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**AN ALGORITHM FOR COMPUTING IN-SITU COMBUSTION
OIL RECOVERY PERFORMANCE**

SUPRI TR-25

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Work Performed for the Department of Energy
Under Contract No. DE-AC03-76ET12056

Date Published—October 1981

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AN ALGORITHM FOR COMPUTING IN-SITU COMBUSTION
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INTRODUCTION

During in-situ combustion oil recovery, a burning front moves through the formation displacing all of the water and most of the oil in the formation. Often, oil recovery from in-situ combustion is computed considering only the oil displaced by the burning front. This leads to a constant, high value of injected air to oil displaced ratio. The oil displacement is more complex than this simple model indicates. Combustion gas and steam and distilled hydrocarbons move ahead of the burning front. Heat transmission from this vaporizing-condensing region ahead of the burning front, solution of carbon dioxide from the combustion gases, and many other mechanisms are involved in oil displacement. A simple method to consider the frontal displacement, thermally aided gravity drainage, steam distillation, oil swelling and viscosity reduction, and other significant mechanisms ahead of and adjacent to the burning front has been published in a correlation of field and laboratory physical model studies of combustion oil recovery.¹ This method is called the oil-recovery/volume-burned method. This method indicates that the air/oil ratio passes through a minimum, and that oil is recovered more rapidly than is indicated by a simple frontal displacement.

The oil-recovery/volume-burned method can be used to make accurate engineering and economic evaluations for the design and monitoring of in-situ combustion projects. In this paper an algorithm based on this method is presented to provide a quick estimate of the oil recovery, air/oil ratios, oil rates, and economic limits of in-situ combustion projects.

OIL-RECOVERY/VOLUME-BURNED METHOD

Figure 1 is a graph of oil displaced vs volume burned for both laboratory and field combustion experiments.¹ The abscissa represents the percent of the combustion tube's total length travelled by the combustion front in the laboratory or percent of the total pattern volume burned in the field. The percent of total oil displaced is graphed on the ordinate and differs from the original oil in place by the amount of oil consumed as fuel.

The straight, dashed line represents the amount of oil displaced from the burned volume only. However, the data taken in both laboratory and field show higher oil recovery and, therefore, a lower air/oil ratio than indicated by the straight, dashed line. This difference appears to be due to the oil recovery mechanisms of in-situ combustion which affect oil movement ahead of the burning front. These mechanisms include hot water, gas and steam drive, vaporization, miscible displacement, expansion, and gravity drainage. The example cited in Fig. 1 assumed zero gas saturation.

Similar curves can be obtained for different gas saturations. Obviously, a high gas saturation would require a longer fillup time. Figure 2 shows this behavior for several combustion tube runs using

San Ardo crude oil.² The ordinate is normalized with respect to consumed fuel to yield total oil displacement at total volume burned. As is shown at the higher gas saturations, the oil recovery curve is straighter. These results also match those previously obtained by Gates and Ramey¹ which are graphed in Fig. 3. Field and laboratory data were combined to obtain the results in Fig. 3. These curves are applicable to heavy oil fields similar to the South Belridge field.

METHODOLOGY

To determine the amount of displaced oil, initial oil and gas saturations must be determined using conventional well logging, coring, material balance or tracer techniques. The displaced oil is the initial oil minus the final oil minus the burned oil. Fuel concentration (C_f) is another important parameter in evaluating an in-situ combustion project. Fluid properties, lithology of formation and operating conditions all affect the value of C_f .

Several methods can be used to estimate C_f . These are described in detail in reference 1. They are: a) coring the reservoir as the combustion progresses; b) measuring the water cut and correlating with C_f by material balance; c) averaging the value of C_f obtained from combustion tube runs with natural core; d) history-matching the combustion behavior in the field using a numerical simulation; and e) using the burning velocity/air flux correlation. In the absence of other data, engineering calculations can be made using correlations of fuel concentration vs oil gravity to determine C_f .^{3,4}

To compute the cost of air compression, the value of the combustion air requirement should be determined. This can be calculated if oxygen

utilization (U_t) and the volume of air needed to burn a unit weight of fuel (AFR) are known. AFR can be computed from the combustion chemistry.⁵ After the burning front breakthrough, more air must be injected to compensate for the air produced because of channeling. Figure 4 is a correlation of excess air with oil recovery.¹ Knowing the AOR, the oil production rate can be determined if the air compressor capacity is known.

The data for air requirement, fuel concentration, initial oil and gas saturations, and oxygen utilization can be combined with an oil-recovery/volume-burned correlation using the following relationships to make an estimate of the potential of an in-situ combustion project.

$$B = \frac{C_f}{\rho_f} \cdot \frac{43560}{350} \quad (1)$$

$$R = S_{oi} - B \quad (2)$$

$$N_p = \frac{N_p, \%}{100} \cdot R \cdot A \cdot H \quad (3)$$

$$\text{Excess air} = \frac{0.9 (N_p, \%) - 15.85}{100} \quad (4)$$

$$\text{ASR} = C_f \cdot \text{AFR} (43.56) \quad (5)$$

$$\text{Cur. AOR} = \frac{\text{ASR}}{\frac{d(N_p, \%)}{d(V_B)} \cdot R} \quad (6)$$

$$\text{Cum. AOR} = \frac{(V_B) \cdot \text{ASR}}{N_p} \quad (7)$$

$$\text{Air Required} = \frac{V_B}{100} \text{ASR} \cdot A \cdot H \quad (8)$$

$$\text{Inj. Air/Prod. Oil} = (\text{Cur. AOR}) \left(1 + \frac{\text{Excess air, \%}}{100} \right) \quad (9)$$

$$\text{Time} = \frac{\text{Air Required}}{(\text{Air Injection Rate})} \quad (10)$$

where:

- A = Pattern Area, acres
- AFR = Air/Fuel Ratio, mcf/lb
- ASR = Air/Sand Ratio, mcf/ac-ft
- B = Fuel Consumed, bbl/ac-ft
- C_f = Fuel concentration, lb/cf of rock
- Cum. AOR = Cumulative Air/Oil Ratio, mcf, bbl
- Cur. AOR = Current Air/Oil Ratio, mcf/bbl
- H = Thickness, ft
- N_p = Oil Recovered, bbl
- $N_p, \%$ = Oil Recovered, % of pore volume
- R = Ultimate Recovery, bbl/ac-ft
- S_{oi} = Initial Oil Saturation, bbl/ac-ft
- V_B = Volume Burned, % of bulk volume
- ρ_f = Fuel Specific Gravity

To facilitate calculations, the suite of oil-recovered/volume-burned graphs shown on Fig. 3 were curve-matched. It was possible to correlate the lines on Fig. 3 into one curve using non-linear regression method so that only one equation was needed.

CURVE-FITTING PROCEDURE

The first step in developing an algorithm is to curve-fit the oil recovery-volume burned curves shown in Fig. 3. To do this, it was first assumed that the recovery curves could be approximated by straight lines with intercepts $V_B(0)$ at initial oil breakthrough as shown in Fig. 5. By redefining the abscissa as:

$$x = \frac{V_B - V_B(0)}{100 - V_B(0)} \quad (11)$$

all of the straight lines were put into a single line. Then, a relationship between $V_B(0)$ and gas saturation (Fig. 6) was obtained by curve-fitting:

$$V_B(0) = 0.14714 S_g + 0.01071 S_g^2 \quad (12)$$

The difference between actual oil recovery and estimates obtained from the straight lines was determined. It was found that for each level of gas saturation, there is a maximum calculated deviation (Maximum Deviation). These maxima were correlated with respect to gas saturation (Fig. 7).

$$\text{Maximum Deviation} = 26.8229 - 0.4678 S_g \quad (13)$$

The calculated deviations were normalized on the basis of maximum deviations and were graphed with respect to x (Fig. 8). A fourth order polynomial fit the data with the following parameters:

$$\frac{\text{Deviation}}{\text{Maximum Deviation}} = 6.7752 x - 15.9478 x^2 + 16.1872 x^3 - 7.0146 x^4 \quad (14)$$

These equations simplify the problem of curve-fitting, and extend the range of applicability of the correlations.

CALCULATOR PROGRAM

the above equations were implemented for us on a Texas Instruments' TI-59 hand-held programmable calculator. This program calculates C_f and AFR from the gas analysis data taken from either the combustion tube or the field. However, if the values of C_f and AFR are available, they can be used independently. Then, cumulative and current AOR, oil recovered, and time are calculated for each burned volume. The program with the supplementary equations and procedure are shown in the Appendix.

COMPARISON OF RESULTS

First, the slope of the oil-recovered/volume-burned correlation was checked for negative values. Then, precautions were taken to prevent both excess air and maximum deviation from having negative answers. When these parameters are less than zero, they will be set to zero. Figure 9 shows the computed results (circles) as well as those of Gates and Ramey¹ (straight lines) for three different gas saturations. In general, the answers are within $\pm 1\%$ of the actual ones.

CONCLUSIONS

An algorithm was developed to estimate the in-situ combustion performance in the field. A calculator program was prepared using this algorithm. The program is efficient, simple and accurate. Given estimates of fuel concentration, air/fuel ratio, gas and oil saturations, and injection rate, for each volume burned, oil recovery, air requirement, and time may be calculated.

REFERENCES

1. Gates, C. G., and Ramey, H. J., Jr.: "A Method for Engineering In-Situ Combustion Oil Recovery Projects," J. Pet. Tech. (Feb. 1980), 285-294.
2. Fassihi, M. R., Ramey, H. J., Jr., and Brigham, W. E.: "The Frontal Behavior of In-Situ Combustion," Paper SPE 8907, presented at the 50th California Regional Meeting of the SPE, Los Angeles, Ca. (April 9-11, 1980).
3. Alexander, J. D., Martin, W. L., and Dew, J. N.: "Factors Affecting Fuel Availability and Composition During In-Situ Combustion," J. Pet. Tech. (Oct., 1962), 1154-1164.
4. Showalter, W. E.: "Combustion Drive Tests," Soc. Pet. Eng. J. (Mar., 1963), 53-58.
5. Nelson, T. W., and McNeil, J. S., Jr.: "How to Engineer an In-Situ Combustion Project," Oil and Gas J. (1961), 39, No. 23, 58.

ACKNOWLEDGEMENT

This work was performed under the Department of Energy Contract DE-AC03-76ET12056. This financial support is gratefully acknowledged.

APPENDIX A

Table 1 gives the execution procedure for the TI-59 calculator program. Either combustion tube data (steps 4 through 10) or field estimates (steps 12 and 13) may be used for C_f and ASR. If the results for a different volume burned are desired, only step 18 needs to be repeated.

Table 2 is a listing of the data registers after execution of the program. The constants in registers 00-20 are stored on bank 4 of the magnetic cards (Table 3).

Figure 10 is a listing of the calculator program.

Table 4 gives all the equations used in the calculator program.

Table 5 gives the input data and the output from an execution of the program. The data is taken from Ref. 1.

Table 1

PROCEDURE FOR PROGRAM EXECUTION

<u>Step</u>	<u>Procedure</u>	<u>Enter</u>	<u>Press</u>	<u>Display</u>
1	Repartition calculator	4	OP 17	639.39
2	Read magnetic cards		Clr	1,2,3,4
3	If combustion tube data are to be used, continue. If field values are to be used, go to step 12.			
4	Enter tube radius	r_t (ft)	E'	r_t
5	Enter CO ₂ concentration	CO ₂ (%)	D'	CO ₂
6	Enter CO concentration	CO (%)	R/S	CO
7	Enter O ₂ concentration	O ₂ (%)	R/S	O ₂
8	If display value of N ₂ is incorrect, enter N ₂ concentration	N ₂ (%)	R/S	N ₂
9	Enter front velocity	V_f (ft/hr)	C'	V_f
10	Enter gas flowrate	q_g (scf/hr)	R/S	ASR
11	Go to Step 14			
12	Enter fuel concentration	C_f (lb/Cf)	B'	C_f
13	Enter air/fuel ratio	AFR (scf/lb)	R/S	ASR
14	Enter field gas saturation	S_g (%)	A'	S_g
15	Enter field oil saturation	S_o (bbl/acre-ft)	A	S_o
16	Enter pattern volume	AH (acre-ft)	B	AH
17	Enter field injection rate	q (mcf/day)	C	q
18	Enter volume burned	V_B , (%)	D	printer output

Table 2

DATA REGISTERS AFTER PROGRAM EXECUTION

<u>Register</u>	<u>Value</u>	<u>Register</u>	<u>Value</u>
00	1541353517	20	7.014659
01	3137001332	21	C_f
02	3500640000	22	ASR
03	1541303040	23	$V_B(0)$
04	13323564	24	x
05	3732371327	25	Maximum Deviation
06	1324350035	26	y
07	1734400064	27	$\frac{dy}{dx}$
08	3224270035	28	Current AOR
09	1715400064	29	Cumulative AOR
10	14142736	30	S_g
11	3724301764	31	R
12	16134536	32	AH
13	0.147143	33	q
14	0.010714	34	V_B
15	26.82295	35	Total AOR
16	0.46787	36	Air Required
17	6.775267	37	$N_p, \%$
18	15.947794	38	N_p
19	16.187187	39	Time

Table 3

CONSTANTS STORED IN BANK 4

1541353517.	00
3137001332.	01
3500640000.	02
1541303040.	03
13323564.	04
3732371327.	05
1324350035.	06
1734400064.	07
3224270035.	08
1715400064.	09
14142736.	10
3724301764.	11
16134536.	12
0.147143	13
0.010714	14
26.82295	15
0.46787	16
6.775267	17
15.947794	18
16.187187	19
7.014659	20
0.	21
0.	22
0.	23
0.	24
0.	25
0.	26
0.	27
0.	28
0.	29

Table 4
CALCULATOR EQUATIONS

$$H/C = \frac{4[0.2658 N_2 - CO_2 - O_2 - 0.5 CO]}{CO_2 + CO}$$

$$C_f = \frac{1.209 \times 10^{-3} q_g [CO_2 + CO][12 + H/C]}{V_f r_t^2}$$

$$AFR = \frac{479.7 N_2}{(CO_2 + CO)(12 + H/C)}$$

$$ASR = (AFR)C_f(43.56)$$

$$B = (C_f)(124.4)$$

$$R = S_{O_1} - B$$

$$V_B(0) = 0.147143 S_g + 0.010714 S_g^2$$

$$x = \frac{V_B - V_B(0)}{100 - V_B(0)}$$

$$\text{Maximum Deviation} = \text{M.D.} = 26.82295 - 0.46787 S_g$$

$$y = \frac{\text{Deviation}}{\text{Maximum Deviation}} = 6.775267 x - 15.947794 x^2 + 16.187187 x^3 - 7.014659 x^4$$

(Table Continued Next Page)

Table 4 (Continued)

$$\text{Slope} = \frac{100}{100 - V_B(0)} + \frac{\text{M.D.}}{100 - V_B(0)} \frac{dy}{dx}$$

$$\text{Current AOR} = \frac{\text{ASR}}{(\text{Slope})(R)}$$

$$N_p, \% = 100 x + (y)(\text{M.D.})$$

$$N_p = \frac{(N_p, \%) (R) (A) (H)}{100}$$

$$\text{Air Required} = \frac{(\text{ASR}) (A) (H) V_B}{100}$$

$$\text{Cum. AOR} = \frac{\text{Air Required}}{N_p}$$

$$\text{Time} = \frac{\text{Air Required}}{q}$$

$$\text{Excess Air} = \frac{.9(N_p, \%) - 15.85}{100}$$

$$\text{Total AOR} = \text{Current AOR}(1 + \text{Excess Air})$$

TABLE 5

Input data: $C_f = 2.1$
 $AFR = 184.$
 $S_g = 4.$
 $S_o = 1540.$
 $AH = 1.$
 $q = 1.$
 $V_B = 30.$

Calculator Output:

CURRENT AOR =
 10.72022967

CUMM. AOR=
 7.34770305

TOTAL AOR=
 14.20611437

AIR REQ. =
 5049.4752

OIL REQ. =
 53.74098277 $\frac{1}{2}$ PV
 687.2181913 BBLs

TIME=
 5049.4752 DAYS

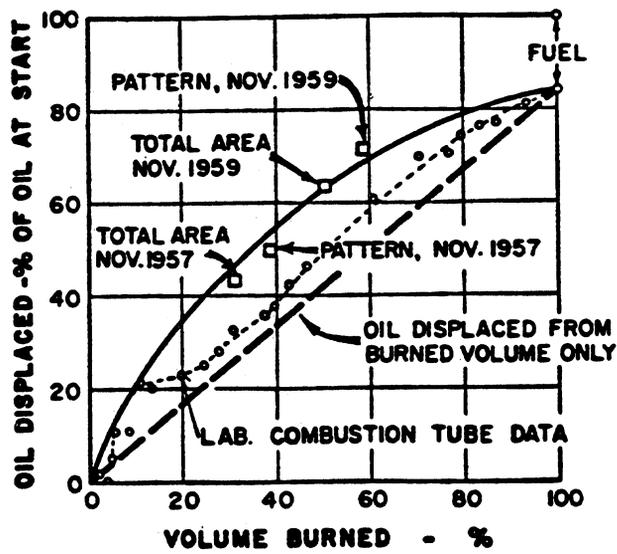


Fig. 1: OIL DISPLACED VS VOLUME BURNED
(From Ref. 1)

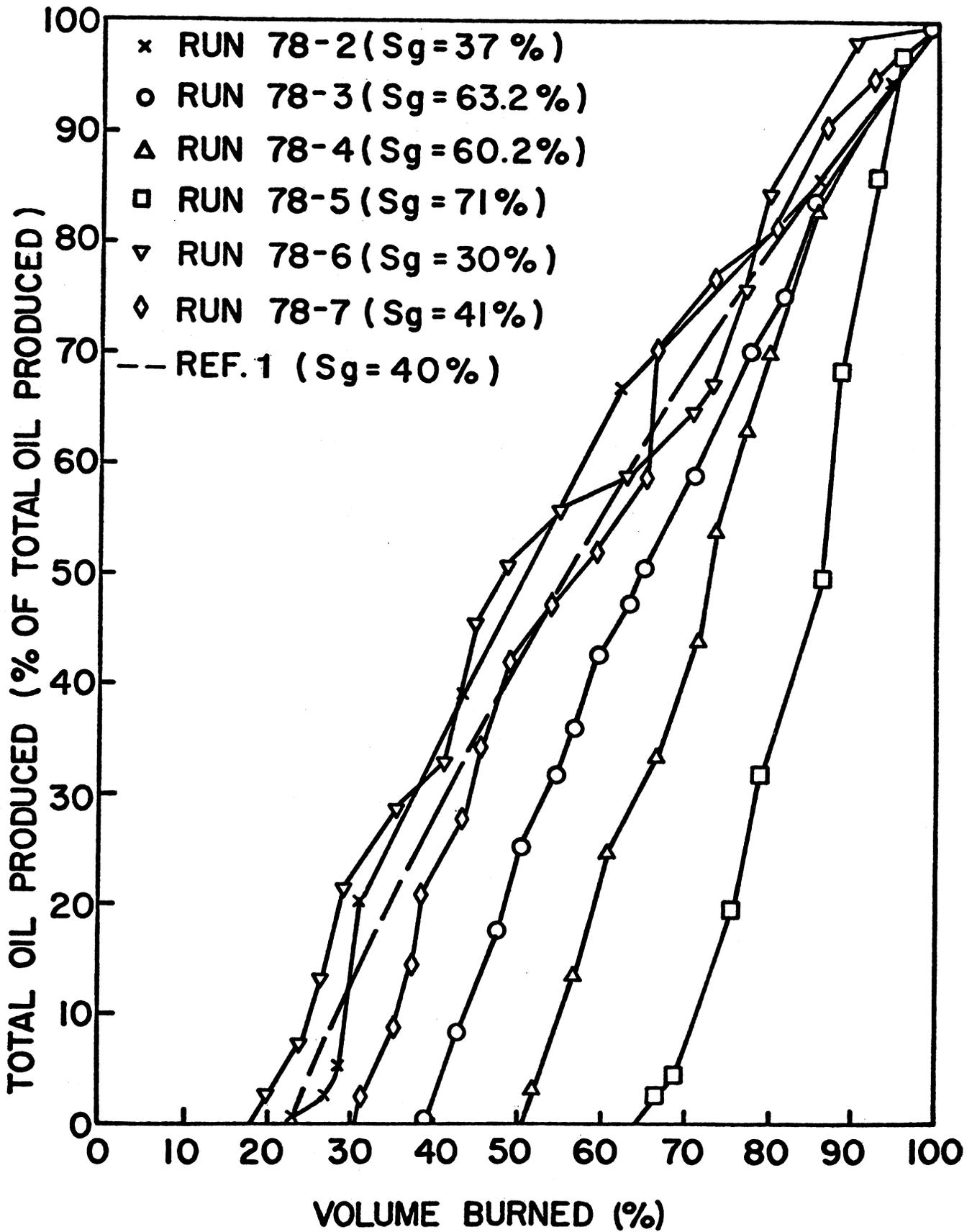


Fig. 2: OIL RECOVERY VS VOLUME BURNED FOR LABORATORY COMBUSTION TUBE RUNS (From Ref. 2)

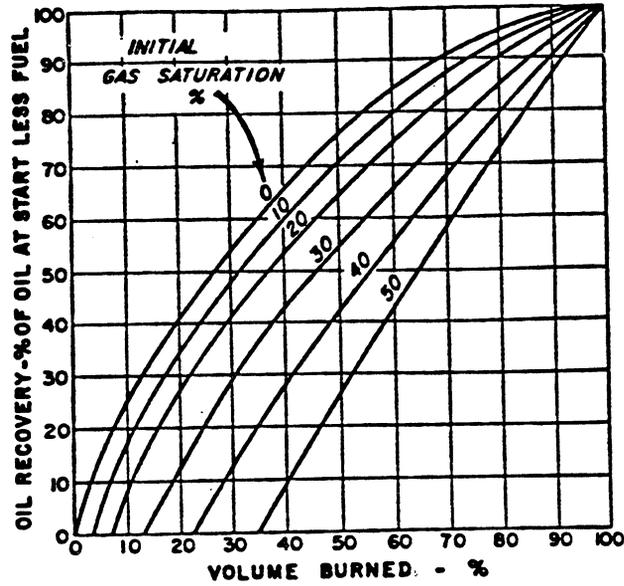


Fig. 3: ESTIMATED OIL RECOVERY VS VOLUME BURNED (From Ref. 1)

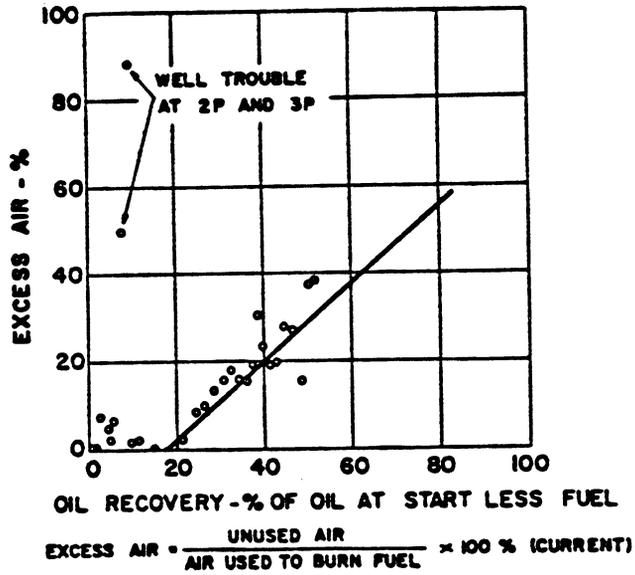


Fig. 4: EXCESS AIR VS OIL RECOVERY (From Ref. 1)

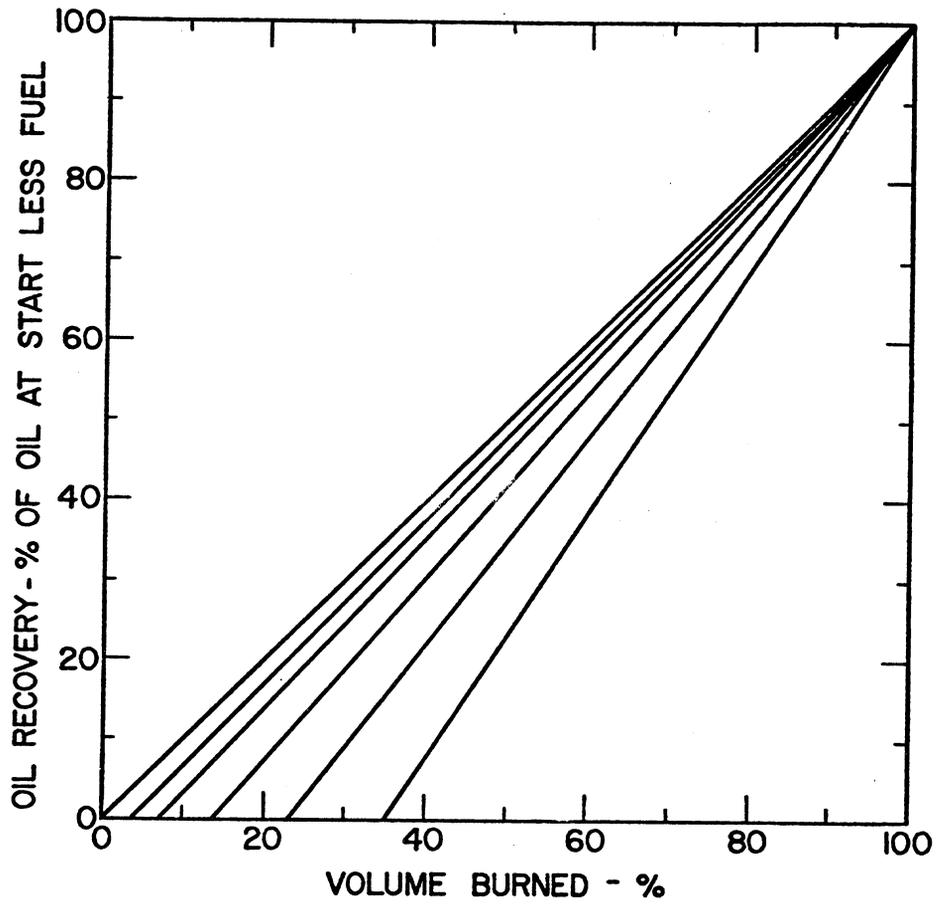


Fig. 5: OIL DISPLACED FROM VOLUME BURNED ONLY

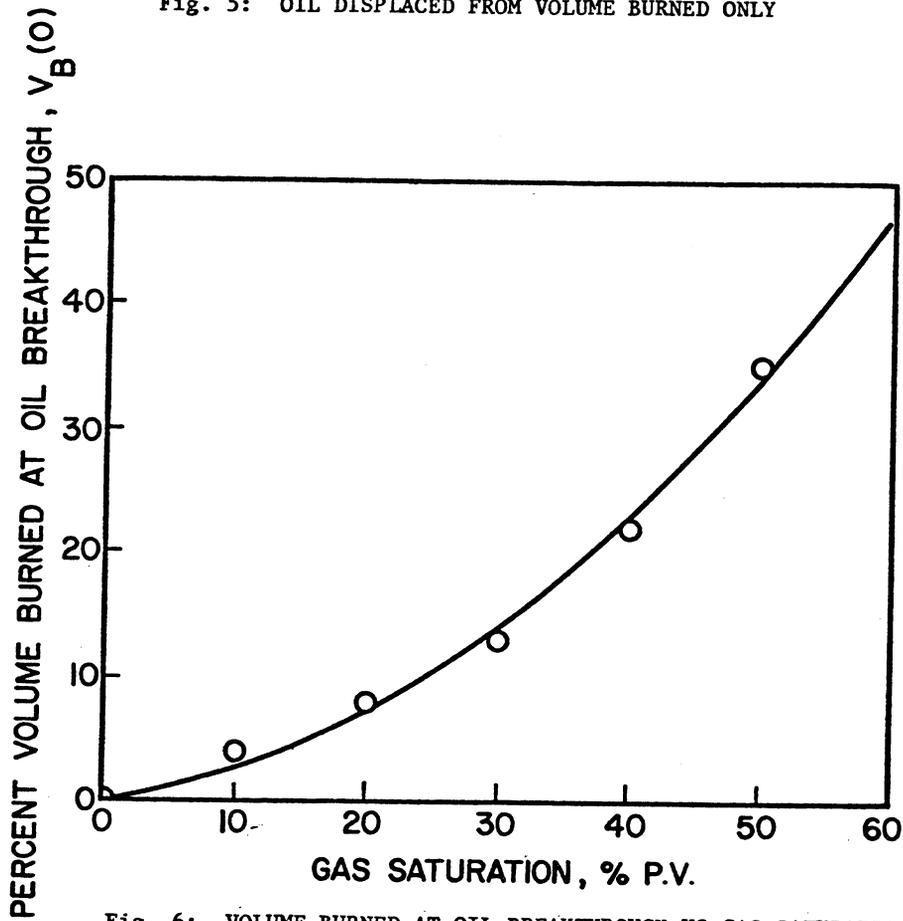


Fig. 6: VOLUME BURNED AT OIL BREAKTHROUGH VS GAS SATURATION

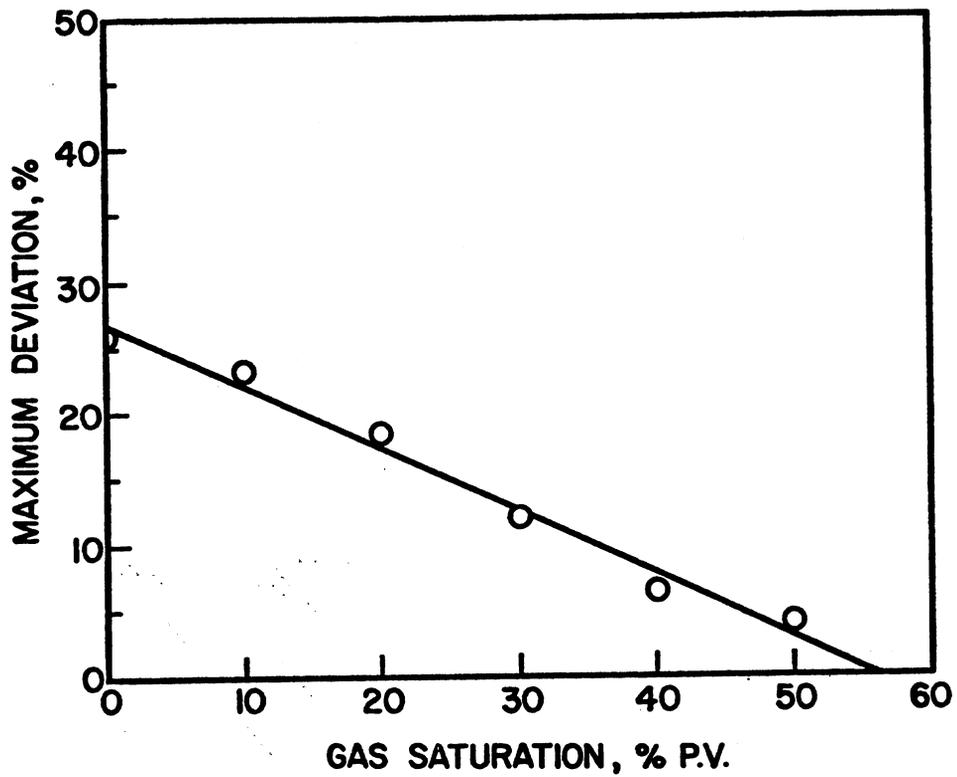


Fig. 7: MAXIMUM DEVIATION VS GAS SATURATION

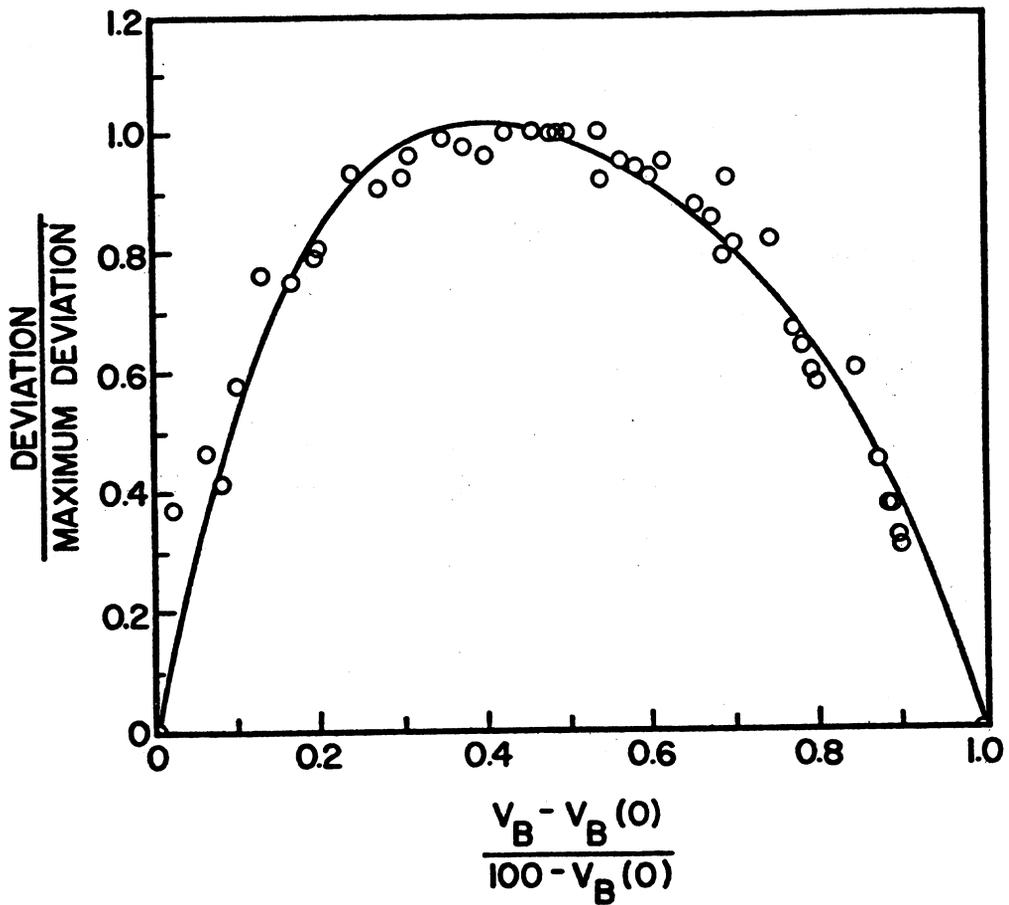


Fig. 8 : NORMALIZED DEVIATION VS NORMALIZED VOLUME BURNED.

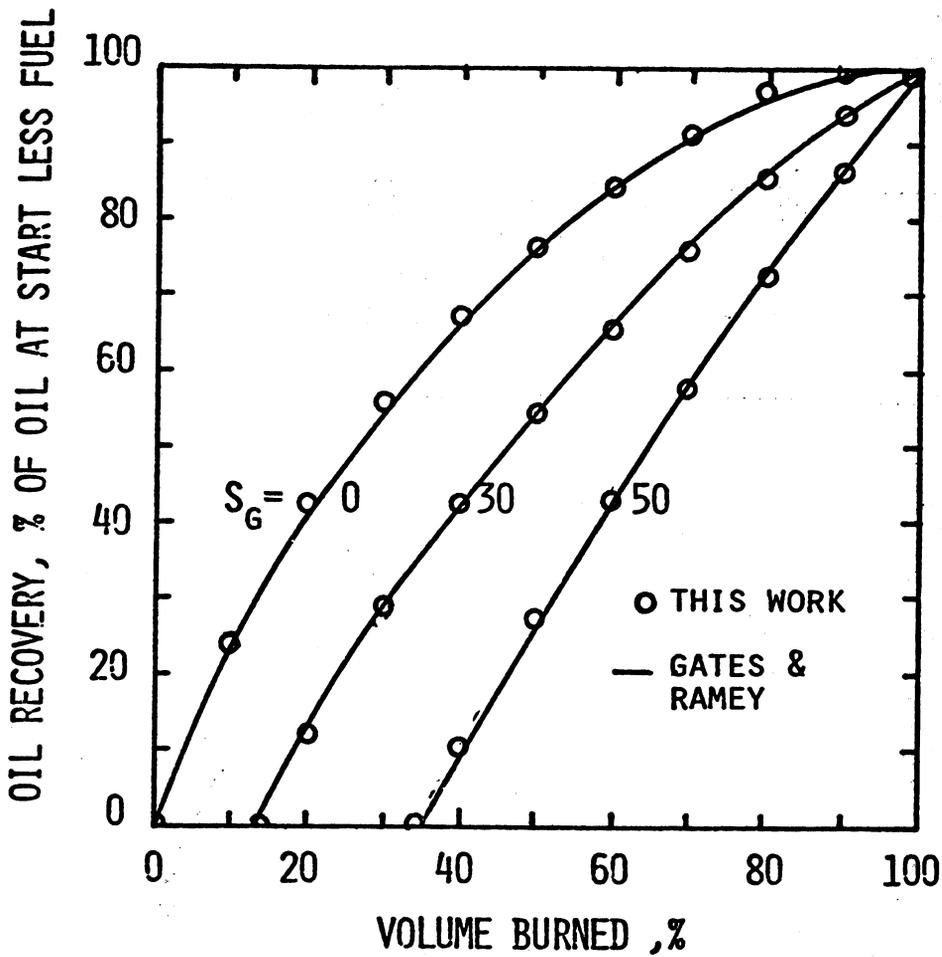


Fig. 9: COMPARISON BETWEEN THIS ALGORITHM AND GATES AND RAMEY'S RESULTS

LOC	CODE	KEY	COMMENTS	LOC	CODE	KEY	COMMENTS	LOC	CODE	KEY	COMMENTS
000	76	LBL		055	93	.		110	07	7	
001	10	E'		056	05	5		111	65	x	
002	42	STD		057	65	x		112	43	RCL	
003	21	21		058	43	RCL		113	26	26	
004	91	R/S		059	23	23		114	55	+	
005	76	LBL		060	95	=		115	43	RCL	
006	19	D'		061	65	x		116	24	24	
007	42	STD		062	04	4		117	55	+	
008	22	22		063	55	+		118	43	RCL	
009	42	STD		064	43	RCL		119	29	29	
010	24	24		065	24	24		120	65	x	
011	91	R/S		066	85	+		121	43	RCL	
012	42	STD		067	01	1		122	21	21	
013	23	23		068	02	2		123	65	x	
014	44	SUM		069	95	=		124	04	4	
015	24	24		070	42	STD		125	03	3	
016	91	R/S		071	29	29		126	93	.	
017	42	STD		072	65	x		127	05	5	
018	25	25		073	43	RCL		128	06	6	
019	94	+/-		074	24	24		129	95	=	
020	85	+		075	65	x		130	42	STD	
021	09	9		076	43	RCL		131	22	22	
022	09	9		077	28	28		132	91	R/S	
023	75	-		078	65	x		133	76	LBL	
024	43	RCL		079	93	.		134	17	B'	
025	24	24		080	00	0		135	42	STD	
026	95	=		081	00	0		136	21	21	
027	42	STD		082	01	1		137	65	x	
028	26	26		083	02	2		138	01	1	
029	91	R/S		084	00	0		139	02	2	
030	42	STD		085	09	9		140	04	4	
031	26	26		086	55	+		141	93	.	
032	91	R/S		087	43	RCL		142	04	4	
033	76	LBL		088	21	21		143	95	=	
034	18	C'		089	33	X ²		144	94	+/-	
035	42	STD		090	55	+		145	42	STD	
036	27	27		091	43	RCL		146	31	31	
037	91	R/S		092	27	27		147	43	RCL	
038	42	STD		093	95	=		148	21	21	
039	28	28		094	42	STD		149	91	R/S	
040	93	.		095	21	21		150	65	x	
041	02	2		096	65	x		151	43	RCL	
042	06	6		097	01	1		152	21	21	
043	05	5		098	02	2		153	65	x	
044	08	8		099	04	4		154	04	4	
045	65	x		100	93	.		155	03	3	
046	43	RCL		101	04	4		156	93	.	
047	26	26		102	95	=		157	05	5	
048	75	-		103	94	+/-		158	06	6	
049	43	RCL		104	42	STD		159	95	=	
050	22	22		105	31	31					
051	75	-		106	04	4					
052	43	RCL		107	07	7					
053	25	25		108	09	9					
054	75	-		109	93	.					

MERGED CODES

82	83	84	85	72	73	74	75	83	84	85	86
82	83	84	85	72	73	74	75	83	84	85	86
82	83	84	85	72	73	74	75	83	84	85	86
82	83	84	85	72	73	74	75	83	84	85	86

TEXAS INSTRUMENTS
INCORPORATED

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TI-24181

Fig. 10: HAND CALCULATOR PROGRAM

LOC	CODE	KEY	COMMENTS	LOC	CODE	KEY	COMMENTS	LOC	CODE	KEY	COMMENTS
160	42	STD		215	35	1/X		270	45	YX	
161	22	22		216	65	X		271	04	+	
162	91	R/S		217	53	(272	95	=	
163	76	LBL		218	43	RCL		273	42	STD	
164	16	A'		219	34	34		274	26	36	
165	42	STD		220	75	-		275	43	RCL	
166	30	30		221	43	RCL		276	17	17	
167	91	R/S		222	23	23		277	75	-	
168	76	LBL		223	54)		278	02	2	
169	11	A		224	95	=		279	65	X	
170	44	SUM		225	42	STD		280	43	RCL	
171	31	31		226	24	24		281	18	18	
172	91	R/S		227	43	RCL		282	65	X	
173	76	LBL		228	15	15		283	43	RCL	
174	12	B		229	75	-		284	24	24	
175	42	STD		230	43	RCL		285	85	+	
176	32	32		231	16	16		286	03	3	
177	91	R/S		232	65	X		287	65	X	
178	76	LBL		233	43	RCL		288	43	RCL	
179	13	C		234	30	30		289	19	19	
180	42	STD		235	95	=		290	65	X	
181	33	33		236	77	GE		291	43	RCL	
182	91	R/S		237	02	02		292	24	24	
183	76	LBL		238	42	42		293	33	X ²	
184	14	D		239	00	0		294	75	-	
185	42	STD		240	93	.		295	04	4	
186	34	34		241	00	0		296	65	X	
187	43	RCL		242	42	STD		297	43	RCL	
188	13	13		243	25	25		298	20	20	
189	65	X		244	43	RCL		299	65	X	
190	43	RCL		245	17	17		300	43	RCL	
191	30	30		246	65	X		301	24	24	
192	85	+		247	43	RCL		302	45	YX	
193	43	RCL		248	24	24		303	03	3	
194	14	14		249	75	-		304	95	=	
195	65	X		250	43	RCL		305	42	STD	
196	43	RCL		251	18	18		306	27	27	
197	30	30		252	65	X		307	65	X	
198	33	X ²		253	43	RCL		308	43	RCL	
199	95	=		254	24	24		309	25	25	
200	42	STD		255	33	X ²		310	55	+	
201	23	23		256	85	+		311	53	(
202	75	-		257	43	RCL		312	01	1	
203	43	RCL		258	19	19		313	00	0	
204	34	34		259	65	X		314	00	0	
205	95	=		260	43	RCL		315	75	-	
206	77	GE		261	24	24		316	43	RCL	
207	38	SIN		262	45	YX		317	23	23	
208	01	1		263	03	3		318	54)	
209	00	0		264	75	-		319	85	+	
210	00	0		265	43	RCL					
211	75	-		266	20	20					
212	43	RCL		267	65	X					
213	23	23		268	43	RCL					
214	95	=		269	24	24					

MERGED CODES

62	72	83	73	84	92
63	74	85	75	86	93
64	76	87	77	88	94

TEXAS INSTRUMENTS
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Fig. 10 (Cont.)

LOC	CODE	KEY	COMMENTS	LOC	CODE	KEY	COMMENTS	LOC	CODE	KEY	COMMENTS
320	01	1		375	00	0		430	93	.	
321	00	0		376	01	1		431	00	0	
322	00	0		377	95	=		432	85	+	
323	55	÷		378	42	STD		433	01	1	
324	53	(379	38	38		434	54)	
325	01	1		380	43	RCL		435	65	x	
326	00	0		381	22	22		436	43	RCL	
327	00	0		382	65	x		437	28	28	
328	75	-		383	43	RCL		438	95	=	
329	43	RCL		384	32	32		439	42	STD	
330	23	23		385	65	x		440	35	35	
331	54)		386	43	RCL		441	69	DP	
332	95	=		387	34	34		442	00	00	
333	77	GE		388	65	x		443	43	RCL	
334	03	03		389	93	.		444	00	00	
335	39	39		390	00	0		445	69	DP	
336	00	0		391	01	1		446	01	01	
337	93	.		392	95	=		447	43	RCL	
338	00	0		393	42	STD		448	01	01	
339	42	STD		394	36	36		449	69	DP	
340	28	28		395	55	÷		450	02	02	
341	43	RCL		396	43	RCL		451	43	RCL	
342	22	22		397	38	38		452	02	02	
343	55	÷		398	95	=		453	69	DP	
344	43	RCL		399	42	STD		454	03	03	
345	28	28		400	29	29		455	69	DP	
346	55	÷		401	43	RCL		456	05	05	
347	43	RCL		402	36	36		457	43	RCL	
348	31	31		403	55	÷		458	28	28	
349	95	=		404	43	RCL		459	99	PRT	
350	42	STD		405	33	33		460	98	ADV	
351	28	28		406	95	=		461	69	DP	
352	01	1		407	42	STD		462	00	00	
353	00	0		408	39	39		463	43	RCL	
354	00	0		409	93	.		464	03	03	
355	65	x		410	09	9		465	69	DP	
356	43	RCL		411	65	x		466	01	01	
357	24	24		412	43	RCL		467	43	RCL	
358	85	+		413	37	37		468	04	04	
359	43	RCL		414	75	-		469	69	DP	
360	25	25		415	01	1		470	02	02	
361	65	x		416	05	5		471	69	DP	
362	43	RCL		417	93	.		472	05	05	
363	26	26		418	08	8		473	43	RCL	
364	95	=		419	05	5		474	29	29	
365	42	STD		420	95	=		475	99	PRT	
366	37	37		421	55	÷		476	98	ADV	
367	65	x		422	01	1		477	43	RCL	
368	43	RCL		423	00	0		478	05	05	
369	31	31		424	00	0		479	69	DP	
370	65	x		425	95	=					
371	43	RCL		426	77	GE					
372	32	32		427	04	04					
373	65	x		428	32	32					
374	93	.		429	00	0					

MERGED CODES

82	83	84	72	73	74	83	84	85
83	84	85	73	74	75	84	85	86
84	85	86	74	75	76	85	86	87

TEXAS INSTRUMENTS
INCORPORATED

Fig. 10 (Cont.)

TITLE _____ PAGE 4 OF 4

TI Programmable
Coding Form 

PROGRAMMER _____ DATE _____

LOC	CODE	KEY	COMMENTS	LOC	CODE	KEY	COMMENTS	LOC	CODE	KEY	COMMENTS					
480	01	01		535	69	DP		590	07	7						
481	69	DP		536	06	06		591	02	2						
482	05	05		537	98	ADV		592	03	3						
483	43	RCL		538	69	DP		593	03	3						
484	35	35		539	00	00		594	05	5						
485	99	PRT		540	43	RCL		595	69	DP						
486	98	ADV		541	11	11		596	03	03						
487	69	DP		542	69	DP		597	04	4						
488	00	00		543	01	01		598	01	1						
489	43	RCL		544	69	DP		599	00	0						
490	06	06		545	05	05		600	00	0						
491	69	DP		546	43	RCL		601	04	4						
492	01	01		547	12	12		602	05	5						
493	43	RCL		548	69	DP		603	01	1						
494	07	07		549	04	04		604	07	7						
495	69	DP		550	43	RCL		605	03	3						
496	02	02		551	39	39		606	07	7						
497	69	DP		552	69	DP		607	69	DP						
498	05	05		553	06	06		608	04	04						
499	43	RCL		554	98	ADV		609	69	DP						
500	36	36		555	98	ADV		610	05	05						
501	99	PRT		556	91	R/S		611	98	ADV						
502	98	ADV		557	76	LBL		612	98	ADV						
503	69	DP		558	38	SIN		613	98	ADV						
504	00	00		559	69	DP		614	91	R/S						
505	43	RCL		560	00	00		5								
506	08	08		561	03	3		6								
507	69	DP		562	01	1		7								
508	01	01		563	03	3		8								
509	43	RCL		564	02	2		9								
510	09	09		565	00	0		0								
511	69	DP		566	00	0		1								
512	02	02		567	03	3		2								
513	69	DP		568	02	2		3								
514	05	05		569	02	2		4								
515	06	6		570	04	4		5								
516	01	1		571	69	DP		6								
517	00	0		572	01	01		7								
518	00	0		573	02	2		8								
519	03	3		574	07	7		9								
520	03	3		575	00	0		0								
521	04	4		576	00	0		1								
522	02	2		577	01	1		2								
523	69	DP		578	04	4		3								
524	04	04		579	03	3		4								
525	43	RCL		580	05	5		5								
526	37	37		581	01	1		6								
527	69	DP		582	07	7		7								
528	06	06		583	69	DP		8								
529	43	RCL		584	02	02		9								
530	10	10		585	01	1		MERGED CODES								
531	69	DP		586	03	3		62	63	72	73	74	83	84	82	
532	04	04		587	02	2		64	65	66	67	68	69	70	71	
533	43	RCL		588	06	6		TEXAS INSTRUMENTS								
534	38	38		589	03	3		INCORPORATED								

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Fig. 10 (Cont.)

