Flameholding Tendencies of Natural gas and Hydrogen Fuel at Gas Turbine Premixer Conditions

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Motivation

Motivation

Premixer/Injector

efore Flashback and After Flashback

After Flashback

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Sources of Flashback

There two broad classes of flashback:

- **Steady state flashback- the flame propagates upstream from the combustion chamber during steady operation.**
- **Transient flashback - the flame is forced upstream into the premixing zone by a transient event.**

Research Questions

How to avoid flashback damage:

- •**Develop flashback resistant combustors**
- **Determine how to prevent flames from holding in the premixer if flashback does occur.**

How to avoid premixer flameholding:

•**Determine the limits of flameholding**

Timeline

Development

Background

Ballal and Lefebvre (1979) developed correlations for Φ $_{\rm{Blowoff}}$ in terms of standard variables (Temperature, Pressure, Velocity, Blockage ratio, and Diameter)

Ballal, D.R., Lefebvre, 1979, Weak Exitinction Limits of Turbulent Flowing Mixtures, ASME Journal of Engineering for Power, pp. 343-348

Background

Plee and Mellor (1979) used the data from Ballal and Lefebvre (1979) but suggest that controlling factors are chemical time scales and physical timescales

Background

Shanbhogue, et al. (2009) conducted a review study that collected data from many other studies on flameholding and attempted to describe all the data with a single equation.

Shanbhogue, S.J., Husain, S., Lieuwen, T., 2009, Lean Blowoff of Bluff Body Stabilized Flames: Scaling and Dynamics, Progress in Energy and Combustion Science, 98-120

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Motivation

Test Rig Assembly

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Test Section

Optical windows and test feature have same base so that the test feature can be moved upstream or downstream of ignition source

Round base of test feature insert allows test feature to be rotated

Test Section Sizing

Test section with cross section of 1.76" x 0.76" is representative of current engine premixing sections

Siemens Gas Injector/Premixer

Test Section Sizing

Test section with cross section of 1.76" x 0.76" is representative of current engine premixing sections

Testing

Testing

Reverse Step Flameholder

1/4" Height Reverse Step Flameholder 5 ATM 500F Inlet Temperature 40 m/s bulk Velocity Natural Gas Fuel, 0.9->0.85 Equivalence Ratio

How does this data compare to the Re-Da correlations developed by Shanbhogue (2009)?

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Potter, A., Wong, E., 1958 Effect of Pressure and Duct Geometry on Bluff-Body Flame Stabilization, NACA TN 4381, National Advisory Committee for Aeronautics

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22/30

Potter, A., Wong, E., 1958 Effect of Pressure and Duct Geometry on Bluff-Body Flame Stabilization, NACA TN 4381, National Advisory Committee for Aeronautics

- •• Why isn't the T_{Chem} decreasing as velocity increases?
	- **Turbulent flame speed increases linearly with turbulent fluctuation magnitude.**
	- **If turbulent magnitude remains approximately constant then turbulent flame speed also increases linearly with velocity**

Beerer, D., McDonell, V., Therkelsen, P., Cheng, R., 2013, Flashback and Turbulent Flame Speed Measurements in Hydrogen Flames Stabilized by a Low-Swirl Injector at Elevated Pressures and Temperatures, J. Eng. Gas Turbines Power, 031501 (1-9)

LDV measurements 5 4.5 $8\degree$ $8\degree$ $8\degree$ ρ **Results are both 20% higher than predicted for fully developed pipe flow:** $I = 0.16 \cdot Re_{Dh}^{-0.125}$ 르 O 295,000 O 146,000 *Total Experiment Range: 81 - 459x10³ 0.5 Ω 10 20 30 40 0 Position (mm) **10/22/2014**25/30

Flame speed alone does not address the influence of the bluff body or flame temperatures.

Higher blockage ratio increases edge velocity, reducing contact time between reactants and hot products.

Higher combustion temperatures increase heat transfer to reactants.

Empirical correlation term was developed:

$$
U \propto S_T \left(\frac{T_{Burned}}{T_{Unburned}} \right) (1 - B)
$$

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Example

A premixer has a blockage ratio of 0.7 and turbulence intensity of 5% Reactants: Hydrogen and Air at 600K and an equivalence ratio of 0.3

Determine the minimum average velocity that will avoid flame holding.

Based on the reactant mixture: ${\sf T_{Burned}}$ = 1467 K, S_L = 0.9 m/s

$$
\frac{T_{Burned}}{T_{Unburned}} = \frac{1467 K}{600 K} = 2.445
$$

$$
S_T = S_L + 3.73 U' = 0.09 \frac{m}{s} + 3.73(0.05)(U)
$$

$$
(0.09 \frac{m}{s} + 0.1865 U)(2.445)(1 - 0.7) = 0.15 U
$$

$$
.1320 \frac{m}{s} = 0.0132 U
$$

$$
10 \frac{m}{s} = U
$$

Summary

- • **Experiments have been carried out on four flameholder geometries with both natural gas and hydrogen**
- **Temperature and fuel type were found to affect flameholding propensity more than any other parameter.**
- **Adiabatic flame temperature can be used as the characteristic temperature**
- \bullet **Chemical timescale does a reasonable job of predicting the point of blow off but does not take into account bluff body effects**
- **The product of turbulent flame speed, dilation ratio and (1-B) correlates well bulk velocity at blow off and captures the stochastic nature of blow off**

Analysis

- \bullet **Scaling parameters investigated:**
	- **Velocity**
	- **Equivalence Ratio**
	- **Adiabatic flame temperature**
	- **Mach Number**
	- **Lewis Number**
	- **Peclet Number**
	- **Reynolds Number**
	- **Damkӧhler Number**
	- **Turbulent flame speed (local displacement)**
	- **Chemical time**
		- **PSR time**
		- **Ignition Delay time at AFT**
		- **Flame thickness/laminar flame speed**

