

Sixth Annual Conference on Carbon Capture & Sequestration

Capture – Advanced Concepts

CO₂ CAPTURE USING DENSE HYDROGEN TRANSPORT MEMBRANES

Doug Jack, David Anderson, Carl Evenson, Michael Mundschau &
Richard Mackay – Eltron Research & Development, Inc

May 7-10, 2007 • Sheraton Station Square • Pittsburgh, Pennsylvania

CO₂ Emissions On The Rise

- EIA Projects over the period 2003 – 2030
 - World annual electricity demand will more than double
 - Leading to a doubling of coal consumption
 - Oil will also rise nearly 50%
- More production from Canadian tar sands

CO₂ emissions are expected to rise from ~25 billion metric tons to over 43 billion annually

Ref: Energy Information Administration, Office of Integrated Analysis and Forecasting, U.S. Department of Energy, “International Energy Outlook, June 2006

Carbon Capture Methods

- Post-Combustion
 - Remove CO₂ from combustion exhaust gases
- Oxy-Fuels
 - Fire combustion with O₂ instead of air
 - Remove CO₂ from combustion exhaust gases
- Pre-Combustion
 - Convert fuel to CO₂ and H₂, remove CO₂ before burning

Pre-Combustion Separation Methods

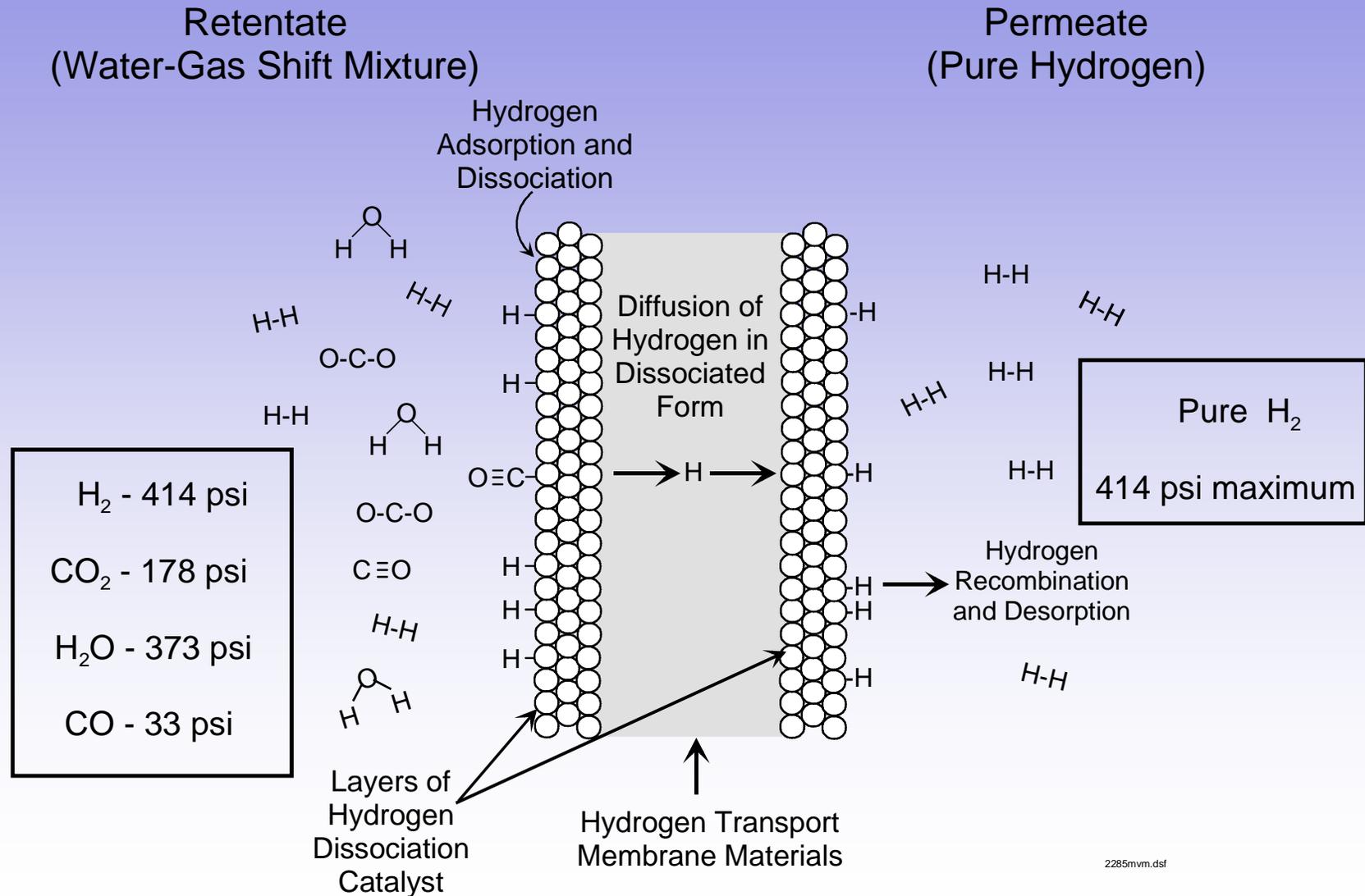
- Amine/Solvent Absorption
- Micro-Scale Filtration
- Pressure Swing Adsorption
- Dense Membranes
 - Ceramic
 - Metallic
 - Composite (e.g., Cermets)

Eltron HTM Project Goals

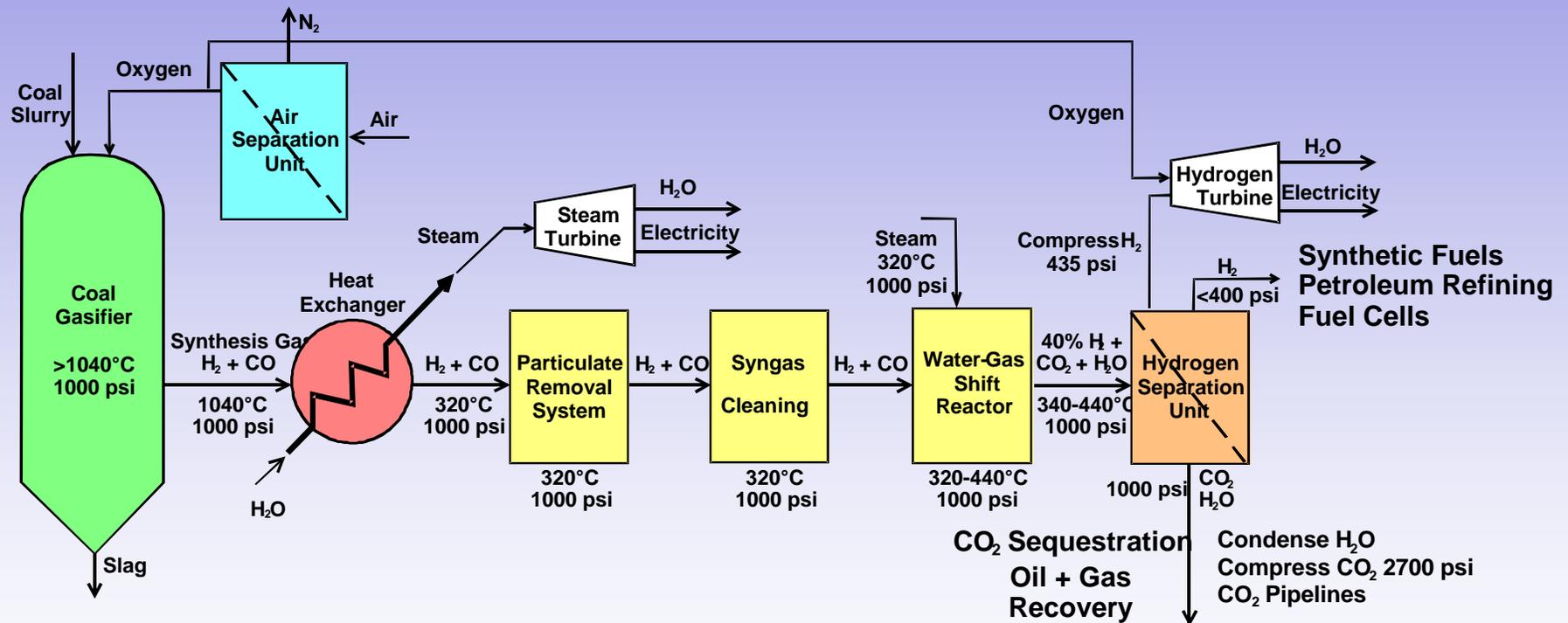
- Develop H₂/CO₂ Separation System, which
 - Retains CO₂ at coal gasifier pressures (450-1000 psig)
 - Operates near water-gas shift conditions (T, P, gas composition)
 - Tolerates reasonably achievable levels of coal-derived impurities
 - Delivers pure H₂ for use in fuel cells, gas turbines, and hydrocarbon processing
 - Is cost effective compared to alternative technologies for carbon capture

Eltron Project being funded through DOE

Membrane Fundamentals



Role of Hydrogen Separation Membranes in CO₂ Sequestration



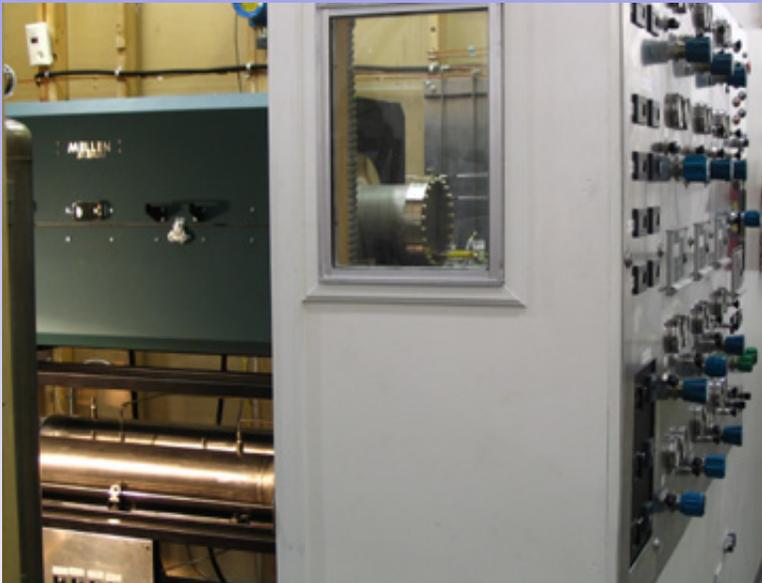
Technology Development Highlights

- Demonstrated a membrane system based on metallic alloys that meets or exceeds the 2010 DOE performance targets
- Developed cermet materials with comparable performance to Pd membranes
- Results from process economic studies show that this system is competitive with conventional technology
 - Reduced cost of electricity
 - Improvement in thermal efficiency
- Operating 1.5 lbs/day pilot plant

Progress Towards DOE FutureGen Targets

<i>Performance Criteria</i>	<i>2005 Target</i>	<i>2010 Target</i>	<i>2015 Target</i>	<i>Current Eltron Membrane</i>
Flux (sccm/cm ² /100 psi Δ P)	50	100	150	160
Operating Temperature ($^{\circ}$ C)	400-700	300-600	250-500	300-400
S Tolerance (ppmv)	N/A	2	20	20 (early)
System Cost (\$/ft ²)	1000	500	<250	<200
Δ P Operating Capability (psi)	100	400	800-1000	1,000
Carbon monoxide tolerance	Yes	Yes	Yes	Yes
Hydrogen Purity (%)	95	99.5	99.99	>99.99
Stability/Durability (years)	1	3	>5	0.9
Permeate Pressure (psi)	N/A	N/A	N/A	270

High Pressure Reactor – Eltron Research



- Pressures up to 1000 psig
- Tests in Water-Gas Shift Mixtures

- Eltron has only facility in U.S. capable of testing hydrogen transport membranes under extreme pressure conditions.



Small Pilot Scale Testing Module

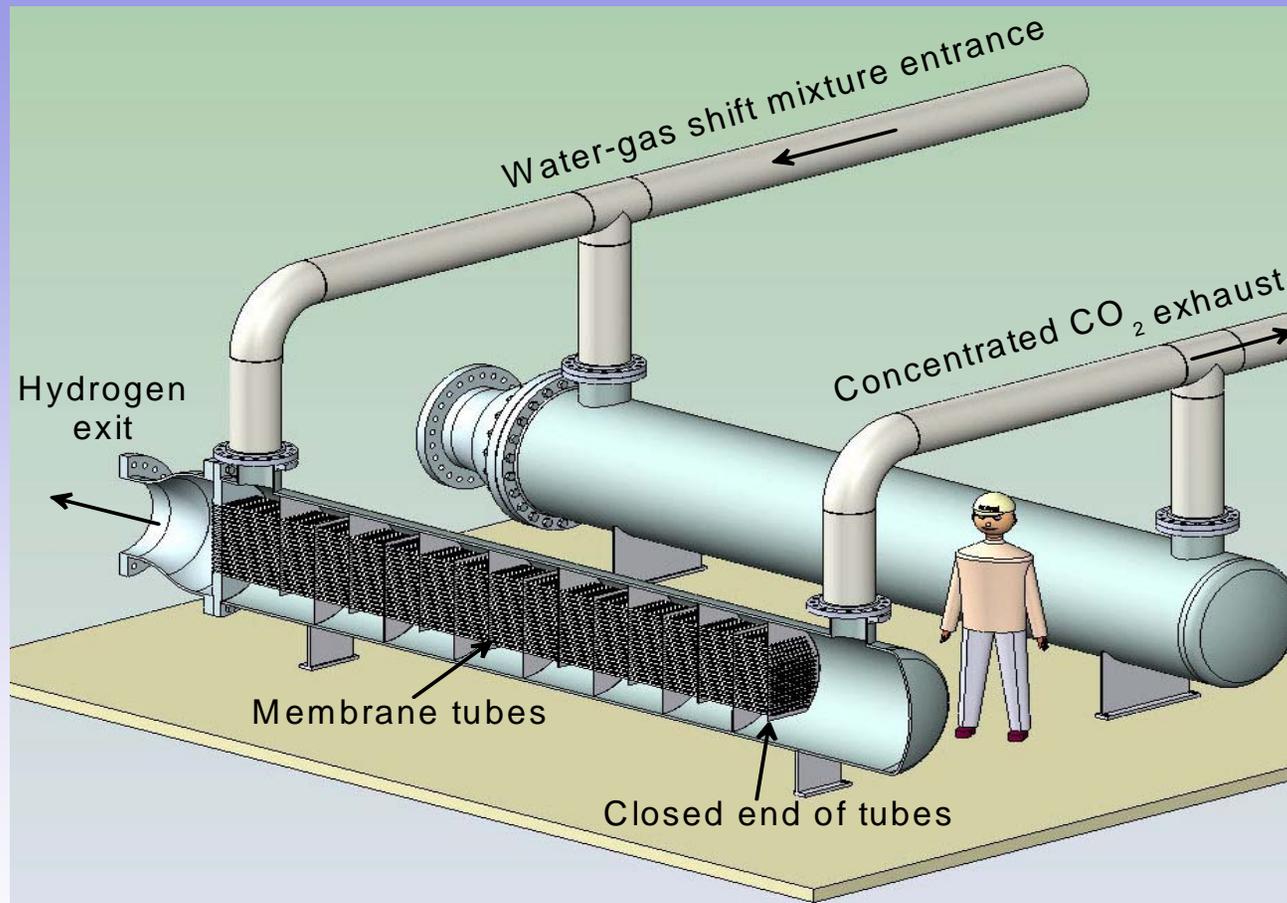


**1.3 lbs H₂ / day Separation
Unit Designed by NORAM**

Current Focus

- Understanding factors affecting longevity of membrane systems
 - Embrittlement
 - Life
- Scaling up manufacturing techniques
 - Tubular versus planar
 - Other mechanical issues (welding, sealing, etc)
 - Catalyst deposition
- Tolerance to impurities
- Process optimization

Scale-Up Designs – Tubular (NORAM)



- ◆ **NORAM conceptual tubular design of a commercial membrane unit capable of separating 25 tons per day (~10 MMSCFD) of hydrogen. Sizing is based upon syngas at 1000 psig (68 barg), 450°C, 50 vol.% H₂ in feed.**

Simplified Project Schedule

Scale Up Hydrogen Transport Membranes for IGCC and FutureGen Coal to Hydrogen Production Plants

	FY2006				FY2007				FY2008				FY2009				FY2010				FY2011			
	Qtr 1	Qtr 2	Qtr 3	Qtr 4	Qtr 1	Qtr 2	Qtr 3	Qtr 4	Qtr 1	Qtr 2	Qtr 3	Qtr 4	Qtr 1	Qtr 2	Qtr 3	Qtr 4	Qtr 1	Qtr 2	Qtr 3	Qtr 4	Qtr 1	Qtr 2	Qtr 3	Qtr 4
Design / Build 1.3 lb/day H2 Sep Unit	█	█	█	█	Completed																			
Improve Membrane Components	█	█	█	█	█	█	█	█	█	█	█	█												
Develop Methods of Low-Cost Membrane Manufacturing			█	█	█	█	█	█	█	█	█	█	█	█	█	█								
Process Economic Analysis	█	█	█	█	█	█	█	█	█	█	█	█	█	█	█	█	█	█	█	█				
Design / Build / Operate Impurity Management System					█	█	█	█	█	█	█	█												
Design / Build / Operate Life Studies Unit					█	█	█	█	█	█	█	█												
Design/Build/Operate 220 lb/day Pilot Plant									█	█	█	█	█	█	█	█	█	█						
Design/Build/Operate 4 TPD Unit															█	█	█	█	█	█	█	█	█	█