the turbulence-chemistry coupling.
- Turbulent flame speed deviates from the conventional  $S_T$  correlation.

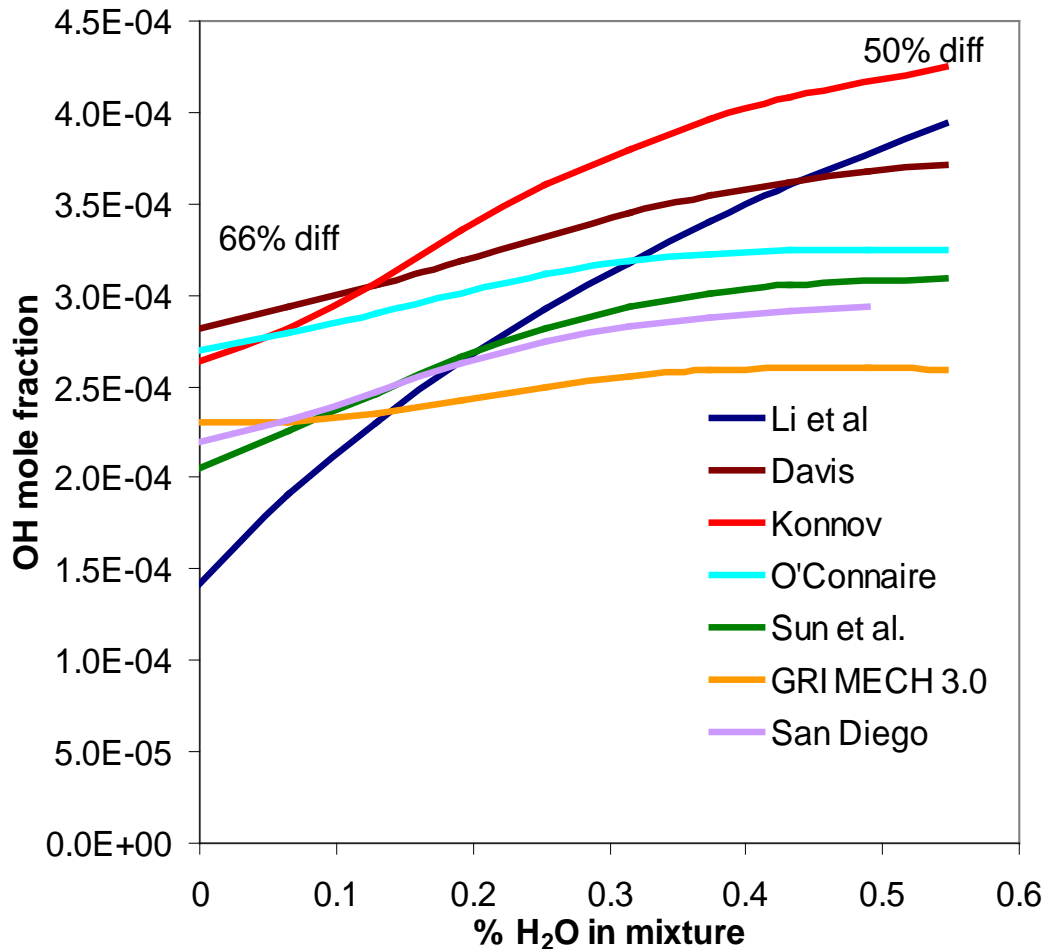


# Conclusions

1.  $\text{H}_2\text{O}$  and  $\text{CO}_2$  dilution have strong thermal, transport, and chemistry effects on the turbulent flame speed of methane. The conventional  $S_T/S_L$  vs.  $u'/S_L$  correlation may not apply.
2. Thermal effects are the dominant factor in affecting burning velocity for both  $\text{H}_2\text{O}$  and  $\text{CO}_2$  dilution.
3. At constant adiabatic flame temperature,  $\text{H}_2\text{O}$  dilution does not produce significant impacts on the normalized burning velocity  $S_T/S_L$  due to the opposing effects of kinetics and transport.
4. For  $\text{CO}_2$  dilution, in the corrugated flame regime, the competition between transport effect and chemistry effect results in an increase in  $S_T/S_L$ , thus stronger dependence of turbulent flame speed on Reynolds number.
5. In the thin reaction zone,  $\text{CO}_2$  addition results in stronger chemistry effect at higher Reynolds number and an approximately constant  $S_T/S_L$ , deviating from the conventional turbulent flame speed correlation.

## Future Plans

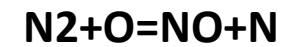
- Development of HP-Mech with **NO<sub>x</sub> at high pressure**.
- CH<sub>4</sub>/air + CO<sub>2</sub>, H<sub>2</sub>/air + H<sub>2</sub>O/CO<sub>2</sub> will be further investigated in turbulent premixed flames at higher pressure. ( $S_T$  and flame structures)
- Studies of the transport effects on turbulent flame structure



### Big problem:

Comparison of predicted **peak OH concentrations** of hydrogen flames by seven different kinetic models.

**Radicals prediction is not constrained in existing models!**  
**Large uncertainty to predict NO<sub>x</sub> emissions!**



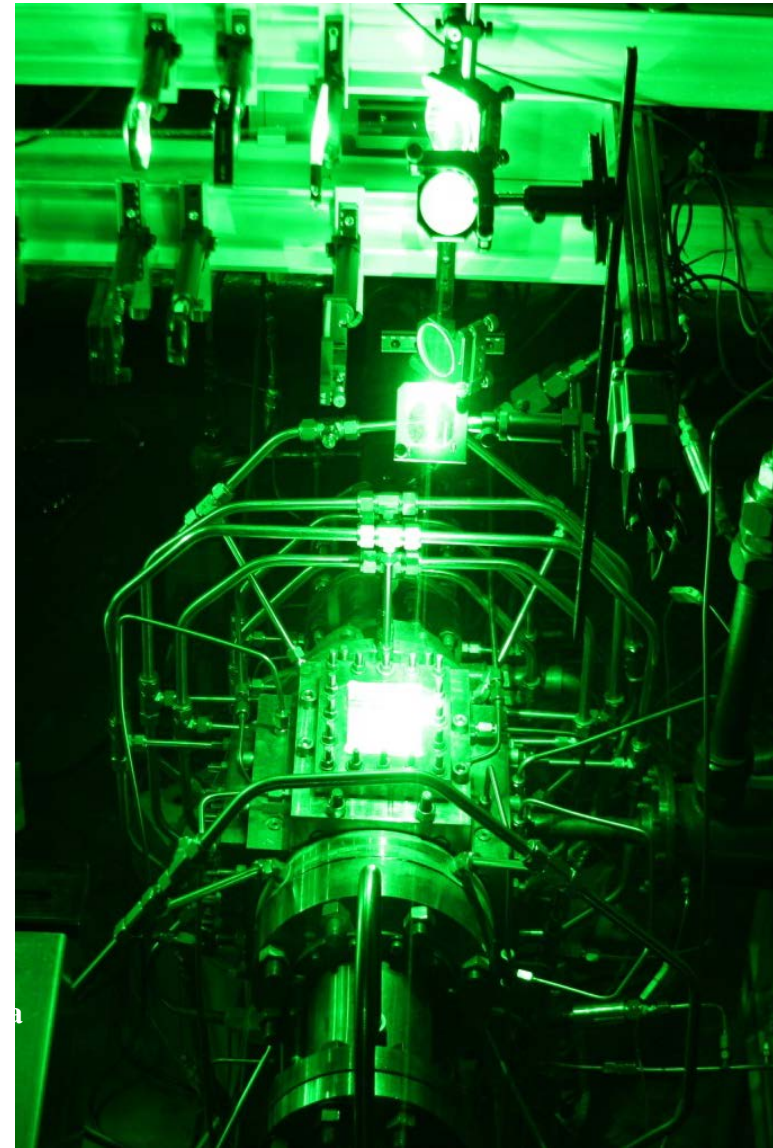
# High-Pressure PARAT Burner Studies

Robert Lucht and Jay Gore  
Purdue University

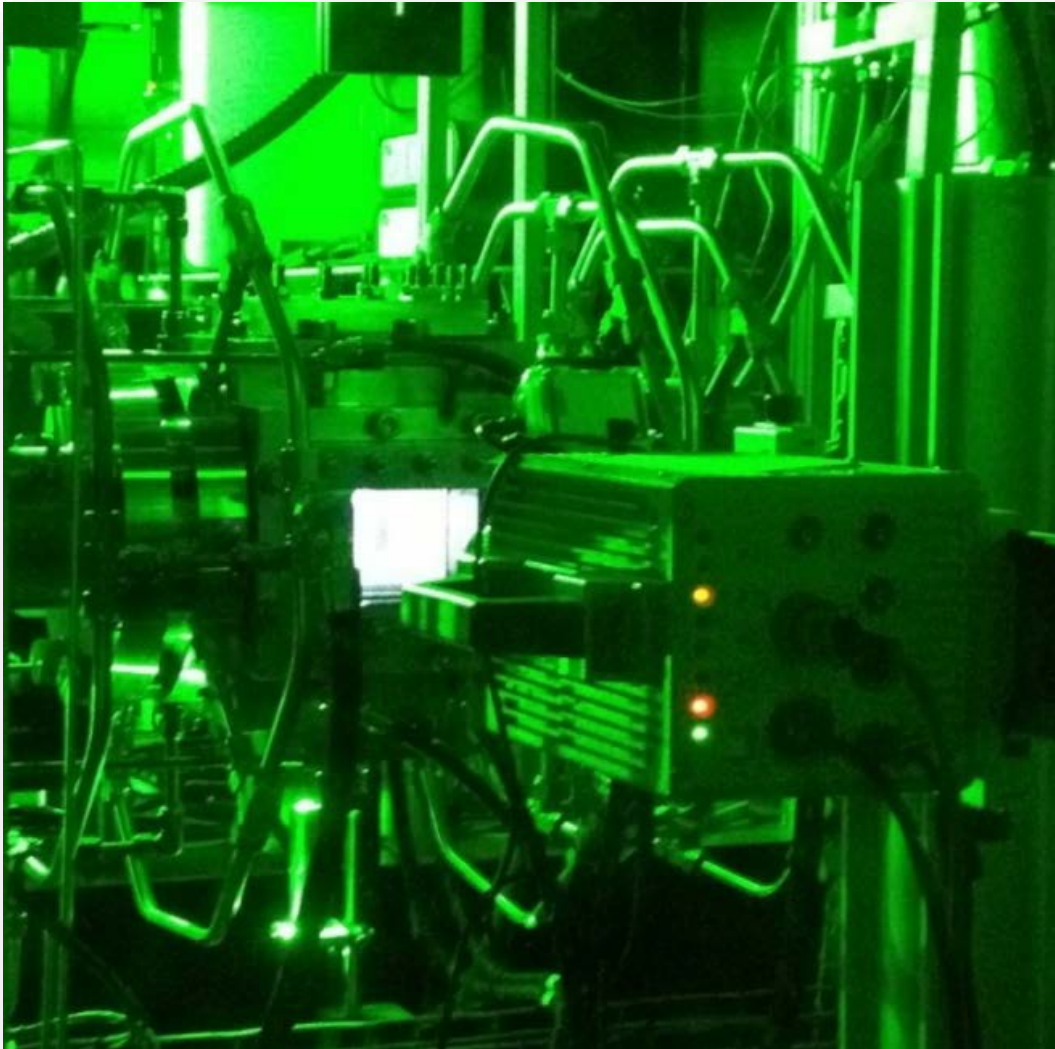
- Design and fabrication of PARAT burner
- Initial measurements at atmospheric pressure
- Planned high-pressure measurements

# Purdue Gas Turbine Combustion Facility (GTCF)

<b>High Pressure Lab System</b>	<b>Maximum Flow Capacity</b>	<b>Max Operating Condition</b>
Natural Gas Heated High Pressure Air	9 lbm/s 4 kg/s	700 psi / 1100 K 1500 F
Electric Heated Air or Nitrogen	1 lbm/s 0.5 kg/s	600 psi / 800 K 1000 F
Nitrogen	5 lbm/s 2 kg/s	1,500 psi
Liquid Aviation Fuel (Kerosene)	1 lbm/s 0.5 kg/s	1,500 psi
Natural Gas	1 lbm/sec 0.5 kg/s	3500 psi

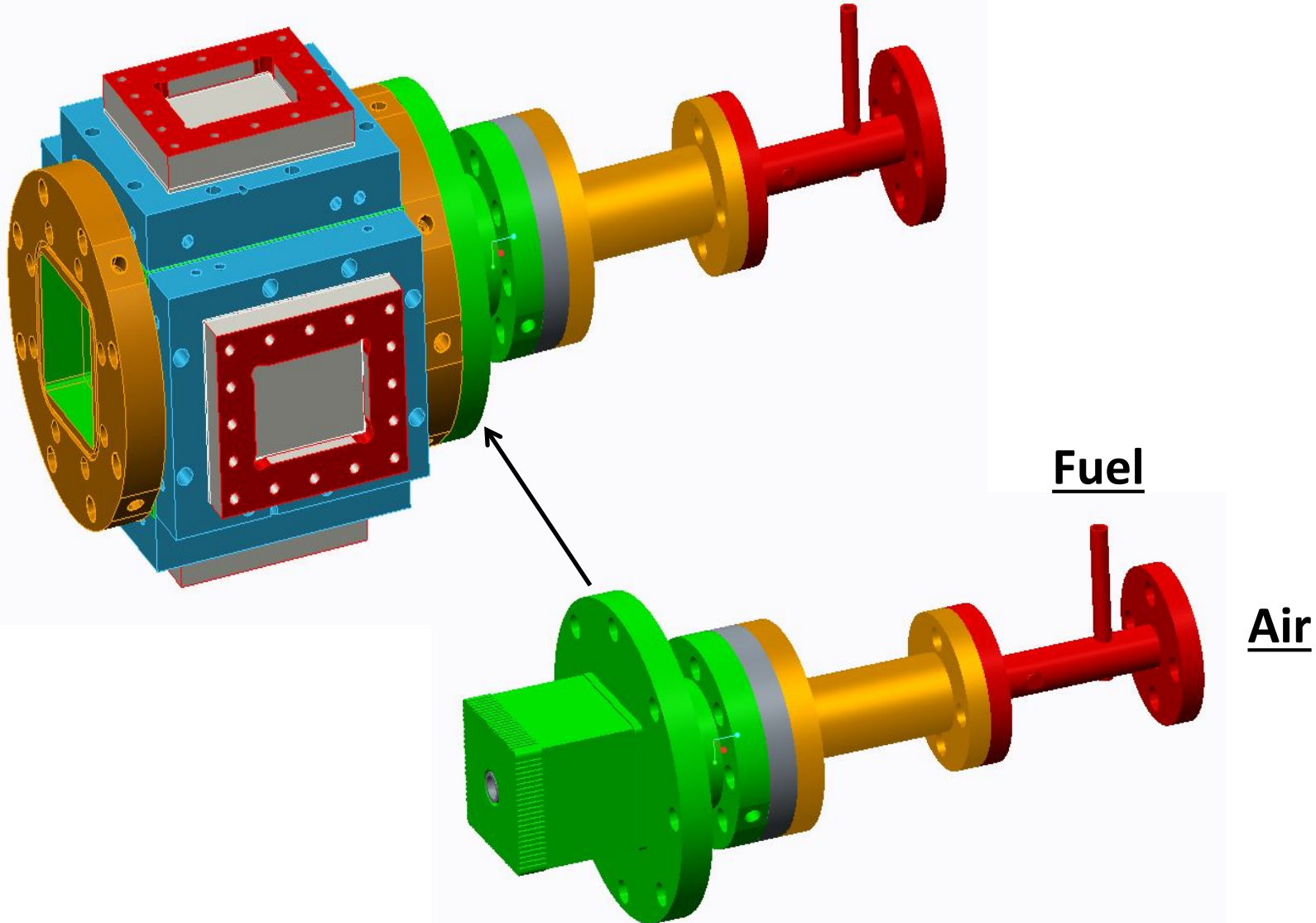


# Laser Diagnostics for High-Pressure Test Rig



- 10 kHz stereo PIV
- 10 kHz OH PLIF
- Pulse burst laser is being delivered this week for PIV, PLIF at data rates up to 100 kHz

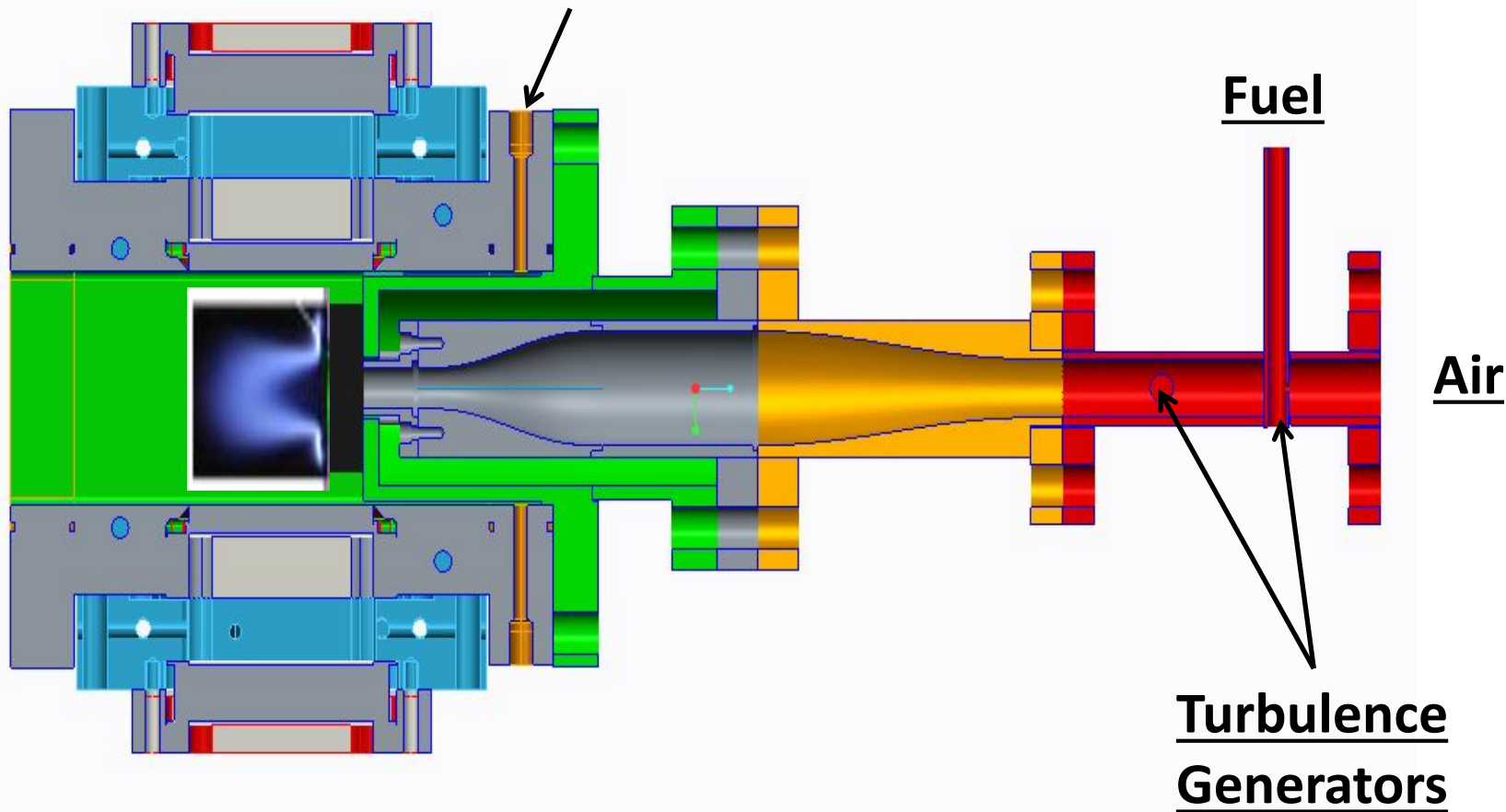
# Assembly of PARAT Burner into the Windowed High-Pressure Test Rig





# Cross-sectional View of PARAT Burner into the Windowed High-Pressure Test Rig

Pilot Fuel/Air Mixture



# Initial Operation of the PARAT Burner at Atmospheric Pressure: Operating Conditions

	Without EGR		With EGR	
Flame No.	1	2	3	4
Re	10000	20000	10000	10000
Equivalence ratio	0.8	0.8	0.8	0.8
CO <sub>2</sub> percentage by mass%	0.0	0.0	10.0	20.0
Air flow rate (l/min)	122.2	244.4	107.6	93.4
CH <sub>4</sub> flow rate (l/min)	10.3	20.5	10.1	9.9
CO <sub>2</sub> flow rate (l/min)	0.0	0.0	8.3	16.2
CO <sub>2</sub> /CH <sub>4</sub> mass flow rate ratio	0.0	0.0	2.26	4.5
H <sub>2</sub> flow rate (l/min)	2.0	2.0	2.0	2.0

# IR Imaging of PARAT Burner Flames

- **Turbulent lean premixed methane flame**

- $Re = 8950$
- Burner diameter ( $D$ ) = 15 mm

- **FLIR Infrared Camera**

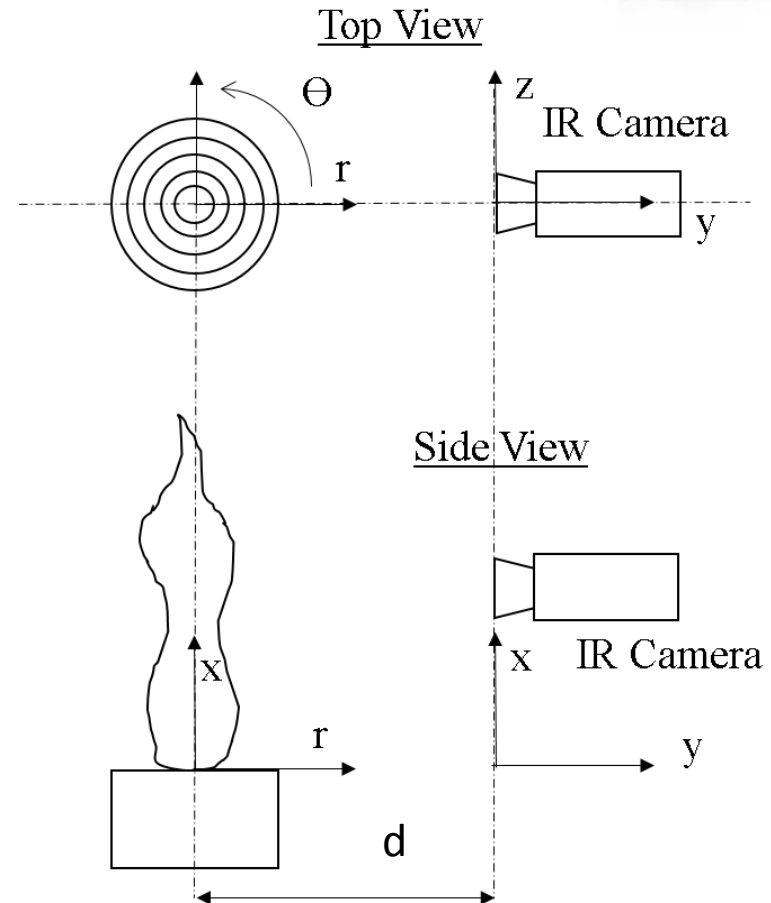
w/ band pass filters

- $H_2O$ :  $2.58 \pm 0.03 \mu m$
- $H_2O$  and  $CO_2$ :  $2.77 \pm 0.1 \mu m$
- $CO_2$ :  $4.38 \pm 0.08 \mu m$

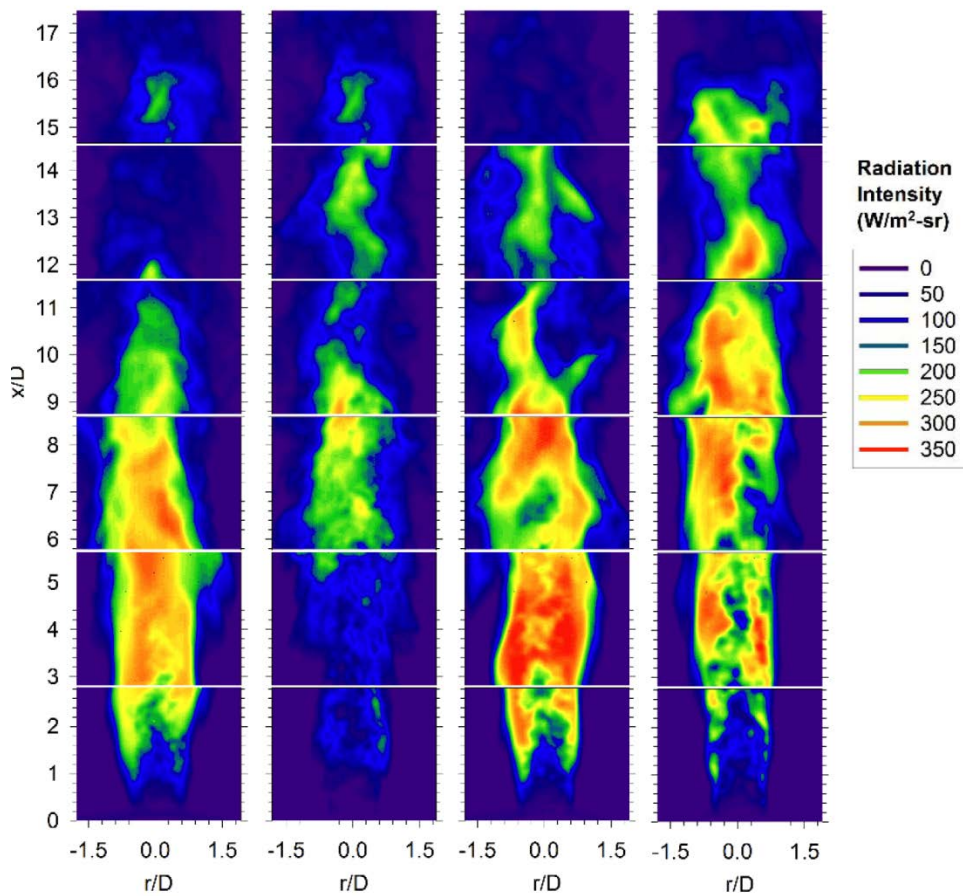
- **Distance between camera and flame**

$d = 0.5 m$

- **Sampling frequency=430 Hz**



# IR Imaging of PARAT Burner Flames



Flame #1    Flame #2    Flame #3    Flame #4

Infrared images of the CO<sub>2</sub> (4.3 micrometer band) for the four different flames at a representative exposure time of 20  $\mu$ s

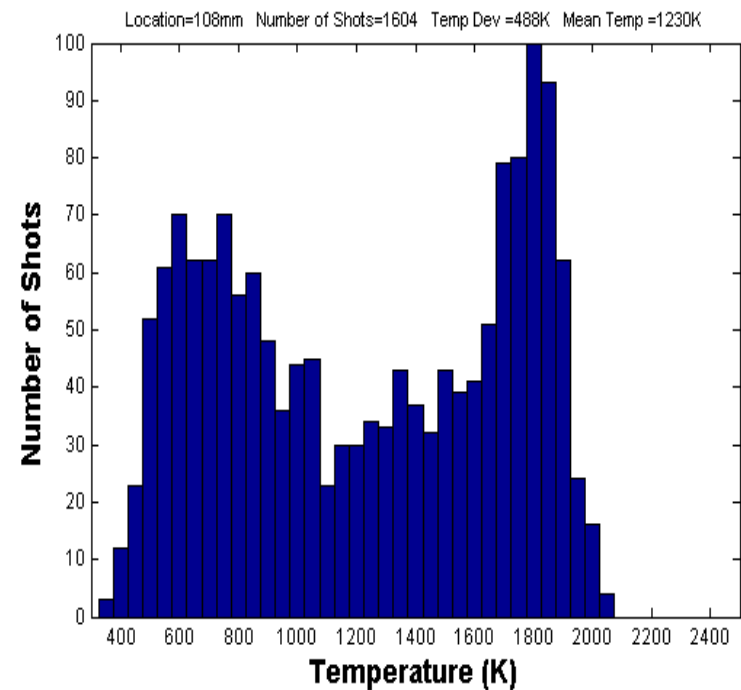
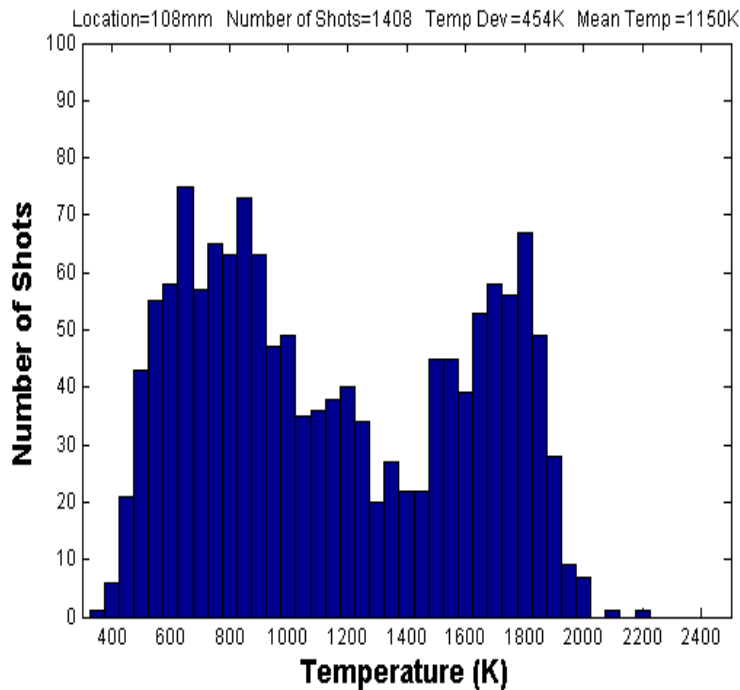
Flame No.	Without EGR		With EGR	
	1	2	3	4
Re	10000	20000	10000	10000
Equivalence ratio	0.8	0.8	0.8	0.8
CO <sub>2</sub> percentage by mass%	0.0	0.0	10.0	20.0
Air flow rate (l/min)	122.2	244.4	107.6	93.4
CH <sub>4</sub> flow rate (l/min)	10.3	20.5	10.1	9.9
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# CARS Measurements in Atmospheric Pressure PARAT Burner Flames: Temperature PDFs Along Centerline

Axial Location

108 mm

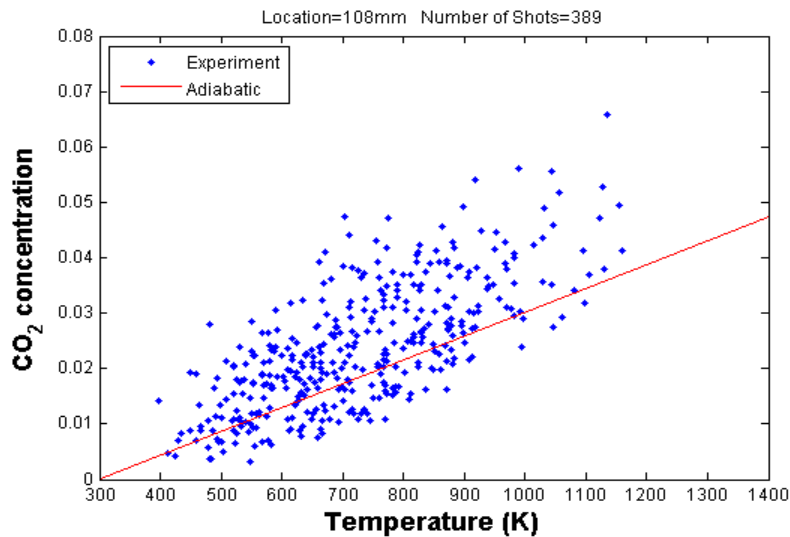
113 mm



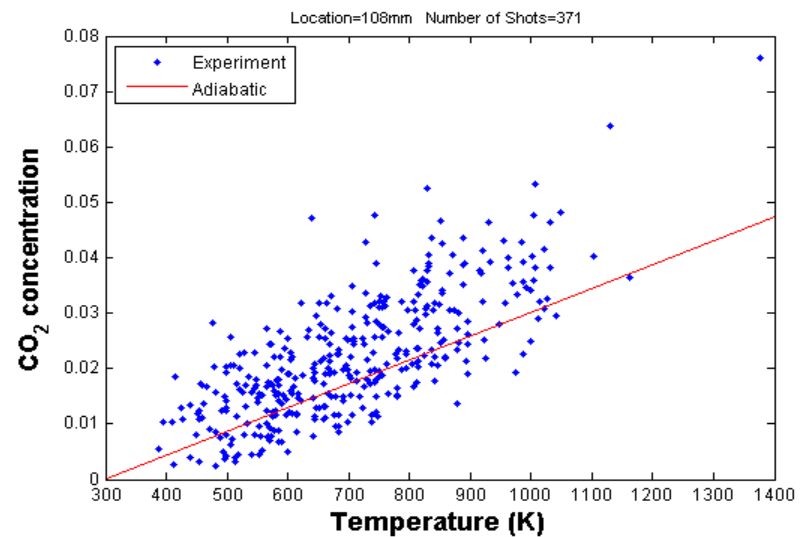
# CARS Measurements in Atmospheric Pressure PARAT Burner Flames: Temperature PDFs Along Centerline

Axial Location

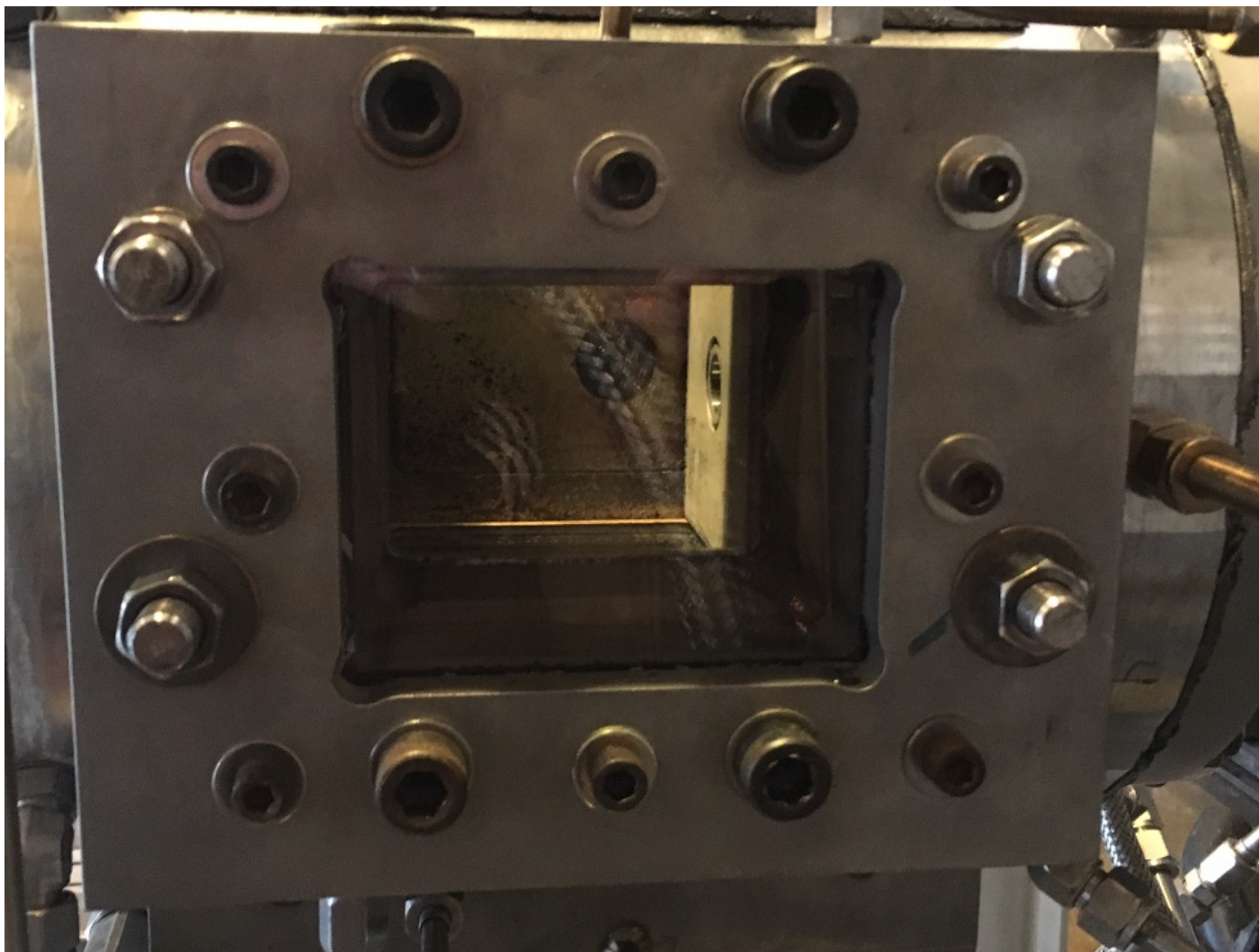
108 mm



113 mm



# CARS Measurements at High Pressure: PARAT Burner Now Installed in HP Test Rig



# High-Pressure PARAT Burner Studies

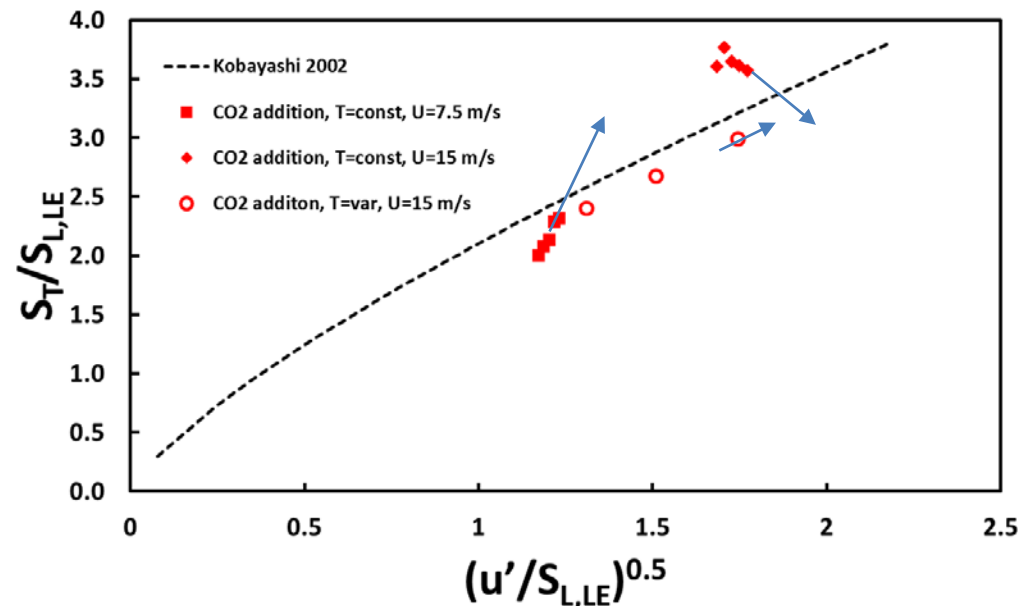
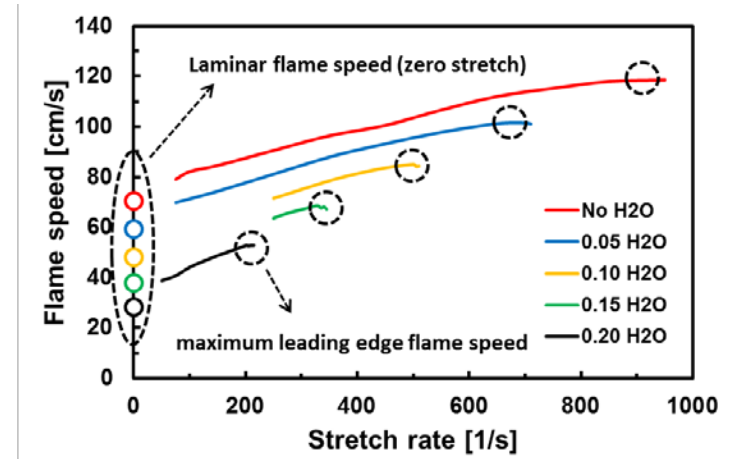
## Future Work

- **Initial tests for operability**
- **High-speed stereo PIV, OH PLIF for comparison with numerical modeling**
- **Nox, CO emission measurements for comparison with numerical modeling**



# Correlation of Turbulent Flame Speed using leading edge flame speed

- In the corrugated flame regime, where the Lewis number effect is important.  $\text{CO}_2$  dilution leads to an increase in  $S_T/S_{L,LE}$
- In the thin reaction zone, however,  $S_T/S_{L,LE}$  now decreases with  $\text{CO}_2$  dilution, indicating stronger turbulence-chemistry effect.
- However, the leading edge speed does not improve the correlation of turbulent flame speed with  $u'$ .



# Effects on flame speed with EGR dilution at constant temperature

- To remove thermal effects, we hold the adiabatic flame temperature  $T_{ad}$  constant
- The 10%  $\text{CO}_2$  cases ( $T_{ad} = 2025 \text{ K}$ ) is used as a baseline—all other cases with extra  $\text{N}_2$  dilution.
- Modified Damköhler scaling analysis contains elements of both transport ( $Le$ ) and kinetics ( $S_L$ ):

$$\frac{S_T}{S_L} \sim \left(\frac{u'}{S_L}\right)^{0.5} \left(\frac{1}{Le}\right)^{0.5}$$

- How will the chemistry effect change when we move from the corrugated flame to thin reaction zone regime?

