

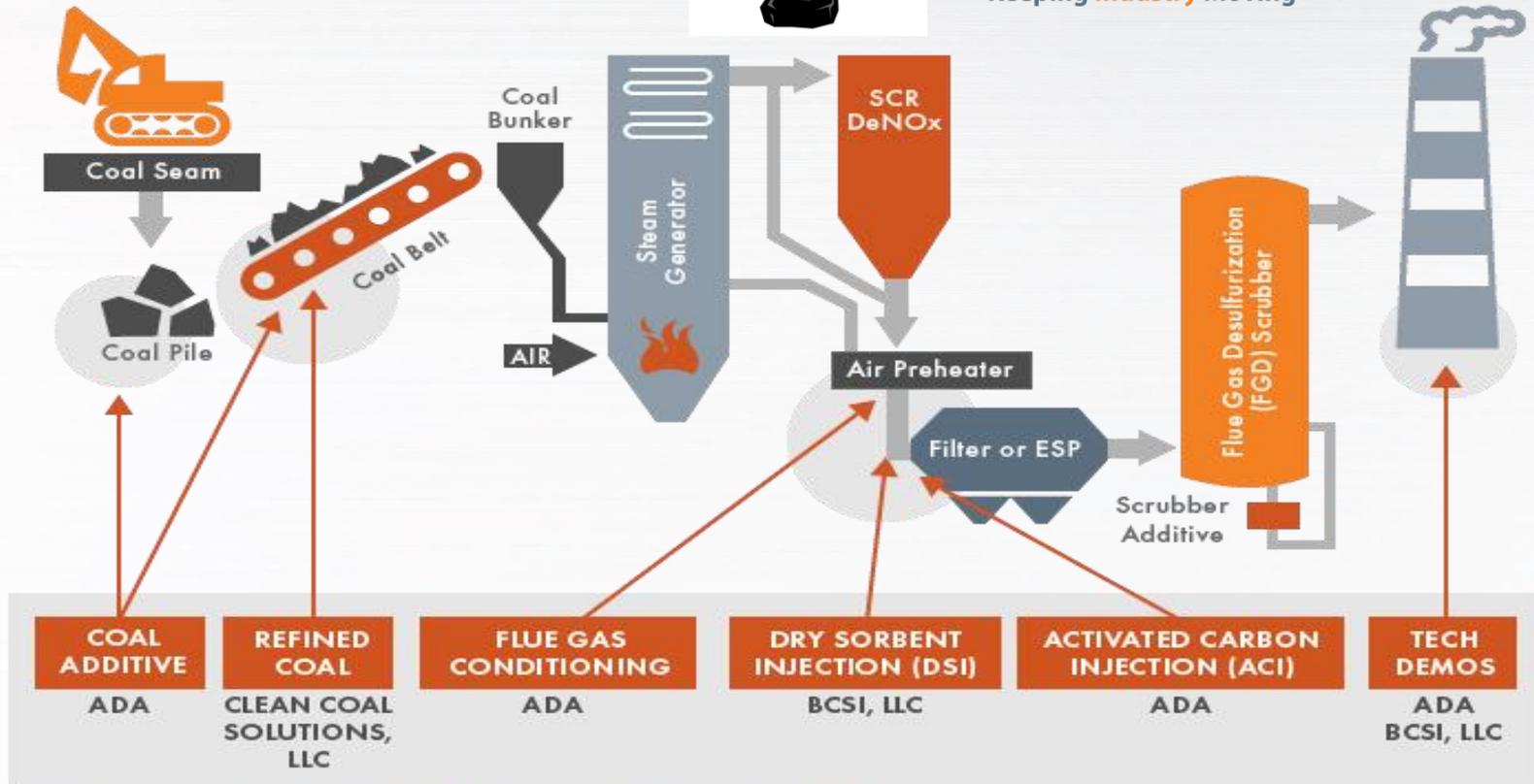


Evaluation of Solid Sorbents as a Retrofit Technology for CO₂ Capture

June 25, 2015
ADA-ES, Inc.

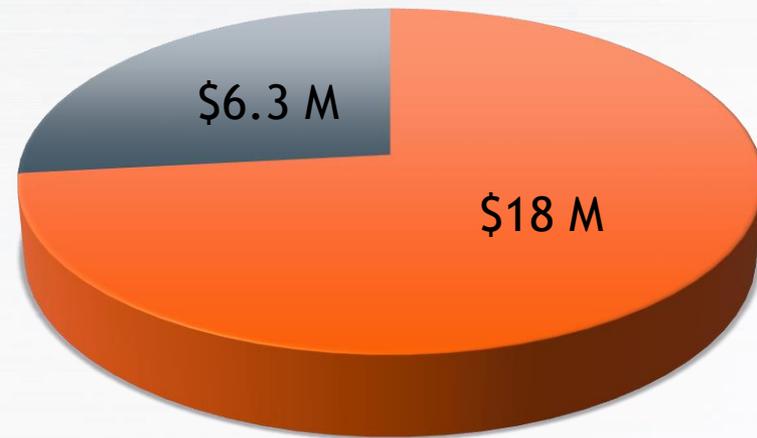
DE-FE0004343

Advanced Emissions Solutions, Inc.



Project Funding and Goals

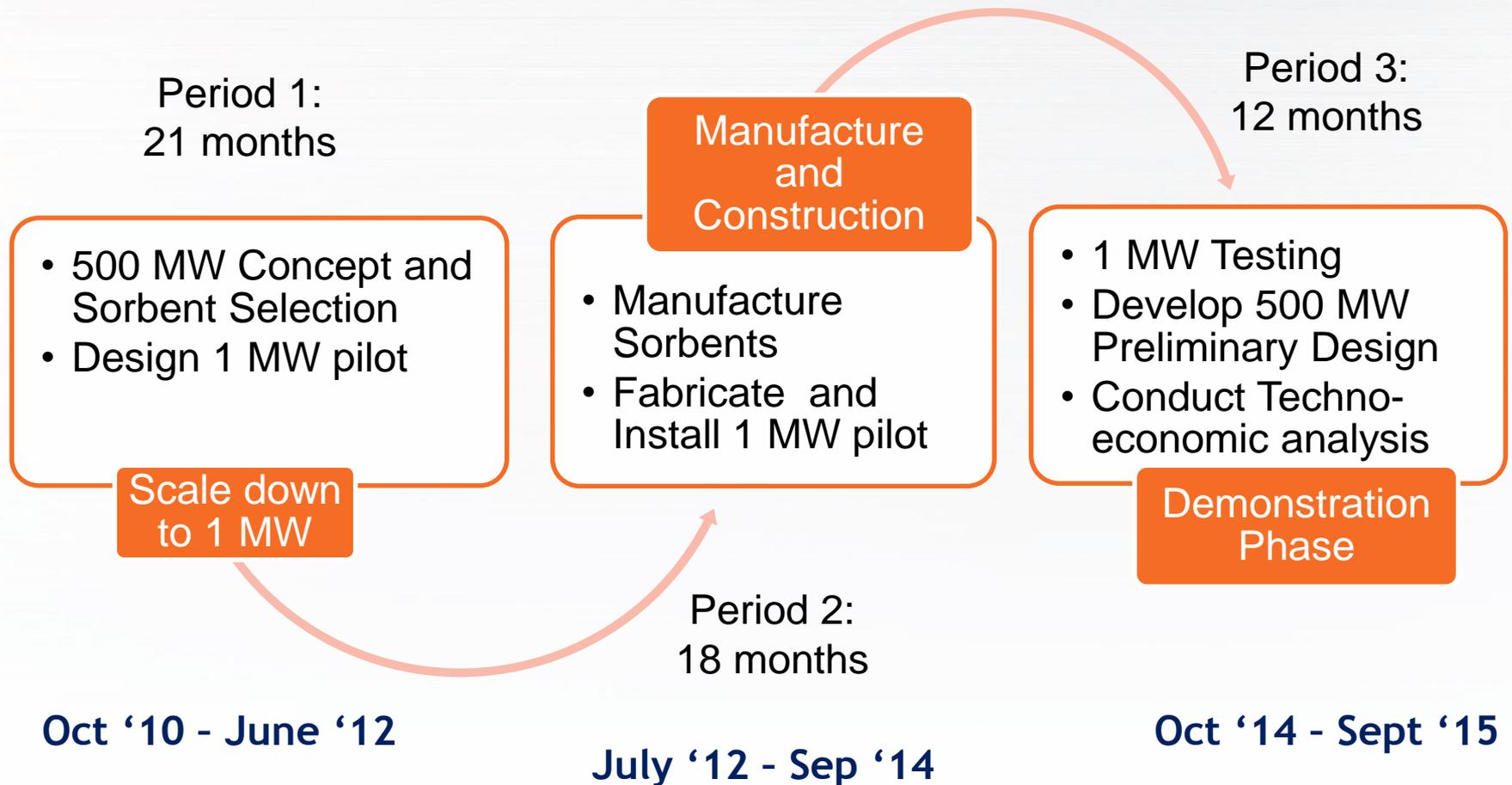
- ▶ The overall objective of this funding stage is to validate solid sorbent-based post combustion CO₂ capture through slipstream pilot testing.
- ▶ Project Goals:
 - Achieve 90% CO₂ Capture
 - Reduce costs of carbon capture
Progress towards <35% LCOE Goal
 - Generate a high purity CO₂ stream
 - Successfully scale sorbents



■ DOE Funds ■ Industry Cost Share

*Cooperative Agreement (Award No. DEFE0004343)
 American Recovery and Reinvestment Act of 2009
 Administered by DOE-NETL: Project Manager Bruce Lani*

Project Overview



Project Team



- DOE - NETL
 - Project Sponsor
- ADA-ES, Inc.
 - Project Management
 - Developed Process Concept
 - Sorbent Eval & Selection
 - Process Validation Testing
 - Techno-Economic Assessment
 - Primary Cost Share
- Technip Stone and Webster Process Technology
 - Detailed Engineering Services

Significant Experience with Fluidized Bed Reactor Design



- Stantec Consulting, Ltd.
 - Cost Analysis, Plant Integration

Owners Engineer Perspective



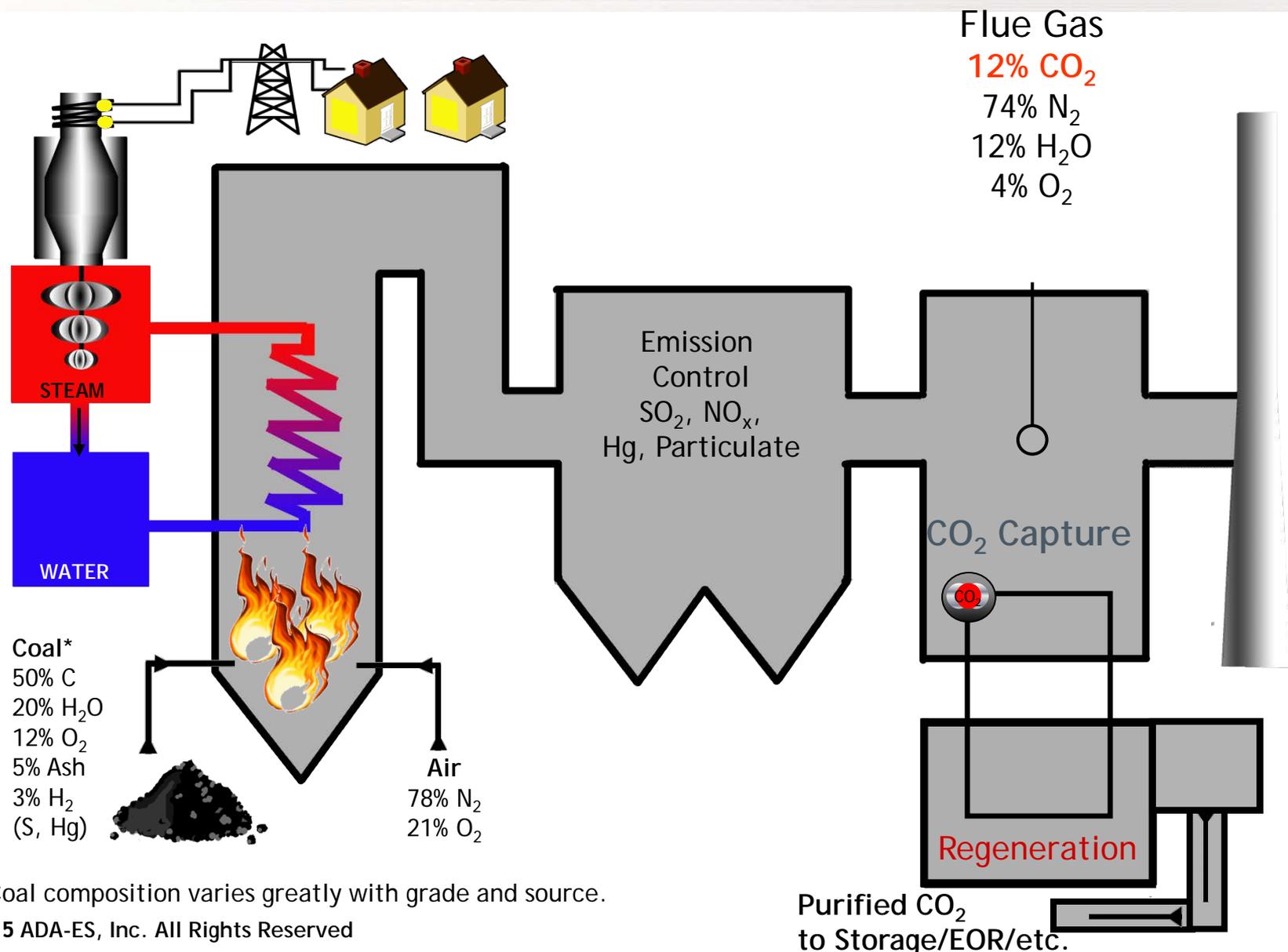
- McAbee Construction
 - Pilot fab and installation
- EPRI
 - Technical Advisor
 - Cost Share
 - Independent Performance Evaluation and Techno-Economic Assessment



- Southern Company
 - Host Site, Cost Share
- Luminant
 - Cost Share



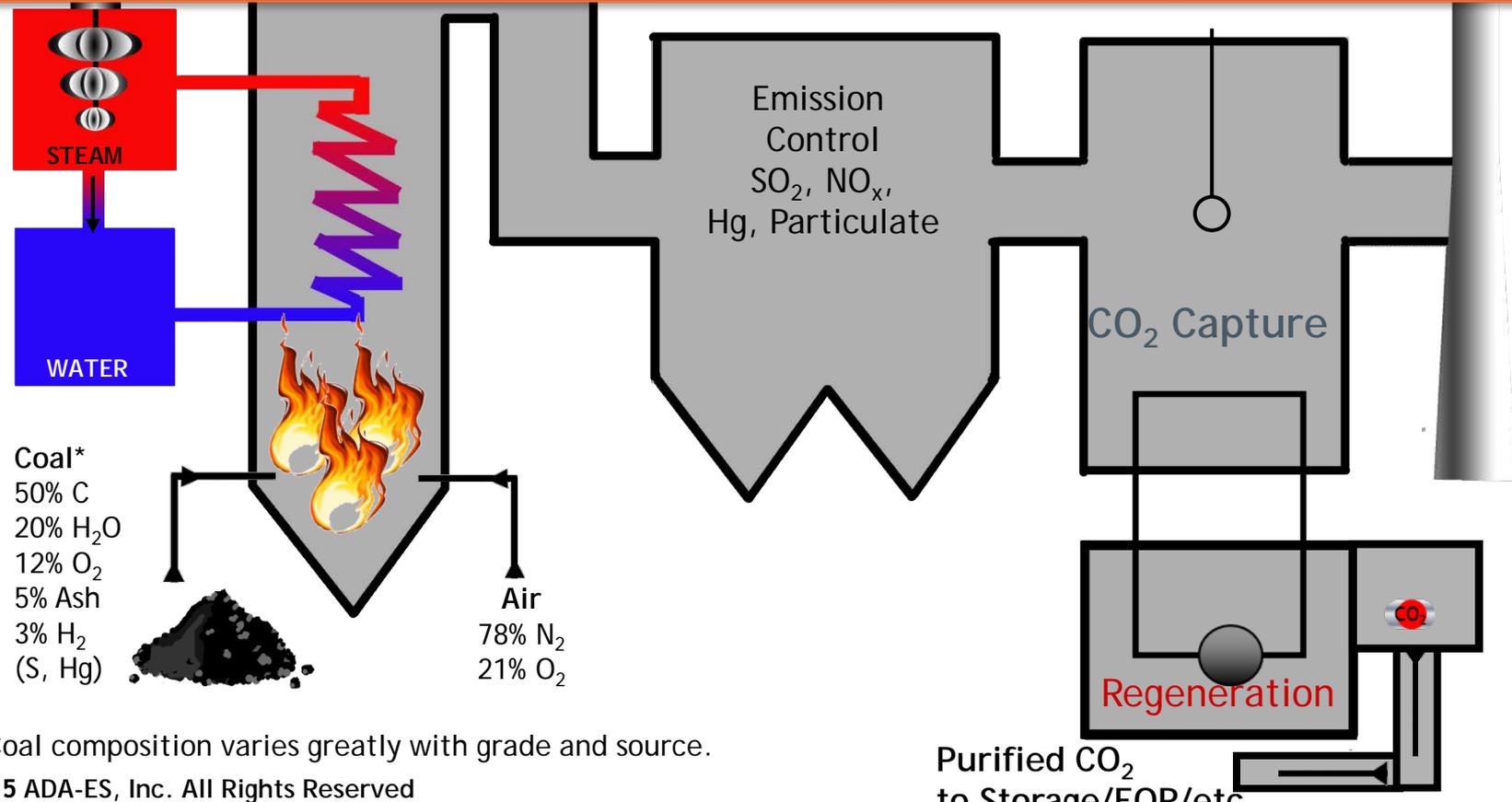
Post-Combustion CO₂ Capture



*Coal composition varies greatly with grade and source.

Post-Combustion CO₂ Capture

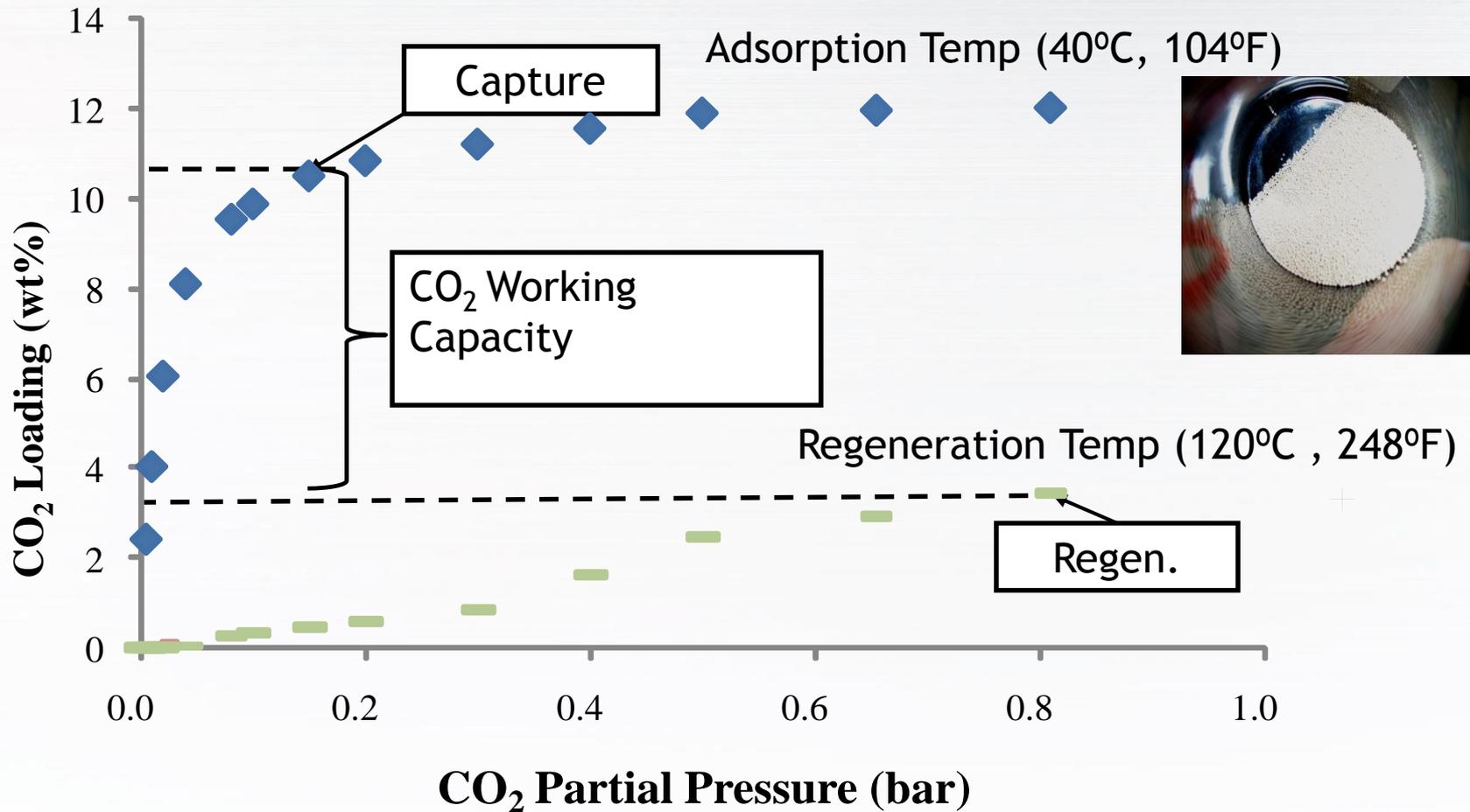
Solids functionalized with amines react with CO₂ at "low" temperatures
 Solids are heated to reverse reaction with CO₂
Temperature swing adsorption (TSA)



*Coal composition varies greatly with grade and source.

Purified CO₂
to Storage/EOR/etc.

Sorbent Isotherms

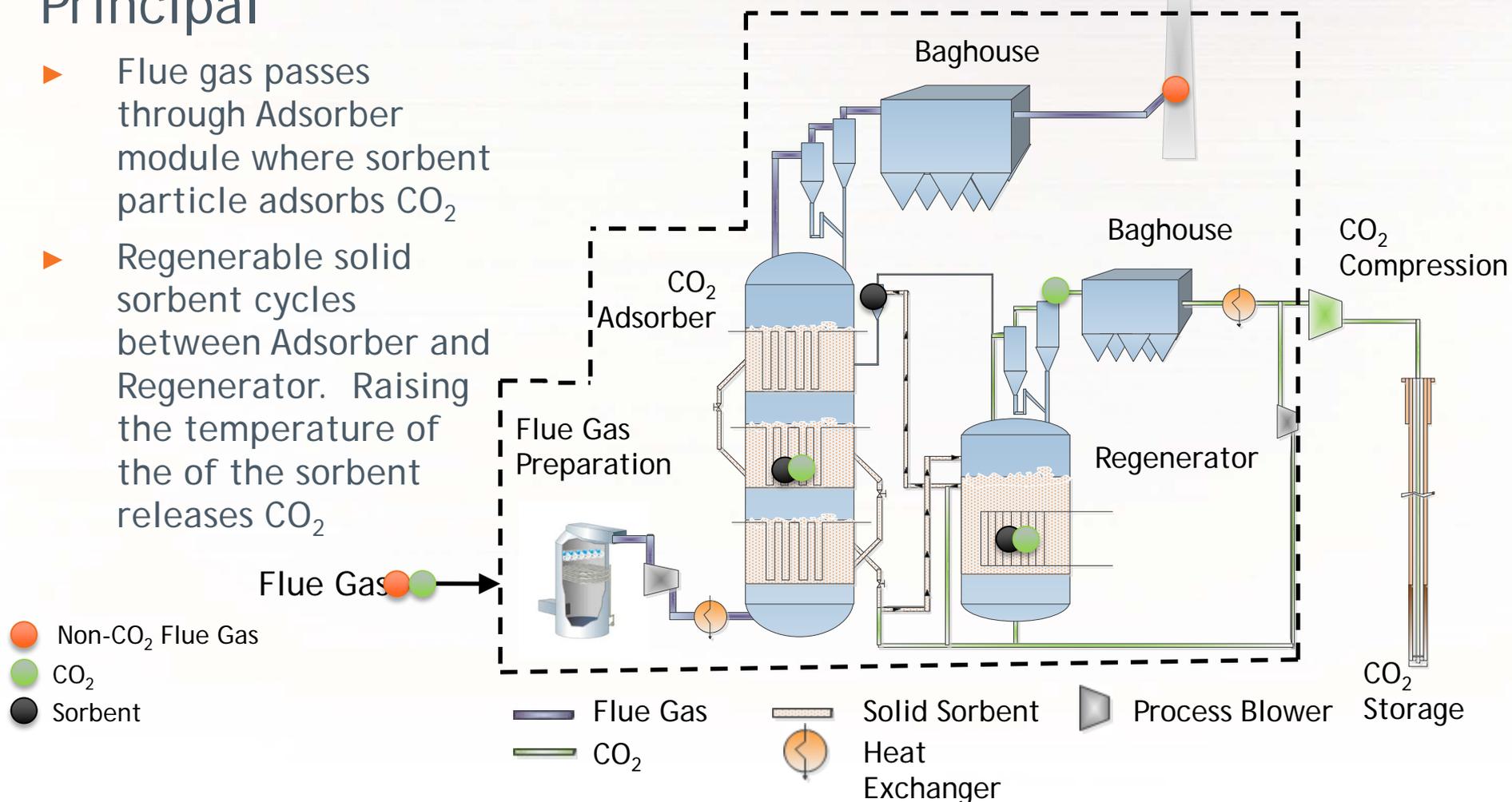


Process Conceptual Design

Principal

- ▶ Flue gas passes through Adsorber module where sorbent particle adsorbs CO₂
- ▶ Regenerable solid sorbent cycles between Adsorber and Regenerator. Raising the temperature of the sorbent releases CO₂

1 MW Process Validation Unit



ADAsorb™ CO₂ Capture Process

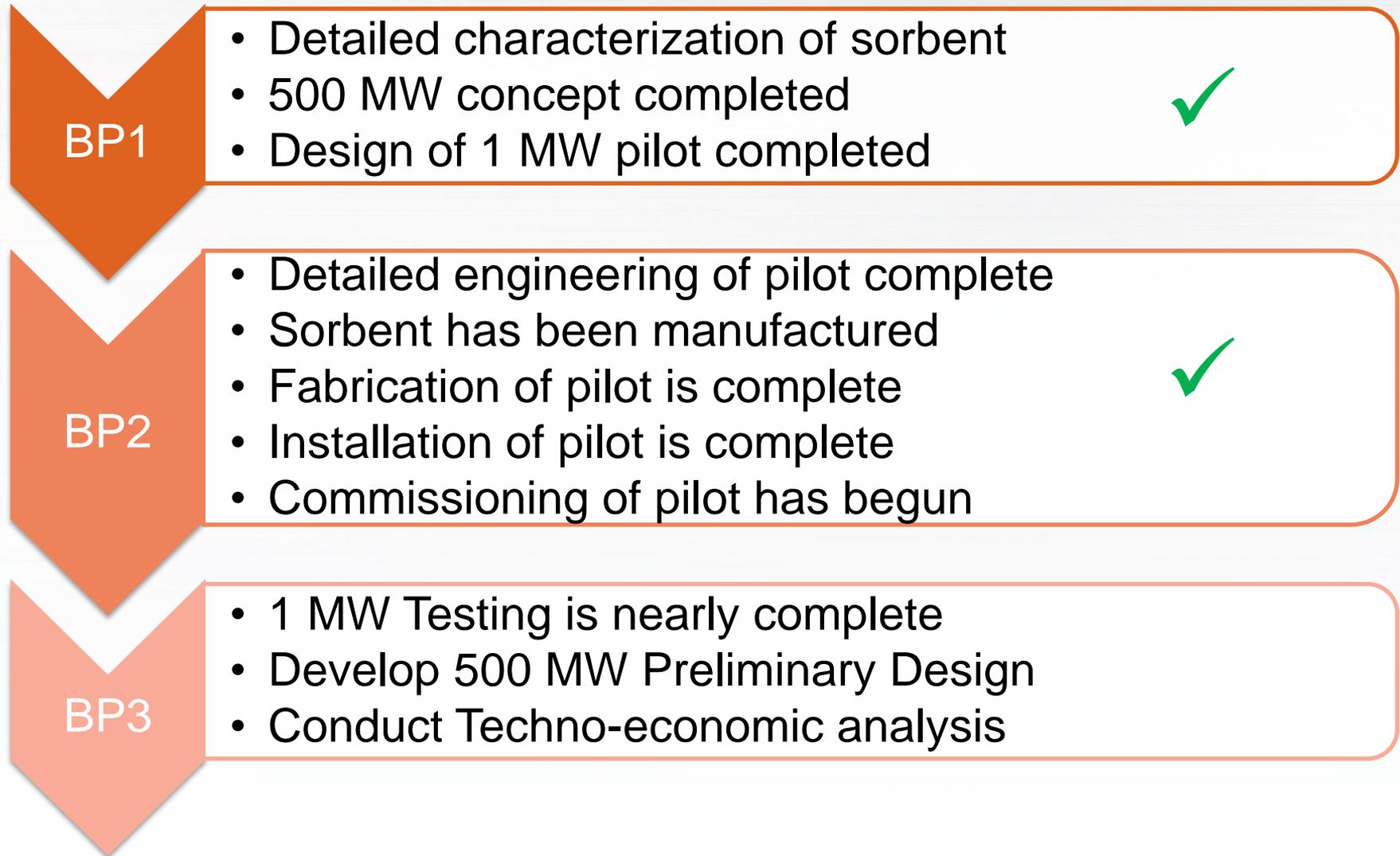
Advantages

- ▶ Heat transfer
Isothermal operation
- ▶ Mass transfer favorable
- ▶ Proven at the industrial scale
- ▶ Approaches counter-current gas/solids contacting
- ▶ Process Flexibility
Can be applied to cycling plant “load following”

Challenges

- ▶ Pressure drop
- ▶ Solids circulation
- ▶ Sorbent attrition
- ▶ Water adsorption
- ▶ Heat recovery

Project Status



BP 3: Pilot Testing

- ▶ Host Site:
 - Southern Company Plant
 - PRB Coal
 - WFGD
- ▶ Pilot Designed for
 - 90% CO₂ Capture
 - ~2,300 lb CO₂/hr
 - Flue Gas Flow Rate ~ 2,600 SCFM
 - Operation above freezing



Pilot Schedule

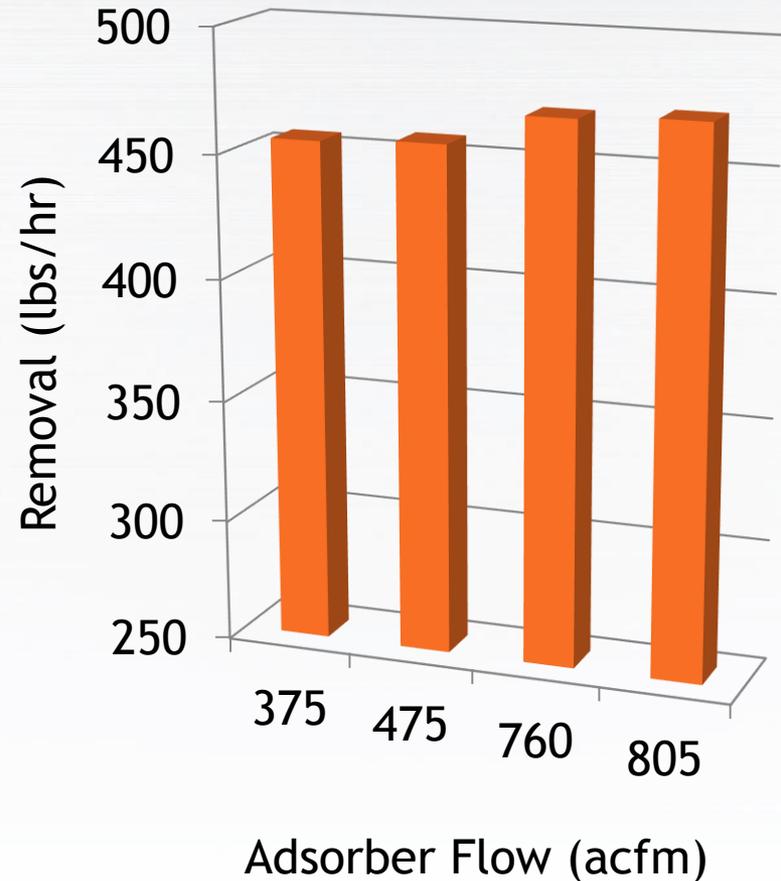
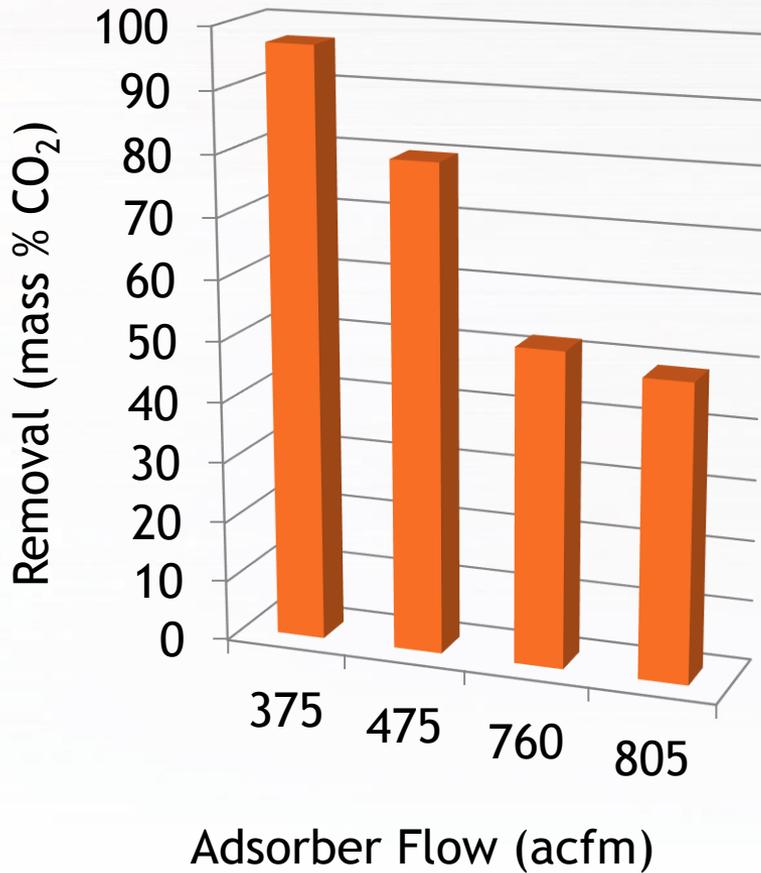
<u>Task</u>	<u>Date</u>
Commissioning/Dry Startup	Aug-Sept '14
Field Testing Round 1	Oct-Nov '14
Field Testing Round 2	April - June '15



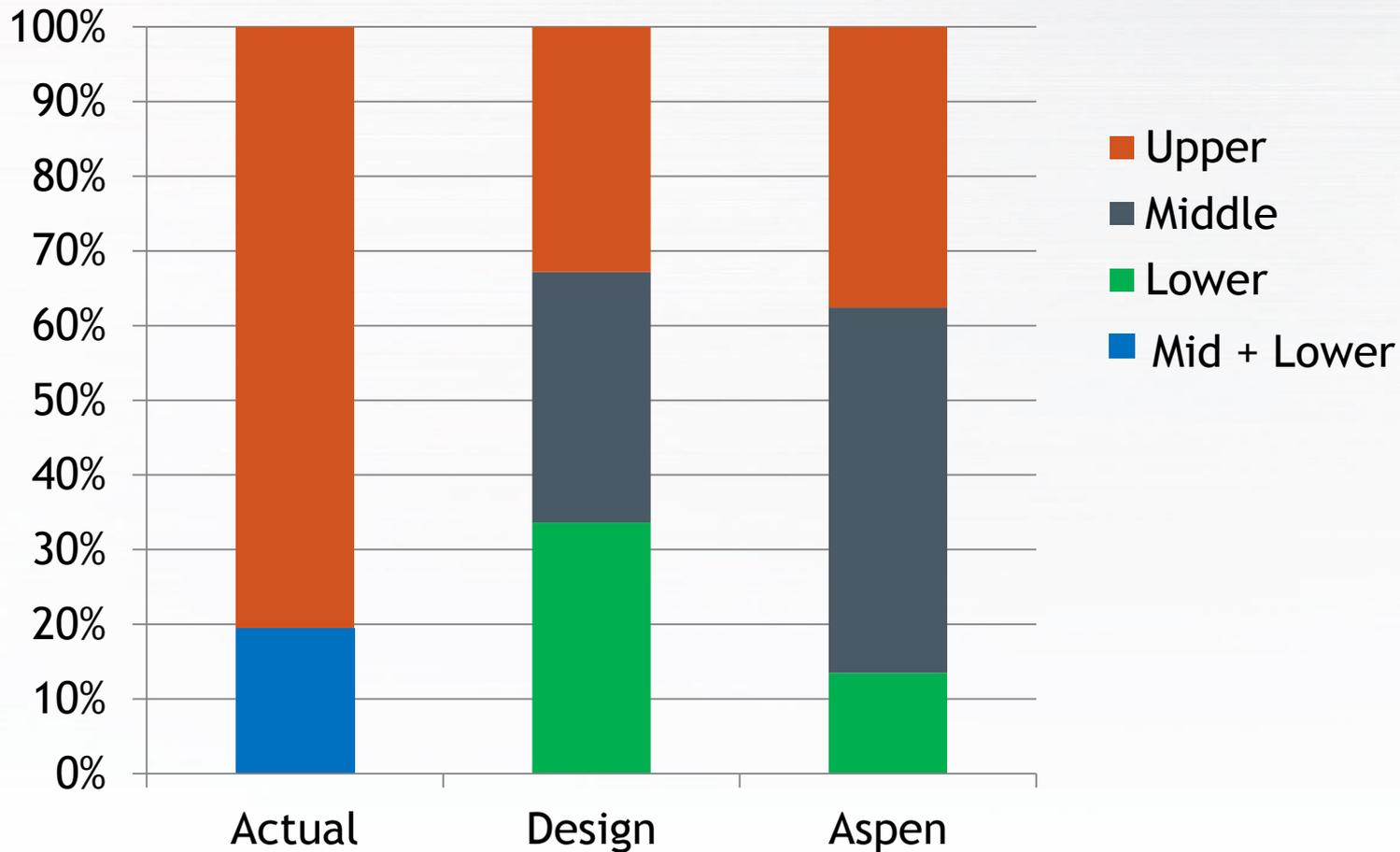
Key Observations from Pilot Testing

- ▶ **90% capture** can be achieved at very low flows but cannot be achieved at high flow rates
 - Capacity limitations
 - Sorbent handling characteristics at full regeneration temperature
- ▶ Data suggests relatively **fast adsorption kinetics**
- ▶ **Moisture uptake** on the sorbent appears to be higher than predicted from laboratory testing
- ▶ It is possible to circulate sorbent in a stable and consistent fashion, but system is sensitive to sorbent particle density, temperature, and CO₂ loading

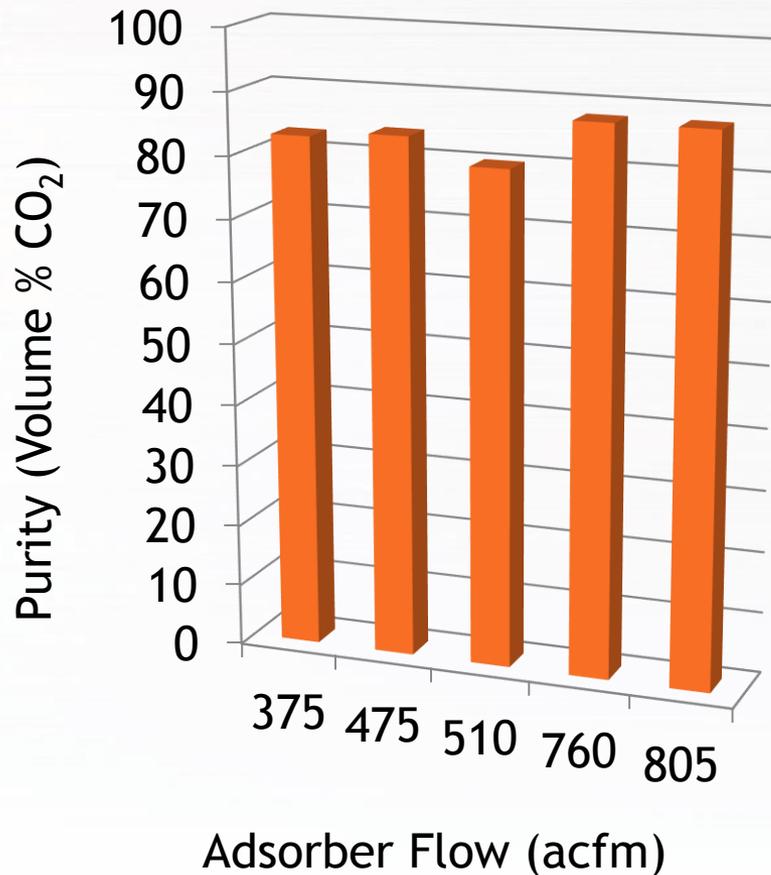
CO₂ Removal at Varying Adsorber Flow Rates



CO₂ Removal in Adsorber

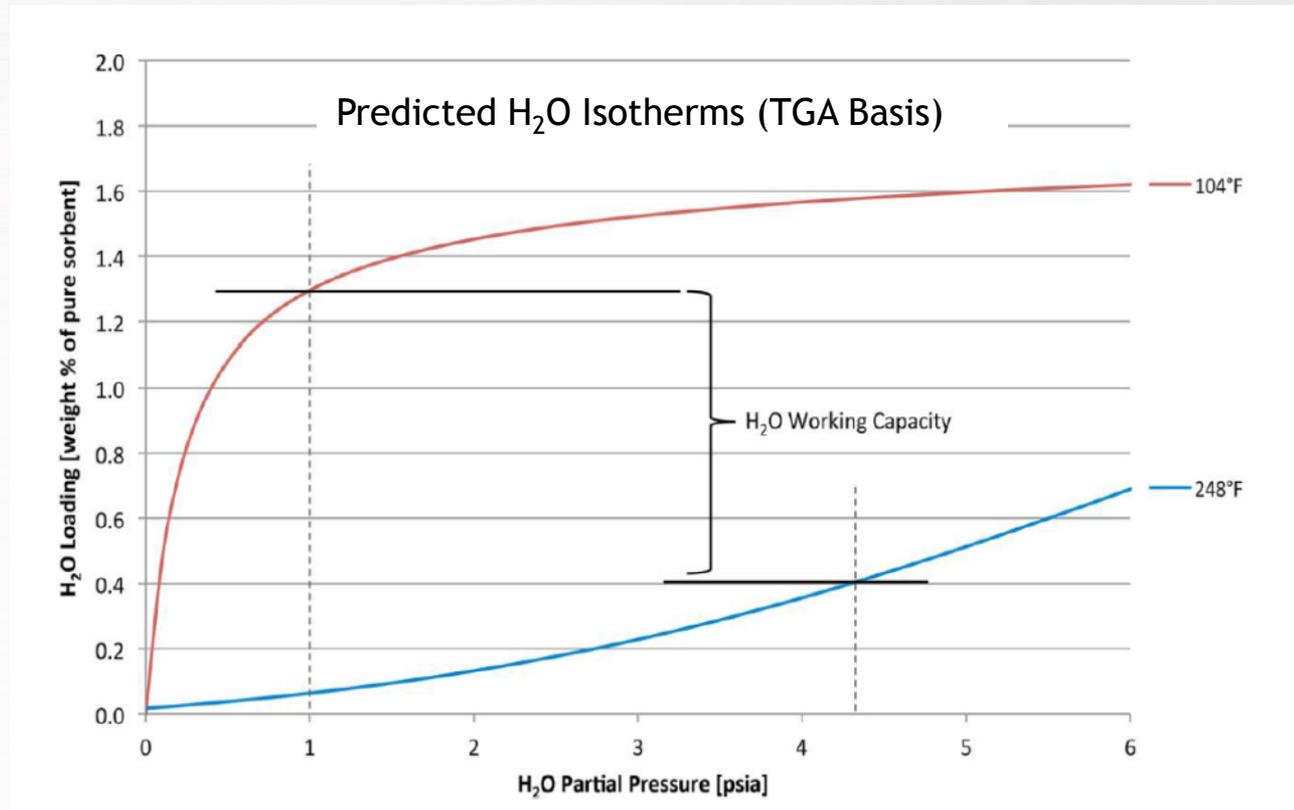


CO₂ Removal at Varying Adsorber Flow Rates



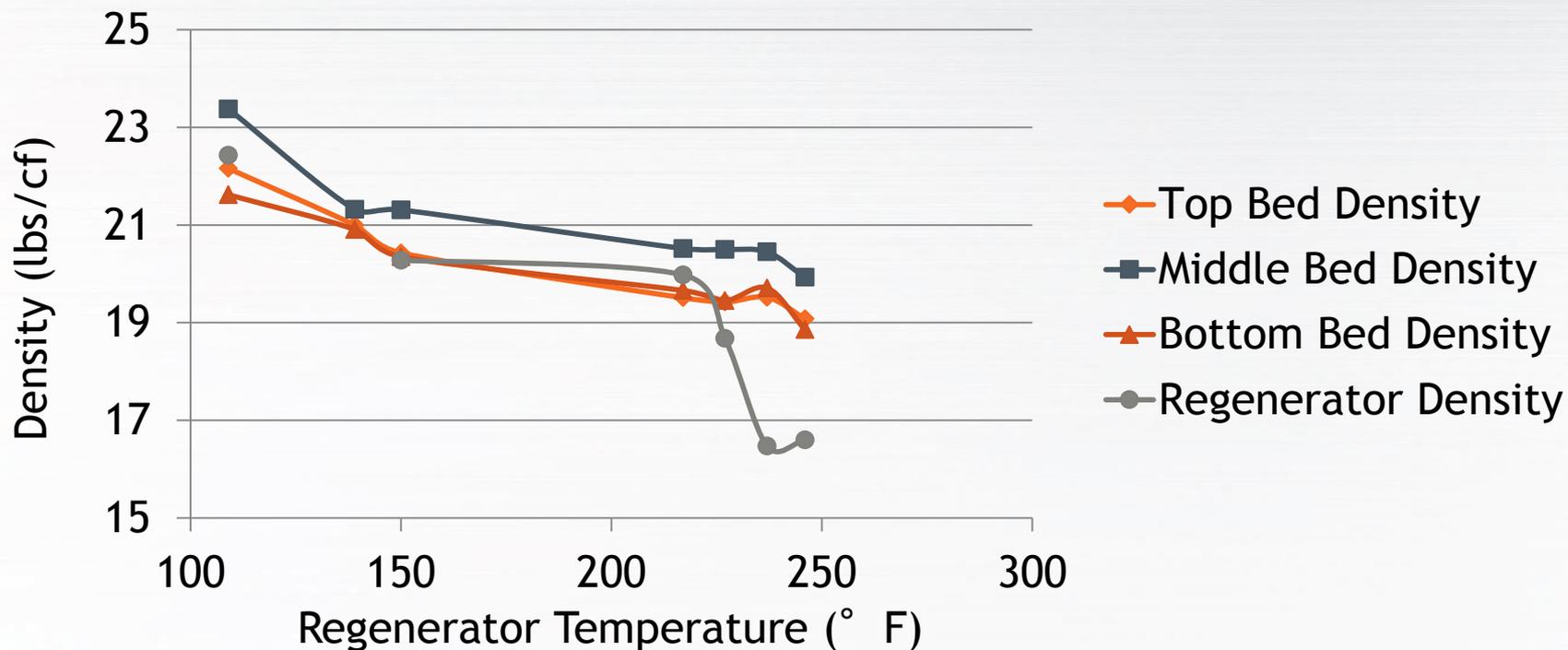
- ▶ Product stream purity 80% to 90% CO₂ during prolonged periods of stable pilot operation
- ▶ High moisture in CO₂ product

Moisture Uptake



- ▶ Pilot results indicate working capacity may be higher than predicted from TGA testing

Sorbent Density



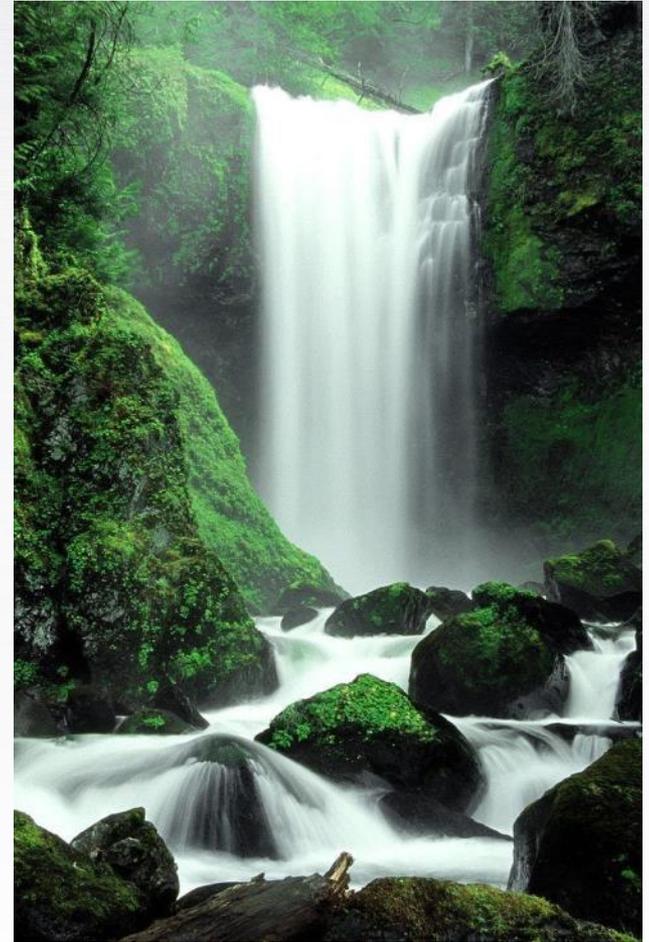
Location At 248F	Design (lbs/cf)	Measured (lbs/cf)
Regenerator	26.0	16.6
Adsorber	15.0	18.9 - 19.9

Environmental Testing

- ▶ **Liquid discharge samples**
all condensate locations
all discharge points
 - Total suspended solids
 - HEM / “Oil and Grease”

- ▶ **Sorbent samples**
collected bi-weekly from both the regenerator and the adsorber
 - RCRA 8 Metals

- ▶ All testing performed has produced results below the recordable limit for the tests



Additional Testing

- ▶ TGA results after approximately 3 weeks in the process indicated sorbent had not degraded in flue gas



Key Challenges from Testing

- ▶ Balance of plant issues
 - SO₂ scrubber operation and subsequent blower issues
 - Electrical grounding issues
 - Unseasonably cold weather and inadequate freeze protection
 - Supply water contamination
 - Analyzer Reliability
- ▶ Managing sorbent flow
 - Changes in sorbent behavior at high temperatures
 - Insufficient fluidization
 - Sorbent carryover
- ▶ Significant reliance on manual operation



Retrospective on Bench Testing and Modeling

Additional bench-scale testing could improve design and performance expectations in pilot

- ▶ Hot sorbent flow characteristics
- ▶ Sorbent moisture uptake

Modeling from CCSI efforts have been improving throughout testing program. Confidence in models may allow performance estimates with improved sorbent characteristics

Summary

- ▶ **90% CO₂ capture** can be achieved
- ▶ **Moisture adsorption by sorbent** will impact sorbent working capacity and overall performance
- ▶ Reducing the moisture adsorption of the sorbent and managing sorbent flow at higher temperatures could **significantly improve process results**

Next Steps

- ▶ Complete pilot testing and data analysis
- ▶ Techno-economic analysis
- ▶ Continue evaluating options for post-pilot scale-up
 - Will final regulations and oil prices support large-scale use of fossil-generated CO₂?
 - Today, regulatory drivers alone do not justify continued investment
- ▶ Work with DOE to make pilot facility available to other contractors



Questions?

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