

# Large Scale Mercury Control Field Testing – Phase II

---

## “Advanced Utility Mercury-Sorbent Field-Testing Program”

Progress Report - July 2005



**DOE National Energy Technology Laboratory**

Lynn Brickett, Project Officer



**Sorbent Technologies Corporation**

Sid Nelson Jr., Project Director

# Project Participants

---

## Host Sites

- Duke Energy
- Detroit Edison

## Project Contractors

- W. Kentucky Univ., (CMMs)
- Fuel Tech Inc. (CFD)

## Field Test Partners

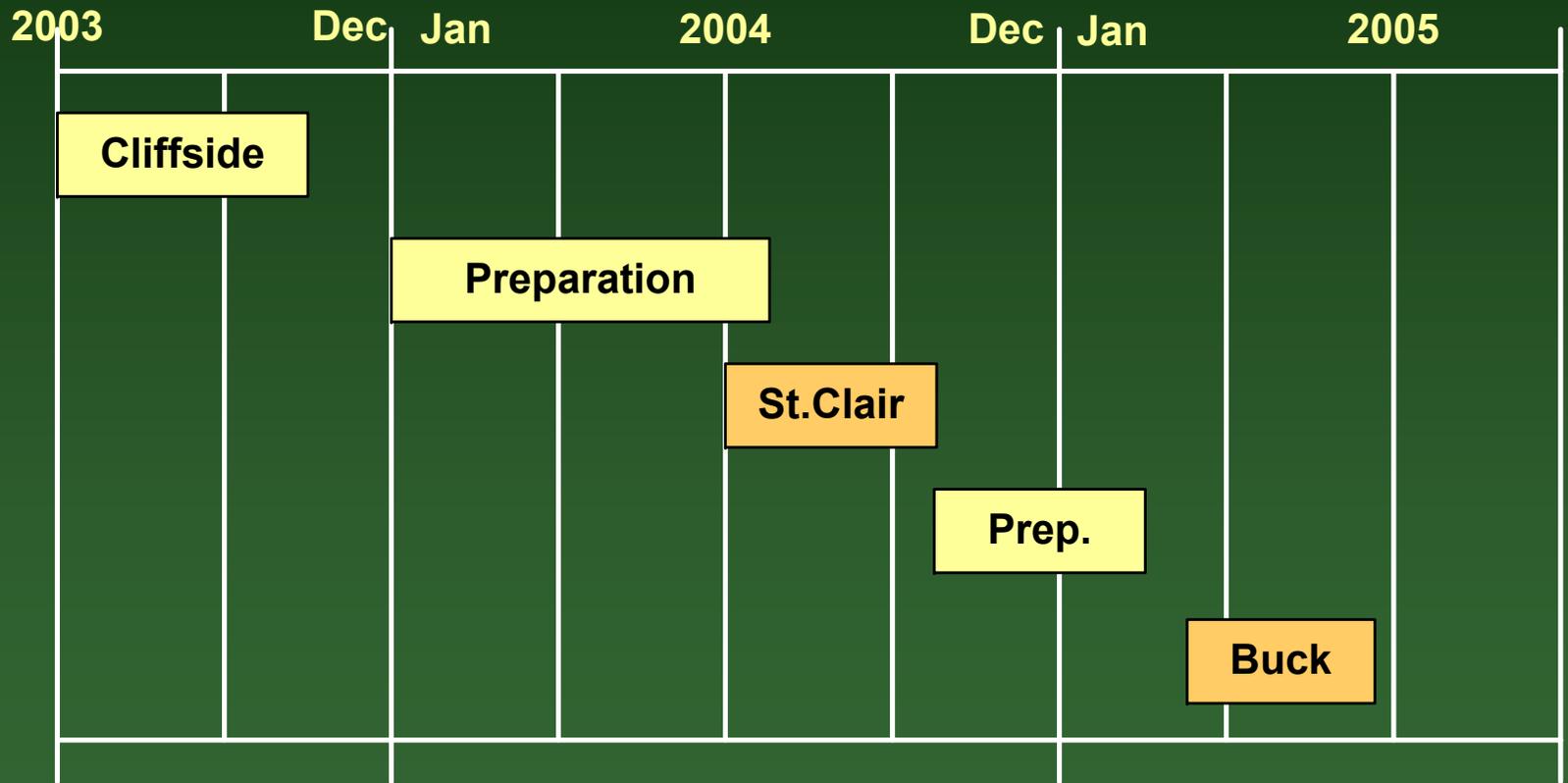
- PS Analytical Ltd. (Dry Converter)
- Spectra Gases (Hg Standards)
- Headwaters Clean Coal (Byproducts)

# Unique Features

---

- Brominated PAC (B-PAC™)
- Subbituminous (85%) Blend
- Hot-Side ESP
- Field-Testing Partners

# Schedule



# Detroit Edison – St. Clair Station

Southeast Michigan

Cold-Side ESP

290°F

85 Sub/15 Bitum. Blend

80 MW

700 (580) ft<sup>2</sup>/K acfm

0.06 ppm

Mostly Hg<sup>(0)</sup>



# Continuous Mercury Monitors (CMMs)

---

- 2 Latest PS Analytical Ltd. CMMs & an experimental Ohio Lumex unit
- Dual Wet/Dry Hg<sup>(+2)</sup> Converters
- Baldwin & Apogee Inertial Separators
- Also Ontario Hydro & Method 324 Hg Sampling
- Baseline Native Hg Removal: 0%—~30%



# Injection Trailer & Instruments in Place

---

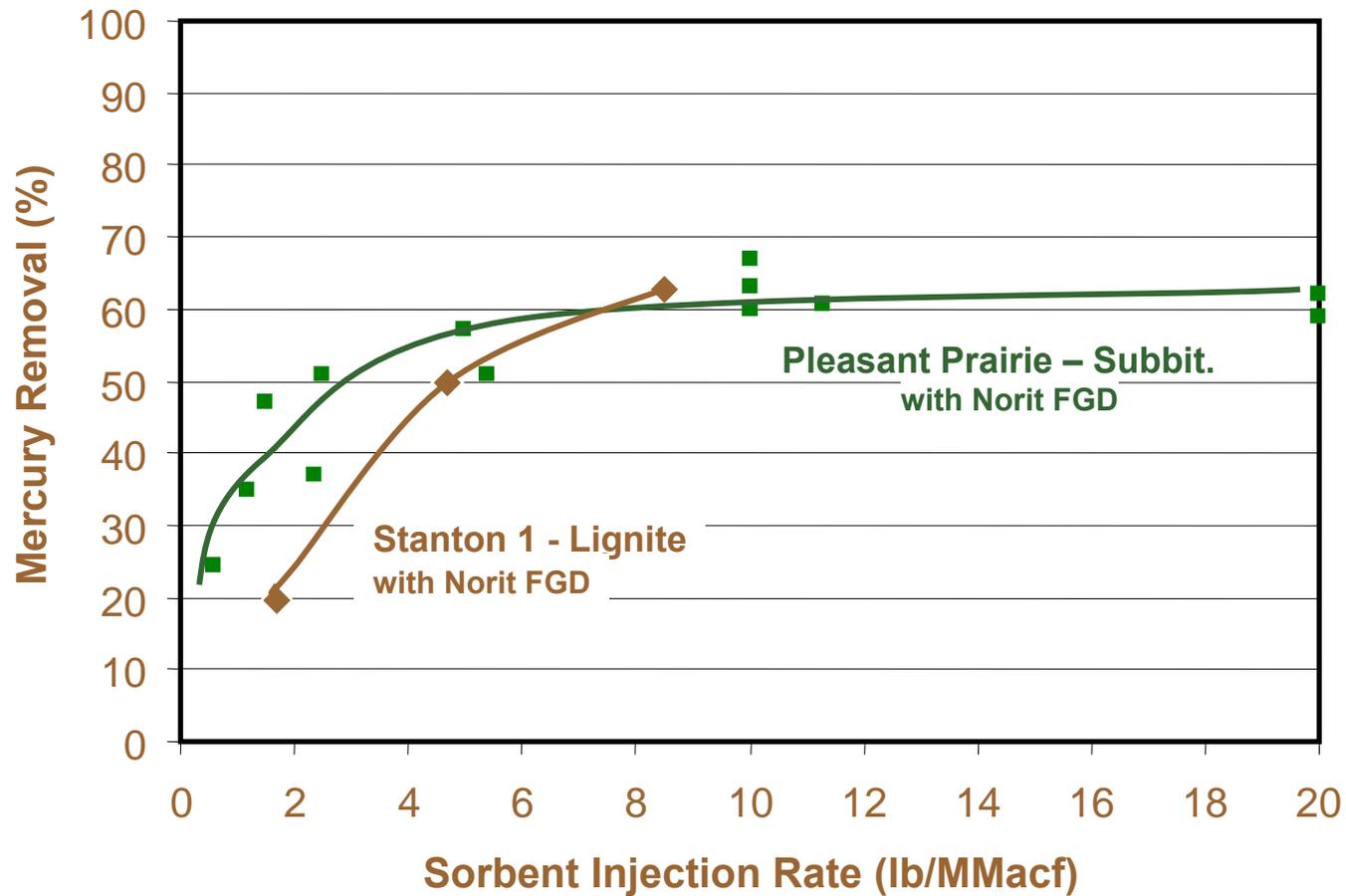


Mobile injection trailer (patent pending) in place.

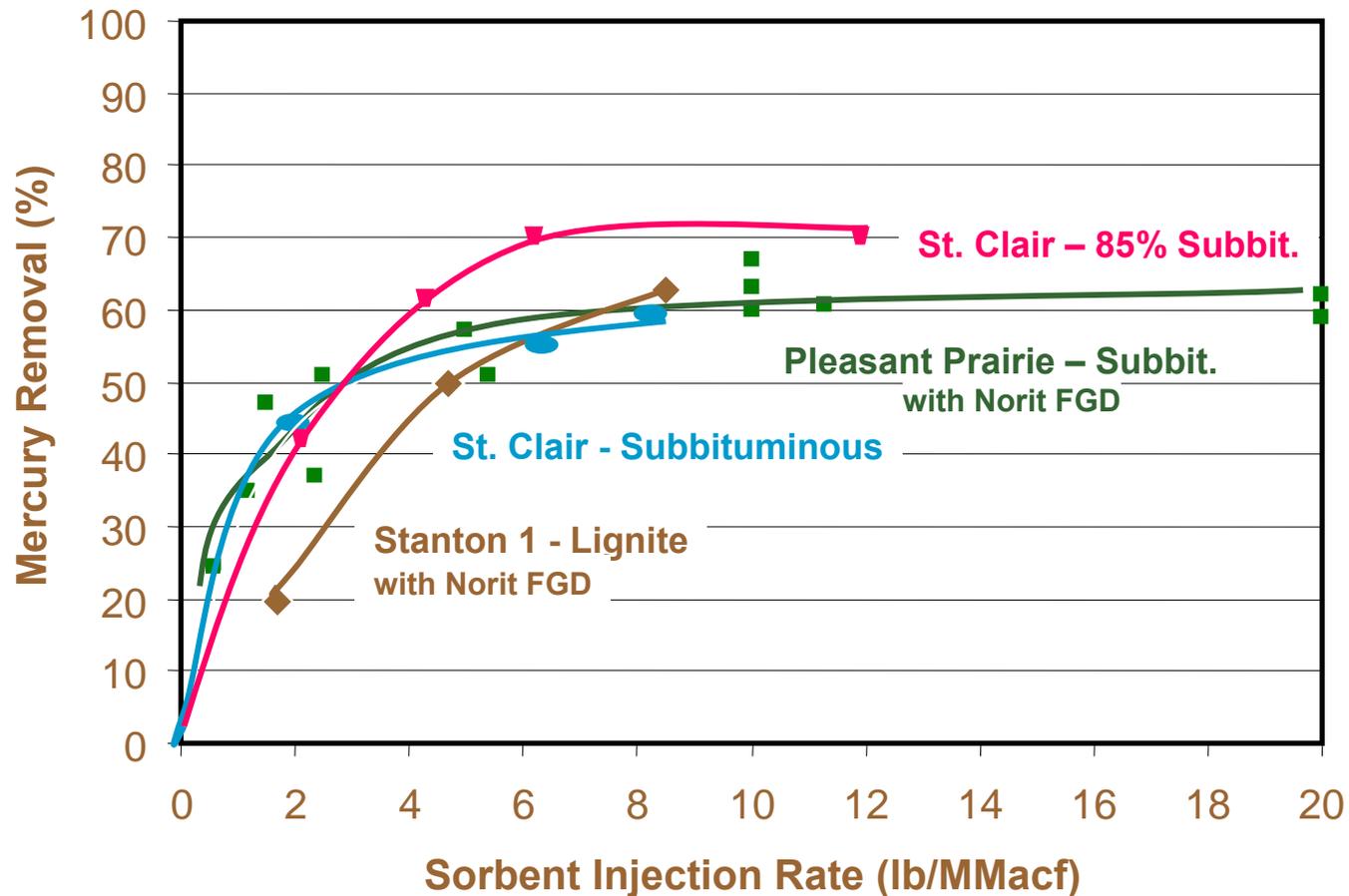


ESP outlet Hg measurement.

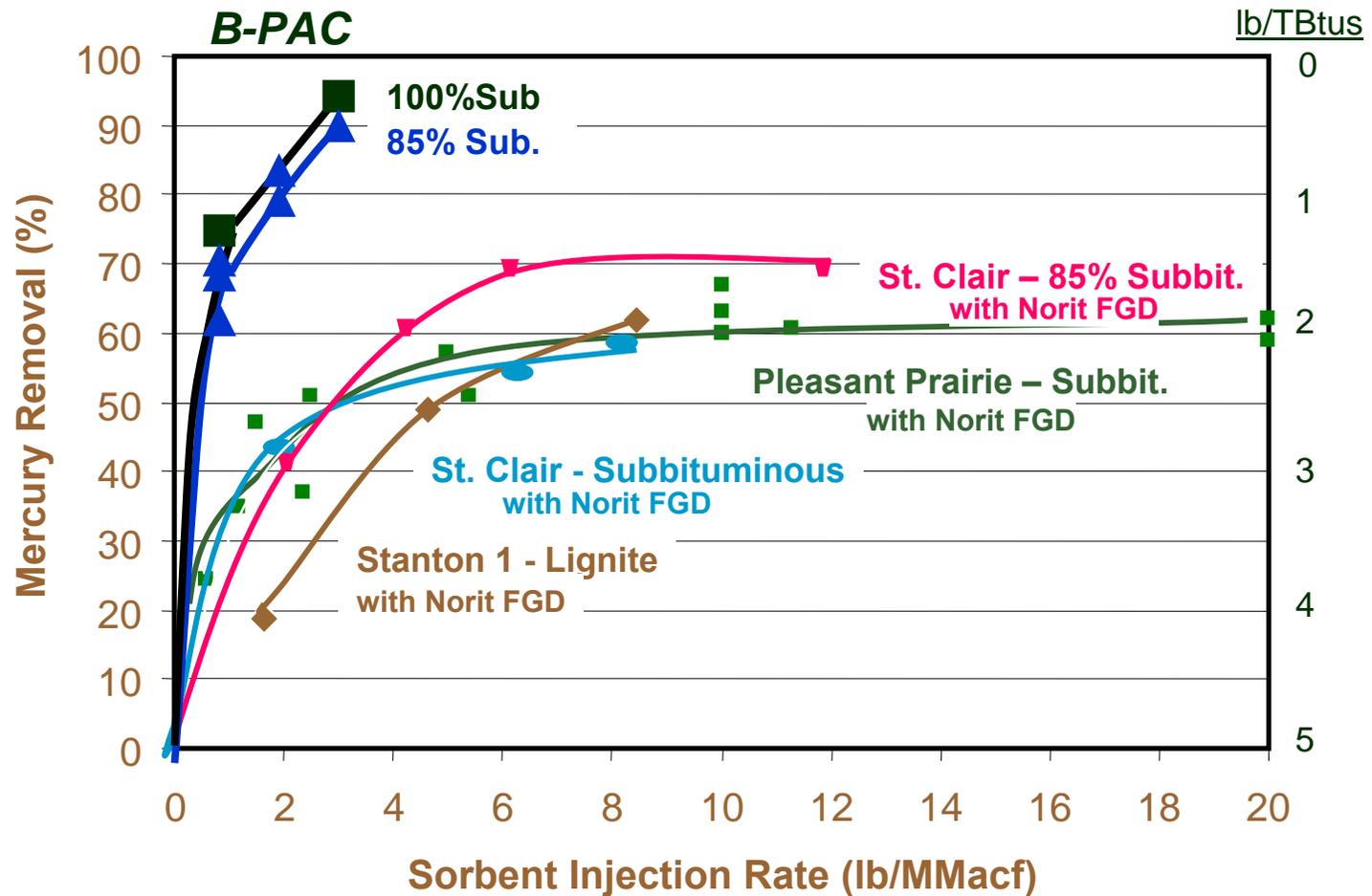
# Western Coals with ESPs – Full-Scale



# Western Coals with ESPs – Full-Scale

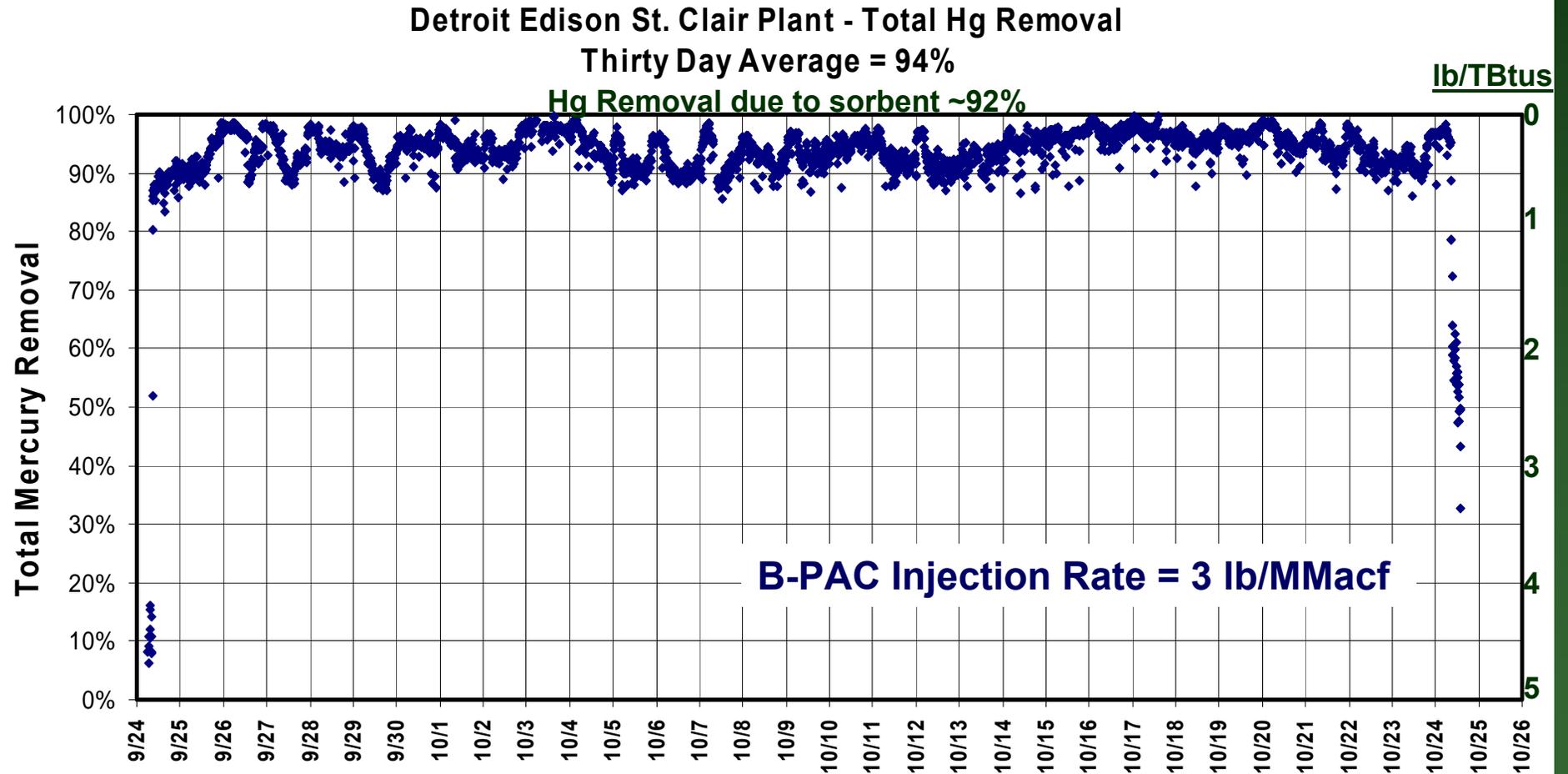


# Western Coals with ESPs – Full-Scale

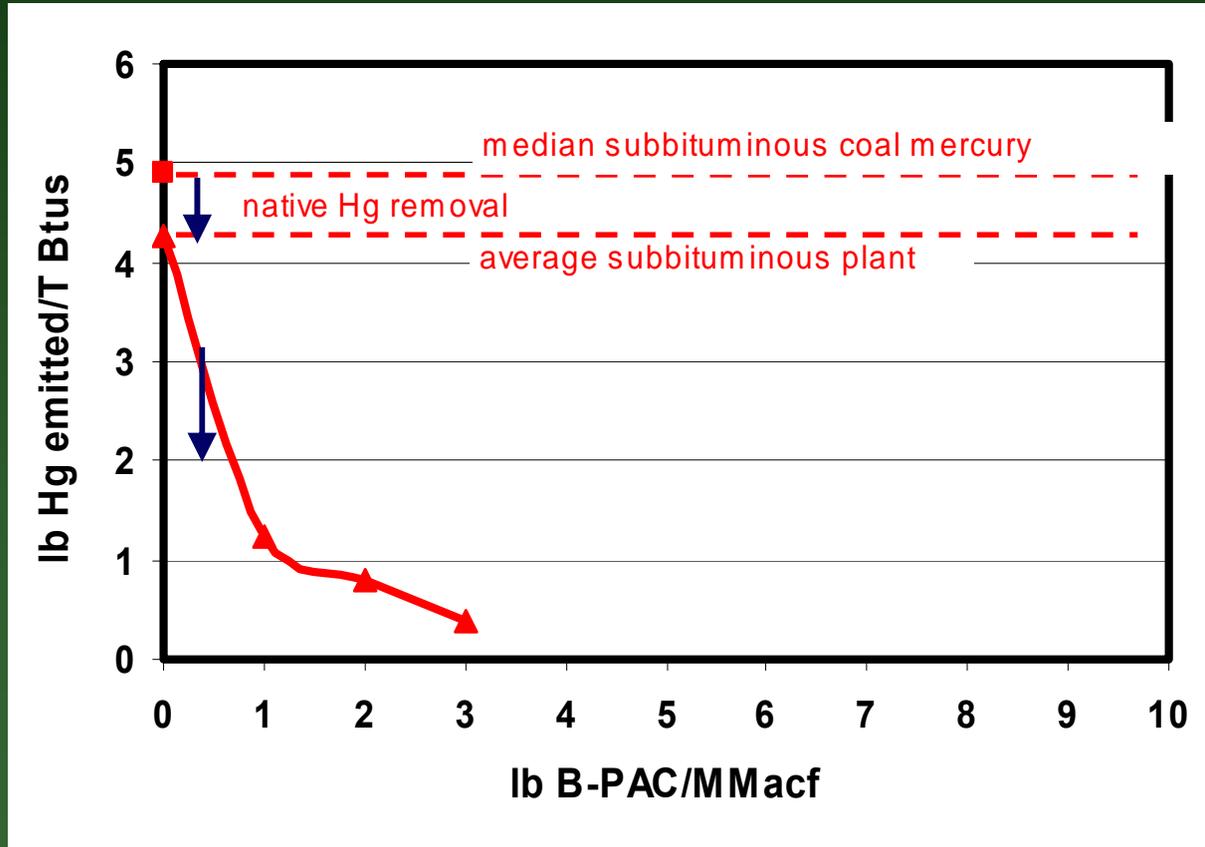


# Long-Term Continuous B-PAC Run at St. Clair

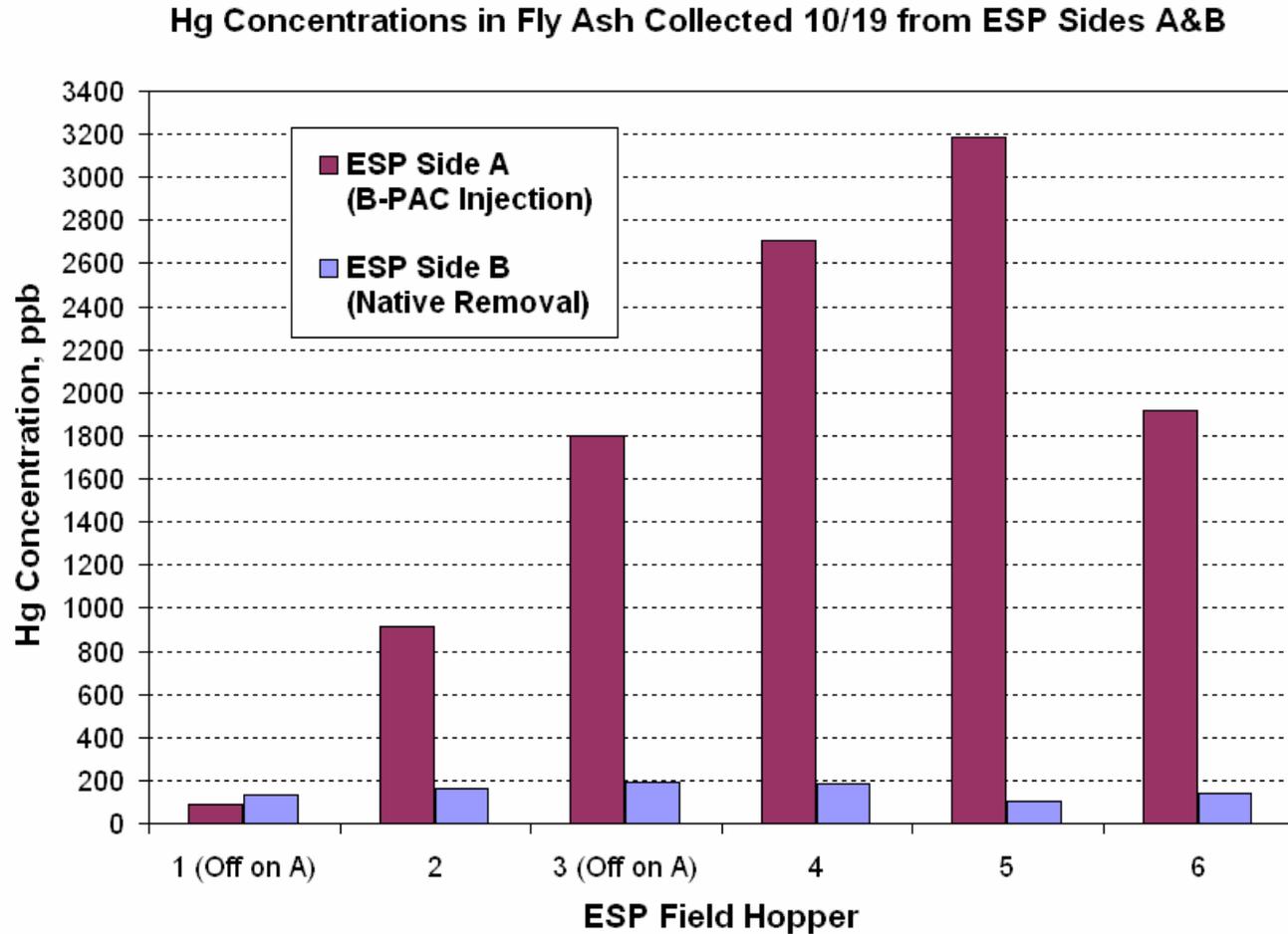
## Thirty Day Average Mercury Removal = 94%



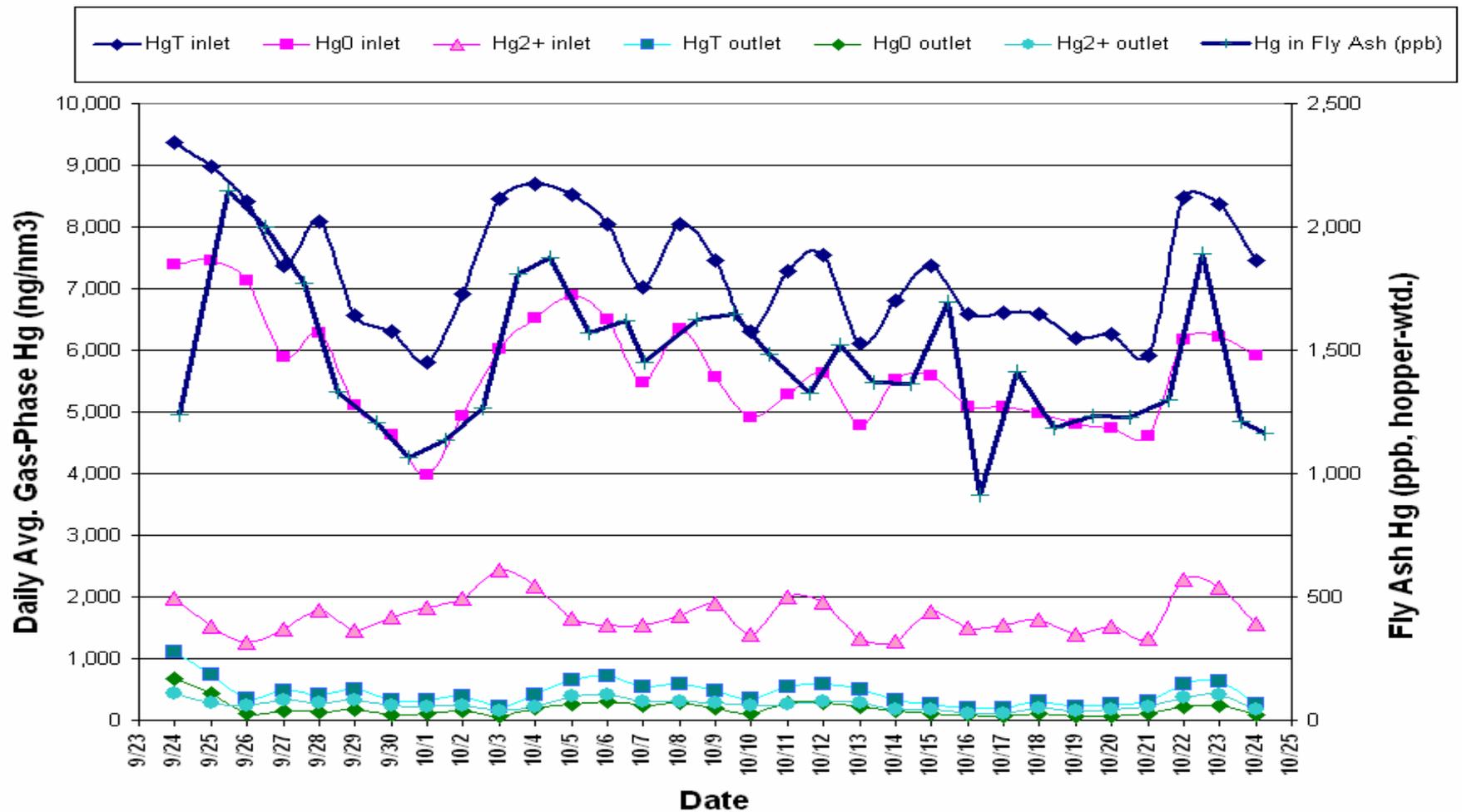
# 1-2 lb B-PAC/MMacf Gets to 1 lb Hg/T Btus



# Mercury Sequestered in the Fly Ash

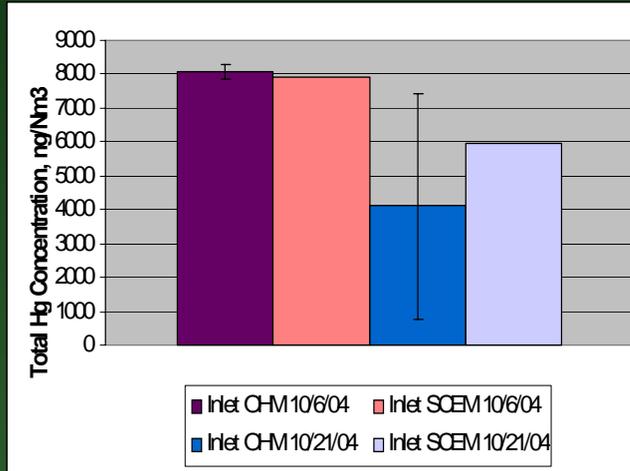


# Fly Ash Hg Tracked CMM Hg Closely

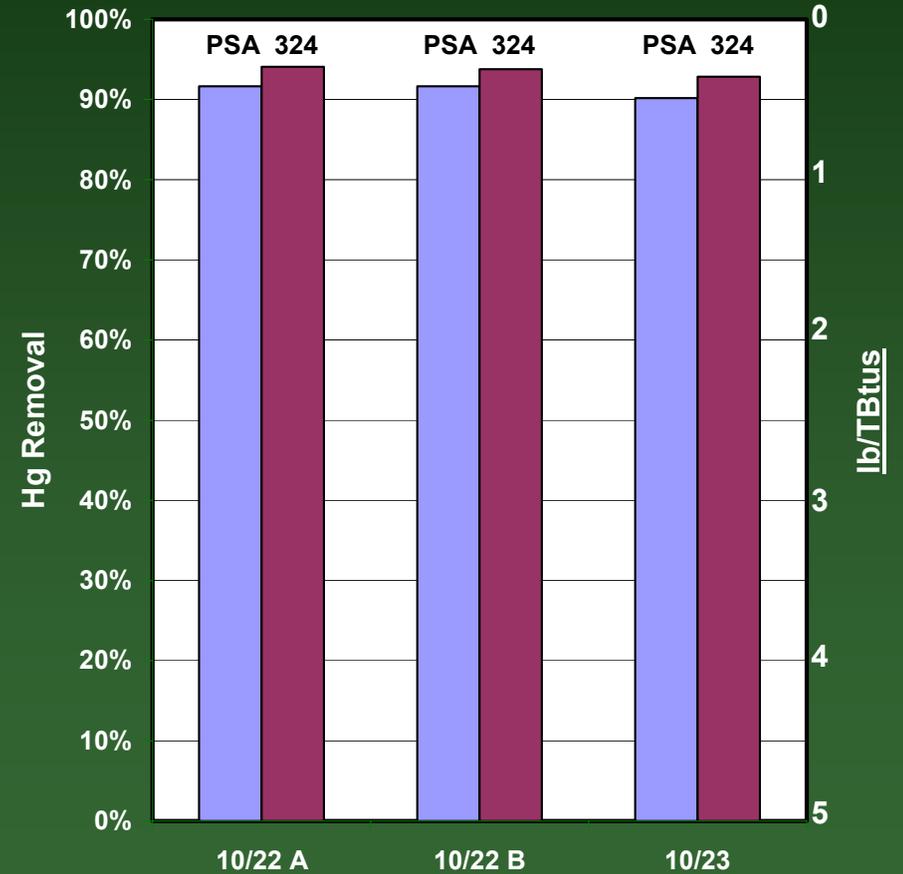
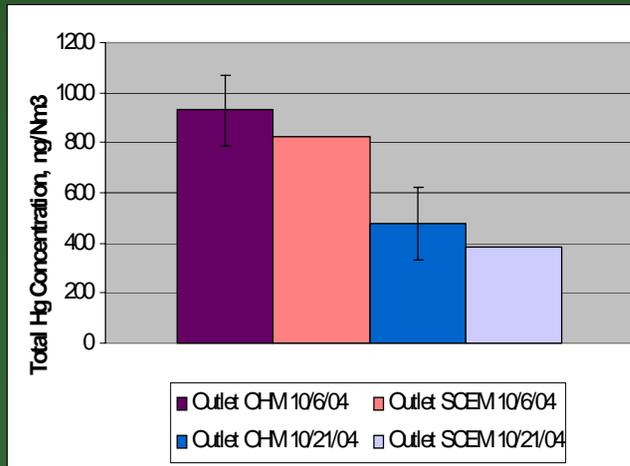


# Ontario Hydro & Method 324 Verification

Inlet – Twice in Long-Term Run



Outlet – Twice in Long-Term Run



# Cost Effectiveness with PRB at St. Clair

If 1 lb/MMacf of \$0.75/lb B-PAC is injected into a CS-ESP with 7  $\mu\text{g Hg}/\text{Nm}^3$  provides 70% Hg removal:

$$\left( \frac{1 \text{ lb sorbent}}{1,000,000 \text{ acf}} \right) \left( \frac{\text{Nm}^3}{(70\%) 7 \mu\text{g Hg}} \right) \left( \frac{\$0.75}{\text{lb sorbent}} \right) \left( \frac{1.5 \text{ acf @ } 300\text{F}}{1 \text{ scf}} \right) \left( \frac{35.3 \text{ scf}}{\text{Nm}^3} \right) \left( \frac{10^9 \mu\text{gHg}}{2.2 \text{ lb Hg removed}} \right) = \$3,700 / \text{lbHg}.$$

**Cost < \$4,000 /lb Hg removed,**

**>90% cost reduction from the current technology baseline.**

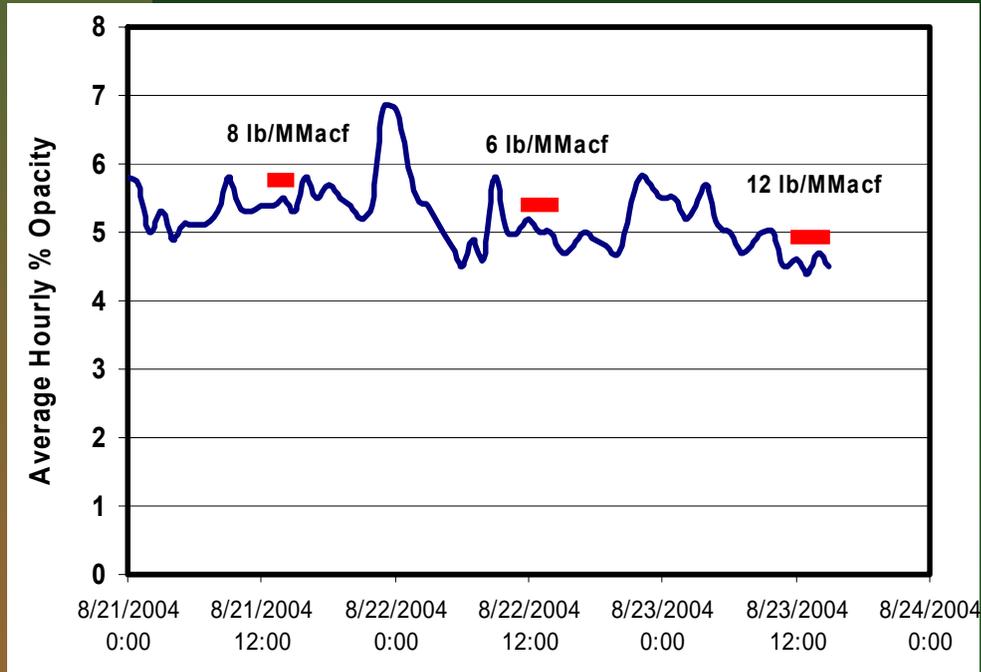
Similarly, if 3 lb/MMacf of B-PAC is injected into a cold-side ESP provides 90% Hg removal:

**Cost < \$10,000 /lb Hg removed,**

**85% cost reduction from the current technology baseline.**

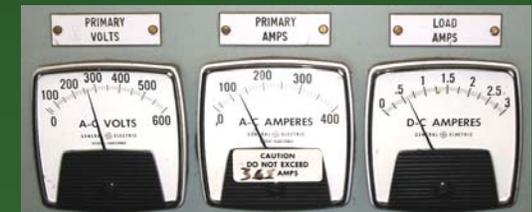
# No Balance-of-Plant Effects Observed

## No Changes in ESP Performance



Never any Sparking.  
All Data at High Load.

Field	G-R Set		Load on Wire		Load on Plate		
	Primary Volts	Before	During	Primary Amps	Before	During	Load Amps
<b>B-PAC</b>	2	220	210	100	80	0.35	0.35
<b>6 lb/MMacf</b>	4	290	290	150	150	0.80	0.80
85% Subbituminous	5	250	250	140	140	0.75	0.75
8/10/2004	6	270	270	150	150	0.75	0.75
<b>Plain PAC</b>	2	225	230	40	40	0.15	0.15
<b>8 lb/MMacf</b>	4	300	300	110	110	0.60	0.60
100% Subbituminous	5	220	220	90	90	0.35	0.35
8/21/2004	6	290	290	150	150	0.75	0.75



## No Leachate Hg

B-PAC in the fly ash had net adsorption of Hg from the leaching solutions

# No Balance-of-Plant Effects Observed

Very low off-gassed bromine.

Method 26A Results – All data in ppm.

No Br<sub>2</sub> was ever detected.

Without Sorbent	Baseline 07/28	Inlet-Long-Term 10/21
HF	1.0	0.4
HCl	8.1	3.6
Cl <sub>2</sub>	<0.1	0.3
HBr	0.1	<0.1

B-PAC 3lb/MMacf	Parametric 09/09	L-T 10/06	L-T 10/21
HF	2.2	0.1	0.4
HCl	5.9	6.0	4.3
Cl <sub>2</sub>	0.1	0.2	0.4
HBr	1.0	0.3	0.2

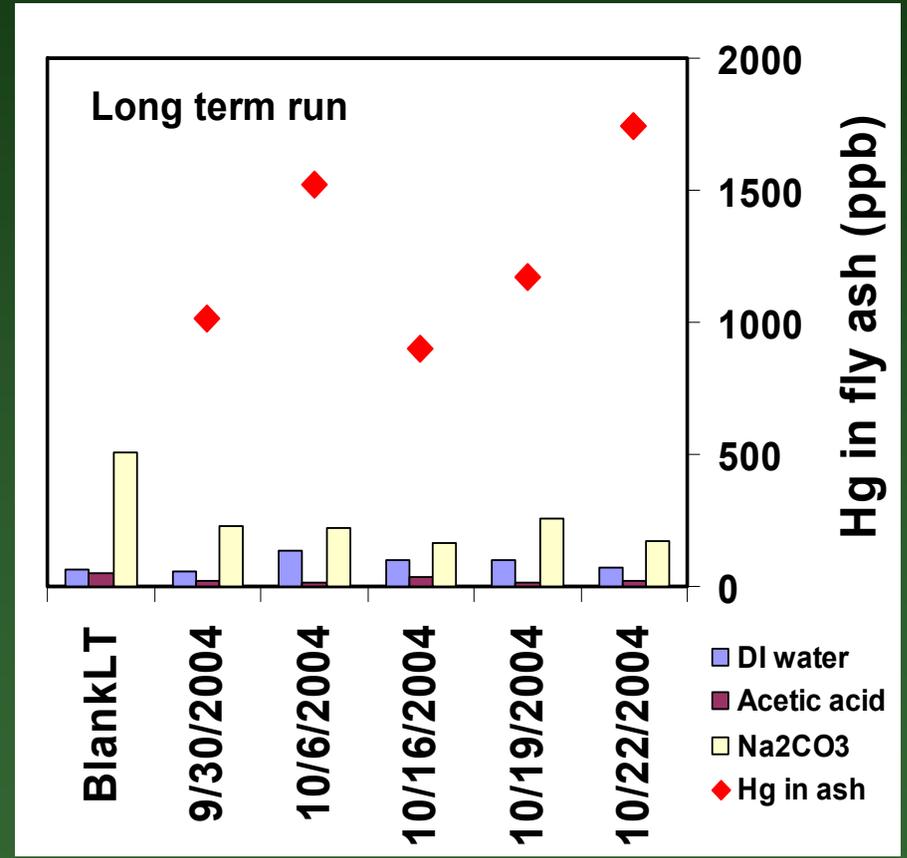
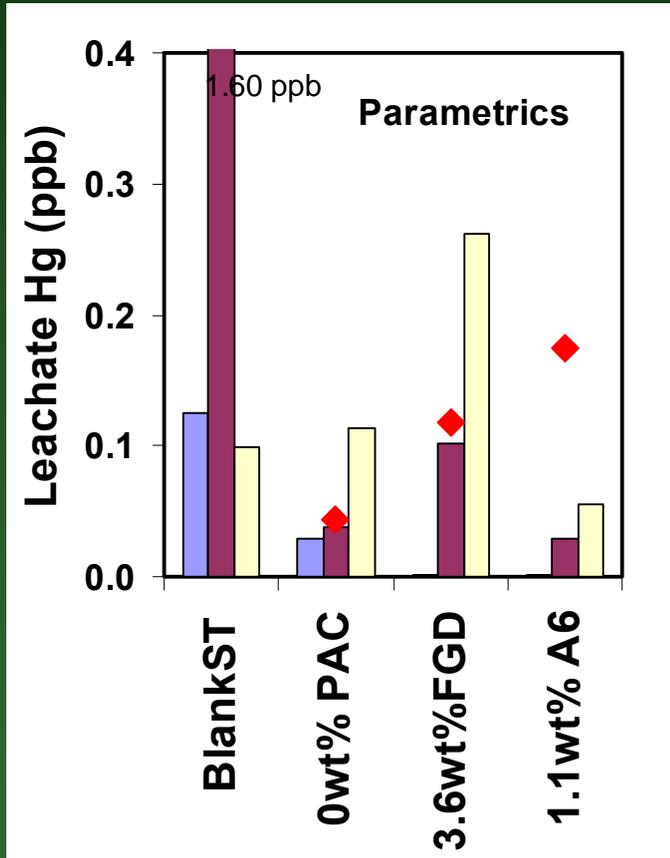
## Carbon Steel Corrosion Coupons

(4 each, 30 days)

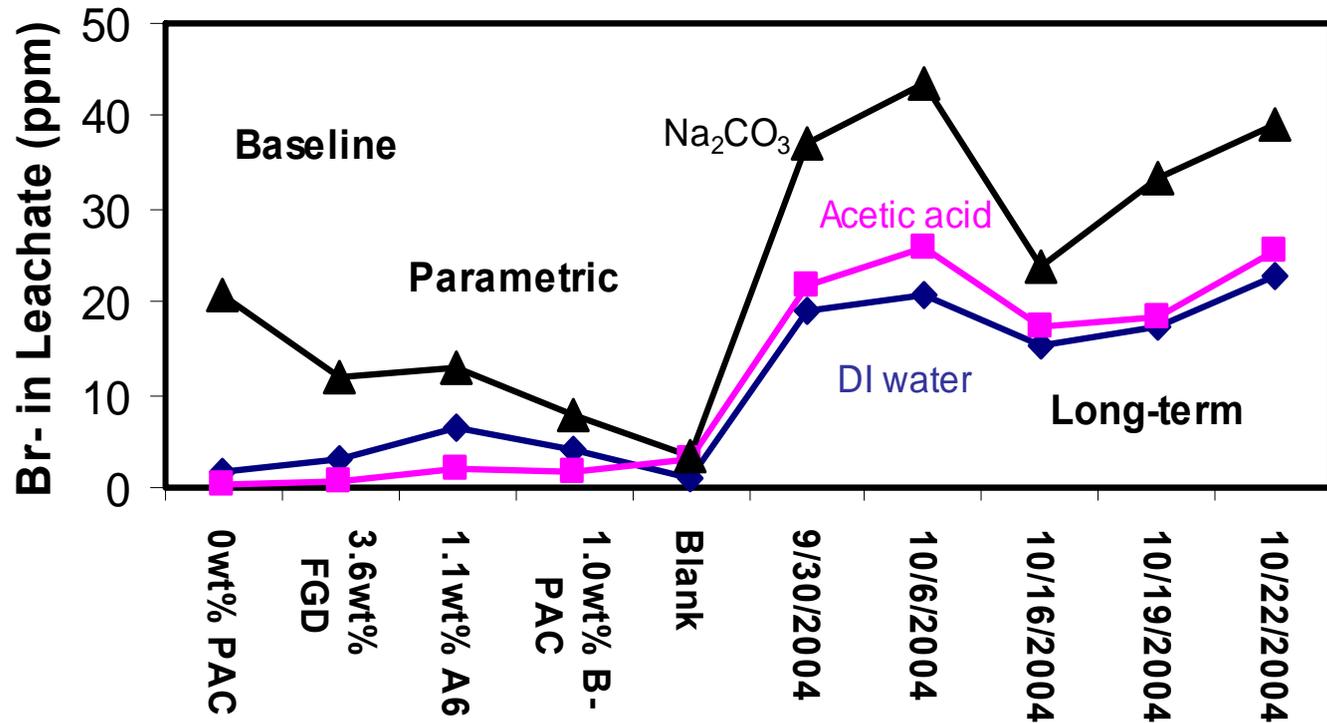
	<u>Avg. ΔWt.</u>
<b>Baseline</b>	<b>+0.13%</b>
<b>B-PAC</b>	<b>+0.13%</b>

**No corrosion detected.**

# Hg Is Not Leachable



# Leachate Br- from St. Clair Fly Ash



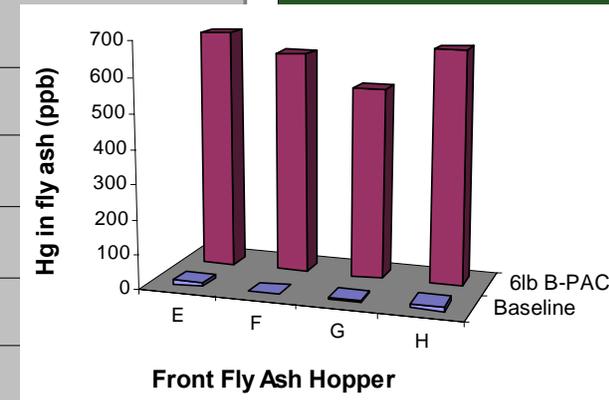
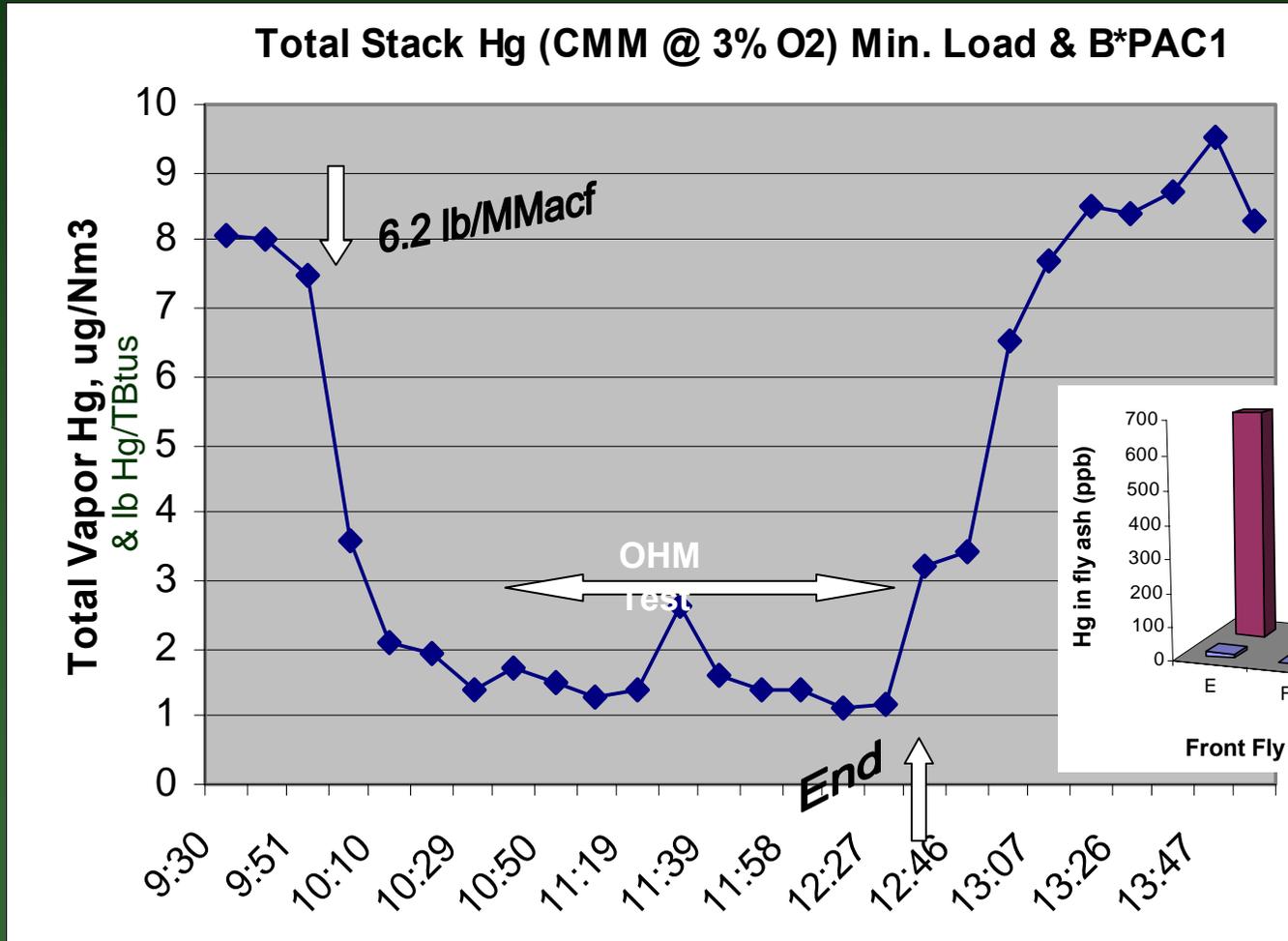
# Hot-Side Testing at Duke's Cliffside Plant



Coal Type:	Low-S Bitumin.
Boiler:	No. 2 (Unit 2)
Boiler Type:	Tangential
Particulates:	Hot-Side ESP
ESP Stream Size:	40 MWe
ESP Inlet Temp.:	700°F
SCA :	240 ft <sup>2</sup> /K acfm
Avg. Coal Hg:	0.08 ppm
Avg. Coal Cl:	500 ppm

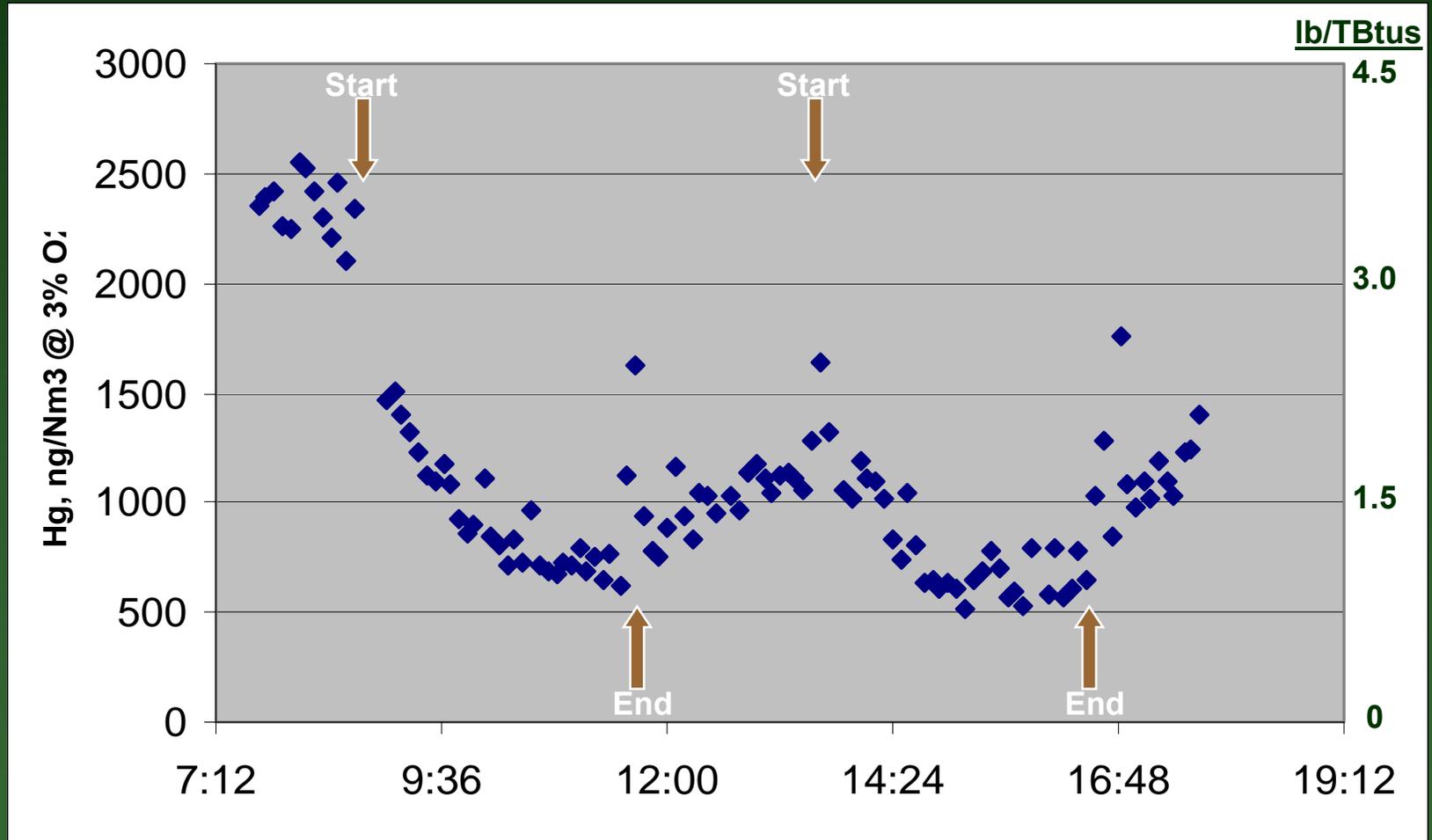
# Cliffside 2003 Results

## H-PAC at 6.2 lb/MMacf

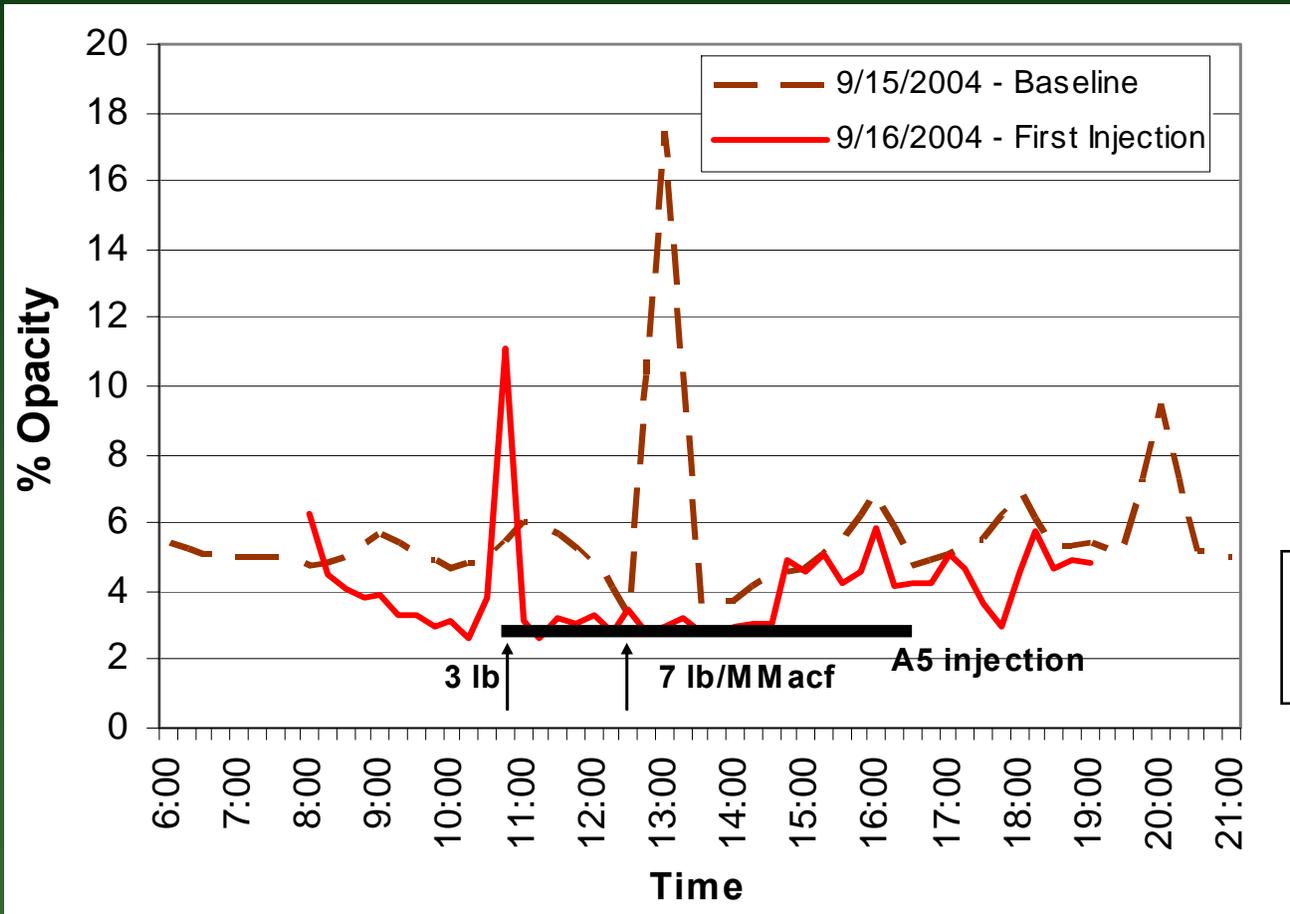


# Cliffside 2004 Results – Two B-PAC Sorbents

## H-PAC at 5.0 lb/MMacf @ Min. Load



# Balance-of-Plant Effects: Opacity



SCA=240 ft<sup>2</sup>/K acfm

# Duke Energy – Buck Plant – Hot-Side ESP

North Carolina

Hot-Side ESP

640°F Inlet

Low-S Bituminous

½ x140 MW (~100MW)

240 ft<sup>2</sup>/K acfm SCA

~ 0.06 ppm Hg

~ 5.4 µg/Nm<sup>3</sup> @ O<sub>2</sub>

~ 60-80% Hg<sup>(+2)</sup>



# Parametric Tests

## Preliminary Results

<u>Boiler Load</u>	<u>Inj.Temp.</u>	<u>lb/MMacf</u>	<u>H-PAC1</u> <u>% Removal</u>	<u>H-PAC2</u> <u>% Removal</u>
60 MW	540F	4.0	56%	65%
60 MW	540F	7.0	57%	63%
100 MW	590F	2.0	54%	44%
100 MW	590F	5.0	62%	N.D.
100 MW	590F	7.0	63%	62%
140 MW	640F	7.0	64%	54%
140 MW	640F	7.0	3%	Norit FGD

# Preliminary Conclusions from Parametrics

---

- essentially no native Hg removal
- essentially no Hg removal with plain PAC
- generally 50-65% removal at 2-7 lb/MMacf with both H-PACs
- gas temperature & load appeared to have little affect
- Hg removal appeared to plateau with injection rate

# Long-Term Testing

---

- **30 days, but periodic shutdowns**
  - boiler tube leak, 2 flameouts, etc.
  - coal went to ~20% ash
  - some inertial-separator or analyzer outages
- boiler switched to low-NO<sub>x</sub> mode/OFA
- switched inlet monitoring to untreated outlet
- difficulty in getting representative ash samples
- M324s + 3 days of Apogee co-measurement + OHMs

# Long-Term Test

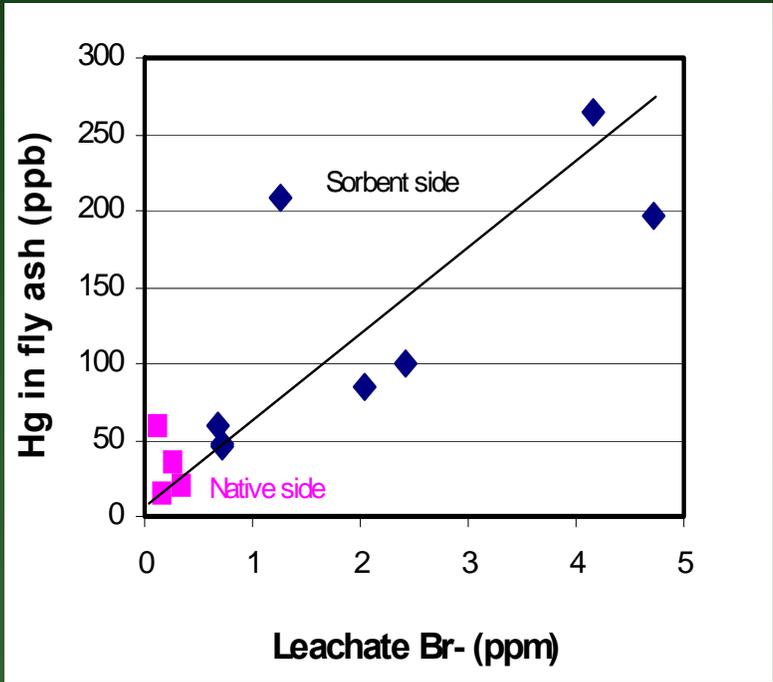
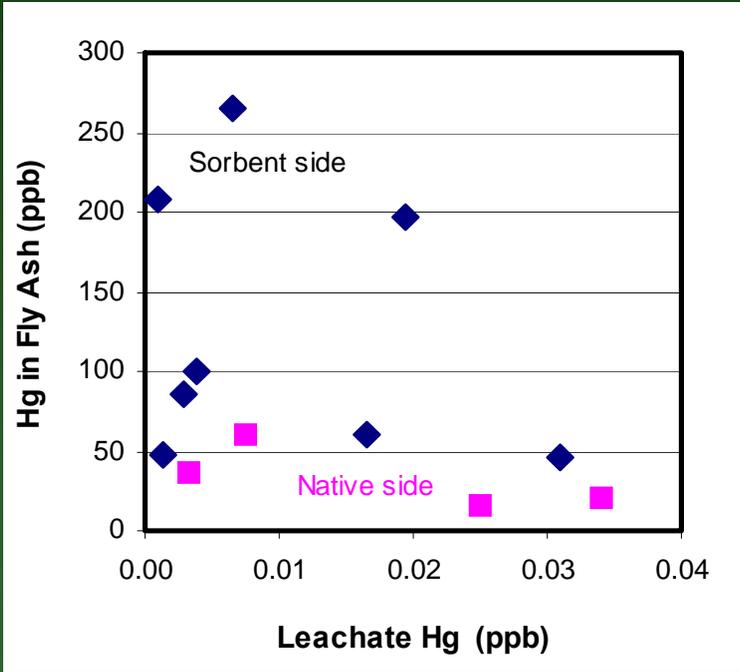
Preliminary Results

- H-PAC1 injected at 5 lb/MMacf (~ 3.5 lb/MMacf)

<u>Load</u>	<u>Inj.Temp.</u>	<u>Ib/MMacf</u>	<u>Time Fraction</u>	<u>Wtd.Avg. %Remov.</u>	<u>Ib/TBtus</u>
60 MW	~ 540F	5.0	28%	49%	3.0
140 MW	~ 640F	5.0	50%	50%	3.0
60 MW	~ 540F	10.0	22%	71%	1.8

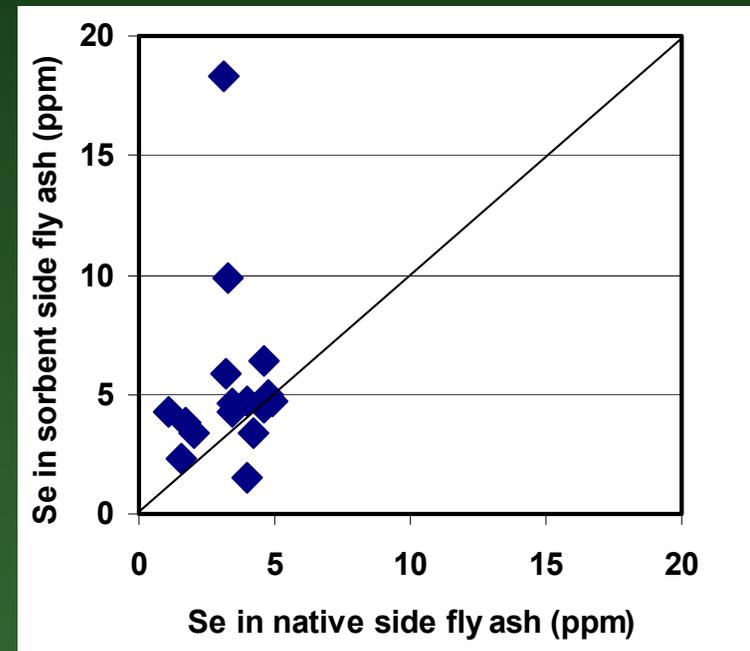
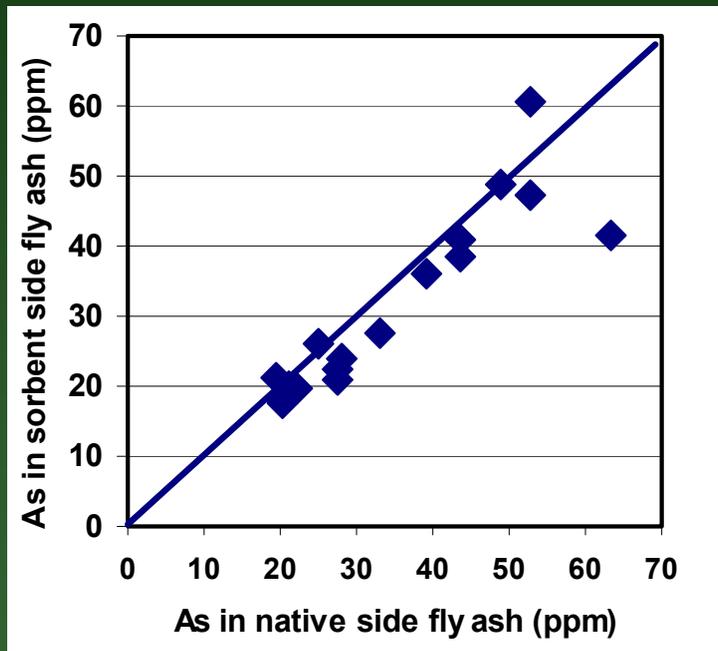
# Hg & Br Leachates at Buck

Preliminary Results



# As & Se Concentration at Buck

Preliminary Results



# The B-PAC & H-PAC Were Supplied in Bulk

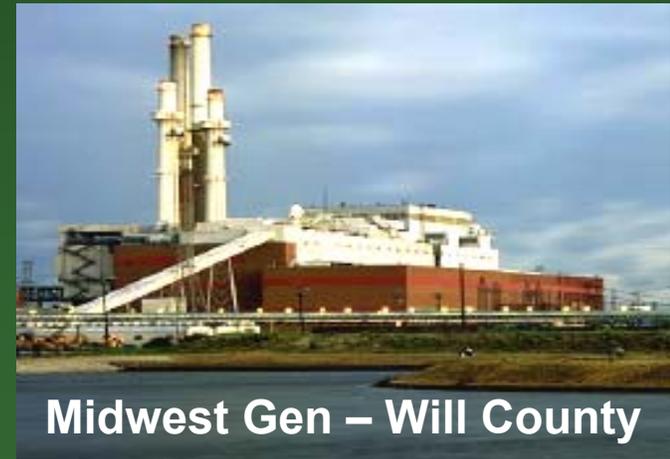
---

- Our first B-PAC™ plant can serve numerous power plants



# Future DOE B-PAC, C-PAC, & H-PAC Demos

---



(plus additional short-term non-DOE trials at other utility sites)

# Conclusions

---

1. Judging from the 2004 DOE full-scale results at St. Clair (& Meramec, Holcomb, & Stanton 10) – and contrary to regulations & popular belief – a high level of retrofit Hg control with subbituminous coal & N.D. lignites appears relatively easy, inexpensive, & is available today.
2. While ACI is more difficult with hot-side ESPs, with Brominated PAC it is indeed possible.