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# Long-Term Demonstration of Sorbent Enhancement Additive Technology for Mercury Control

## Contractors Review Meeting

Pittsburgh PA

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# Presentation Outline

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- Introduction
- Previous work at Hawthorn
- Current Results at Hawthorn
- Introduce Phase III Project
- Schedule
- Acknowledgements

# Sorbent Enhancement Additive (SEA) Technology

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- SEA1 (B&W/Niro, U.S. patent 5,435,980)
  - Chloride added to coal feed.
  - Hg capture can be enhanced with carbon.
- SEA2 T2
  - Alternative method of adding SEA2.
  - Reduce effects of alkaline material.
- Questions about the technology can be addressed by B&W.

# Hawthorn Unit 5

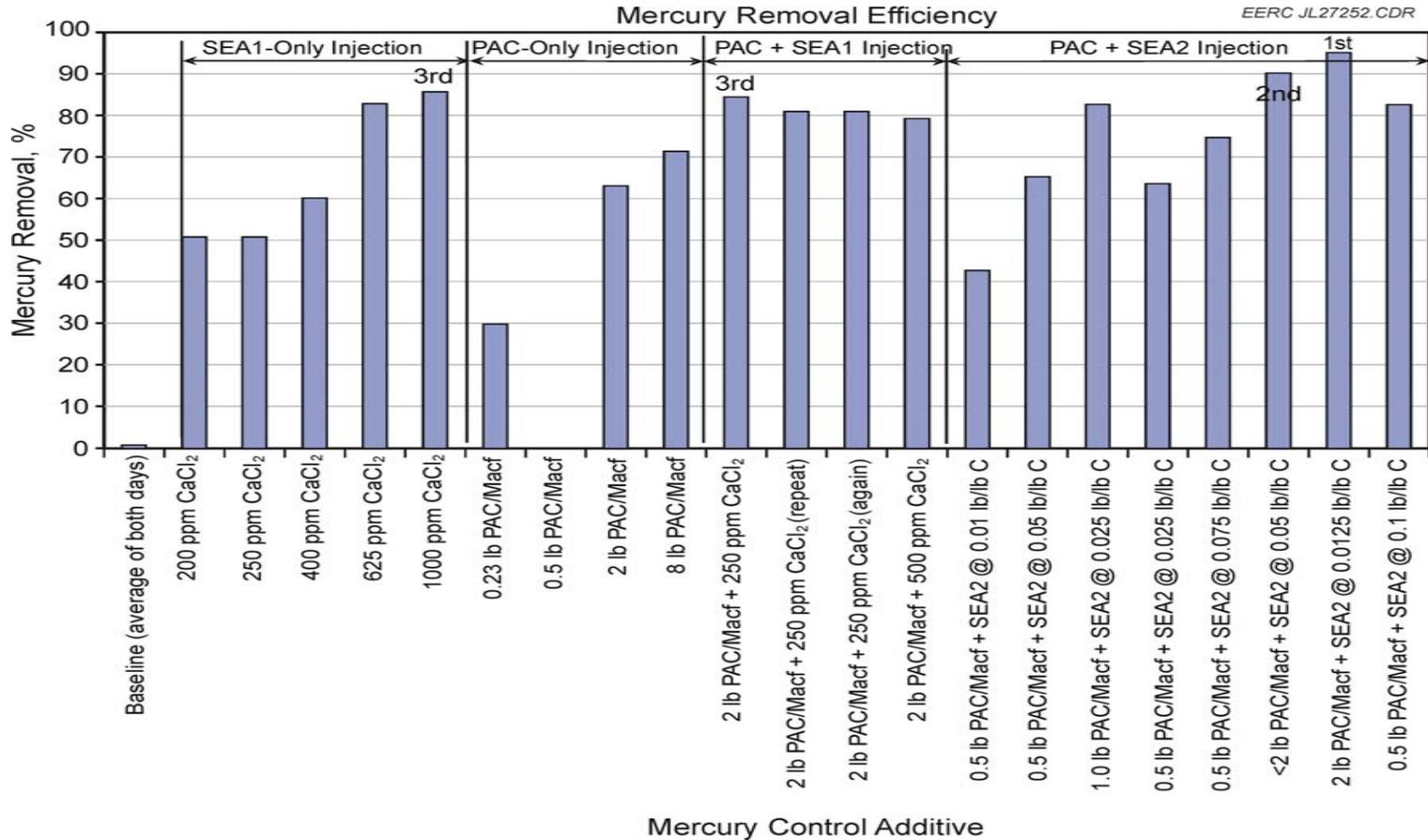
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Plant	Utility Owner	Coal	Boiler Type	Boiler Size, MW	Particulate Control	SO <sub>2</sub> Control	NO <sub>x</sub> Control
HAW5	KCP&L	PRB	Wall-fired	550	FF	SDA	LNB <sup>1</sup> , OFA <sup>2</sup> , SCR

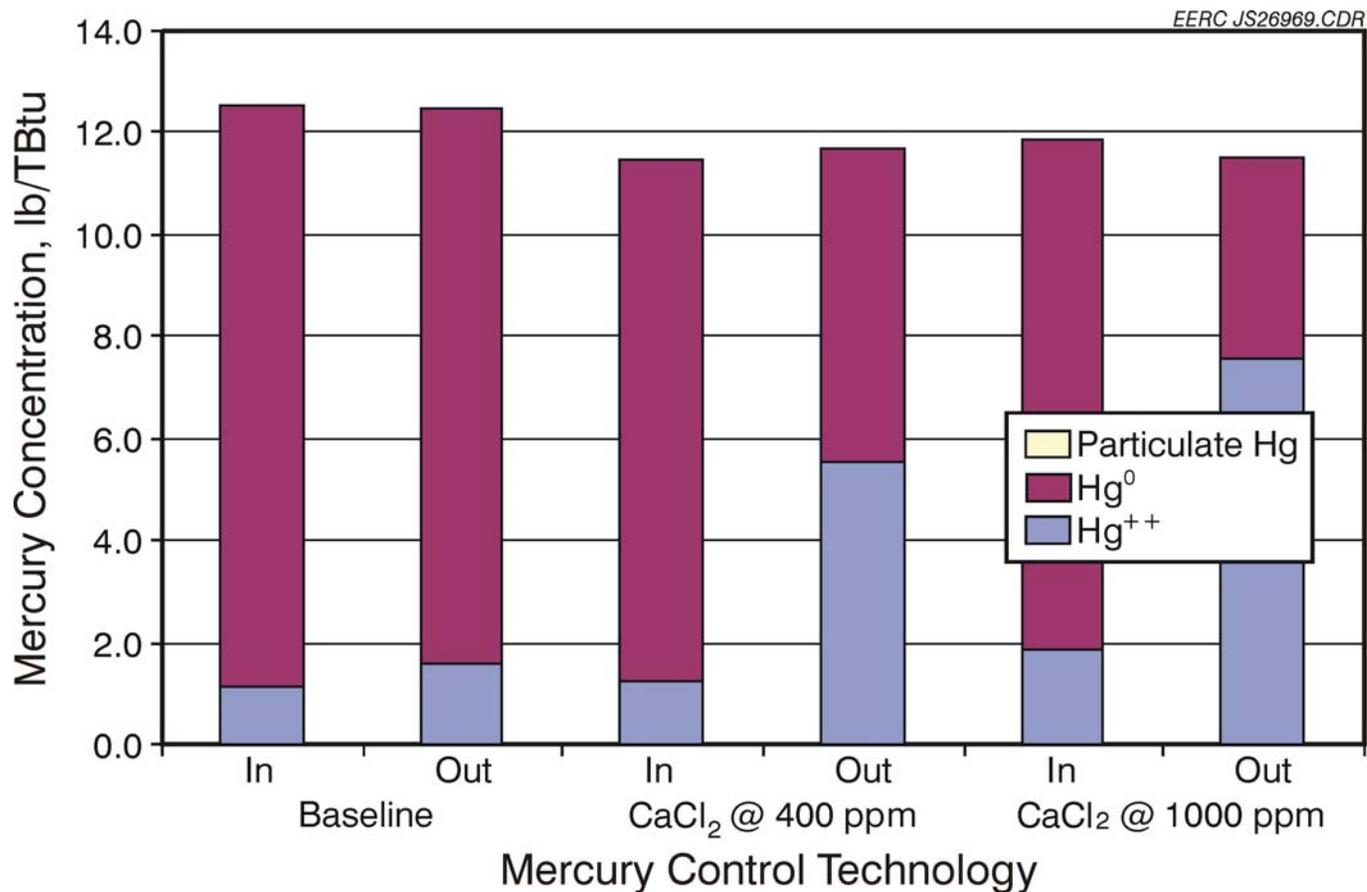
<sup>1</sup> Low-NO<sub>x</sub> burners.

<sup>2</sup> Overfire air.

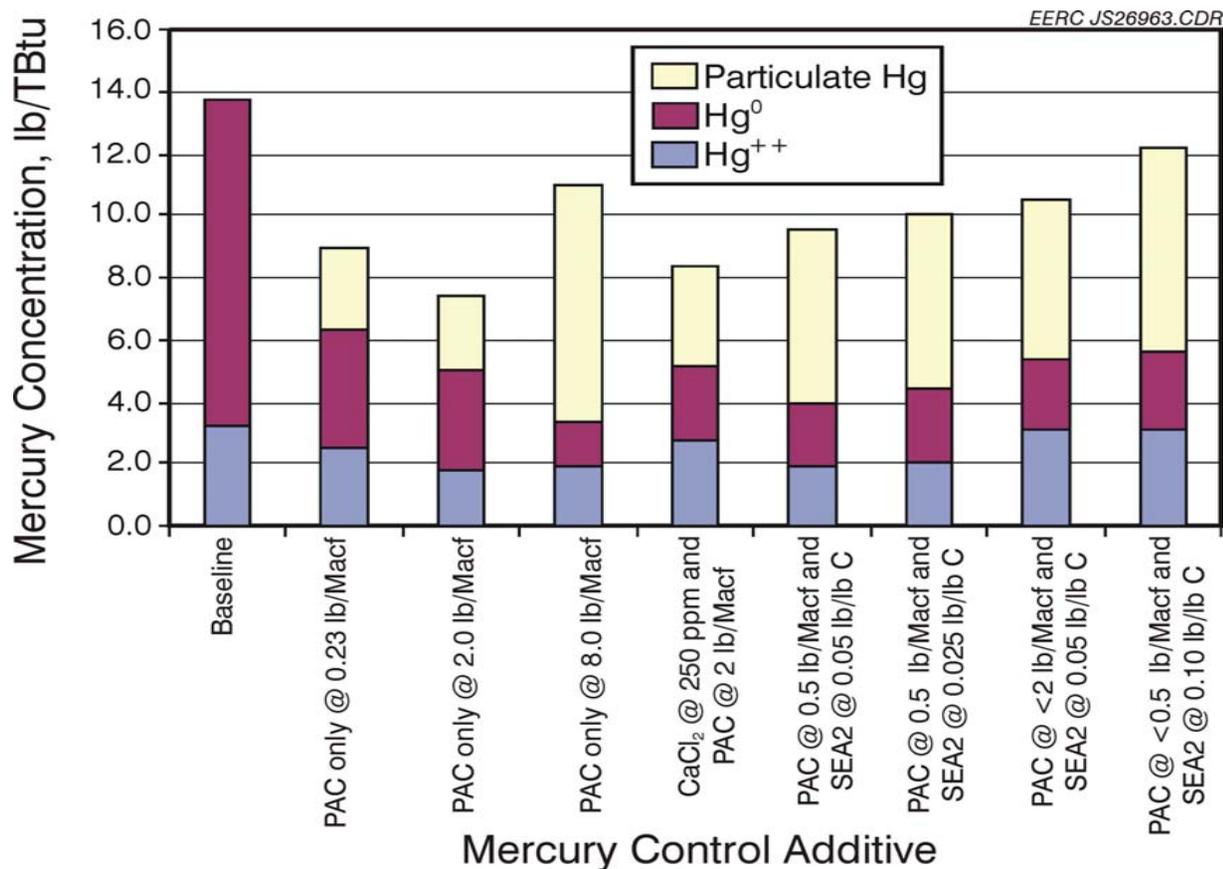
# Previous Hawthorn Test Results



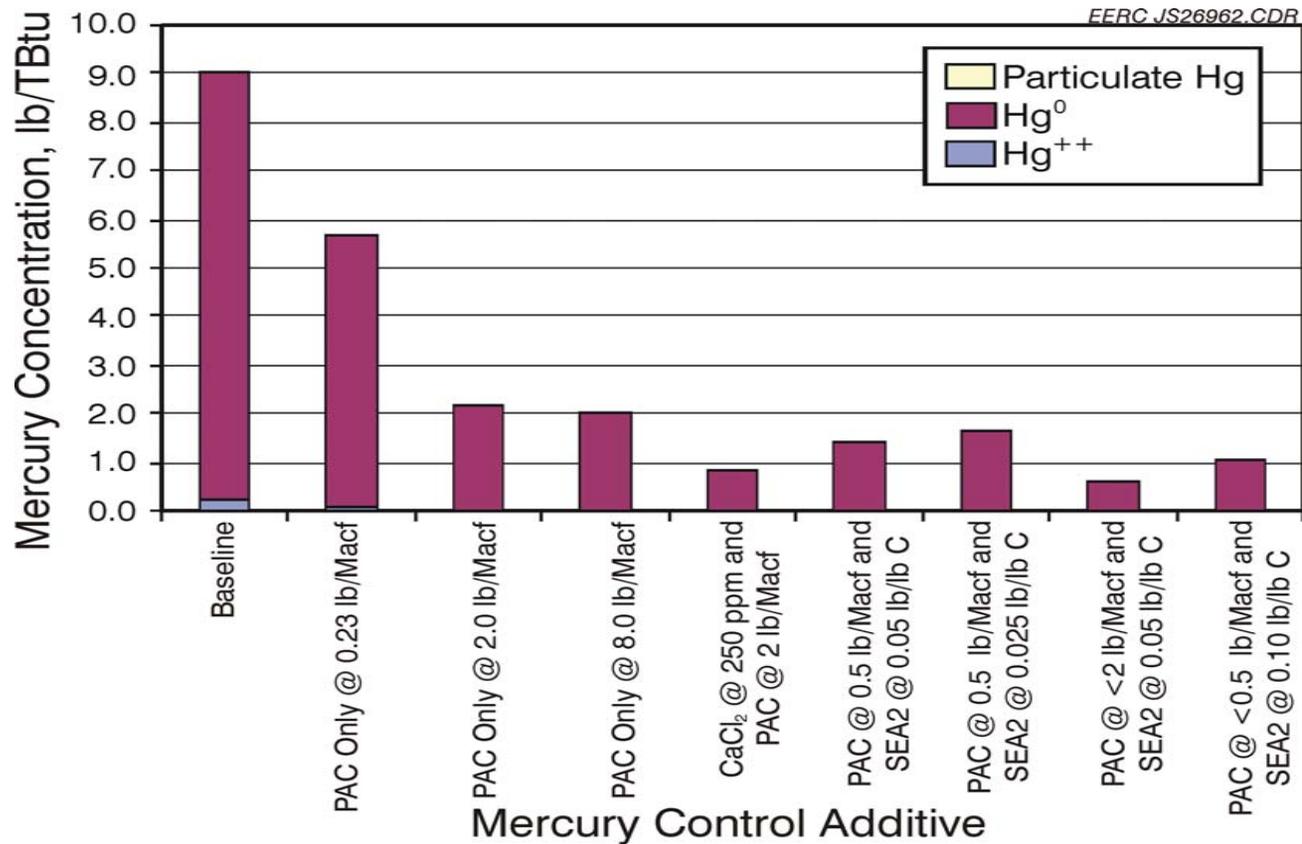
# Previous Hg Speciation at SCR Outlet



# Previous Hg Speciation at SDA Inlet



# Previous Hg Speciation at Stack



# Conclusions

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- 1000 ppm Cl addition (no PAC) at Hawthorn provided an 80%+ Hg capture for 6 hours.
- >90% Hg capture was possible (for short periods of time) using SEA2 and PAC.
- >90% REDUCTION is possible with SEA2 T2.

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# Phase III Project

# Project Overview

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- Goals & Objectives
  - To demonstrate 90% REDUCTION in mercury emissions at Hawthorn Unit 5 and Mill Creek Unit 4.

# Sites

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Plant	Utility Owner	Coal	Boiler Type	Boiler Size, MW	Particulate Control	SO <sub>2</sub> Control	NO <sub>x</sub> Control
HAW5	KCP&L	PRB	Wall- fired	550	FF	SDA	LNB <sup>1</sup> , OFA <sup>2</sup> , SCR
MC4	LG&E	Eastern bituminous	Wall- fired	530	ESP/SCA= 232	Wet FGD	LNB, SCR

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<sup>1</sup> Low-NO<sub>x</sub> burners.

<sup>2</sup> Overfire air.

# Task Structure/Schedule

Task Name	2006			2007				2008			
	Qtr 2	Qtr 3	Qtr 4	Qtr 1	Qtr 2	Qtr 3	Qtr 4	Qtr 1	Qtr 2	Qtr 3	Qtr 4
<b>Task Name</b>											
<b>Task 1. Hawthorn Unit 5 (HAW5)</b>											
<b>1.1 Parametric Tests</b>											
<b>1.2 Longer-Term Tests</b>											
Ontario Hydro Sampling (Three 1-week occurrences during a 2-month period)											
<b>1.3 Management and Reporting</b>											
Site Report - Go/No Go											
Quarterly Reports											
Project Final Report											
<b>Task 2. Mill Creek Station Unit 4 (MC4)</b>											
<b>2.1 Parametric Tests</b>											
Parametric/Baseline SCR On											
Parametric/Baseline SCR Off											
<b>2.2 Longer-Term Tests</b>											
Ontario Hydro Sampling (Three 1-week occurrences during a 2-month period)											
<b>2.3 Management and Reporting</b>											
Site Report - Go/No Go											
Quarterly Reports											
Project Final Report											
<b>Task 3. Project Planning</b>											
Kick-off Meeting											
Test Plan Development											
QA/QC Plan Development											
Data Reduction/Analysis											

# Test Plan for Hawthorn

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- Based on previous work the test plan for Hawthorn will concentrate on the following technologies:
  - SEA 1 Only
  - SEA 1 + PAC
  - SEA 2 T2

# Parametric Test Plan for Hawthorn

Test #	Date	Hg Control Technology	Test	CaCl <sub>2</sub> Coal Equiv.	SEA 2 lb/lb PAC	PAC lb/Macf
1	18-Sep	None	Baseline			
	19-Sep	None	Baseline			
2	20-Sep	SEA1 only (CaCl <sub>2</sub> )	Rate 1	600		
3	21-Sep	SEA1 only (CaCl <sub>2</sub> )	Rate 2	800		
4	22-Sep	SEA1 only (CaCl <sub>2</sub> )	Rate 3	1000		
5	23-Sep	SEA1 + PAC	Rate 1	600		1 & 3
6	24-Sep	SEA1 + PAC	Rate 2	800		1 & 3
7	25-Sep	SEA1 + PAC	Rate 3	1000		1 & 3
8	26-Sep	SEA2-T2 + PAC	Rate 1		0.0125	1 & 3
9	27-Sep	SEA2-T2 + PAC	Rate 2		0.05	1 & 3
10	28-Sep	SEA2-T2 + PAC	Rate 3		0.1	1 & 3

# Previous Data-Mill Creek Unit 4

Sample Location	SCR Inlet, $\mu\text{g}/\text{Nm}^3$	SCR Outlet, $\mu\text{g}/\text{Nm}^3$	wet-FGD inlet, $\mu\text{g}/\text{Nm}^3$	Stack, $\mu\text{g}/\text{Nm}^3$	Removal %
<i>With the SCR in Service</i>					
Hg <sup>P</sup>	0.02	0.03	0.00	0.00	
Hg <sup>0</sup>	8.32	2.83	0.33	3.97	
Hg <sup>2+</sup>	0.94	5.05	7.60	0.54	
Hg <sub>total</sub>	9.27	7.90	7.93	4.50	<b>43.3</b>
<i>With the SCR Bypassed</i>					
Hg <sup>P</sup>			0.07	0.05	
Hg <sup>0</sup>			2.44	2.63	
Hg <sup>2+</sup>			6.79	0.55	
Hg <sub>total</sub>			9.30	3.23	<b>65.3</b>

# Mill Creek Unit 4 Cont.

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- Mill Creek offers challenges with the SCR in service!
  - Possibly due to reactions with sulfur species.
  - Lower halogen levels in scrubber?
- SEA2 T2 will be primary technology tested at Mill Creek.
- B&W Re-emission additive will also be added to scrubber, if necessary.

# Mill Creek Test Plan

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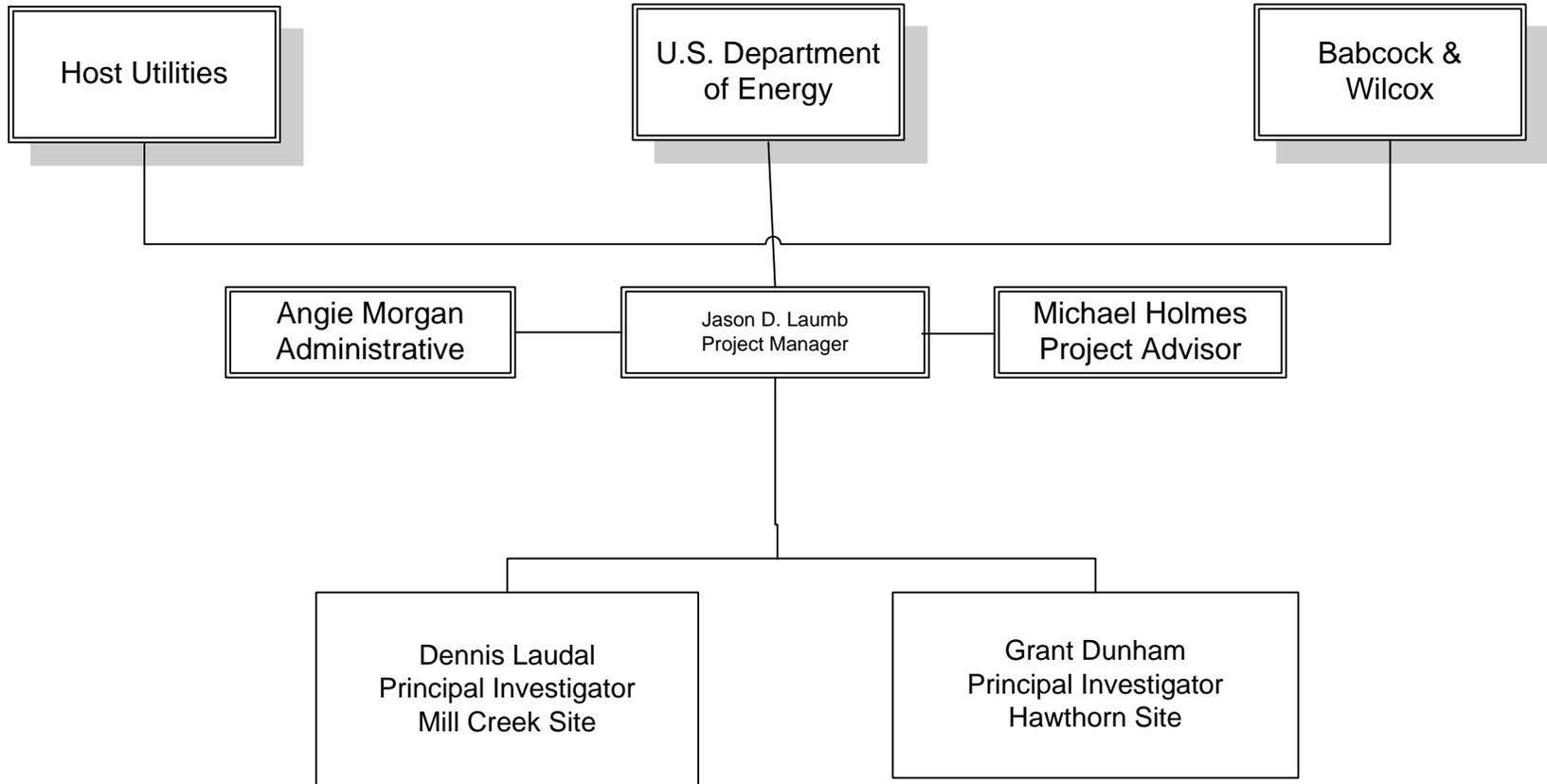
- Parametric study with SCR in and out of service.
- Two Month demonstration with the SCR in service.
- Plan to be developed upon completion of negotiations with plant.

# Sampling Locations (Both Sites)

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- Continuous Mercury Monitors – PCD inlet and stack for parametric tests. Stack only for long-term.
- Ontario Hydro – PCD inlet and stack for parametric tests and long term.
- Solid Samples – Daily coal, ash, slurry samples during parametric. Three per week during long term.
- EPA Method 5 – PCD inlet & stack?

# Personnel



# Current Coal Results

Parameters, Unit	9/18/2006	9/19/2006	9/20/2006	Average	Standard Deviation
<b>Mercury, ppm (dry)</b>	0.114	0.106	0.105	<b>0.108</b>	0.005
<i>Proximate</i>					
Moisture, wt%	19.1	20.6	20.9	20.20	0.964
Volatile Matter, wt%	34.86	34.22	34.14	34.41	0.395
Fixed Carbon, wt%	40.66	40	39.75	40.14	0.470
Ash, wt%	5.38	5.18	5.21	5.26	0.108
<i>Ultimate Analysis</i>					
Hydrogen, wt%	6.12	6.1	6.1	6.11	0.012
Carbon, wt%	55.17	54.06	53.6	54.28	0.807
Nitrogen, wt%	1.05	0.97	0.96	0.99	0.049
Sulfur, wt%	0.45	0.38	0.5	0.44	0.060
Oxygen, wt%	31.83	33.32	33.62	32.92	0.959
Heating Value, Btu/lb	9613	10942	9365	9973	848
<i>Calculated Parameters</i>					
F <sub>d</sub> , dscf/10 <sup>6</sup> Btu	9636	8238	9542	9139	782
Sulfur, wt% (dry)	0.56	0.48	0.63	0.56	0.077
Heating Value, Btu/lb (dry)	11883	13781	11839	12501	1109
<b>Hg, µg/Nm<sup>3</sup> (flue gas basis)</b>	13.67	12.82	12.76	<b>13.08</b>	0.509
Hg, lb/Tbtu (flue gas basis)	9.59	7.69	8.87	8.72	0.960

# Current Baseline Results

- **Baseline Hg measurements indicate a native Hg capture average of 17.8 %\***
- **Coal and OH inlet measurements are consistent.**
- **CMM inlet and outlet measurements tend to be low for the baseline period when compared to OH and Coal results, but agree well during Hg control technology testing**

Date	Test Description	Coal (Inlet) μg/Nm <sup>3</sup>	CMM Inlet μg/Nm <sup>3</sup>	OH Inlet μg/Nm <sup>3</sup>	CMM Outlet μg/Nm <sup>3</sup>	OH Outlet μg/Nm <sup>3</sup>	Coal-to-Stack Hg Removal, %	
							OH	CMM
9/18/2006	Baseline	13.67	7.23	14.28	8.7	11.37	16.9	36.4
9/18/2006	Baseline	13.67	7.52	13.61	8.64	10.86	20.5	36.8
9/19/2006	Baseline	12.82	6.24	11.27	8.28	10.54	17.8	35.4
9/19/2006	Baseline	12.82	6.93	12.67	8.64	10.78	15.9	32.6

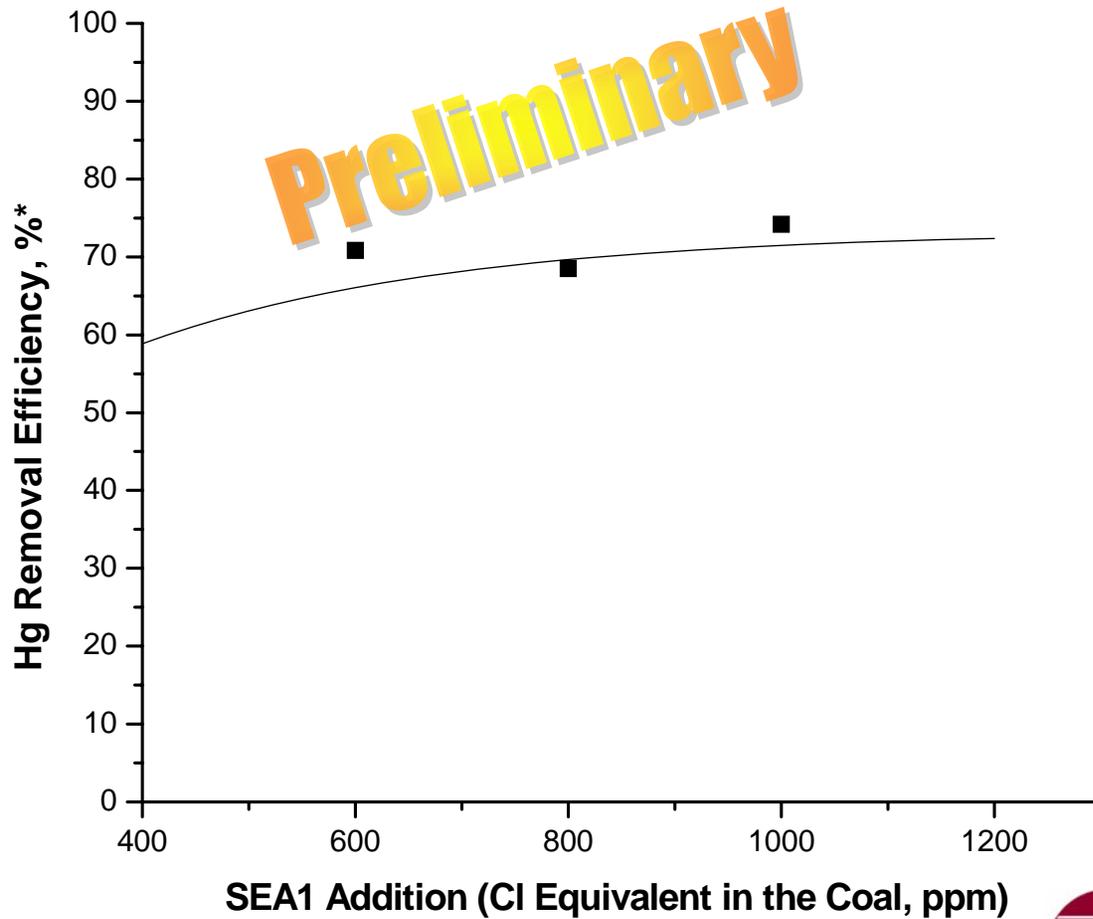
\*Coal inlet to OH outlet basis

# Current SEA1 Results

- Testing of SEA1 occurred during 9/20/06-9/22/06
- Results indicate a positive effect on Hg capture when compared to baseline removals.
- Hg removal efficiencies appear to only slightly increase with increasing SEA1 rate.

Date	Test Description	Coal (Inlet) μg/Nm <sup>3</sup>	CMM Inlet μg/Nm <sup>3</sup>	OH Inlet μg/Nm <sup>3</sup>	CMM Outlet μg/Nm <sup>3</sup>	OH Outlet μg/Nm <sup>3</sup>	Coal-to-Stack Hg Removal, %	
							OH	CMM
9/18/2006	Baseline	13.67	7.23	14.28	8.7	11.37	16.9	36.4
9/18/2006	Baseline	13.67	7.52	13.61	8.64	10.86	20.5	36.8
9/19/2006	Baseline	12.82	6.24	11.27	8.28	10.54	17.8	35.4
9/19/2006	Baseline	12.82	6.93	12.67	8.64	10.78	15.9	32.6
9/20/2006	SEA1 Only (600 ppm)	12.76	11.54	12.46	3.72	4.67	63.4	70.8
9/21/2006	SEA1 Only (800 ppm)	13.08	12.93	12.15	4.12	4.53	65.4	68.5
9/22/2006	SEA1 Only (1000 ppm)	13.08	10.41	13.88	3.37	8.05	38.4	74.2

# Current SEA1 Results



\*Coal inlet to CMM outlet Basis

# Conclusions

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- Baseline removals at Hawthorn are considerably higher than previous work.
  - Different coal?
- Preliminary results with  $\text{CaCl}_2$  are also different (lower) from previous work.
  - Catalyst age?

# Acknowledgments

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